## Supporting Information

# Dendritic NiS<sub>2</sub>@Co-N-C nanoarchitectures as bifunctional electrocatalysts

## for long-life Zn-air batteries

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#### S1. Material characterization

The samples were analyzed by X-ray diffractometry (XRD) on Rigaku D/ MAX-2500. X-ray photoelectron spectroscopy (XPS) data were collected by Thermofisher K-Alpha, The C 1s peak was used to calibrate the binding energy at 284.5 eV. Nitrogen adsorption-desorption measurement is performed on a MicroMertics analyzer (ASAP 2020 PLUS HD88), and the specific surface area (SSA) is measured using Brunauer-Emmett-Teller (BET). Morphological information was obtained by Gemini SEM500 field emission scanning electron microscopy (FESEM) and transmission electron microscopy (TEM: JEOL jem-2100). Energy Dispersive X-ray Spectroscopy (EDS) was performed on EDAX OCTANE SUPER to observe the element distributions in SEM images.

### S2. Preparation and testing for oxygen reaction catalyst

All electrochemical measurements were made at room temperature (~25 °C) using a 760E bipotentiostat (Shanghai Chenhua Instrument, China) in a conventional three-electrode cell. The suspension was prepared by ultrasonic dispersion of 5 mg catalyst in 50  $\mu$ L Nafion (5 wt %) solution and 500  $\mu$ L ethanol-water (volume ratio 5:4.5) solution. Working electrode adopts polished glassy carbon electrode (diameter: 3 mm). A certain volume of catalyst ink is uniformly dispersed on the surface of a rotating disk electrode (RDE) or a rotating ring disk electrode (RRDE), and then dried in air to obtain an electrode coated with a catalyst film. Commercial Pt/C (20 wt %) and IrO<sub>2</sub> were used as control catalysts. The catalyst loading is 0.5 mg cm<sup>-2</sup>.

The ORR measurements were made in an O2-saturated 0.1 M KOH solution using a saturated calomel electrode (SCE) as a reference electrode and a graphite carbon rod s a counter electrode. All measured were potentials converted RHE scale by а calibration to an equation. E<sub>RHE</sub>=E<sub>SCE</sub>+0.059pH+0.241. Thin-film rotating disk electrode (RDE) technique was employed to evaluate the ORR activities of different electrocatalysts. Linear sweep voltammetry (LSV) curves were recorded in an O<sub>2</sub>-saturated 0.1 M KOH solution with RDE rotation rates of 400, 625, 900, 1225, 1600, 2025, and 2500 rpm at a scanning rate of 10 mV s<sup>-1</sup>, and the catalyst was tested in the potential range of 0.2-1.1 V (vs. RHE). The accelerated durability test of the catalyst was performed by recording the LSV curves before and after 2000 cycles in 50 mV s<sup>-1</sup> O<sub>2</sub> saturated 0.1 M KOH solution. The long-term stability test of the catalyst was characterized by chronoamperometry for 18000 s. A methanol durability test was performed by adding 3 M methanol at 1200 s by chronoamperometry to characterize its methanol resistance. The electron transfer number (n) of ORR is calculated by Kouteck-Levich (K-L) equation <sup>[1,2]</sup>:

$$\frac{1}{j} = \frac{1}{j_L} + \frac{1}{j_K} = \frac{1}{\frac{1}{B\omega^2}} + \frac{1}{j_K}$$
(1)

$$B = 0.62nFC_0 D^{\frac{2}{3}} v^{-\frac{1}{6}}$$
(2)

where *j* is the measured current density,  $j_K$  is the dynamic current density,  $j_L$  is the limit current density,  $\omega$  is the angular velocity of electrode rotation, n is the electron transfer number, F is the Faraday constant (96485 C mol<sup>-1</sup>), C<sub>o</sub> is the volume concentration of O<sub>2</sub> (1.2 × 10<sup>-6</sup> mol cm<sup>-3</sup> in 0.1 M KOH) and D is the diffusion coefficient of O<sub>2</sub> (1.9 × 10-5 cm<sup>2</sup> s<sup>-1</sup> in 0.1 M KOH). v is the kinetic viscosity of electrolyte (0.01 cm<sup>2</sup> s<sup>-1</sup> for 0.1 M KOH).

