

**Selective hydrogenolysis of agricultural straw-based
cellulose to propylene glycol and acetol over acidic
 WO_x/ZrO_2**

Zhicheng Luo^[a], Zhiguo Zhu^[b], Lupeng Han^[c], Rui Xiao^{[a]*}, Dawang Chu^{[d]*}

^[a] Dr. Z. Luo, Dr. R. Xiao

MOE Key Laboratory of Energy Thermal Conversion & Control, School of Energy and Environment, Southeast University, Nanjing 210096 (China)

E-mail address: ruixiao@seu.edu.cn

^[b] Dr. Z. Zhu

College of Chemistry and Chemical Engineering, Yantai University, Yantai 264005 (China)

^[c] Dr. L. Han

Department of Chemistry, College of Sciences, Shanghai University, Shanghai 200444 (China)

^[d] Dr. D. Chu*

School of Chemistry and Molecular Engineering, East China Normal University, Shanghai 200062 (China)

E-mail address: David__Chu@163.com

Characterization

X-ray diffraction (XRD) patterns were tested by Rigaku Ultima IV X-ray diffractometer equipped with Cu K α radiation operating at 35 kV and 25 mA ($\lambda = 1.5405 \text{ \AA}$) scanning from 5° to 90° at a speed of $30^\circ \text{ min}^{-1}$.

The temperature-programmed reduction (H₂-TPR) analysis of WO₃/ZrO₂ catalysts were performed by Micromeritics tp5080 apparatus using a 5% H₂/He mixture (flowing rate: $30 \text{ mL}\cdot\text{min}^{-1}$) and a heating rate of $10 \text{ K}\cdot\text{min}^{-1}$ with a thermal conductor detector (TCD).

Nitrogen sorption isotherms were collected on a BELSORP-MAX instrument, and reduced samples were kept on 77 K after degassing for 10 h under vacuum at 573 K. The special surface areas were calculated by the Brunauer-Emmett-Teller (BET) method. Surface density (SD, W/nm^2) = Concentration of W ($\text{g}_\text{W}/\text{g}_\text{Cat.}$) \times Avogadro number ($1/(\text{mol W})$) / BET area ($\text{m}^2/\text{g Cat.}$) \times Atomic weight of W ($\text{g}_\text{W}/\text{mol}_\text{W}$) $\times 10^{18}$ (nm^2/m^2)

The transmission electron microscopy (TEM) was measured on the FEI Tecnai G2 F30 microscope (operating at 300 kV).

X-ray photoelectron spectroscopy (XPS) were tested by a Thermo Scientific K-Alpha spectrometer equipped with Al K α ($h\nu = 1486.6 \text{ eV}$) radiation.

In CO₂/NH₃-TPD measurement, the samples were purged under He flow for 60 min at 723 K. The sample was cooled down to 393 K to be ready for adsorption. After adsorption saturation with purging CO₂/NH₃, the samples were heated from 393 K to 1073 K in He flow at a temperature rate of 10 K/min, and the desorbed NH₃ was monitored by a TCD detector.

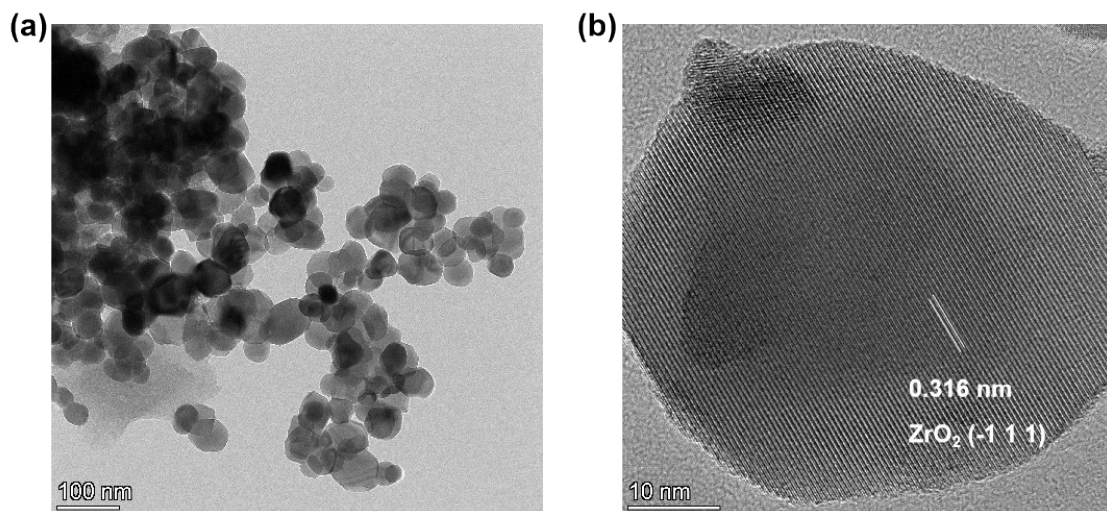


Figure S1. TEM image of WO_x/ZrO₂(600).

