

## Electronic Supporting Information

### **Electrostatically Driven Unidirectional Molecular Flux for High Performance Alkaline Flow Batteries**

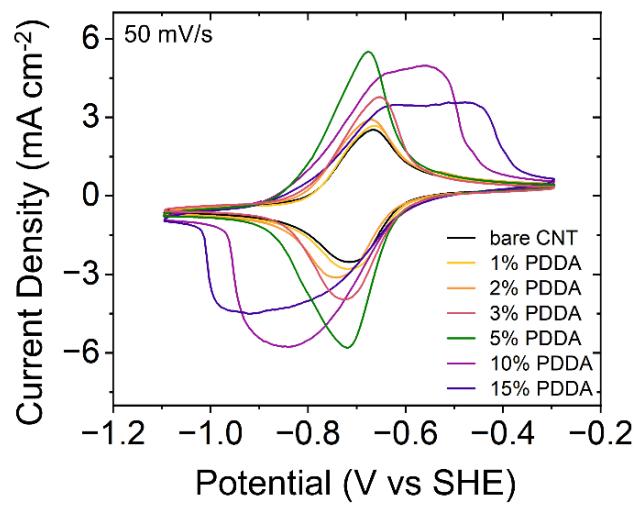
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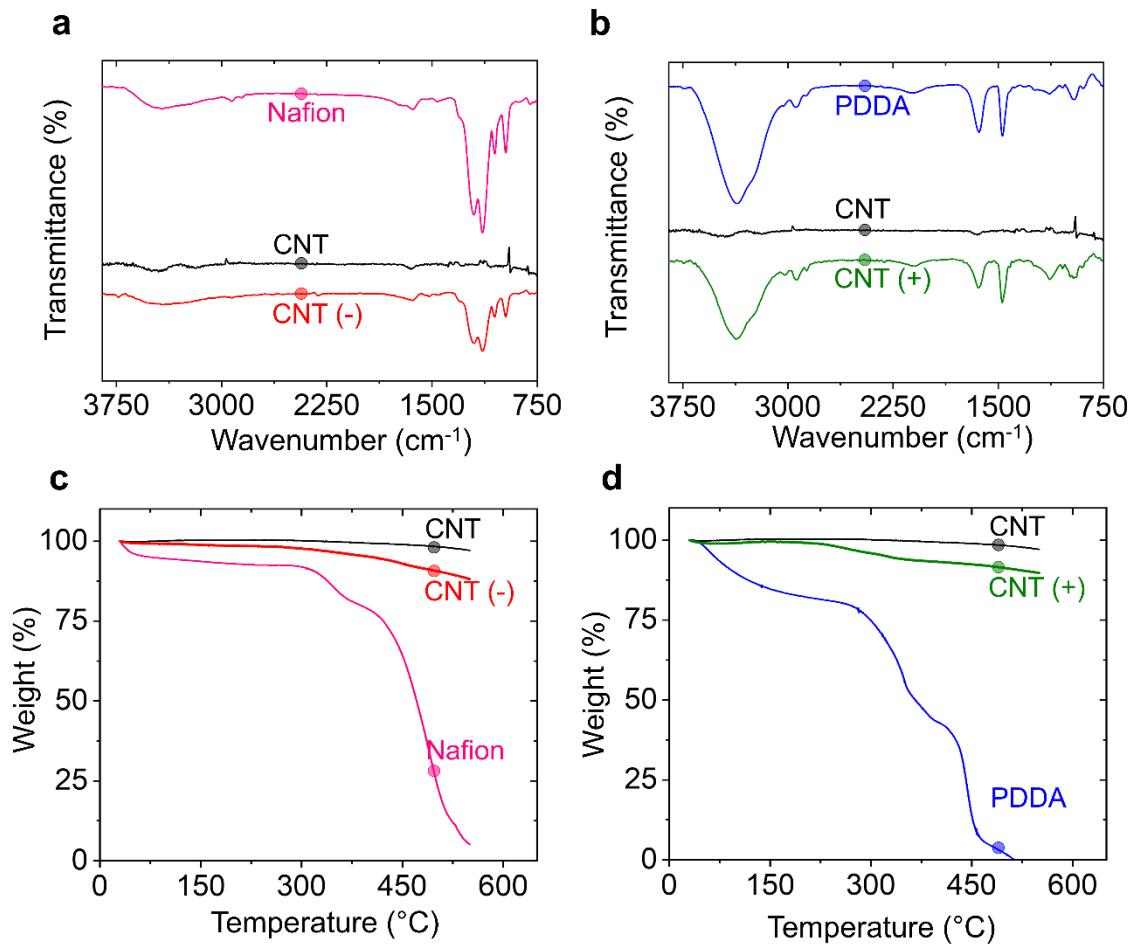