In the RRDE test, hydrogen peroxide ( $H_2O_2\%$ ) yield and electron transfer number (n) were calculated using the following formula <sup>[3,4]</sup>:

$$HO_{\frac{1}{2}}\% = \frac{200i_{r}}{N(i_{d} + \frac{i_{r}}{N})}$$
(3)

$$n = \frac{4i_d}{i_d + \frac{i_r}{N}} \tag{4}$$

where  $i_d$  and  $i_r$  are disk current and ring current, respectively. N is the current collection efficiency of Pt ring (0.42).

The OER measurements were conducted in an O<sub>2</sub>-saturated 1 M KOH solution using Hg/HgO and a graphite as reference and counter electrodes, respectively. All measured potentials were converted to RHE scales by a calibration equation,  $E_{RHE}=E_{Hg/HgO}+0.059pH+0.098$ . The OER polarization curve was measured at a potential range of 0.2–1.0 V (vs. RHE) at a scanning rate of 5 mV s<sup>-1</sup>. The Tafel slope was calculated from the LSV curve by plotting the relationship between the overpotential ( $\eta$ ) and the logarithm of current density (j). The electrochemically active surface area (ECSA) of the samples was estimated based on the electrochemical double-layer capacitance ( $C_{dl}$ ) and determined by CV curves recorded at different scanning rates in the non-Faraday interval (0.95-1.05 V).

$$C_{dl} = \frac{j_a - j_c}{2\nu} = \frac{\Delta j}{2\nu} \tag{5}$$

Where  $\Delta j$  is the difference between the anode and cathode current density recorded under the selected potential range, and v is the scan rate. The electrochemical impedance spectroscopy (EIS) test was performed at 1.60 V (vs. RHE), the frequency range is 0.1 Hz-10 kHz, and the amplitude is 10 mV.

The oxygen electrode activity ( $\Delta E$ ) is evaluated by the potential of the OER at a current density of 10 mA cm<sup>-2</sup> and the half-wave potential of ORR:

$$\Delta E = E_{OER} - E_{ORR} = E_{j=10} - E_{\frac{1}{2}}$$
(6)

### S3. Zinc-air battery assembly and testing

NiS<sub>2</sub>@Co-N-C/CNF catalyst and Nafion adhesive (5%) were weighed with a mass ratio of 7:3, and ultrasonic dispersion was carried out in DMF solution to obtain uniform catalyst slurry. Then the catalyst slurry was uniformly coated on the nickel foam to prepare the air cathode (mass load: 1 mg

cm<sup>-2</sup>). A gas diffusion layer (GDL) is pressed on the back of the nickel foam to make oxygen enter the battery smoothly. For comparison, the same method was used to prepare Pt/C, a Pt/C and IrO<sub>2</sub> mixed catalyst with a mass ratio of 1:1 to prepare an air cathode. A 0.2 mm polished zinc foil was used for the anode, and a mixture of 0.2 M Zn(OAc)<sub>2</sub> and 6 M KOH was used as the liquid electrolyte of the rechargeable ZABs, and a self-made liquid ZABs was assembled. All tests were carried out in an ambient atmosphere with a constant current discharge-charge cycle in the LAND test system using CHI760E electrochemical workstation with open circuit potential as the initial potential. The polarization curves were recorded at a scanning rate of 5 mV s<sup>-1</sup> and the current and power were normalized to the geometric surface area of the air cathode.

To assemble flexible solid state ZABs, a 0.08 mm polished zinc foil was used as the anode, and the catalyst-coated nickel foam was used as the air cathode. 1 g PVA in 10 mL deionized water under 95 °C for 2 h to form a uniform viscous solution, then slowly add a certain amount of a mixed solution of 18 M KOH and 0.2 M Zn(OAc)<sub>2</sub> dropwise with constant heating and stirring for 20 min to form electrolyte.

Under the current density of 1 mA cm<sup>-2</sup>, the performance of constant current discharge-charge cycle was tested, discharging for 5 min and charging for 5 min. the formula for calculating the power density of a ZABs is as follows:

$$P = IV \tag{7}$$

Where I is the discharge current density, and V is the voltage. The calculation formula of specific capacity is as follows<sup>[5]</sup>:

$$Specific \ capacity = \frac{current * service \ hours}{weigh \ of \ consumed \ zinc}$$
(8)  
S4. Computational methodology