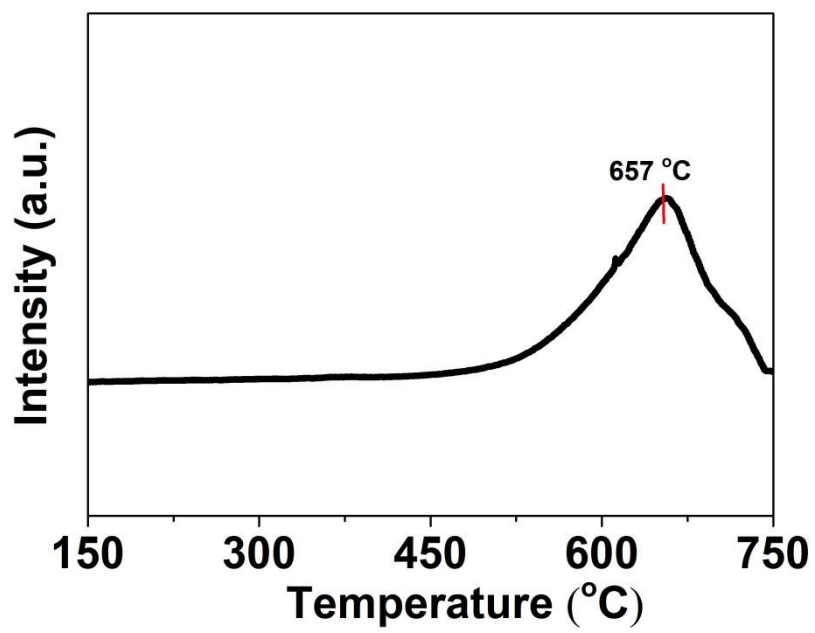


Figure S2. H₂-TPR profile of the WO₃/ZrO₂ sample.

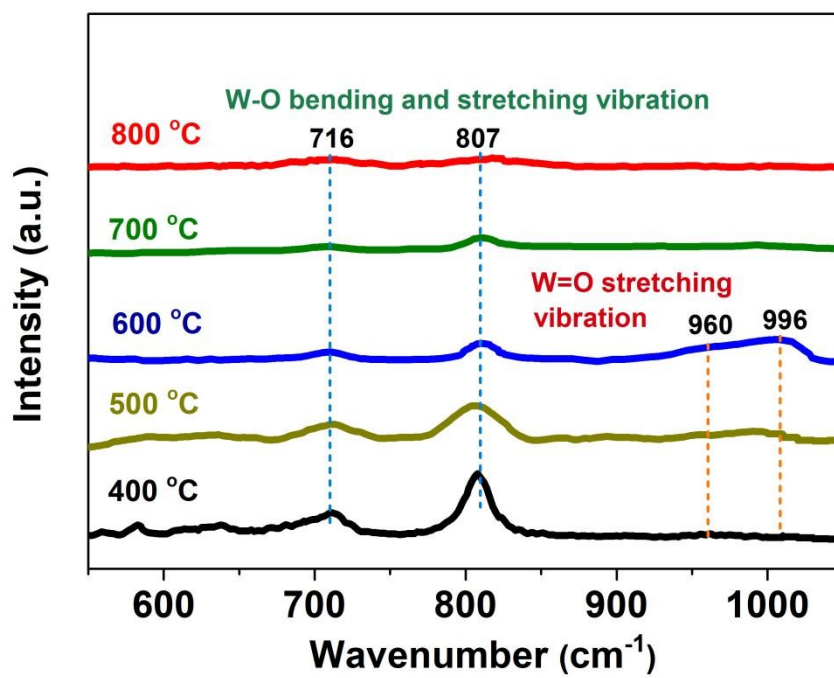


Figure S3. Raman spectra of different WO_x/ZrO₂(T) catalysts.