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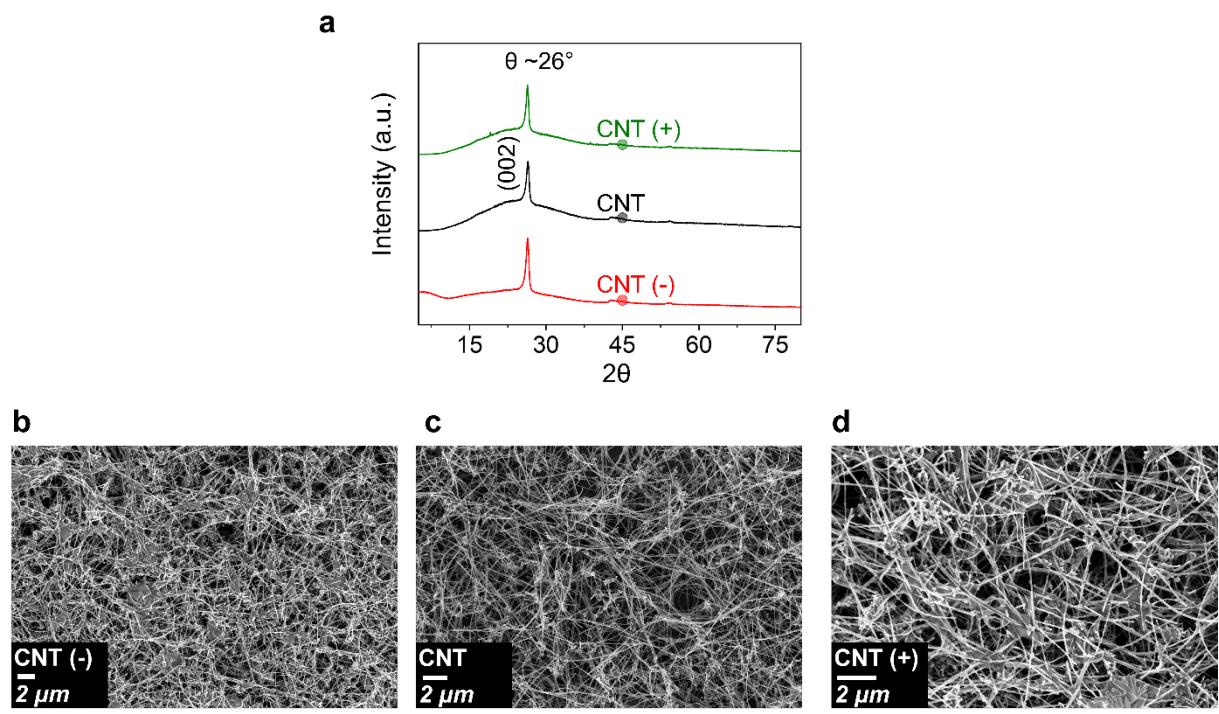
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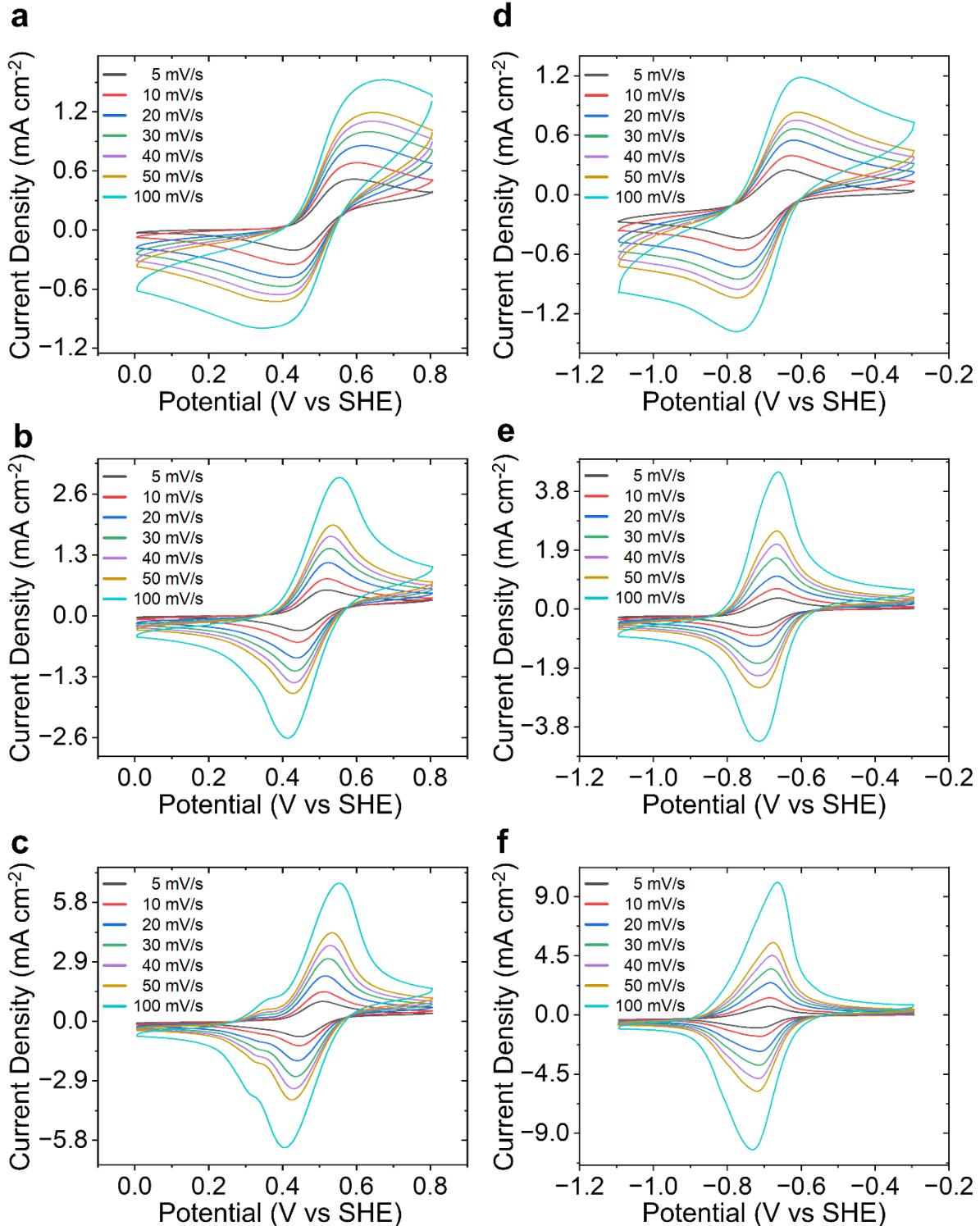
**Fig. S1** Cyclic voltammogram of 2,6-DHAQ molecule on the CNT (+) electrode with varying concentrations of PDDA in the modifying solution.



