

Electronic Supporting Information

Subcritical CO₂-H₂O Hydrolysis of Polyethylene Terephthalate as a Sustainable Chemical Recycling Platform

Dacosta Osei,^{a,b,c} Lakshmiprasad Gurralla,^{a,b} Aria Sheldon,^{a,b} Jackson Mayuga,^{a,b} Clarissa Lincoln,^{d,e} Nicholas A. Rorrer^{d,e} and Ana Rita C. Morais^{a,b*}

^a Department of Chemical and Petroleum Engineering, University of Kansas, Lawrence, Kansas 66045, USA

^b Wonderful Institute for Sustainable Engineering, Lawrence, Kansas, 66045, USA

^c Center for Environmentally Beneficial Catalysis, University of Kansas, Lawrence, Kansas 66047, USA

^d Renewable Resources and Enabling Sciences Center, National Renewable Energy Laboratory, Golden, CO, 80401 USA

^e BOTTLE Consortium, Golden, CO 80401 USA

*Corresponding author: ana.morais@ku.edu

Table S1. Effect of CO₂ addition (versus N₂) and CO₂ pressure on the hydrolysis of PET.

Reaction conditions					Product yield (%)		
T (°C)	t (min)	Gas	Initial pressure (psi)	Final pressure (psi)	TPA	MHET	BHET
180	100	CO ₂	208	385±2	39.1±0.7	14.3±1.2	2.3±0.4
180	100	N ₂	208	384±1	1.9±0.4	2.0±0.3	1.1±0.2
180	100	CO ₂	108	258±1	12.6±1.4	7.3±0.8	2.3±1.6
180	100	CO ₂	308	539±1	59.4±0.8	11.4±2.2	1.6±0.4
180	100	CO ₂	408	694±2	73.6±0.6	7.1±0.6	0.9±0.1

Reaction condition:
s:
PET
to
H₂O
ratio
1:8

w/w (2.5 g PET: 20 g of H₂O); ^a Reactions were performed, at least, in duplicate.

Table S2. Performance of hot compressed H₂O (in absence of N₂ and CO₂) on the hydrolysis of PET at varying temperatures.

Reaction conditions		Product yield (%) ^a		
T (°C)	t (min)	TPA	MHET	BHET
180	100	0.5±0.0	0.5±0.5	0.2±0.2
190	100	0.1±0.2	0.2±0.2	0.1±0.0
200	100	2.4±3.4	2.7±3.4	1.4±1.9

Reaction conditions: PET to H₂O ratio 1:8 w/w (2.5 g PET: 20 g of H₂O); ^a Reactions were performed in duplicate. High product yield variability was obtained due to extremely low concentration of products dissolved in both H₂O and DMSO.

Table S3. Effect of H₂O and PET loading on the performance of subcritical CO₂-H₂O process on PET hydrolysis.

Reaction conditions					TPA yield (%)	PET conversion (%)
PET:H ₂ O loading (w/w)	T (°C)	t (min)	Initial pressure (psi)	Final pressure (psi)		
2.5g PET:20g H ₂ O	200	100	208	464	85.0	99.0
3.75g PET:20g H ₂ O	200	100	208	479	85.1	98.6
3.75g PET:30g H ₂ O	200	100	208	366	7.1	37.5

PET conversion is given as mass conversion into DMSO-soluble products.

Table S4. Effect of varying subcritical CO₂-H₂O conditions on the hydrolysis of PET.

Reaction conditions					Product yield (%)			PET conversion (%)
CS_{pCO_2}	T (°C)	t (min)	Initial pressure (psi)	Final pressure (psi)	TPA	MHET	BHET	
-0.65	180	10	208	383±1	0.0±0.0	0.6±0.7	0.5±0.2	1.95±2.8
-0.05	180	40	208	383±1	5.8±4.3	5.0±4.3	2.1±2.4	28.8±2.0
0.35	180	100	208	385±2	39.1±0.7	14.3±1.2	2.3±0.4	88.2±0.5
-0.41	190	10	208	421±2	0.0±0.8	1.7±0.8	1.5±1.1	21.1±1.5
0.20	190	40	208	420±4	30.2±2.3	12.0±1.2	3.3±0.1	95.6±0.8
0.59	190	100	208	421±3	68.3±0.4	6.7±3.1	0.8±0.6	96.6±1.1
-0.16	200	10	208	461±4	0.8±0.4	4.5±1.0	2.8±0.1	41.0±2.3
0.44	200	40	208	465±1	59.8±2.7	12.1±0.8	2.3±1.3	97.2±1.8
0.84	200	100	208	466±0	85.0±1.3	3.1±1.0	0.2±0.0	99.0±1.4

Reaction conditions: PET to H₂O ratio 1:8 w/w (2.5 g PET: 20 g of H₂O); ^a Reactions were performed, at least, in duplicate. CS_{pCO_2} values of -0.65, -0.41 and -0.16 were not included in Figure 3B in the manuscript because an insignificant production of TPA was observed under these reaction conditions. The effect of all calculated CS_{pCO_2} values as a function of PET conversion (%) can be found in Figure S8. PET conversion is given as mass conversion into DMSO-soluble products.

