

ELECTRONIC SUPPLEMENTARY INFORMATION

Towards a greener synthesis of dianhydrohexitol esters

Katrin Städtke¹, Andreas W. Göpfert², Alexandra Inayat²

¹ Erlangen Center for Interface Research and Catalysis, Friedrich-Alexander-Universität Erlangen-Nürnberg, Egerlandstrasse 3, 91058 Erlangen, Germany

² Institute of Chemical Reaction Engineering, Friedrich-Alexander-Universität Erlangen-Nürnberg, Egerlandstrasse 3, 91058 Erlangen, Germany

| <u>Table of Contents</u> | Page |
|--|------|
| Fig. S1 Dean-Stark apparatus for the esterification using Route 1 | 2 |
| Fig. S2 Mass spectra of isosorbide (A) and isomannide (B) | 2 |
| Fig. S3 Mass spectra of isomannide monoester 2-propionyl isomannide (right) and diester 2,5-dipropionyl isomannide (left) | 2 |
| Fig. S4 Mass spectra of isosorbide monoesters 2-propionyl isosorbide (left) and 5-propionyl isosorbide (right) | 3 |
| Fig. S5 Mass spectra of isosorbide diesters 2,5-dipropionyl isosorbide (left) and byproduct 5-propionyl-2-sulfon isosorbide (right) | 3 |
| Fig. S6 ¹ H NMR spectra of isosorbide (starting material), 2,5-diacetyl isosorbide, 2,5-dipropionyl isosorbide and 2,5-dibutyryl isosorbide | 3 |
| Fig. S7 ¹ H NMR spectra of isomannide, 2,5-diacetyl isomannide and 2,5-dipropylisomannide | 4 |
| Fig. S8 Reaction progress for the esterification of isosorbide with butyric acid: gas chromatograms of esterification with entrainer n-propyl acetate, mass spectra of the new peak 'a' at retention time 4.4 min indicating butyric acid propyl ester (right) | 4 |
| Fig. S9 Gas chromatograms of the purified dianhydrohexitol esters | 4 |
| Tab. S1 Elementary or process flows of the chemicals and energy quantities for the production of 1t DAIS | 5 |
| References | 6 |



Fig. S1 Dean-Stark apparatus for the esterification using Route 1

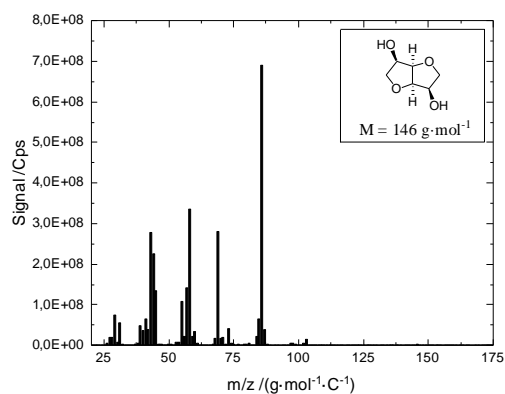
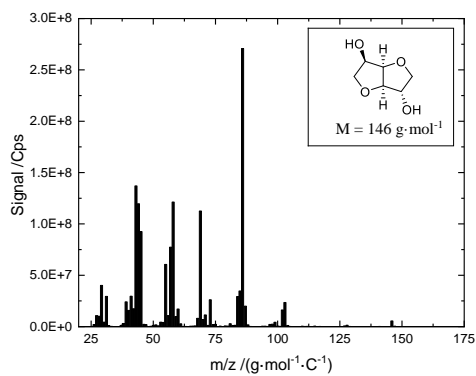


Fig. S2 Mass spectra of isosorbide (left) and isomannide (right)

