

## Supplementary Material

### **Sulfur doped Porous Carbon Sheets Embedded with Rich Iron Sites for the $^1\text{O}_2$ Dominated Peroxymonosulfate Activation**

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**Table S1** The analytical conditions of Phenol, BPA, TC, and SMX. The HPLC was equipped with C-18 chromatographic column and a UV detector.

<b>Organics</b>	<b>mobile phase (v/v)</b>	<b>Flow rate (mL/min)</b>	<b>Detection wavelength (nm)</b>
<b>Phenol</b>	Methanol/Water = 70/30	1	270
<b>BPA</b>	Methanol/Water = 60/40	1	230
<b>TC</b>	Methanol/0.1% Methanoic acid = 25/75	1	355
<b>SMX</b>	Acetonitrile/0.2% Methanoic acid = 30/70	1	270

**Table S2** BET surface area, pore properties of catalysts.

<b>Samples</b>	<b>BET surface area (m<sup>2</sup>/g)</b>	<b>Pore volume (cm<sup>3</sup>/g)</b>	<b>Pore size (nm)</b>
<b>N-C</b>	544.80	0.42	3.06
<b>Fe-NC</b>	537.75	0.54	4.01
<b>Fe-SNC-0.2</b>	509.89	0.53	4.01

**Table S3** The surface elemental composition and content of Fe–NC and Fe–SNC–0.2.

<b>Samples</b>	<b>XPS (at.%)</b>				
	C	N	O	Fe	S
<b>Fe–NC</b>	74.30	15.57	10.00	0.50	0
<b>Fe–SNC–0.2</b>	75.56	16.29	7.10	0.54	0.51

**Table S4** The fitting results for the N 1s spectra of Fe–NC and Fe–SNC–0.2.

<b>Samples</b>	<b>XPS (at.%)</b>			
	Fe–Nx	pyridinic N	graphitic/pyrrolic N	Oxidized N
<b>Fe–NC</b>	28.14	51.66	8.55	11.66
<b>Fe–SNC–0.2</b>	24.53	49.25	11.55	14.67

**Table S5** Parameters of Xinxiang natural surface water collected from Weihe River.

<b>Parameter</b>	<b>Water matrices</b>	
	<b>Weihe river</b>	<b>Tap water</b>
<b>pH</b>	8.45	7.56
<b>BOD<sub>5</sub> (mg/L)</b>	12.83	0.36
<b>COD (mg/L)</b>	22.57	1.28
<b>TDS (mg/L)</b>	694	132
<b>TN (mg/L)</b>	1.02	0.005
<b>TP (mg/L)</b>	0.12	N.D.

N.D.: not detected.

**Table S6** The percentage of each component in XPS spectra before and after reaction.

<b>Samples</b>	<b>XPS (at.%)</b>				
	C	N	O	Fe	S
<b>Before reaction</b>	75.56	16.29	7.10	0.54	0.51
<b>After reaction</b>	79.58	7.85	11.83	0.4	0.34

**Table S7** The percentage of each component in S 2p before and after reaction.

<b>Samples</b>	<b>XPS (at.%)</b>	
	Oxidized-S groups	C-S-C
<b>Before reaction</b>	69.61	30.39
<b>After reaction</b>	73.37	26.63



**Table S8** The percentage of each component in N1s before and after reaction.

<b>Samples</b>	<b>XPS (at.%)</b>			
	Fe-Nx	pyridinic N	graphitic/pyrrolic N	Oxidized N
<b>Before reaction</b>	24.51	49.25	11.55	14.67
<b>After reaction</b>	23.31	48.40	11.20	17.02

**Table S9** The percentage of each component in Fe 2p before and after reaction.

<b>Samples</b>	<b>XPS (at.%)</b>		
	Fe <sup>0</sup>	Fe(II)	Fe(III)
<b>Before reaction</b>	19.56	49.39	31.05
<b>After reaction</b>	34.43	39.38	26.19

**Table S10** Comparison of different oxidative degradation techniques of phenol in the last two years.

Degradation methods	Contaminant	Removal efficiency (%)	$\eta_{\text{TOC}}$ (%)	$k$ ( $\text{min}^{-1}$ )	Ref.
Photoelectrochemical	Phenol	96 (120 min)	/	0.035	1
UV-ZnO	Phenol	99 (150 min)	/	/	2
UV-H <sub>2</sub> -Rh/WO <sub>3</sub>	Phenol	100 (180 min)	27.6 (180 min)	0.0018	3
O <sub>3</sub> -RPB	Phenol	100 (10 min)	96.42 (30 min)	/	4
UV-H <sub>2</sub> O <sub>2</sub> -CoP/Fe <sup>2+</sup>	Phenol	80 (120 min)	/	/	5
PMS/Fe-SNC-0.2	Phenol	99 (10 min)	92 (20 min)	0.3569	This work

