Pilot-scale evaluation of the sustainability of membrane desalination systems for concentrate volume minimization of coal chemical wastewater

Fayuan Chen^{a*}, Linnan Ma^a, Zhong Zhang^b, Xiao Wang^c, Qinghong Wang^a, Xiaolong, Wang^d, Chunmao, Chen^a, Linyu Jiang^e, Xianhui Li^{b*}

^a State Key Laboratory of Heavy Oil Processing, State Key Laboratory of Petroleum Pollution Control, China University of Petroleum-Beijing, Beijing 102249, China ^b Key Laboratory for City Cluster Environmental Safety and Green Development of the Ministry of Education, School of Ecology, Environment and Resources, Guangdong University of Technology, Guangzhou 510006, China

^c State Key Laboratory of Water Resource Protection and Utilization in Coal Mining, China Energy Investment, Beijing, 102211, P.R. China

^d Ningxia Ningdong Xingrong Water Treatment Co., Ltd., Yinchuan, 750041, P.R. China

^e Xiamen Jiarong Technology Co., Ltd., Xiamen, 361000, P.R. China

Corresponding Author

Fayuan, Chen

State Key Laboratory of Heavy Oil Processing, State Key Laboratory of Petroleum Pollution Control, China University of Petroleum-Beijing, Beijing 102249, China fychen@cup.edu.cn

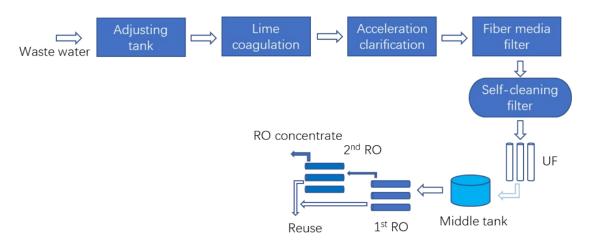


Fig. S1. The schematic diagram of wastewater reclamation plant for a coal chemistry industry.

Table S1. Membrane parameters in VSEP scenario

| Item | VESP | |
|------------------------------|---------------------|--|
| Manufacturer | DOW | |
| Membrane Model | RO-11 | |
| Membrane material | Composite Polyamide | |
| Water permeability (LMH) | 40 | |
| Membrane effective area (m²) | 120 | |
| Operating temperature (°C) | 60 | |
| Range of feed pH | 2-10 | |
| Operational pressure (bar) | 70 | |
| Rejection (%) | 99.7% | |

Table S2. Membrane parameters in DTRO scenario

| Item | DTRO | | |
|----------------------------|----------------------------|--|--|
| Manufashuusu | Unisol Membrane Technology | | |
| Manufacturer | GmbH | | |
| Model Number | MP-DT-RO3 | | |
| Membrane material | Composite Polyamide | | |
| Water permeability | 29 | | |
| Membrane effective area | 0.405 | | |
| (m^2) | 9.405 | | |
| Operating temperature | ~ 15 | | |
| (°C) | ≤ 45 | | |
| Range of feed pH | 2–12 | | |
| Operational pressure (bar) | ≤ 90 | | |
| Rejection (%) | ≥97.5% | | |

Table S3. Membrane parameters in FO-RO scenario

| Item | FO | RO-1 | RO-2 | RO-3 |
|------------------------------|----------------------------|-------------------|------------|------------|
| Manufacturer | FTS | FTS | Dow | Dow |
| Model Number | FO-CTA- 8040-45- VDS | HBCR-TFC- 4040 | SW30- 8040 | BW30- 8040 |
| Membrane | СТА | Composite | Composite | Composite |
| material | CIA | Polyamide | Polyamide | Polyamide |
| Water permeability | | 150 LMH | 32 | 45 |
| Membrane effective area (m²) | 9.9 | 37 | 37 | 37 |
| Operating temperature (°C) | ≤ 40 | 30 | 45 | 45 |
| Range of feed pH | 4-7.5 | 3-10 | 2-11 | 2-11 |
| Operational pressure (bar) | < 10 | < 80 | 83 | 41 |
| Rejection | 99.9% | 60% | 99.6 | 99.5 |

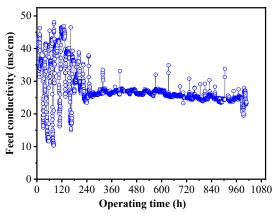


Fig. S2. Feed conductivity of the FO system

Table S4. Details of chemical cost in the VSEP scenario

| Item | Consumption per ton of feed water (kg/m³) | Price USD (\$) | Operating cost per ton of feed water | Note |
|---|---|----------------------|--|------------------------------------|
| Hydrochloric acid (30%) | 1.0 | 0.046 | 0.046 | Adjusting pH to 6.5 |
| Antiscalant | 0.009 | 3.51 | 0.0032 | 5 ppm |
| Acid cleaning-Citric acid | 0.0035 | 2.46 | 0.0172 | Cleaning frequency: Once a week,1% |
| Alkaline cleaning -Sodium hydroxide | 0.034 | 0.62 | 0.0042 | Once a week,0.1% |
| Alkaline cleaning -metal chelating agent (EDTA) | 0.0035 | 4.31 | 0.0030 | Once a week,1% |

Since the statistical data came from the year of 2021, the CNY was converted into USD by the annual average exchange rate (1 USD = 6.5 CNY) in 2021 (<u>National Bureau of Statistics of China (NBSC)</u>, 2021).

Table S5. Details of chemical cost in the DTRO scenario

| Item | Consumption per ton of water (kg/m³) | USD (\$) | Operating cost per ton of water | Note |
|---|--|-------------|---------------------------------------|-----------------------------------|
| Hydrochloric acid (30%) | 1.0 | 0.046 | 0.046 | Adjusting pH of feed water to 6.5 |
| Antiscalant | 0.009 | 3.51 | 0.0032 | 5 ppm |
| Acid cleaning-Citric acid | 0.0035 | 2.46 | 0.0172 | Once a week,1% |
| Alkaline cleaning -Sodium hydroxide | 0.034 | 0.62 | 0.0042 | Once a week,0.1% |
| Alkaline cleaning -metal chelating agent (EDTA) | 0.0035 | 4.31 | 0.0030 | Once a week,1% |

Table S6. Details of chemical cost in the FO-RO scenario

| Item | Consumption per ton of water (kg/m³) | USD (\$/kg) | Operating cost per ton of water | Note |
|-------------------------|--|----------------|---------------------------------------|--|
| Hydrochloric acid (30%) | 1.0 | 0.046 | 0.046 | Adjusting pH |
| Sodium chloride | 0.777 | 0.238 | 0.185 | Supplemental draw solution concentration |