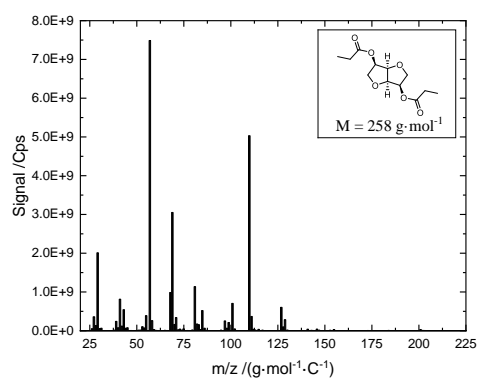
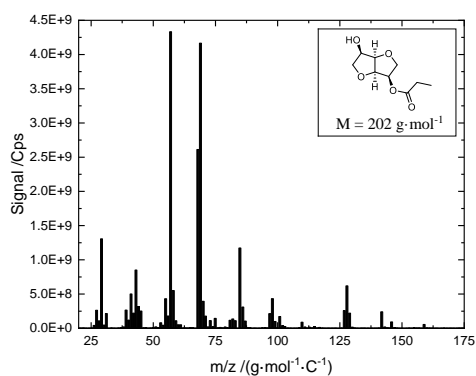


Fig. S3 Mass spectra of isomannide monoester 2-propionyl isomannide (left) and diester 2,5-dipropionyl isomannide (right); there were no further peaks beyond 175 and 225 $\text{g}\cdot\text{mol}^{-1}\cdot\text{C}^{-1}$

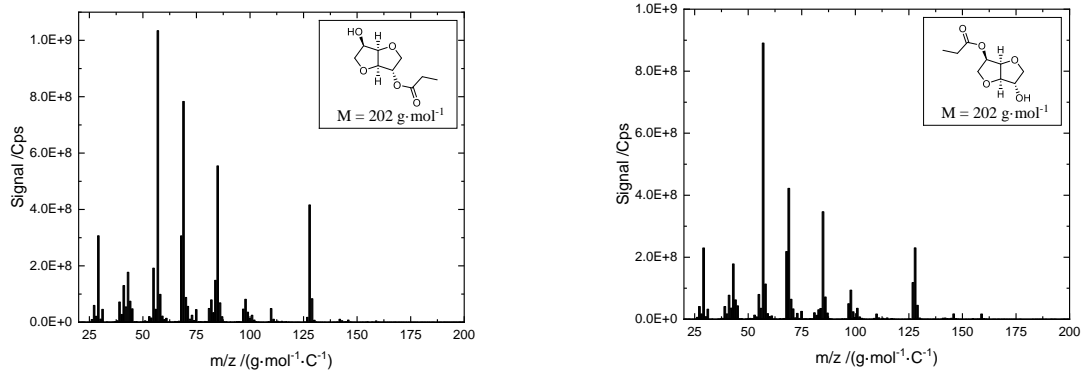


Fig. S4 Mass spectra of isosorbide monoesters 2-propionyl isosorbide (left) and 5-propionyl isosorbide (right); there were no further peaks beyond 200 $\text{g}\cdot\text{mol}^{-1}\cdot\text{C}^{-1}$

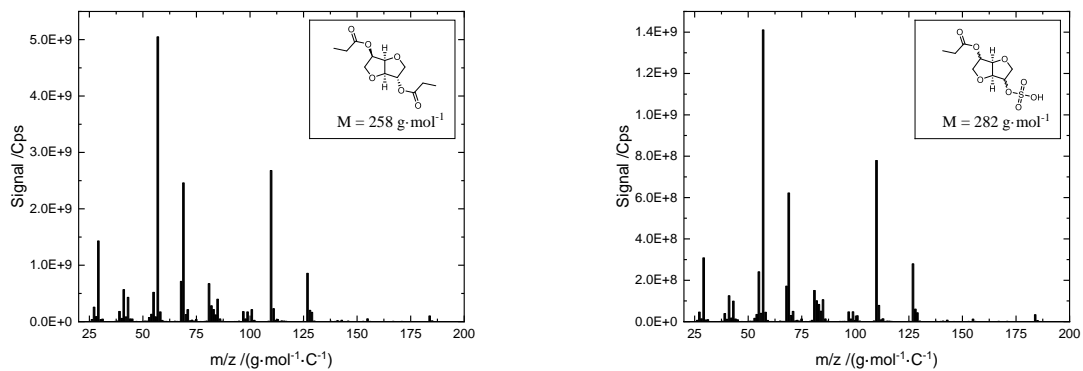


Fig. S5 Mass spectra of isosorbide diester 2,5-dipropionyl isosorbide (left) and byproduct 5-propionyl-2-sulfon isosorbide (right); there were no further peaks beyond 200 $\text{g}\cdot\text{mol}^{-1}\cdot\text{C}^{-1}$