**Fig. S2** **(a)** ATR-FTIR spectra of CNT (-) and individual components. **(b)** ATR-FTIR spectra of CNT (+) and individual components. **(c)** TGA of CNT (-) and individual components. **(d)** TGA spectra of CNT (+) and individual components.



**Fig. S3** (a) Powder-XRD for CNT (+), CNT, and CNT (-). SEM images for (b) CNT (-), (c) CNT, and (d) CNT (+)



**Fig. S4** Scan rate dependence studies in 10 mM  $\text{K}_4[\text{Fe}(\text{CN})_6]$  in 1M KOH with **(a)** CNT(-), **(b)** CNT, and **(c)** CNT(+). Scan rate dependence studies in 5 mM 2,6-DHAQ in 1 M KOH with **(d)** CNT(-), **(e)** CNT, and **(f)** CNT(+).

## Calculation S1

Mass Transfer Coefficient ( $k_m$ ) Calculation

$$k_m = \frac{i}{nFAC}$$

$k_m$  = mass transfer coefficient (cm/s),  $i$  = limiting current (mA),  $n$  = number of electrons,  $A$  = area of electrode ( $\text{cm}^2$ ),  $C$  = concentration ( $\text{mol}/\text{cm}^3$ ),  $F$  = Faraday constant ( $\sim 96485 \text{ C/mol}$ ),

(a) From Fig. 3b

For 10 mM  $\text{K}_4\text{Fe}(\text{CN})_6$  solution in 1 M KOH

$$C = 0.01 \text{ mmol}/\text{cm}^3$$

$$A = 0.196 \text{ cm}^2$$

$$n = 1$$

- For CNT (-)

$$\begin{aligned} k_m &= \frac{i}{nFAC} \\ &= \frac{4.667}{96485 * 0.01} = 0.00483 \text{ cm/s} \end{aligned}$$

- (ii) For CNT

$$\begin{aligned} k_m &= \frac{i}{nFAC} \\ &= \frac{7.137}{96485 * 0.01} = 0.00739 \text{ cm/s} \end{aligned}$$

- (iii) For CNT (+)

$$\begin{aligned} k_m &= \frac{i}{nFAC} \\ &= \frac{10.9}{96485 * 0.01} = 0.0113 \text{ cm/s} \end{aligned}$$

(b) From Fig. 3d

For 5 mM 2,6-DHAQ solution in 1 M KOH

$$C = 0.005 \text{ mmol}/\text{cm}^3$$

$$A = 0.196 \text{ cm}^2$$

$$n = 2$$

- For CNT (-)