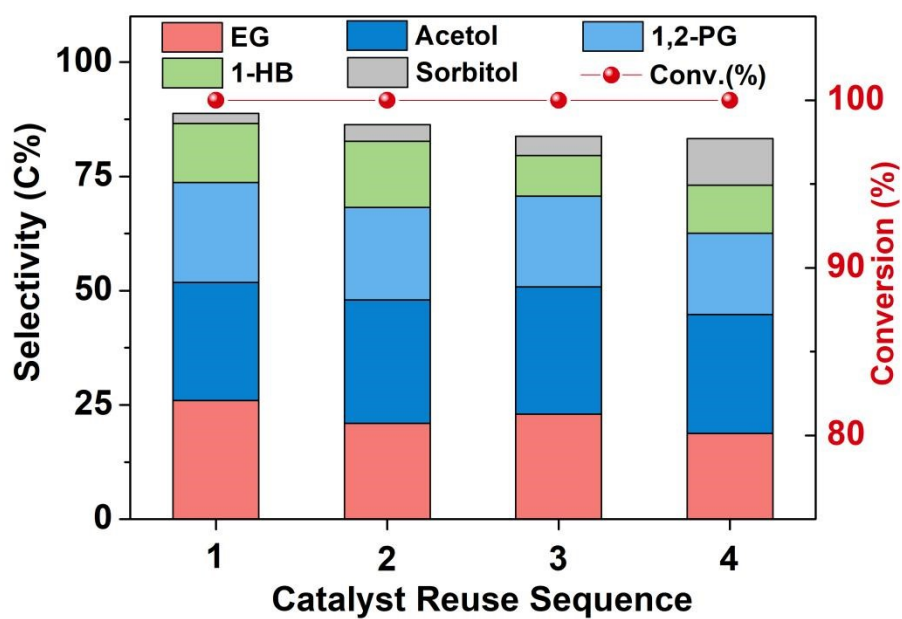


Figure S4. Recycling results of the $\text{WO}_x/\text{ZrO}_2(600)$ catalyst for cellulose hydrogenolysis. Reaction conditions: cellulose, 1.0 g; 20% $\text{WO}_x/\text{ZrO}_2(600)$, 0.2 g; 1%Ru/AC catalyst, 0.2 g; H_2O , 100 mL; H_2 , 4 MPa; 800 rpm; 240 °C; 2 h.

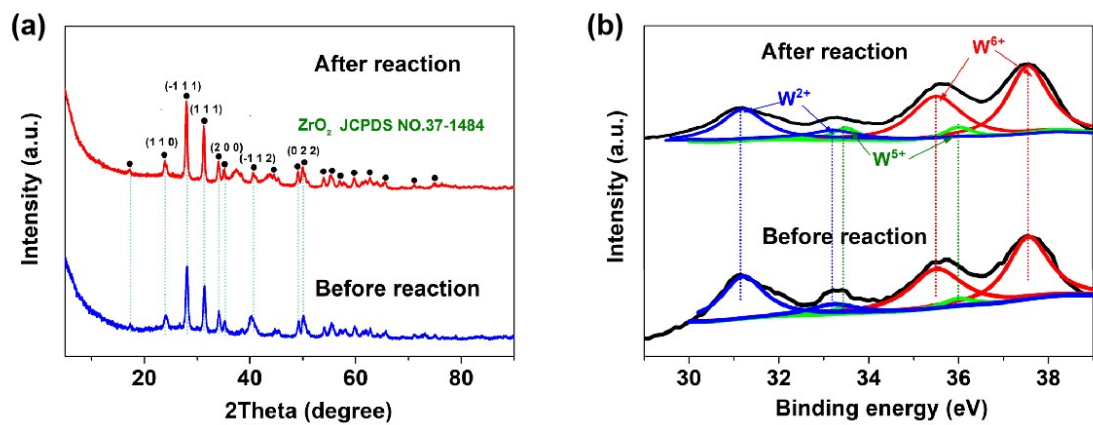


Figure S5. (a) xrd (b) xps spectra of WO_x/ZrO₂(600) catalyst before and after reaction.