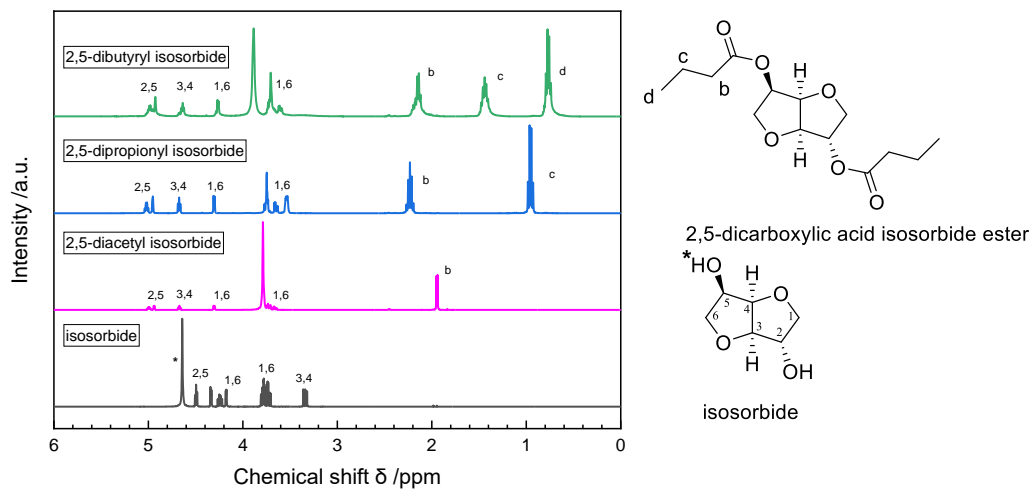


Fig. S6 ^1H NMR spectra of isosorbide (educt), 2,5-diacetyl isosorbide, 2,5-dipropionyl isosorbide and 2,5-dibutyl isosorbide

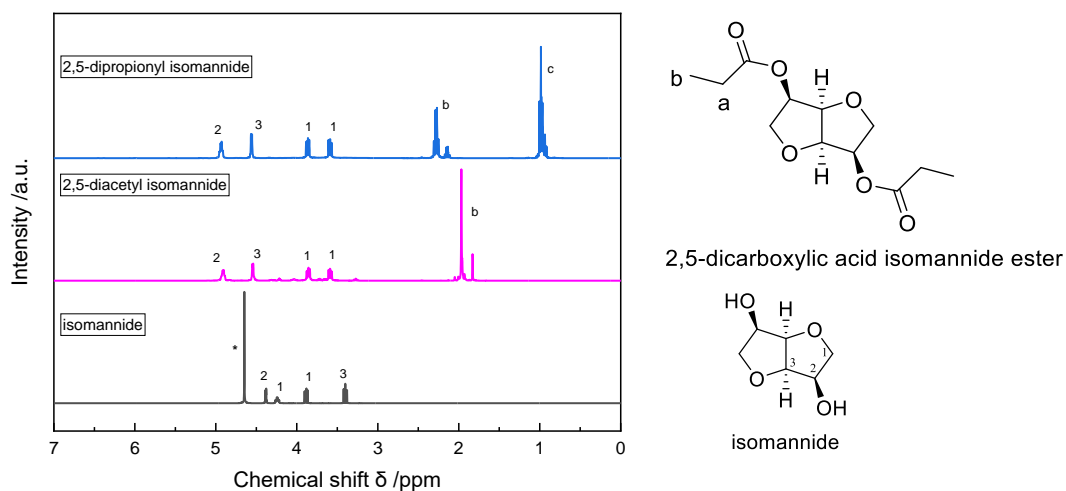


Fig. S7 ^1H NMR spectra of isomannide, 2,5-diacetyl isomannide and 2,5-dipropionyl isomannide