Table S5. Robustness of subcritical CO₂-H₂O to hydrolysis PET: PE mixture and waste PET bottles.

Substrate	Reaction conditions				Product yield (%)		
	T (°C)	t (min)	Initial pressure (psi)	Final pressure (psi)	TPA	MHET	BHET
100 wt% powder PET	200	100	208	455±0	87.2±2.2	3.6±0.7	0.6±0.3
50:50 w/w powder PET:PE	200	100	208	461±4	83.5±0.3	4.2±0.0	0.1±0.0
100 wt% powder colored Canada Dry PET bottle	200	100	208	457±1	86.2±2.2	2.9±0.1	0.2±0.1
100 wt% powder colored Mountain Dew PET bottle	200	100	208	458±2	82.5±3.8	2.8±0.0	0.2±0.1
100 wt% powder colored Twist up PET bottle	200	100	208	452±1	79.8±2.0	3.1±0.4	0.2±0.0
100 wt% powder transparent Pure Life® PET bottle	200	100	208	465±1	87.0±1.0	4.4±0.0	0.4±0.0

Reaction conditions: PET to H₂O ratio 1:8 w/w (2.5 g PET: 20 g of H₂O); ^a Reactions were performed, at least, in duplicate.

Table S6. Crystallinity content, enthalpy of melting (ΔH_m), cold crystallization enthalpy (ΔH_{cc}) of Mountain Dew and Twist Up waste PET soda bottles used in this work.

Substrate	Crystallinity (%)	ΔH_m (J/g)	ΔH_{cc} (J/g)
Mountain Dew bottle	19.5 ± 0.2	27.4 ± 0.3	0
Twist Up bottle	19.7 ± 0.5	27.6 ± 0.7	0