In order to successfully combat pathogenic microorganisms in wastewater and safeguard ecosystems and public health, wastewater treatment plants typically employ chlorination and ozonation as their last stage <sup>6</sup>. However, the reactions of chlorine with organic matters from the wastewater result in the formation of disinfection by-products (DBPs), which contribute to the overall toxicity of the wastewater and may affect potential reuse. Ozone is a disinfectant that can be used instead of chlorine to inactivate pathogens that are resistant to chlorine in drinking water and reduce the toxicity of wastewater <sup>7</sup>. Wert et al. have shown that ozone was capable of reducing DBPs formation potential by at least 20% <sup>8</sup>. Ozone-based advanced oxidation processes show promise for these pollutants' removal, but the mineralization via ozonation alone is unsatisfactory and not cost-effective.

**Table S11** Comparison of catalysts derived from MOFs for PMS activation.

Catalyst (loading, g/L)	PMS (g/L)	Contaminant	C <sub>0</sub> (mg/L)	Removal efficiency	TOF (g <sup>-1</sup> min <sup>-1</sup> )	Ref.
NPC <sub>ZIF-8</sub> (0.2)	0.5	Phenol	20	100% (50 min)	0.395	9
SNG-0.3(0.2)	2	Phenol	20	100% (90 min)	0.215	10
5%Fe-g-C <sub>3</sub> N <sub>4</sub> (1)	1.5	Phenol	10	100% (20 min)	0.183	11
Fe-N-C-3-800(0.5)	0.4	CIP	20	99% (60 min)	/	12
Fe-C@CNS (0.2)	0.24	CIP	20	100% (60 min)	0.609	13
Fe <sub>3</sub> C@NCNT-700 (0.2)	2	Phenol	20	100% (45 min)	0.485	14
Fe@NC-800 (0.2)	0.3	TC	30	95% (60 min)	0.223	15
Co-Fe/NC@GCS (0.2)	0.2	SMX	30	94% (60 min)	0.505	16
CoFe <sub>0.8</sub> @NCNT@CA (0.4)	0.4	TC	40	95% (25 min)	0.803	17
Fe@C-4 (0.1)	0.6	TBBPA		100% (60 min)	1.02	18
FeMn@NC-800 (0.2)	1.68	SMZ	10	97% (30 min)	0.22	19
C-Fe <sub>ZIF</sub> (1)	13.45	TCAA	10	79% (180 min)	/	20
Fe-SNC-0.2(0.4)	0.22	Phenol	20	99% (10 min)	1.784	This work

C<sub>0</sub>: initial concentration of contaminant

The turnover frequency (TOF) was calculated through dividing the reaction rate of pollutant degradation by the catalyst concentration.