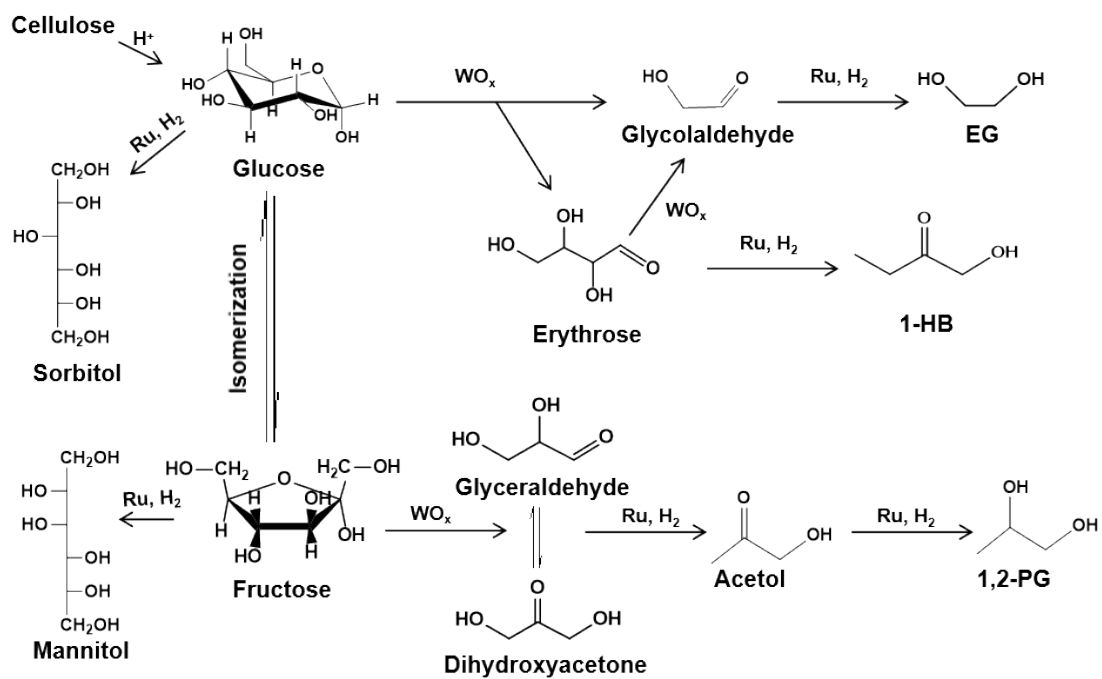


Figure S6. The mechanism of cellulose hydrogenolysis to acetol and 1,2-PG.

Table S1. The evaluation of different catalysts for the retro-aldol condensation of cellulose.

Catalyst	Conv. (C %)	Selectivity (C %)						Carbon balance (%)
		EG	Acetol	1,2-PG	1-HB	Sorbitol	Other	
WO _x /ZrO ₂ (400)+ Ru/AC	97.1	47.4	7.5	7.7	4.1	12.8	8.2	85.7
WO _x /ZrO ₂ (500)+ Ru/AC	98.5	45.1	10.1	14.2	8.5	5.6	2.2	85.7
WO _x /ZrO ₂ (600)+ Ru/AC	100.0	26.0	25.8	21.9	12.9	2.2	6.2	89.9
WO _x /ZrO ₂ (700)+ Ru/AC	100.0	48.8	8.0	12.8	6.5	3.2	2.0	82.3
WO _x /ZrO ₂ (800)+ Ru/AC	100.0	58.7	3.0	15.1	1.2	2.3	0.8	82.1

Reaction conditions: cellulose, 1.0 g; 30%WO_x/ZrO₂(T), 0.2 g; 1%Ru/AC catalyst, 0.2 g; H₂O, 100 mL; H₂, 4 MPa; 800 rpm; 240 °C; 2 h.

Table S2. The evaluation of different catalysts for the retro-aldol condensation of cellulose.

Catalyst	Conv. (C %)	Selectivity (C %)						Carbon balance (%)
		EG	Acetol	1,2-PG	1-HB	Sorbitol	Others	
WO _x /ZrO ₂ (600)	88.1	1.2	0	2.1	0	9.1	8.3	20.7
WO _x /ZrO ₂ (600) + 0.5%Ru/AC	99.0	16.5	19.3	8.2	4.9	3.5	8.1	60.5
WO _x /ZrO ₂ (600) + 1.0%Ru/AC	100.0	26.0	25.8	21.9	12.9	2.2	6.2	89.9
WO _x /ZrO ₂ (600) + 1.5%Ru/AC	100.0	19.3	13.4	16.7	9.3	4.1	10.3	73.1
1%Ru/AC	55.2	15.2	0.1	4.3	0.5	28.3	2.2	50.6

Reaction conditions: cellulose, 1.0 g; 30%WO_x/ZrO₂(600), 0.2 g; 1%Ru/AC catalyst, 0.2 g; H₂O, 100 mL; H₂, 4 MPa; 800 rpm; 240 °C; 2 h.

Table S3. ICP analysis of metal content of 30%WO_x/ZrO₂(600) + 1%Ru/AC catalyst before and after reaction.

Catalyst	Ru loading (wt %)	W loading (wt %)
Fresh	1.0	30.3
After 4 runs	1.0	26.9

Reaction conditions: cellulose, 1.0 g; 30%WO_x/ZrO₂(600), 0.2 g; 1%Ru/AC catalyst, 0.2 g; H₂O, 100 mL; H₂, 4 MPa; 800 rpm; 240 °C; 2 h.

Table S4. Catalytic conversion of glucose catalyzed by WO_x/ZrO₂(T) catalysts.

Catalyst	Conv. (C %)	Selectivity (C %)	
		Fructose	Others
WO _x /ZrO ₂ (400)+Ru/AC	24.3	66.1	9.9
WO _x /ZrO ₂ (500)+Ru/AC	24.7	64.5	10.9
WO _x /ZrO ₂ (600)+Ru/AC	26.8	75.5	13.1
WO _x /ZrO ₂ (700)+Ru/AC	18.1	73.8	6.1
WO _x /ZrO ₂ (800)+Ru/AC	14.6	55.9	11.8

Reaction conditions: 1 g glucose, 0.2 g catalyst, 50 ML DI-water, 120 °C, 2 h.