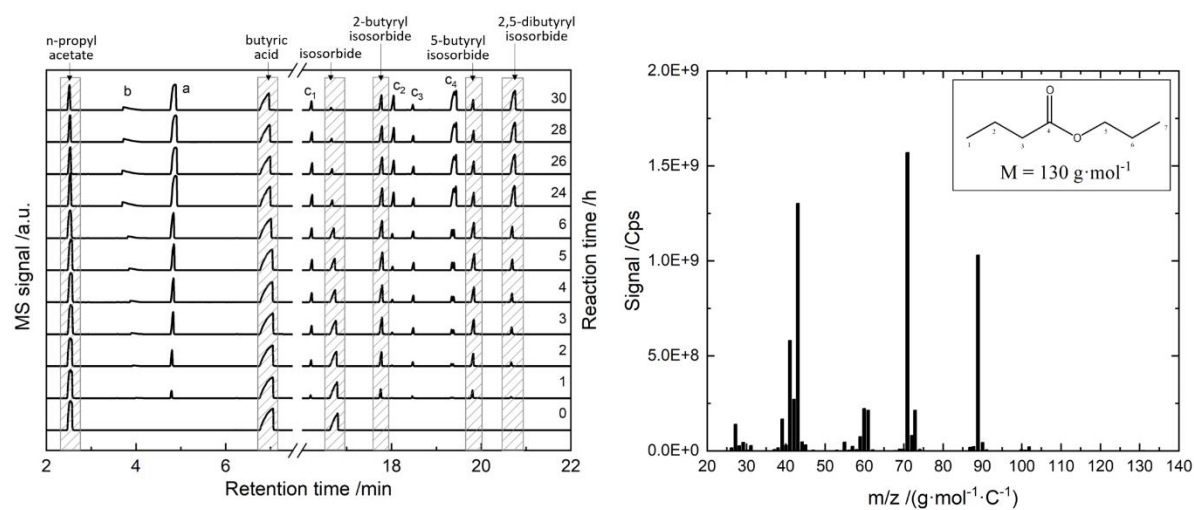


Fig. S8 Reaction progress for the esterification of isoribide with butyric acid: gas chromatograms of esterification of isoribide with entrainer n-propyl acetate, mass spectra of the new peak 'a' at retention time 4.4 min indicating butyric acid propyl ester (right)

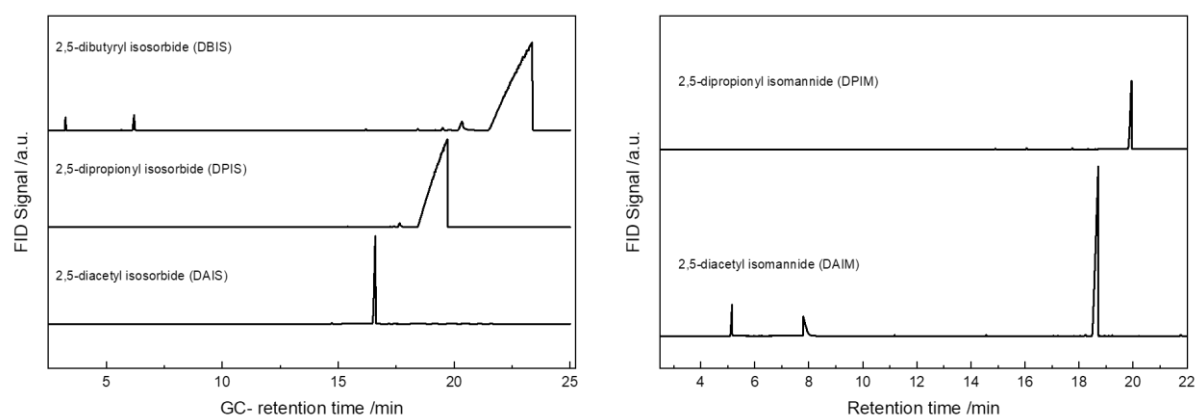


Fig. S9 Gas chromatograms of the purified dianhydrohexitol esters

OpenLCA data

Tab. S1 Elementary or process flows of chemicals and energy quantities for the production of 1000 kg DAIS; implemented processes are based on literature data; ecoinvent based product and elementary flows already contain the pre-processes from cradle-to-gate; output elementary flows are emissions which leave the product system under study and cause emissions and accordingly environmental impacts