$$k_m = \frac{i}{nFAC}$$

$$= \frac{2.961}{2*96485*0.005} = 0.003 \text{ cm/s}$$

- (ii) For CNT

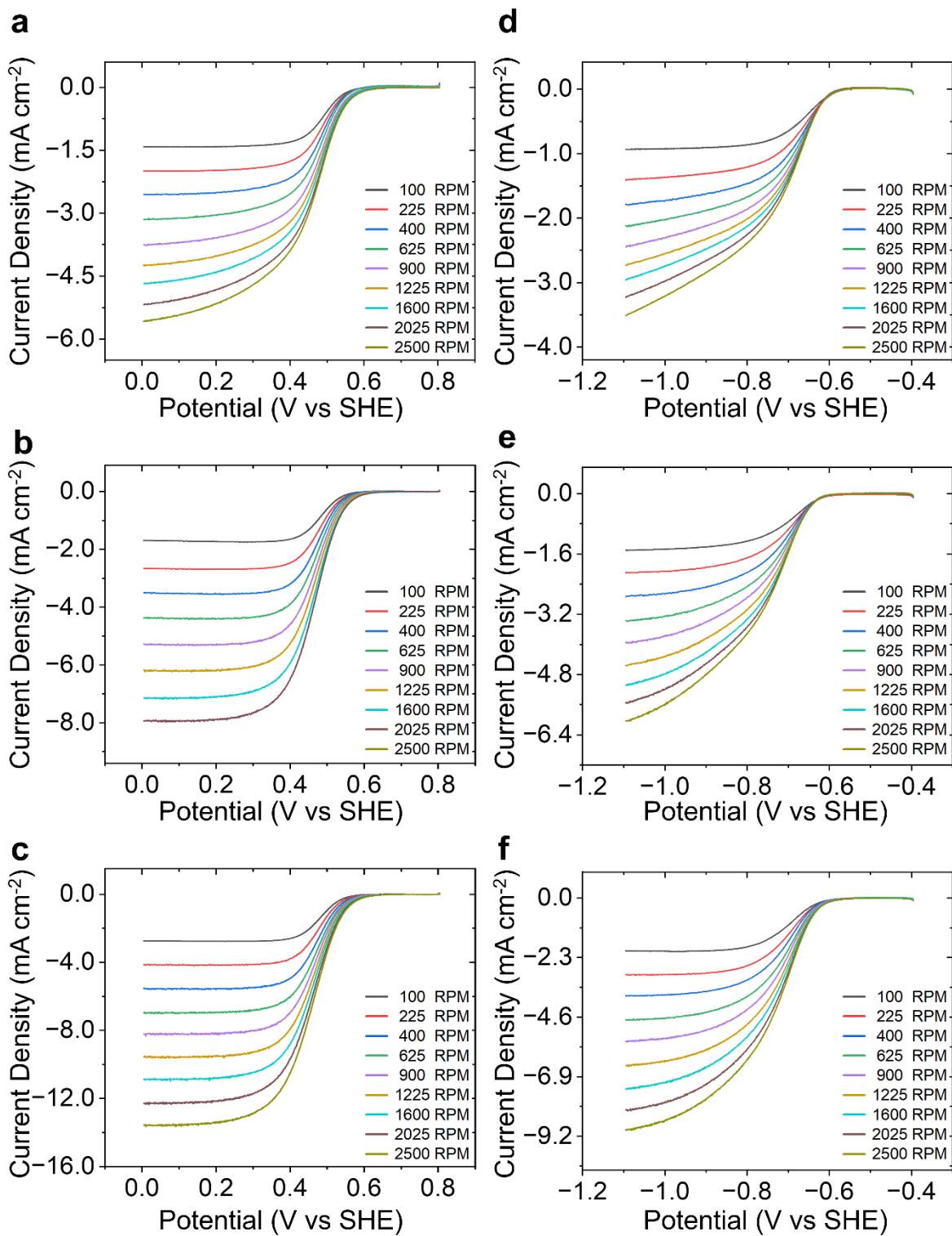
$$k_m = \frac{i}{nFAC}$$

$$= \frac{5.069}{2*96485*0.005} = 0.005 \text{ cm/s}$$

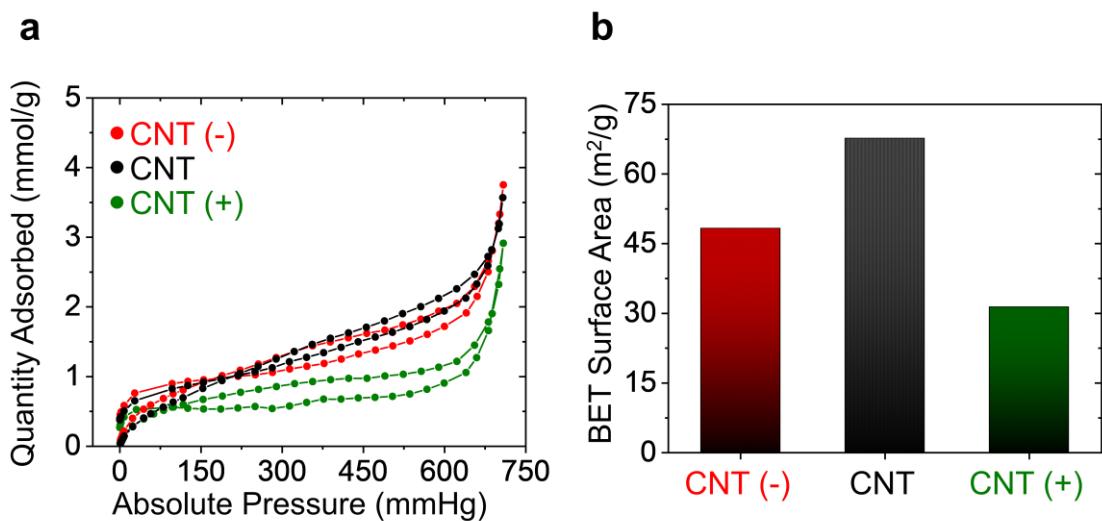
- (iii) For CNT (+)