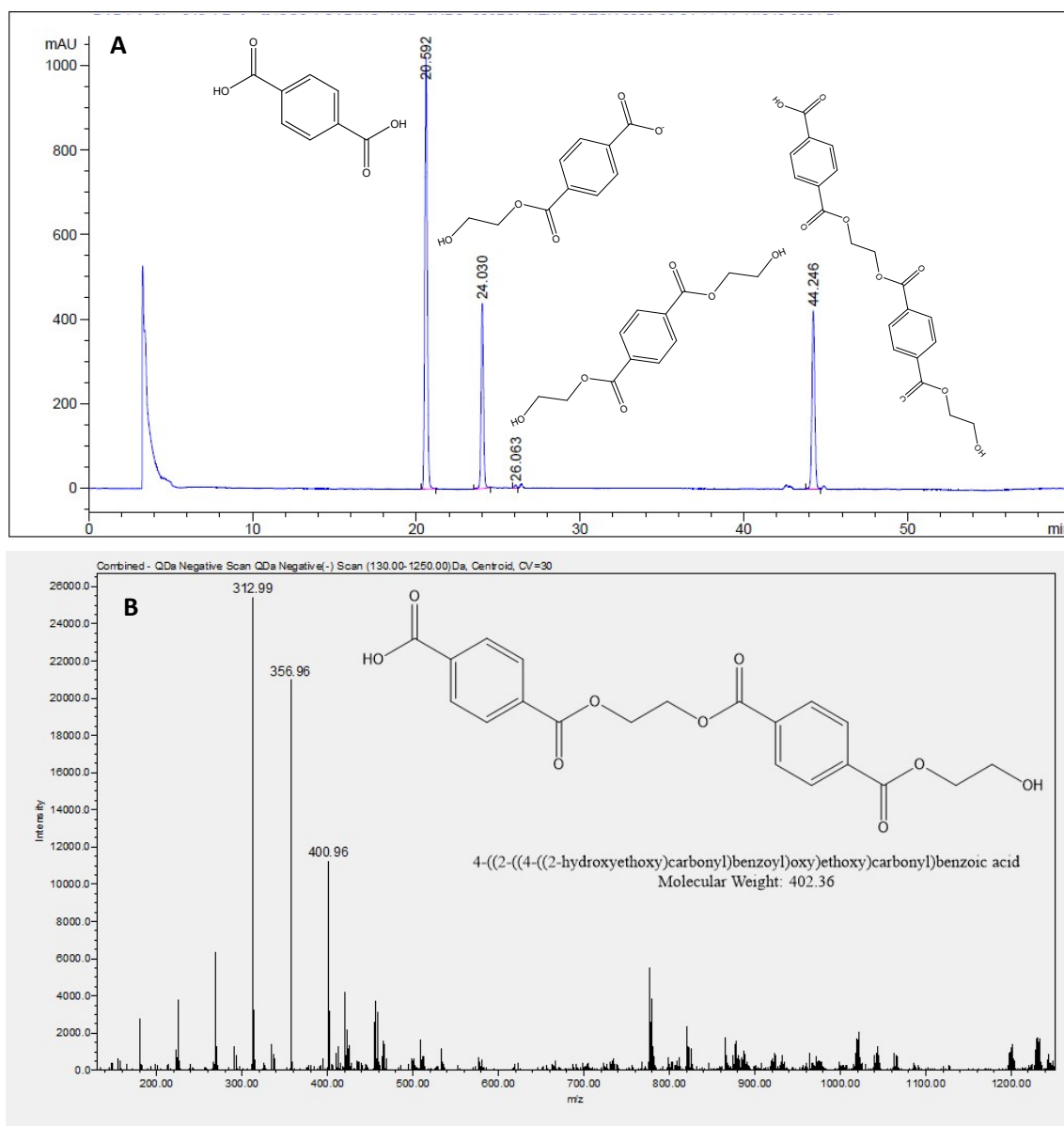


Figure S1 – A) Chromatogram of the liquid fraction obtained from subcritical CO₂-H₂O at 180 °C for 100 min. The compounds at 20.59, 24.03 and 26.06 minutes of retention time were identified using commercially available standards. The compound at 44.25 minutes of retention time was identified through Liquid Chromatography-Mass Spectrometry (LC-MS). B) Ion spectrum of the compound at 44.25 of retention time.

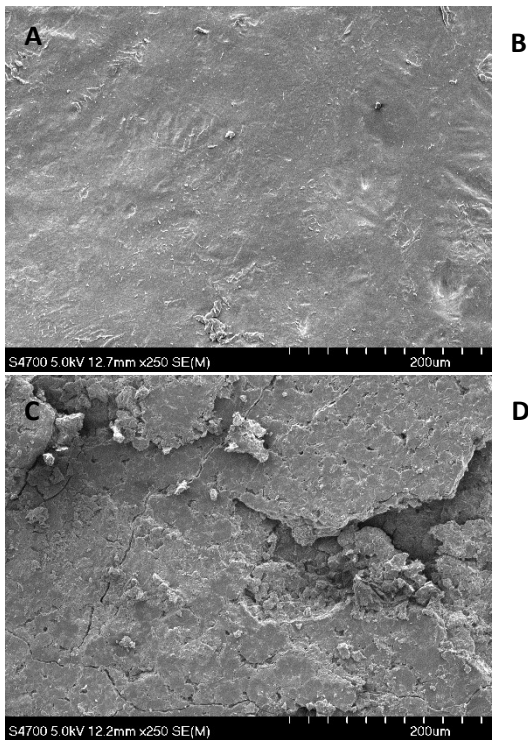


Figure S2 - Scanning electron microscopy of leftover PET samples from hot compressed H₂O (*i.e.* N₂-H₂O) reaction at 165 °C (non-isothermal conditions) (A), hot compressed H₂O (*i.e.* N₂-H₂O) at 180 °C for 10 min (B), subcritical CO₂-H₂O at 165 °C (non-isothermal conditions) with 208 psi of initial CO₂ pressure (C), and subcritical CO₂-H₂O at 180 °C for 10 min with 208 psi of initial CO₂ pressure (D).