| Elementary or process flow | Quantity for the production of 1t DAIS | Data source /Ecoinvent flows and processes used as input and output data for the openLCA impact assessment |
|--|---|---|
| Inputs Route 1 | | |
| Isosorbide | 648.5kg | Implemented process based on literature data [1-4] |
| Glucose | 1024.00 kg | Manufacture of starches and starch products: glucose production glucose Cutoff, U - GLO |
| Hydrogen, liquid | 11.41 kg | Manufacture of basic chemicals: market for hydrogen, liquid hydrogen, liquid Cutoff, U - RER |
| Water, deionised | 1530.61 kg | Water collection, treatment and supply: market for water, deionised water, deionised Cutoff, U - Europe without Switzerland |
| Energy for the catalytic hydrogenation of glucose to sorbitol | 9776.26 kWh | Electric power generation, transmission and electricity voltage: transformation from high to medium voltage electricity, medium voltage Cutoff, U - FR |
| Energy for the dehydration of sorbitol to isosorbide | 6607.19 kWh | Electric power generation, transmission and electricity voltage: transformation from high to medium voltage electricity, medium voltage Cutoff, U - FR |
| Energy and heat for the crystallisation of isosorbide | 1027.36 kWh | Electric power generation, transmission and electricity voltage: transformation from high to medium voltage electricity, medium voltage Cutoff, U - FR |
| Cooling water | 40.53 m ³ | Water collection, treatment and supply: market for water, deionised water, deionised Cutoff, U - Europe without Switzerland |
| Acetic acid | 1199.74 kg | Manufacture of basic chemicals: market for acetic acid, without water, in 98 % solution state acetic acid, without water, in 98 % solution state Cutoff, U - GLO |
| Amberlyst-15 (wet) | 31.74 kg | Implemented process based on literature data [5] |
| Styrene | 23.15 kg | Manufacture of plastics and synthetic rubber in primary forms: market for styrene styrene Cutoff, U - GLO |
| Divinylbenzene, produced from styrene and ethylene | 3.50 kg | Implemented process based on literature data [6] |
| water, deionised | 37.45 kg | Water collection, treatment and supply: market for water, deionised water, deionised Cutoff, U - Europe without Switzerland |
| Energy: polymerisation and functionalisation | 122.51 kWh | Electric power generation, transmission and distribution: electricity voltage transformation from high to medium voltage electricity, medium voltage Cutoff, U - DE |
| sulfuric acid | 3.41 kg | Manufacture of basic precious and other non-ferrous metals: market for sulfuric acid sulfuric acid Cutoff, U - RER |
| carboxymethyl cellulose, powder | 3.02 kg | Manufacture of basic chemicals: carboxymethyl cellulose production, powder carboxymethyl cellulose, powder Cutoff, U - RER |
| Entrainer: Toluene, liquid | Start: 2209.43 kg (recycle: 2099.50 kg) | Manufacture of basic chemicals: market for toluene, liquid toluene, liquid Cutoff, U – RER |
| n-propylacetate | Start: 2260.00 kg (recycle: 2147.00 kg) | Implemented process based on literature data [7] |
| Energy for chemicals production (pre-processes), for esterification [5], for DAIS purification [5] | 20020.32 kWh 10573.58 kWh 3873.64 kWh | Electric power generation, transmission and distribution: electricity voltage transformation from high to medium voltage electricity, medium voltage Cutoff, U - DE |
| Outputs Route 1 | | |
| Diacetyl isosorbide (DAIS) | 1000.0 kg | set output |
| Acetic acid | 62.8 kg | Elementary Flow: Emission to water/fresh water |