$$k_m = \frac{i}{nFAC}$$

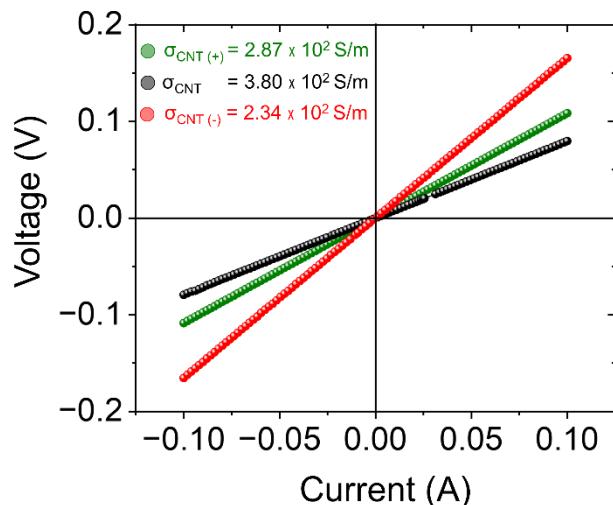
$$= \frac{7.388}{2*96485*0.005} = 0.0076 \text{ cm/s}$$



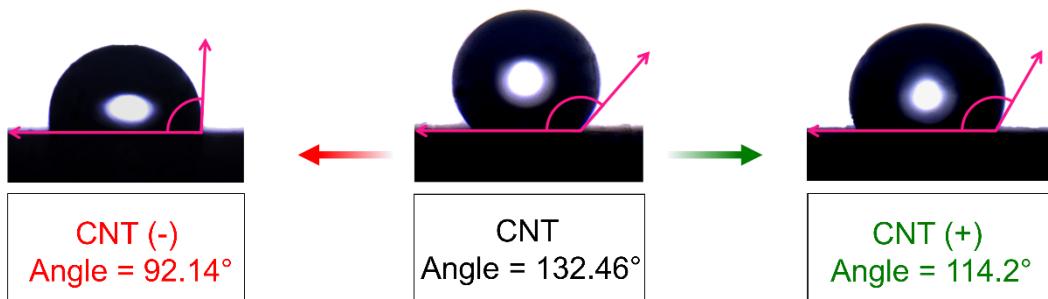
**Fig. S5** RDE studies at different rotations for  $10 \text{ mM K}_3[\text{Fe}(\text{CN})_6]$  in  $1 \text{ M KOH}$  with **(a)** CNT (-), **(b)** CNT and **(c)** CNT (+). RDE studies at different rotations for  $5 \text{ mM 2,6-DHAQ}$  in  $1 \text{ M KOH}$  with **(d)** CNT (-), **(e)** CNT and **(f)** CNT (+).



**Fig. S6 (a) and (b)** BET surface area for CNT (+), CNT and CNT (-).



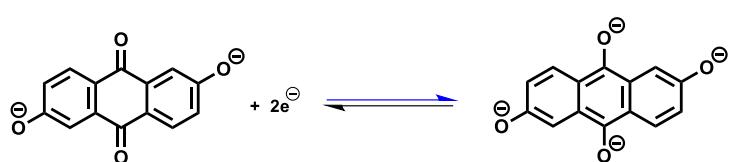
**Fig. S7** I-V data for electrical conductivity measurements extracted from the four-point probe method for CNT (+), unmodified CNT and CNT (-).



**Fig. S8** Contact angle measurements for CNT (-), CNT and CNT (+) (Left to right).

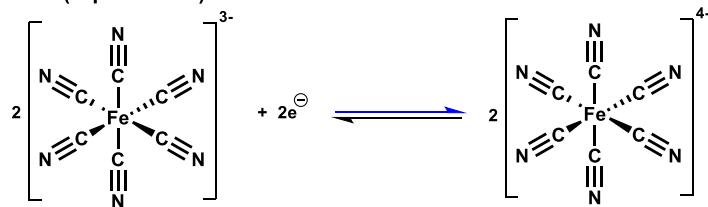
## The battery's half-cell and full-cell chemistries

Anodic Reaction (Equation S1):



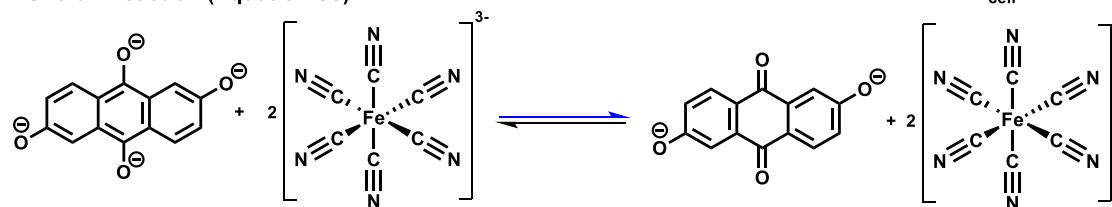
$E^\circ = -0.68 \text{ V vs SHE}$   
(pH 14)