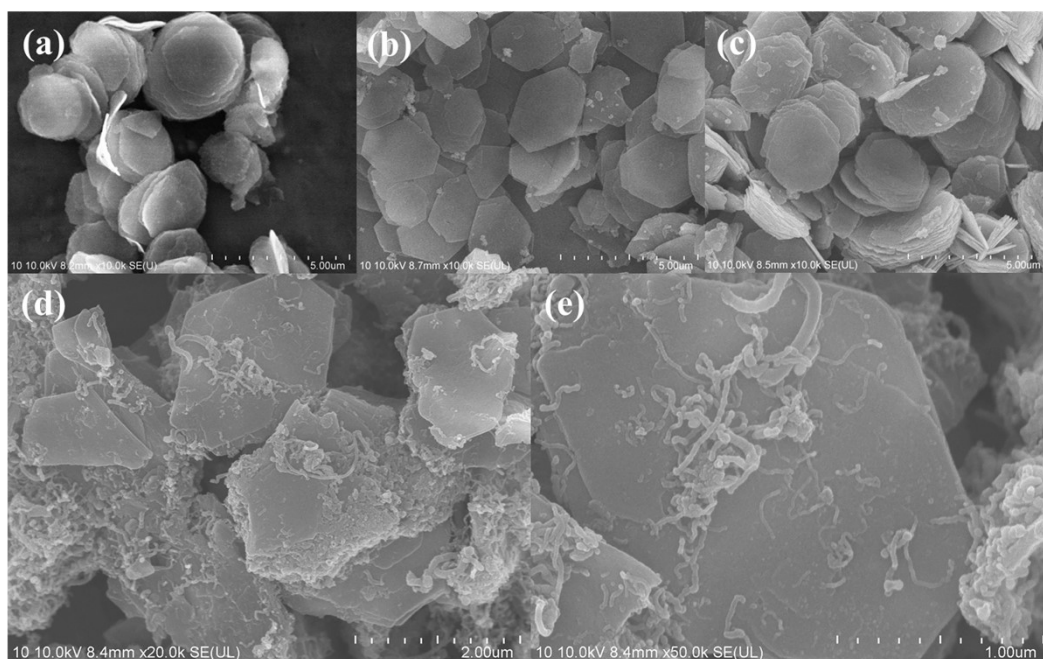
TBBPA: tetrabromobisphenol A

SMZ: sulfamethazine

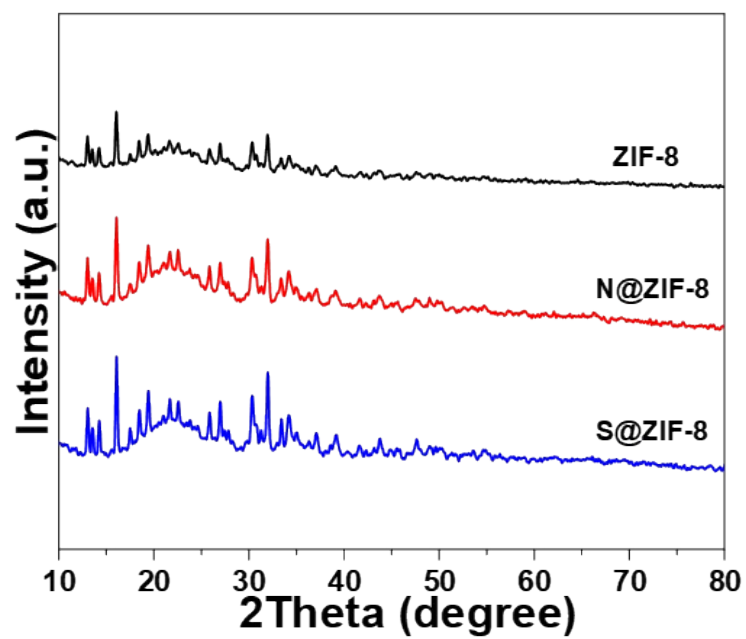
TCAA: trichloroacetic acid

**Table S12** Predicted acute (LC50) and chronic (LD50) toxic levels of phenol and its intermediate byproducts using three living organisms: Fish-96 h, Daphnia magna-48 h and Green algae-96 h.

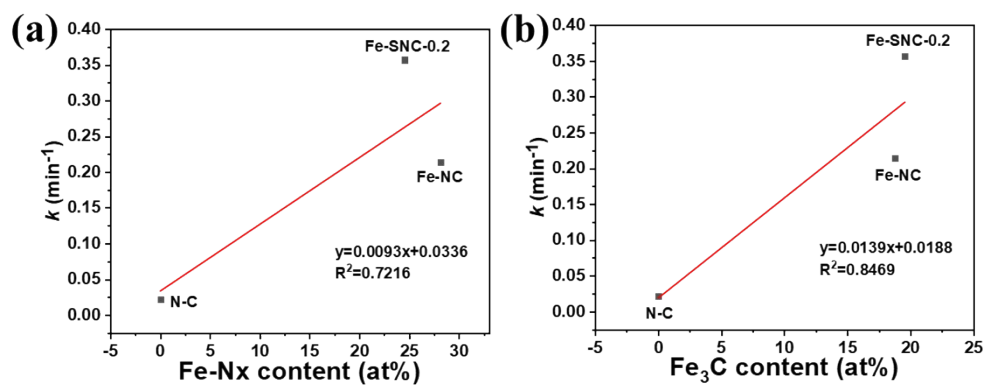
Degraded byproducts	Fish 96h LC <sub>50</sub> (mg/L)	Daphnid 96h LC <sub>50</sub> (mg/L)	Green Alge 96h EC <sub>50</sub> (mg/L)
P (Phenol)	27.7	9.64	2.4
P1	0.095	0.738	0.047
P2	7.01	136	0.736
P3	3.18	36.9	0.242
P4	55979.81	14869.57	2091.37
P5	7.73	25.3	0.962
P6	14.1	115	6.93
P7	491	257	137
P8	66986.86	28903.88	6919.37
P9	7.73	25.3	0.962
P10	0.15	240	94.6
P11	6.08	3.85	4.49
P12	110901.52	51384.62	16512.96
P13	487836.06	189607.45	29465.46
P14	14920475	5647225.5	786367.19