All periodic density functional theory (DFT) calculations were carried out using the CP2K code employed a mixed Gaussian and planewave basis sets <sup>[6,7]</sup>. The generalized gradient approximation functional of Perdew, Burke, and Enzerhof (PBE) <sup>[8]</sup> was used to described the exchange-correlation potential. Core electrons were represented with norm-conserving Goedecker-Teter-Hutter pseudopotentials<sup>[9-11]</sup>. The valence electron wavefunction was expanded in a double-zeta basis set with polarization functions<sup>[12]</sup> along with an auxiliary plane wave basis set with an energy cutoff of 400 Ry. The force convergence criteria of 0.001 hartree/bohr was used. Each adsorption structure was optimized with the Broyden-Fletcher-Goldfarb-Shanno (BGFS) algorithm with SCF convergence criteria of 1.0×10<sup>-8</sup> au. The van der Waals dispersion interaction was compensated using the DFT-D3 scheme<sup>[13]</sup> with an empirical damped potential term in all calculations.

Three model surfaces, i.e., NiS<sub>2</sub>, Co-N-C, and NiS<sub>2</sub>/Co-N-C were constructed. The periodic single NiS<sub>2</sub> layer structure was modeled as a c(2×2) supercell slab containing 12 Ni atoms and 24 O atoms (see **Figure S13**). A vacuum height of 12 Å in the *z* direction was inserted between the NiS<sub>2</sub> surface slabs to eliminate any unphysical interaction. Similarly, a periodic Co-N-C coordinated surface structure ( $C_{42}N_4Co_1$ ) was constructed (see **Figure S14**). The vacuum space in the *z* direction was set to 14.8 Å, ensuring there is no interactions within the periodic boundary. The simulation box size is 9.8400 × 12.7825 × 14.8000 Å<sup>3</sup>. The NiS<sub>2</sub>@Co-N-C surface structure was constructed by placing a NiS<sub>2</sub> layer over the Co-N-C substrate (see **Figure S15**). The simulation box parameters for the NiS<sub>2</sub>@Cu-N-C catalyst is 10.5488 × 12.1807 × 17.9846 Å<sup>3</sup>. After optimization, it is found that the averaged distance between two layered structures is 3.45 Å.

The typical four-electron ORR/OER reaction mechanism was considered in this work. Under acidic conditions, the overall reaction can be represented as:

$$O_2 + 4(H^+ + e^-) \rightarrow 2H_2O$$
  $\Delta G_0 = 4.92 \ eV$  (9)

The Gibbs free energy difference ( $\Delta G_0$ ) is 4.92 eV for the ORR reaction at p = 1 bar and T = 298.15K. The reverse reaction process of ORR is the OER reaction. The reaction was generally believed to proceed in four steps <sup>[14-16]</sup>:

$$O_2 + (H^+ + e^-) + * \to 00H *$$
 (10)

$$00H *+ (H^{+} + e^{-}) + * \to H_2 0 + 0 *$$
(11)

$$0 *+ (H^+ + e^-) + * \to OH *$$
 (12)

$$OH *+ (H^+ + e^-) + * \to H_2 O$$
 (13)

where \* represents the active site of the catalyst, and OOH\*, O\*, and OH\* represent the species adsorbed on the active site. At the standard condition (p = 1 bar and T = 298.15), the Gibbs free energy of  $H^+ + e^-$  equals the Gibbs free energy of  $1/2H_2$ . The Gibbs free reaction energy ( $\Delta G$ ), which is calculated by the binding strengths between the catalyst and the ORR intermediates:

$$\Delta G = \Delta E + \Delta E_{ZPE} - T\Delta S \tag{14}$$

where  $\Delta E$  is the DFT calculated adsorption energy of the intermediate. Herein,  $\Delta E$  of OOH\*, O\* and OH\* intermediates are all referred to gaseous H<sub>2</sub>O and H<sub>2</sub>:

$$\Delta E_{00H*} = E_{00H*} - E_* - (2E_{H_20} - \frac{3}{2}E_{H_2})$$
(15)

$$\Delta E_{0*} = E_{0*} - E_* - (E_{H_20} - E_{H_2}) \tag{16}$$

$$\Delta E_{OH*} = E_{OH*} - E_* - (E_{H_2O} - \frac{1}{2}E_{H_2})$$
(17)

where  ${}^{E_{H_2}o}$  and  ${}^{E_{H_2}}$  are the calculated DFT energies of H<sub>2</sub>O and H<sub>2</sub> molecules in the gas phase using the approaches outlined by Nørskov *et al.*<sup>9,11</sup>