Cathodic Reaction (Equation S2):

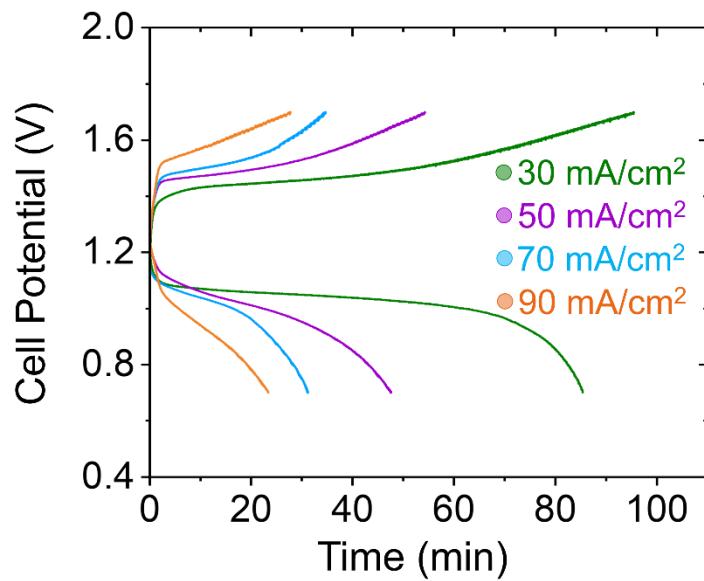


$E^\circ = 0.36 \text{ V vs SHE}$

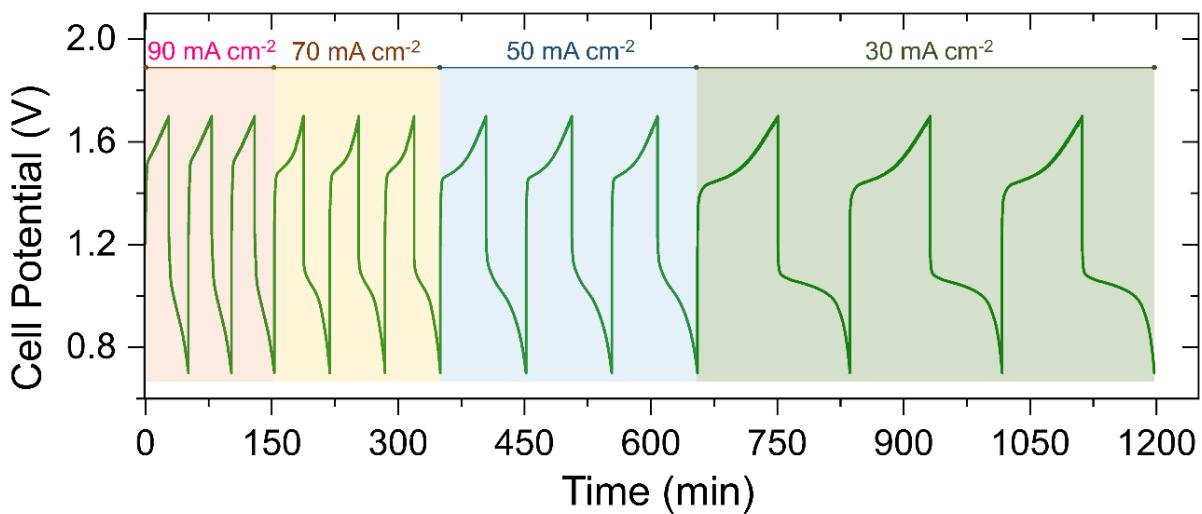
Overall Reaction (Equation S3):



$E^\circ_{\text{cell}} = 1.04 \text{ V vs SHE}$



**Fig. S9** Charge-discharge cycling of the redox flow battery equipped with the CNT (+) electrode at various current densities.



**Fig. S10** Charge-discharge cycling of the redox flow battery equipped with the CNT (+) electrode at various current densities. Here, the data is shown as a function of time.

## Calculation S2

### Energy Efficiency (EE) Calculation

$$EE = \frac{(C*V)_{\text{discharge}}}{(C*V)_{\text{charge}}}$$

From Fig. 4d

- In case of CNT (-)