**Fig. S1** SEM of (a) ZIF-8, (b) N@ZIF-8, (c) S@ZIF-8, and (d) (e) Fe-NC.

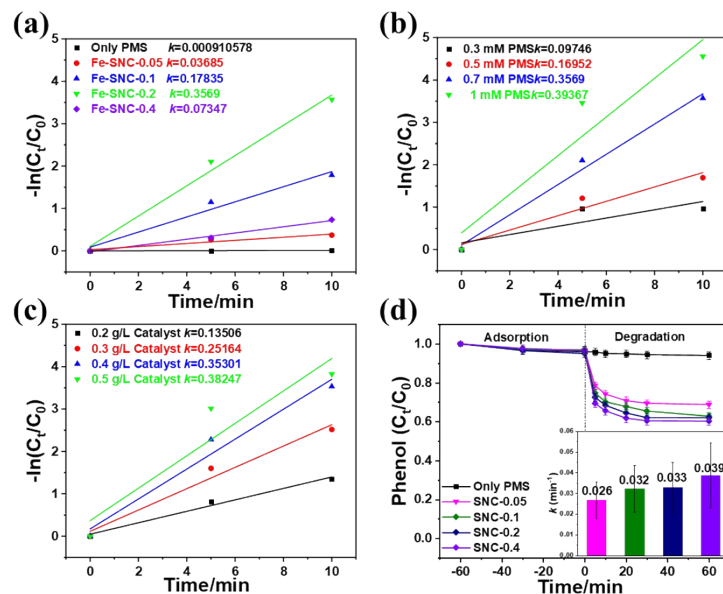


**Fig. S2** XRD of ZIF-8, N@ZIF-8 and S@ZIF-8.

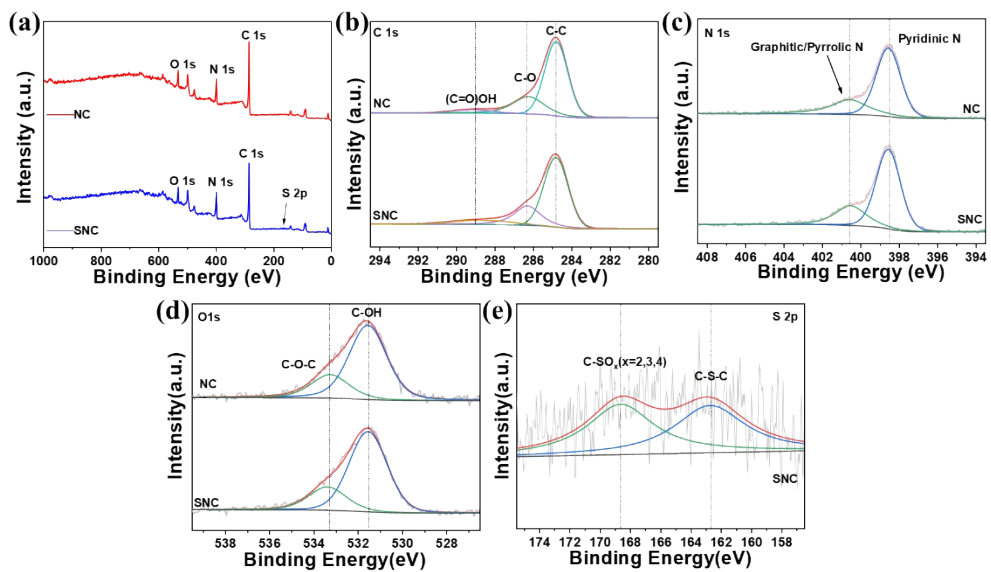


**Fig. S3** The relationship between the content of Fe–Nx and Fe<sub>3</sub>C and the phenol degradation rate constant ( $k$ ).