The zero-point energy (ZPE) contribution is given by:

$$E_{ZPE} = \sum_{i} \frac{hv_i}{2} \tag{18}$$

where h and  $v_i$  are the Plank's constant and vibrational frequencies which are calculated based on the localized harmonic oscillator approximation with a displacement of 0.01 Å. Only the mobile ascorbates and the atoms at the active site were considered while all other atoms on the catalyst surface are treated as fixed. The vibrational entropy contributions (S) can be calculated below:

$$S = k_{B} \sum_{i} \left( \frac{hv_{i}}{\frac{hv_{i}}{k_{B}T \left( e^{\frac{hv_{i}}{k_{B}T}} - 1 \right)}} - ln \left( 1 - e^{\frac{-hv_{i}}{k_{B}T}} \right) \right)$$
(19)

Because the high-spin ground state of an oxygen molecule is difficult to accurately describe in DFT calculation, the Gibbs free energy of  $O_2(g)$  is derived as

$$G_{0_2} = 2G_{H_20} - 2G_{H_2} + 4.92 \ eV \tag{20}$$



**Fig. S1.** (a) The optical photograph of PAN nanofiber film by electrospinning method, (b) FESEM image of PAN nanofiber film.



**Fig. S2.** (a) The optical photograph of the prepared ZIF-67/PAN, (b, c) FESEM images of the prepared ZIF-67/PAN, (d) XRD pattern of the prepared ZIF-67/PAN.



**Fig. S3.** (a) Optical photo of Co-N-C/CNF catalyst prepared by carbonization under N<sub>2</sub> atmosphere, (b) FESEM images of Co-N-C/CNF, (c) Corresponding TEM image, (d) XRD pattern of Co-N-C/CNF.



Fig. S4. (a) XRD pattern of NiS<sub>2</sub>, (b,c) FESEM images of NiS<sub>2</sub>, (d) Corresponding TEM image.



Fig. S5. (a) The ORR and (b) OER LSV curves of Co-N-C/CNF catalyst from 700 °C,800 °C and 900 °C.



Fig. S6. EIS Nyquist plots of Co-N-C/CNF catalyst from 700 °C,800 °Cand 900 °C.



Fig. S7. (a) The ORR and (b) OER LSV curves of NiS<sub>2</sub>@Co-N-C/CNF catalyst from the different

mass ratios between NiS<sub>2</sub> and Co-N-C/CNF.



Fig. S8. EIS Nyquist plots of  $NiS_2@Co-N-C/CNF$  catalyst from the different mass ratio between  $NiS_2$  and Co-N-C/CNF.



**Fig. S9.** (a) LSV curves of Pt/C at various rotation speeds, (b) K-L plots for different voltages according to the LSV curves in (a).



Fig. S10. The CV curves of the (a) CNF, (b) NiS<sub>2</sub>, (c) Co-N-C/CNF, and (d) Pt/C samples



Fig. S11. Optical photos of (a,b) a small bulb and (c,d) LED powered by the assembled liquid ZABs

(Two) in series.



Fig. S12. Optical photo of PVA-KOH gel electrolyte.



Fig. S13. Optimized structures (top and side views) of ORR/OER intermediates adsorbed on the

NiS<sub>2</sub>.



Fig. S14. Optimized structures (top and side views) of ORR/OER intermediates adsorbed on the Co-

N-C.



Fig. S15. Optimized structures (top and side views) of ORR/OER intermediates adsorbed on the NiS<sub>2</sub>@Co-N-C.



Fig. S16. XRD pattern of NiS<sub>2</sub>@Co-N-C/CNF after 100 cycles.



Fig. S17. High resolution Ni 2p of NiS<sub>2</sub>@Co-N-C/CNF after 100 cycles.

 Table S1. The Comparison of ORR catalytic performance of this work with other non-noble metal-based catalysts

 recently reported (0.1M KOH).