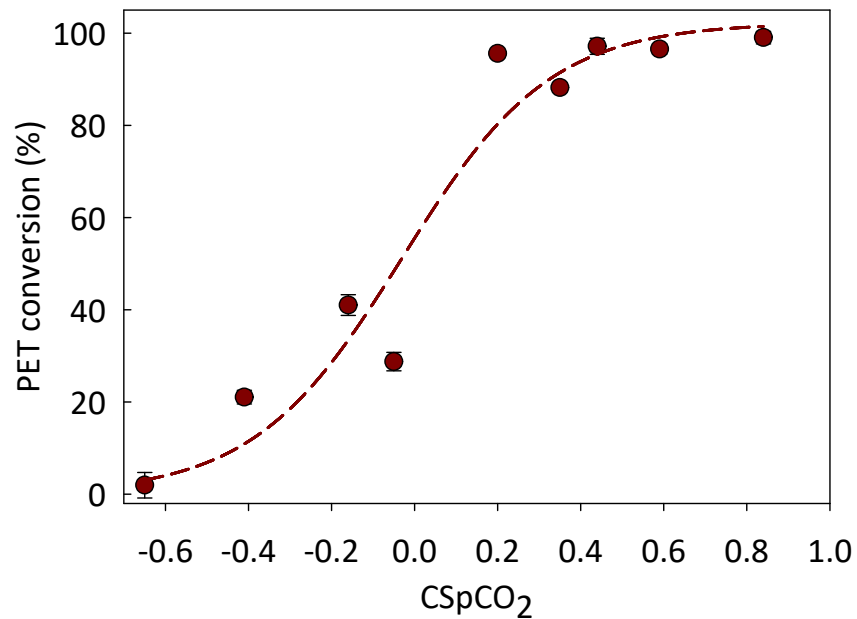


Figure S3 – PET conversion (mass conversion into DMSO-soluble products) as a function of combined severity factor (C_{SpCO_2}) follows a sigmoidal trend ($R^2=0.935$). PET to H₂O ratio 1:8 w/w (2.5 g PET: 20 g of H₂O) and 208 psi of initial CO₂ pressure at varying temperatures (180, 190 and 200 °C), and residence times (10, 40 and 100 min).

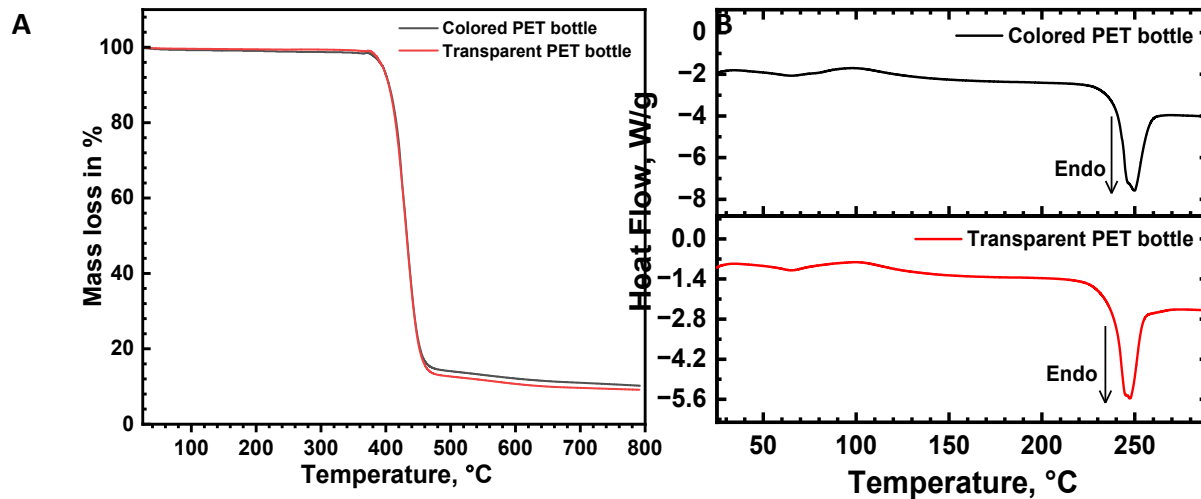


Figure S4 – Results from simultaneous thermogravimetric analysis (A) and differential scanning calorimetry (B) for both colored Canada Dry and transparent Pure Life® waste PET bottles.