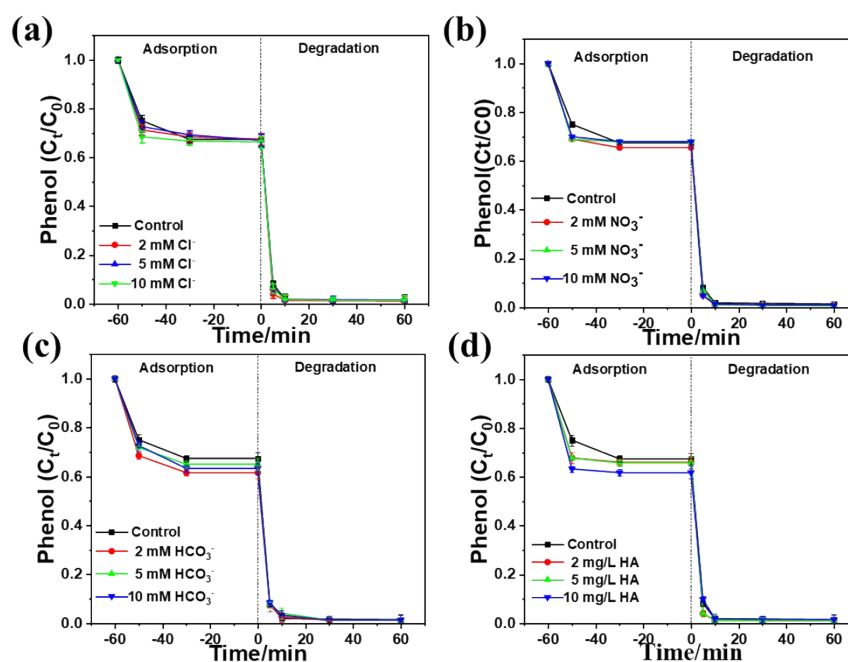




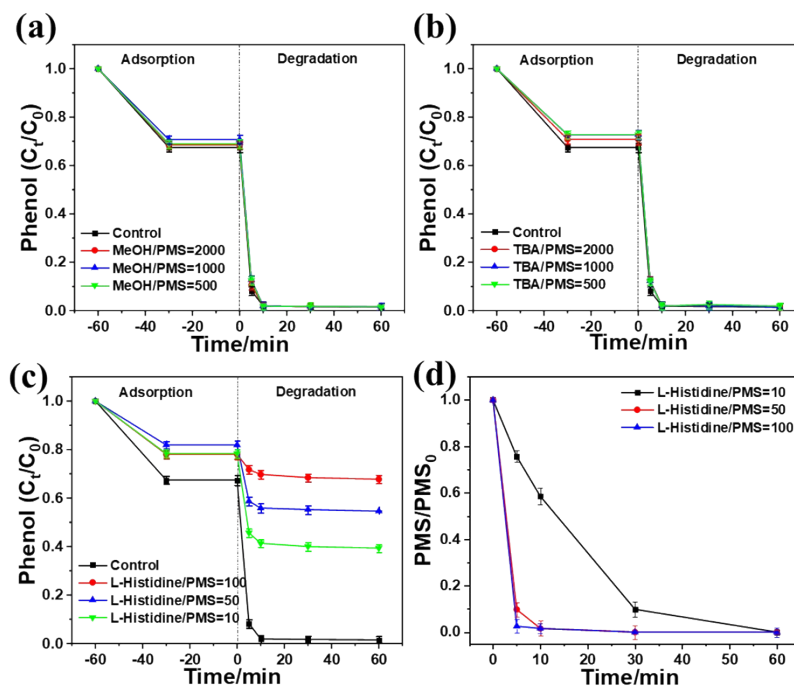
**Fig. S4** The corresponding pseudo-first-order kinetic modeling: (a) Iron salt content; (b) PMS concentration, and (c) catalyst dosage. (d) Different concentrations of sulfur doping activated PMS to degrade phenol (Embedded graph: pseudo-first-order rate constants of phenol degradation). Reaction conditions: [PMS] = 0.7 mM, [phenol] = 20 mg/L, [catalyst] = 0.4 g/L, 25 °C, pH=7.