Catalysts	$E_{\text{onset}}(\mathbf{V})$	$E_{1/2}$ (V)	Tafel slopes	Deference
			(mV dec <sup>-1</sup> )	Keierence
N-CoS <sub>2</sub> YSSs	0.95	0.81	52	[17]
W <sub>2</sub> N/WC	0.93	0.81	58.13	[18]
CoSA/N,S-HCS	0.96	0.85	-	[19]
FeCo/Co <sub>2</sub> P@NPCF	0.85	0.79	62	[20]
Co <sub>3</sub> O <sub>4-X</sub> /NG	0.96	0.84	-	[21]
Co <sub>2</sub> P/NPG-900	0.94	0.81	64.1	[22]
NiFe@N-CFs	0.94	0.82	58	[23]
MnO/Co@NGC	0.91	0.82	-	[24]
NiCo <sub>2</sub> S <sub>4</sub> /RGO <sub>0.02</sub>	0.90	0.78	-	[25]
Co-Ni-S@NSPC	0.95	0.82	-	[26]
Co <sub>9</sub> S <sub>8</sub> /C	0.89	0.78	-	[27]
NiS <sub>2</sub> /CoS <sub>2</sub>	0.90	0.79	-	[28]
CoFe/N-HCSs	0.901	0.791	59	[2]
CoFeP@C	0.90	0.80	66.6 [29]	
NiS <sub>2</sub> @Co-N-C/CNF	0.90	0.80	56	[This work]]

Table S2. The Comparison of OER catalytic performance of this work with other non-noble metal-based catalysts

recently reported (1M KOH).

Catalanta	Overpotential@	Tafel slopes	Defense
Catalysts	10 mA cm <sup>-2</sup> (mV)	(mV dec <sup>-1</sup> )	Kelerence
N-CoS <sub>2</sub> YSS	278	56	[17]
CoSA/N,S-HCS	306	38.1	[19]
Co <sub>3</sub> O <sub>4</sub> -X/NG	296	84.85	[21]
Co <sub>2</sub> P/NPG-900	320	66.6	[22]
NiS <sub>2</sub> /CoS <sub>2</sub>	295	51	[28]
CoFe/N-HCSs	292	58	[2]
CoFeP@C	336	82.5	[29]
FeCo-NCNTs	320	61.5	[30]
N-Mo-holey G	300	47	[31]
CoNC-NB2	350	98	[32]
Co/N@CNTs@CNMF-800	310	61.3	[33]
AlFeCoNiCr	240	52	[34]
(Fe,Co)SPPc-900-sp	353	53	[35]

NiS2@Co-N-C/CNF	300	57	This work
Co/CoFe@NC	300	49	[1]
Co@N-C/PCNF	289	91.86	[40]
Fe@N-CNT/HMCS	340	76	[39]
Fe <sub>2</sub> /Co <sub>1</sub> -GNCL	350	70	[38]
Co <sub>3</sub> O <sub>4</sub> /Mn <sub>3</sub> O <sub>4</sub> /CNX@CNFs	400	105	[37]
CoFe-N-CNTs/CNFs-900	320	92	[36]

Table S3. The Comparison of liquid Zn-air batteries performance of this work with other non-noble metal-based

catalysts	recently	reported.

Catalysts	Open circuit voltage (OCV)	Power density (mW cm <sup>-2</sup> )	Cycling current density (mA cm <sup>-2</sup> )	Stability (h)	Reference
N-CoS <sub>2</sub> YSS	1.41	81	10	165	[17]
CoSA/N,S-HCS	1.50	173.1	10	333	[19]
Co <sub>3</sub> O <sub>4</sub> -X/NG	1.49	166	5	63	[21]
CoFe/N-HCSs	1.387	96.5	5	160	[2]
CoNC-NB2	1.50	246	2	140	[32]
Co/N@CNTs@CNMF-800	1.52	133	10	190	[33]
(Fe,Co)SPPc-900-sp	1.47	158.6	2	50	[35]
CoFe-N-CNTs/CNFs-900	1.462	-	10	85	[36]
FeNi/N-LCN	1.49	162	5	1100	[41]
Co-UA-OCB	1.475	142	10	100	[42]
NiFe/N-CNT	1.48	300	5	100	[43]
CoFe/Co@NCNT/NG	1.4	161	2	100	[44]
FeP/Fe <sub>2</sub> O <sub>3</sub> @NPCA	1.42	130	5	160	[45]
Fe-Co <sub>4</sub> N@N-C	1.46	105	5	36.7	[46]
Co NPs/N,S-CNTs	1.433	153.8	5	120	[47]
NiS <sub>2</sub> @Co-N-C/CNF	1.47	181	5	1050	This work
NiS <sub>2</sub> @Co-N-C/CNF	1.47	181	10	600	This work

### **Supplementary Reference**

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