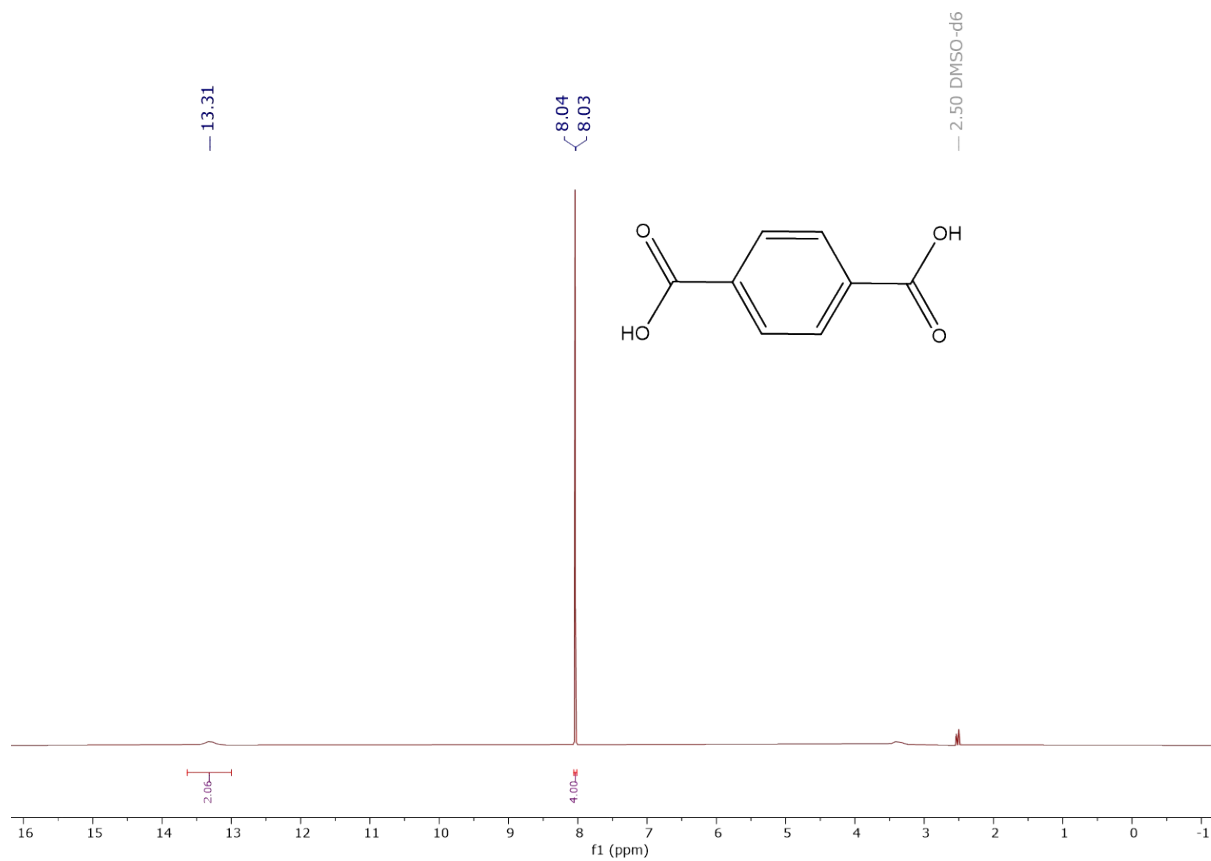


Figure S5 - ¹H NMR spectrum of TPA recovered from standard PET (free of pigments and other additives present in waste PET bottles) processed with subcritical CO₂-H₂O. ¹H NMR (400 MHz, DMSO) δ 13.31 (s, 2H), 8.04 (s, 4H).