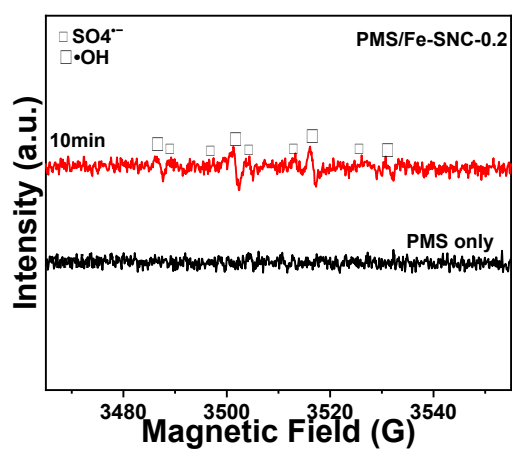
**Fig. S5** XPS survey spectra of NC and SNC-0.2 (a). High resolution XPS spectra of (b) C 1s, (c) N 1s, (d) O 1s, and (e) S 2p.



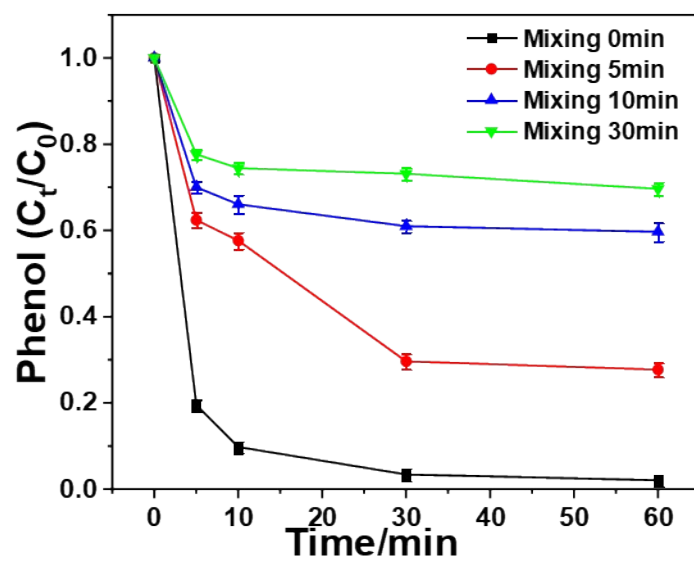
**Fig. S6** Effect of anions and natural organic matter on Phenol removal efficiency in Fe-SNC-0.2 degradation system. (a)  $\text{Cl}^-$ , (b)  $\text{NO}_3^-$ , (c)  $\text{HCO}_3^-$ , and (d) HA. Conditions:  $[\text{PMS}] = 0.7\text{mM}$ ,  $[\text{catalyst}] = 0.4\text{ g/L}$ ,  $[\text{phenol}] = 20\text{ mg/L}$ ,  $[\text{Cl}^-] = 2, 5, 10\text{ mM}$ ,  $[\text{NO}_3^-] = 2, 5, 10\text{ mM}$ ,  $[\text{HCO}_3^-] = 2, 5, 10\text{ mM}$ ,  $[\text{HA}] = 2, 5, 10\text{ mg/L}$ ,  $25\text{ }^\circ\text{C}$ ,  $\text{pH}=7$ .



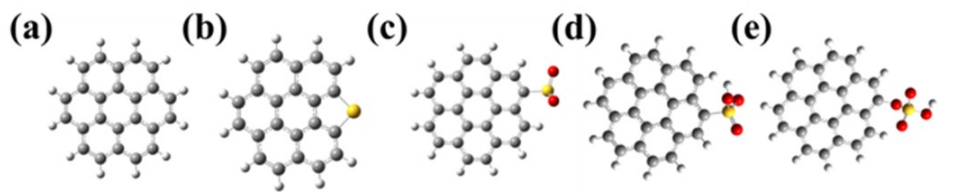
**Fig. S7** Removal efficiency of Fe-SNC-0.2 system with different scavengers for Phenol degradation: (a) MeOH, (b) TBA, and (c) L-histidine; (d) PMS consumption. Experimental conditions: [PMS] = 0.7 mM, [phenol] = 20 mg/L, [catalyst] = 0.4 g/L, 25 °C, pH=7.



**Fig. S8** EPR spectra of  $\text{DMPO-SO}_4^{\bullet-}$  and  $\text{DMPO-•OH}$ .



**Fig. S9** The degradation efficiency of phenol after premixing Fe-SNC-0.2 with PMS. Conditions: [PMS] = 0.7 mM, [catalyst] = 0.4 g/L, [phenol] = 20 mg/L, 25 °C, pH=7.



**Fig. S10** Several different adsorption configurations of sulfur doping sites: (a) graphene, (b) -C-S-C-, (c) -C-SO<sub>2</sub>-, (d) -C-SO<sub>3</sub>-, (e) -C-SO<sub>4</sub>-.

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