| | | |
|--|--|--|
| Entrainer: Toluene | 110.5 kg | Elementary Flow: Emission to water/fresh water |
| n-Propylacetate | 113.0 kg | Elementary Flow: Emission to water/unspecified |
| Waste water (from esterification) | 156.52 kg | Elementary Flow: Emission to water/fresh water |
| <i>Amberlyst-15 (wet and waste)</i> | | |
| Polystyrene waste | 31.74 kg | Elementary Flow: Waste/unspecified |
| Waste water from Amberlyst production, purification, functionalisation | 2568.0 kg | Elementary Flow: Emission to water/fresh water |
| Waste water from isosorbide production from glucose | 74940.0 kg | Elementary Flow: Emission to water/fresh water |
| Inputs Route 2 | | |
| Isosorbide | 634.78 kg | Implemented process based on literature data [1-4] |
| Acetic anhydride | 804.8 kg (recycle 566.2 kg) | acetic anhydride production, ketene route acetic anhydride Cutoff, U - RER |
| Water for hydrolysis | 10.5 kg | Water collection, treatment and supply: market for water, deionised water, deionised Cutoff, U - Europe without Switzerland |
| Energy for chemicals production (pre-processes), for esterification [5], for DAIS purification [5] | 31927.67 kWh 1162.08 kWh 3960.66 kWh | electricity voltage transformation from high to medium voltage electricity, medium voltage Cutoff, U - DE |
| Outputs Route 2 | | |
| Diacetyl isosorbide | 1000.0 kg | set output |
| Acetic acid | 269.33 kg | Elementary Flow: Emission to water/fresh water |
| Inputs Reference Route | | |
| Isosorbide | 634.78 kg | Implemented process based on literature data [1-4] |
| Acetic acid | 1199.74 kg | market for acetic acid, without water, in 98% solution state acetic acid, without water, in 98% solution state Cutoff, U - GLO |
| Sodium bicarbonate (NaHCO ₃) | 950.29 kg | market for sodium bicarbonate sodium bicarbonate Cutoff, U - GLO |
| Sulfuric acid | 1.27 kg | market for sulfuric acid sulfuric acid Cutoff, U - RER |
| Toluene | 2209.04 kg (recycle 2099.5 kg) | Manufacture of basic chemicals: market for toluene, liquid toluene, liquid Cutoff, U - RER |
| Energy for chemicals production (pre-processes), for esterification [5], for DAIS purification [5] | 28479.14 kWh 9163.77 kWh 3874.22 kWh | electricity voltage transformation from high to medium voltage electricity, medium voltage Cutoff, U - DE |
| Outputs Reference Route | | |
| Diacetyl isosorbide | 1000.0 kg | set output |
| Acetic acid | 678.0 kg | Elementary Flow: Emission to water/fresh water |
| Toluene | 110.5 kg | Elementary Flow: Emission to water/fresh water |
| Waste water (containing neutralized sulfuric acid) | 11456.5 kg | Elementary Flow: Emission to water/fresh water |
| Sodium sulfate | 1.27 kg | Elementary Flow: Resource/unspecified |

References

- [1] B. A. Rugg, W. Brenner, U.S. Patent No. 4,316,747, 1982.
- [2] C. Dussenne, T. Delaunay, V. Wiatz, H. Wyart, I. Suisse, M. Sauthier, Green Chemistry, 2007, 19, 5332.
- [3] J. C. Chao, D. T. Huibers U.S. Patent No. 4322569, 1982.
- [4] D. Schreck, M. Bradford, N. Clinton, P. Arbury, Patent No. WO2009126852, 2009.
- [5] P. Akkaramongkolporn, T. Ngawhirunpat, P. Opanasopit, AAPS PharmSciTech, 2009, 10, 641.
- [6] Ecoinvent database 3.7.1 "styrene production | styrene | Cutoff, U - RER".
- [7] Ecoinvent database 3.7.1 "propyl acetate production | isopropyl acetate | Cutoff, U - RER".
- [8] T. Fleiter, B. Schломann, W. Eichhammer, Fraunhofer-Verlag Stuttgart, 2013.