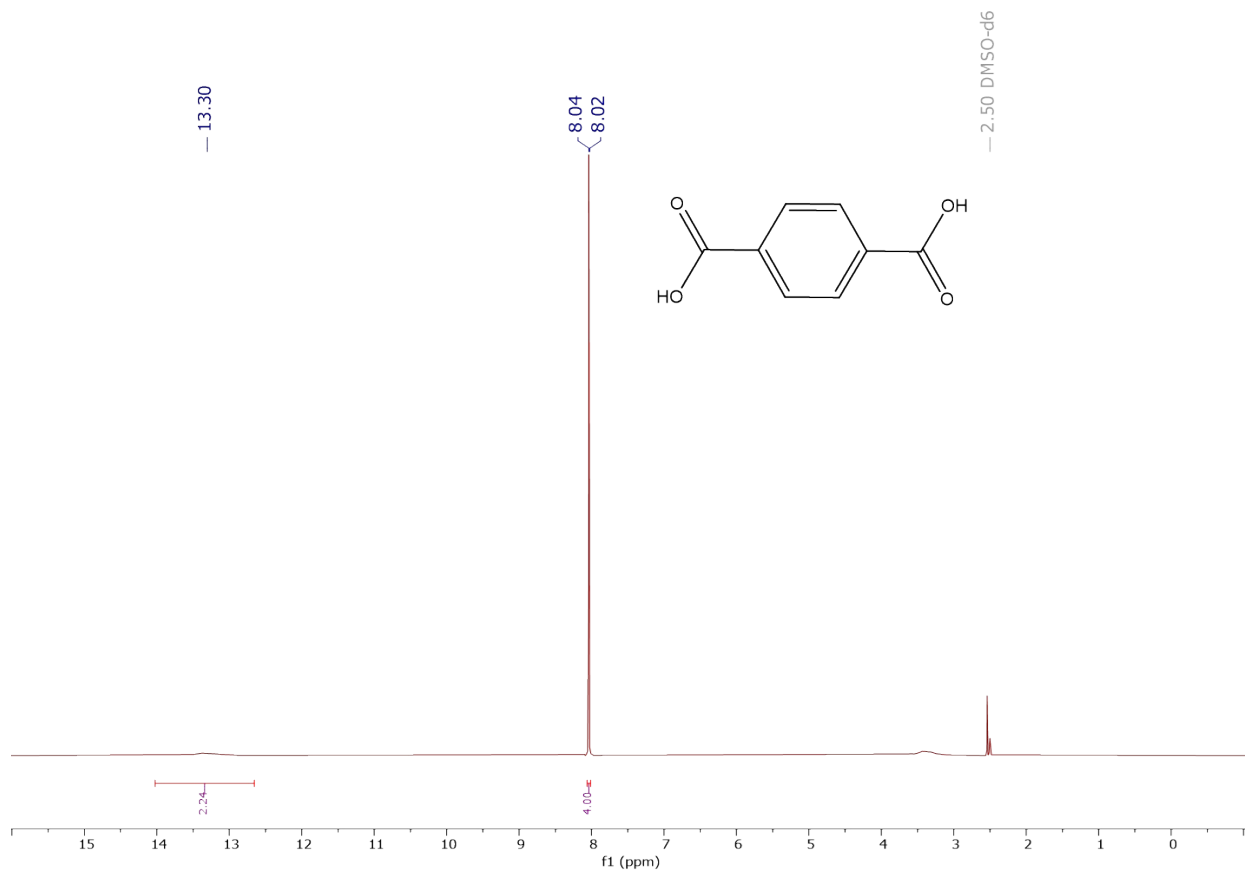


Figure S6 - ^1H NMR spectrum of TPA recovered from colored PET bottle processed with subcritical CO_2 - H_2O . ^1H NMR (400 MHz, DMSO) δ 13.31 (s, 2H), 8.04 (s, 4H).