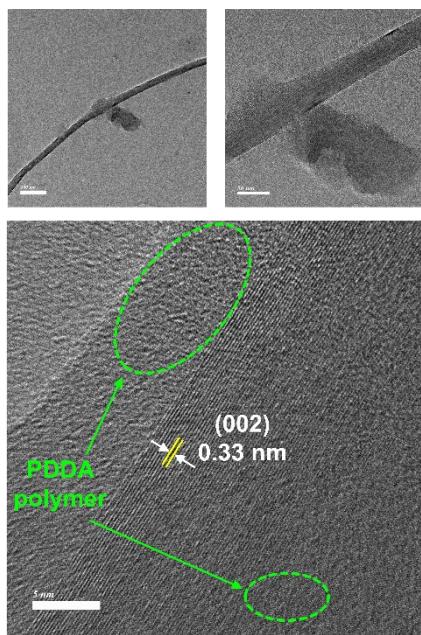
$$EE = \frac{\text{Area under the discharge curve (red discharge trace in Figure 4d)}}{\text{Area under the charge curve (red charge trace in Figure 4d)}}$$
$$= \frac{208.89}{456.10}$$
$$= 45.79 \%$$

- In case of CNT

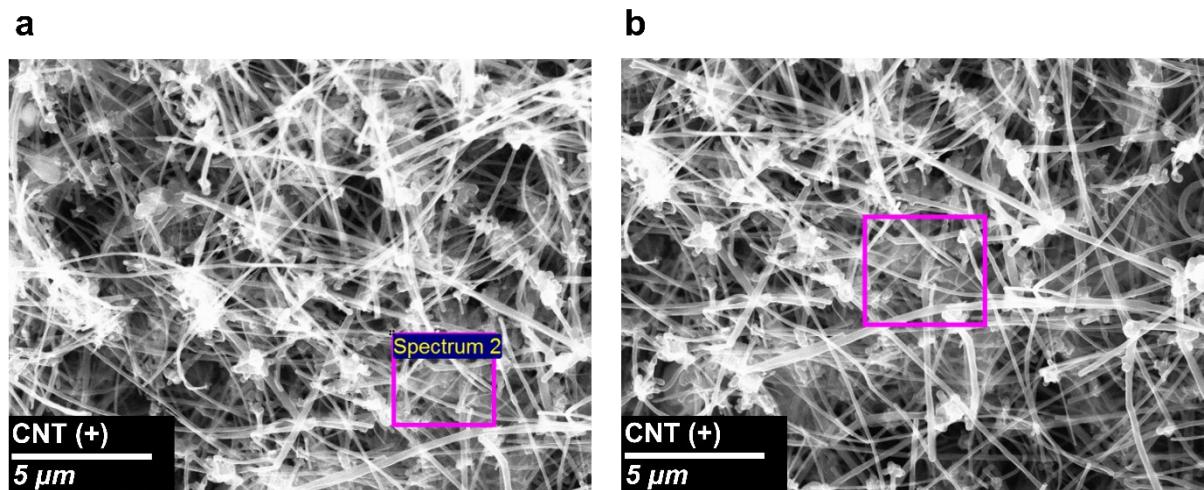
$$EE = \frac{\text{Area under the discharge curve (black discharge trace in Figure 4d)}}{\text{Area under the charge curve (black charge trace in Figure 4d)}}$$
$$= \frac{465.36}{684.21}$$
$$= 68.01 \%$$

- In case of CNT (+)

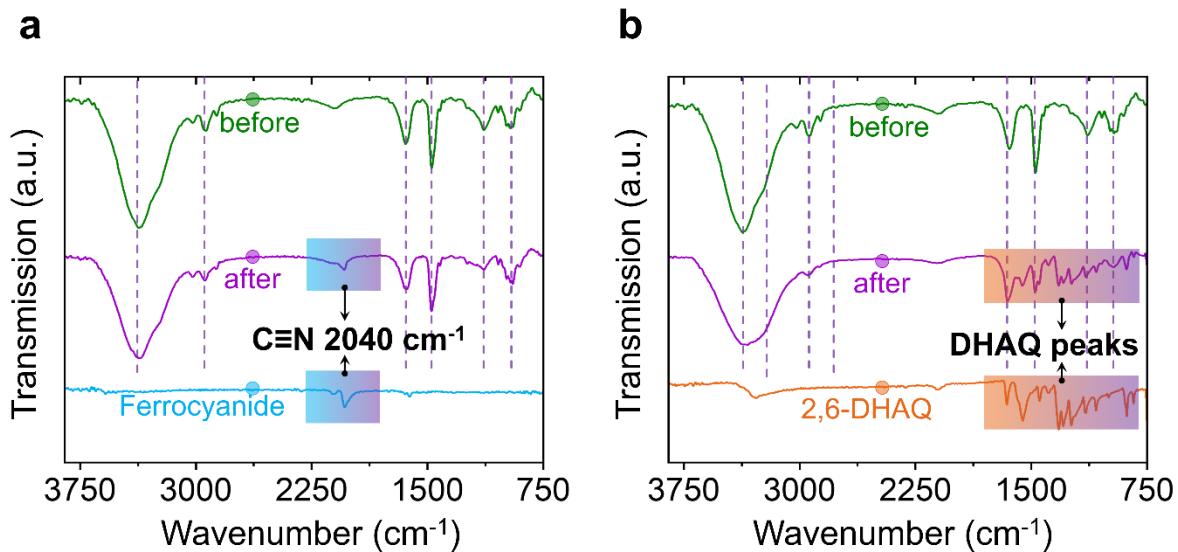
$$EE = \frac{\text{Area under the discharge curve (olive green discharge trace in Figure 4d)}}{\text{Area under the charge curve (olive green charge trace in Figure 4d)}}$$
$$= \frac{857.55}{933.23}$$
$$= 91.89 \%$$