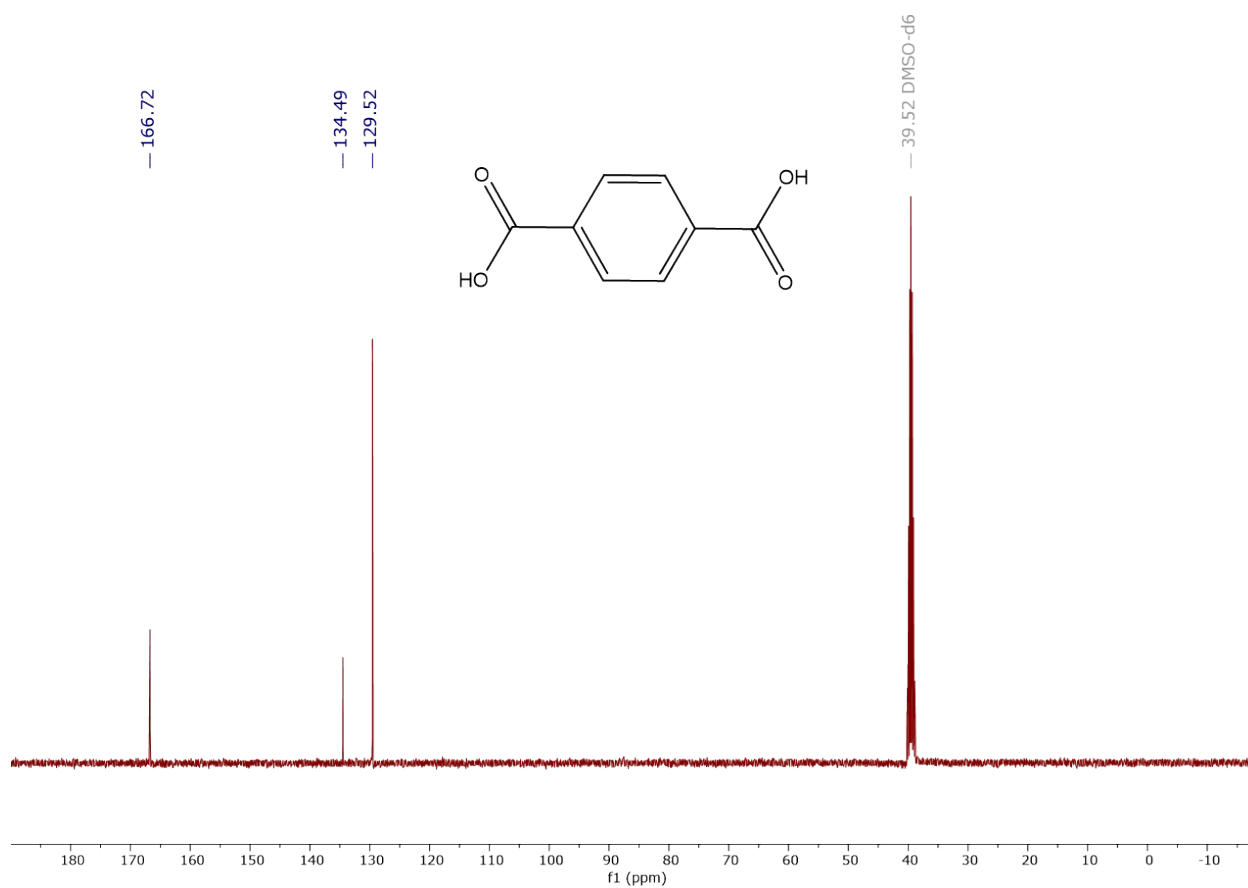


Figure S7. ^{13}C NMR spectrum TPA recovered from standard PET (free of pigments and other additives present in waste PET bottles) processed with subcritical $\text{CO}_2\text{-H}_2\text{O}$. ^{13}C NMR (101 MHz, DMSO) δ 166.72, 134.49, 129.52.

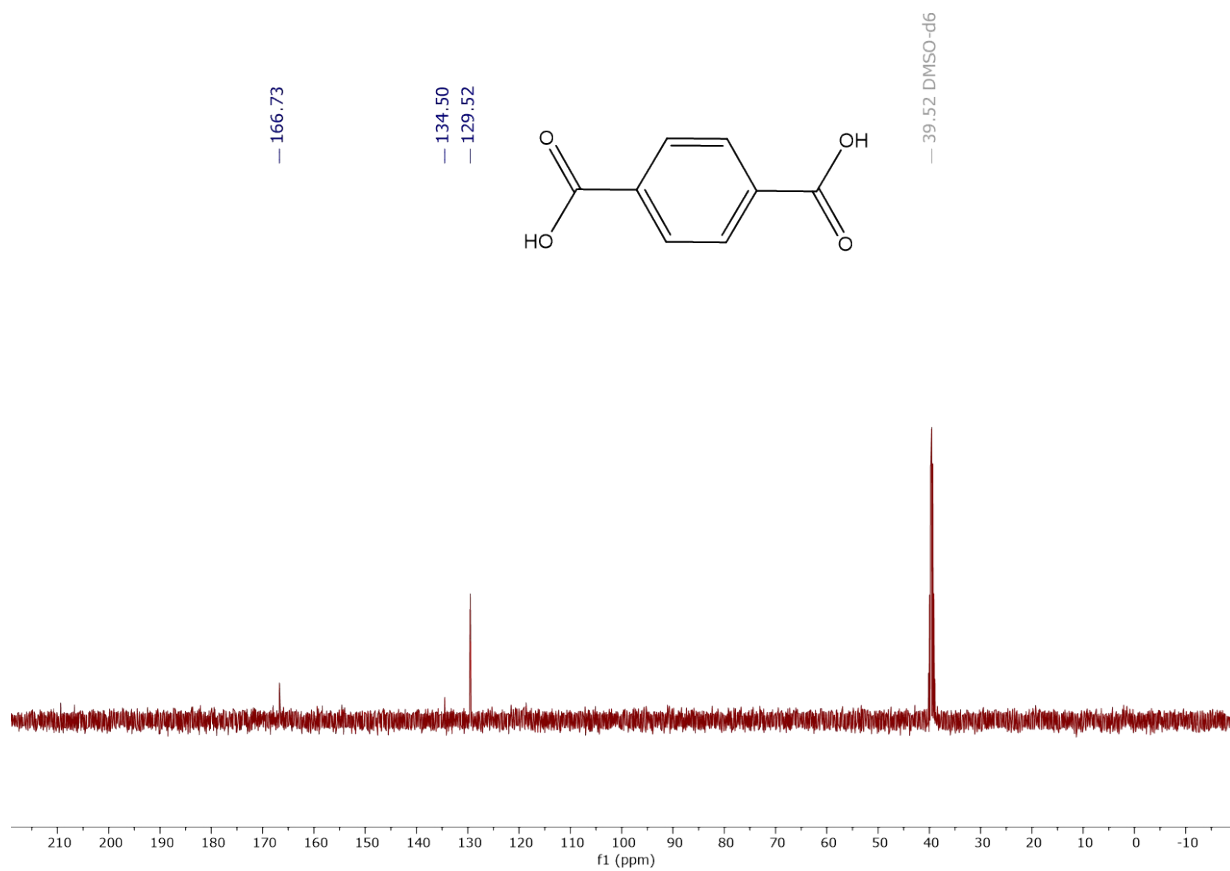


Figure S8. ¹³C NMR spectrum of TPA recovered from colored PET bottle processed with subcritical CO₂-H₂O. ¹³C NMR (101 MHz, DMSO) δ 166.73, 134.50, 129.52.

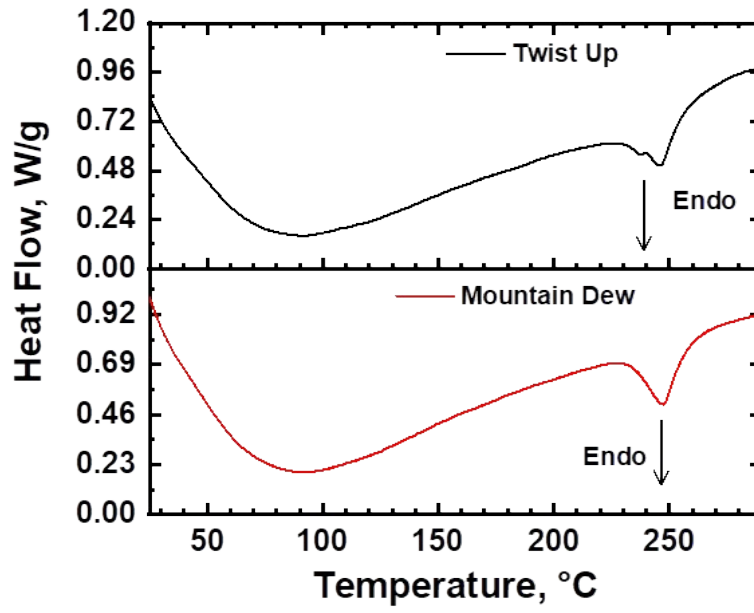


Figure S9 – Differential scanning calorimetry for both colored Twist Up and transparent Mountain Dew waste PET bottles.

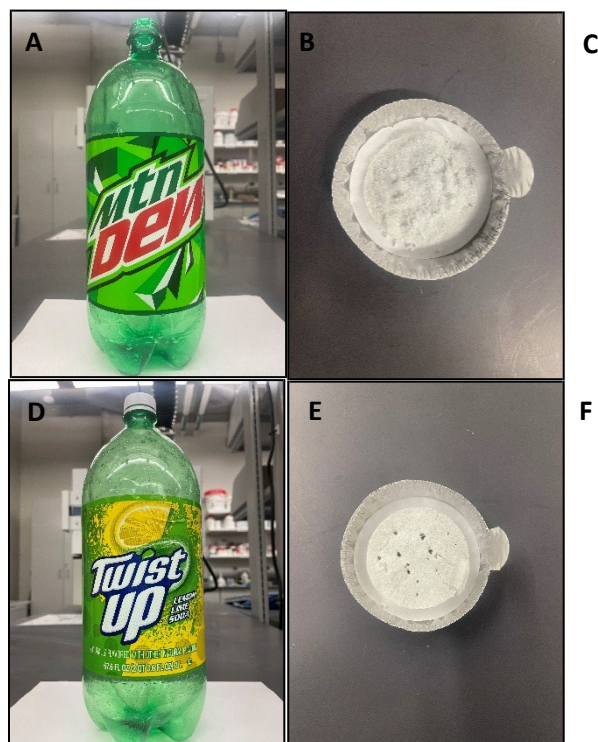


Figure S10 – Reaction with subcritical CO₂-H₂O (2.5 g PET: 20 g of H₂O) at 200 °C for 100 min with 208 psi of initial CO₂ pressure with post-consumer waste bottles, Mountain Dew bottle (A), Mountain Dew post reaction solids (B), Mountain Dew post reaction filtrate (C), and Twist Up bottle (D), Twist up post reaction solids (E), Twist Up post reaction filtrate (F).