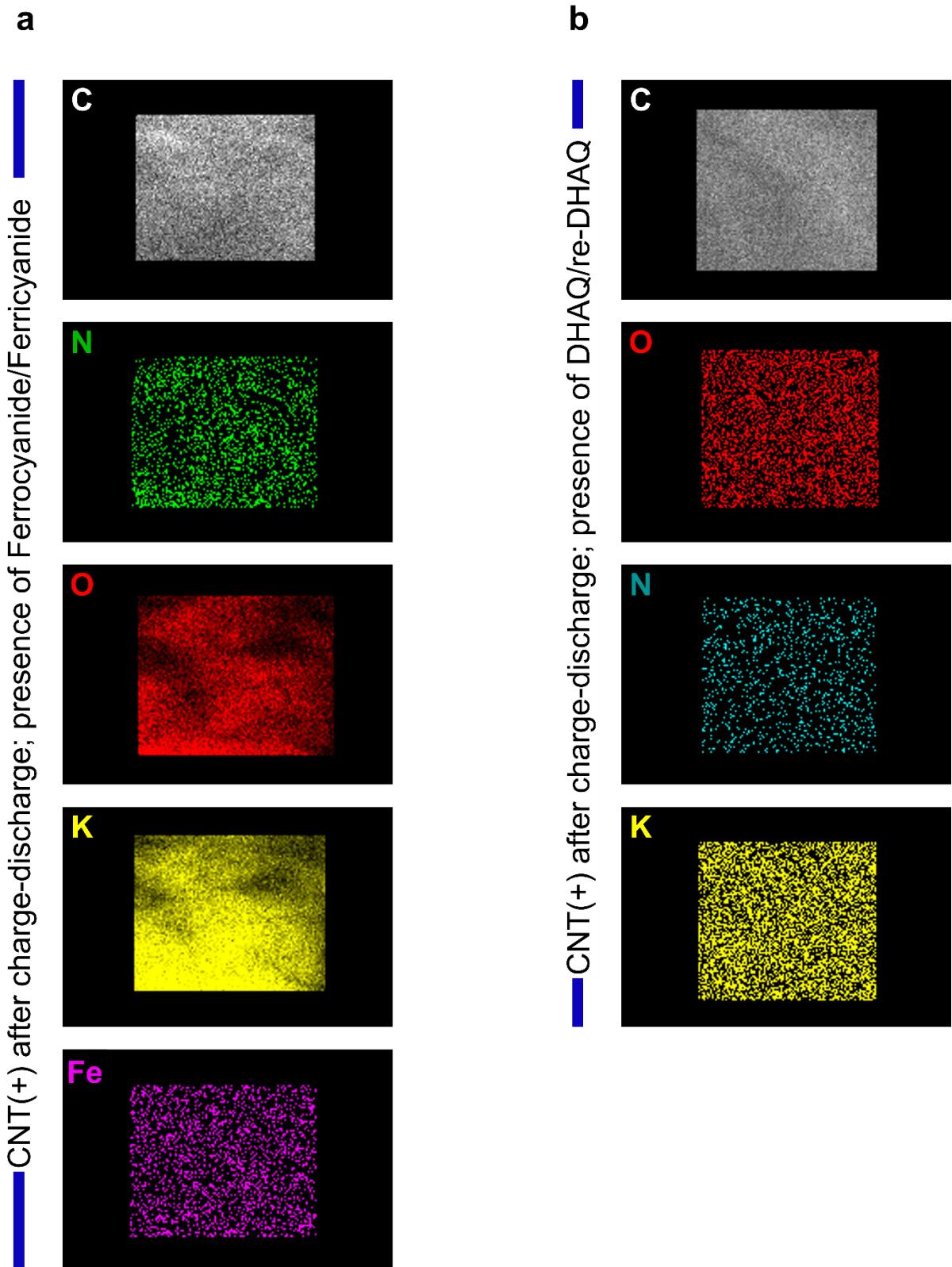
**Fig. S11** TEM images of CNT (+) after charge-discharge cycling.



**Fig. S12** SEM images of CNT (+) electrode utilized **(a)** at the cathodic interface and **(b)** at the anodic interface after long term charge-discharge.



**Fig. S13** ATR-FTIR spectra of CNT (+) electrode utilized **(a)** at the cathodic interface and **(b)** at the anodic interface before and after charge-discharge cycling.



**Fig. S14** EDX elemental mapping of CNT (+) electrode utilized **(a)** at the cathodic interface and **(b)** at the anodic interface after charge-discharge cycling. The signals of O, K and Fe in Fig. S14a originates from adsorbed iron species whereas the signals of K and O in Fig. S14b originates from adsorbed quinone molecule