

Chemicals

Bis(hexamethylene)triamine (143-23-7), nickel(II) chloride hexahydrate (99%, 7791-20-0), and dimethylglyoxime (97%, 95-45-4) were purchased from Sigma-Aldrich. Paraformaldehyde (96%, 30525-89-4) and hypophosphorous acid (50%, 6303-21-5) were purchased from Acros Organics. Sulfuric acid (96%, 7664-93-9), ethanol (96%, 64-17-5), ammonium hydroxide (25%, 1336-21-6) and hydrochloric acid (35–38%, 7647-01-0) were purchased from POCH.

Equipment

The image of the obtained amino-hypophosphite polyampholyte was taken using a JSM-6610LV scanning electron microscope (JEOL Ltd., Akishima, Japan) after sputtering the samples with carbon using a JEC-530 automatic coating machine (JEOL Ltd., Akishima, Japan). The specific surface area of this material was evaluated by research on sorption and desorption of the helium/nitrogen mixture using the FlowSorb 2300 apparatus (Micromeritics Instruments Corp, Norcross, GA, USA). The density of the resin obtained was measured using a pycnometer. XPS spectra were carried out using a multi-chamber UHV analytical system (Prevac, Poland) equipped with a hemispherical R4000 photoelectron energy analyser excited by monochromatic X-rays emitted by an MX-650 lamp with an Al-K α anode (Gammadata Scienta, Sweden). The deconvolution and quantitative spectra analysis was performed using Casa XPS software (Casa Software Ltd., UK). The chemical composition of the applied wastewater was introduced into an ICP MS spectrometer (model 7500cx, Agilent, USA). An Evolution 201 UV-visible spectrophotometer (Thermo Fisher Scientific, Madison, USA) was used for spectrophotometric concentration measurements.

Table S1. The capacities of Ni(II) sorption on different sorbents as follows from the literature reports.

Sorbent	Sorption capacity (mg/g)	Isotherm model	Conditions	References
Amberlite IRA-458 Amberlite IRA-958 Amberlite IRA-67	65.24 53.16 13.19	Langmuir	initial Ni(II) concentration: 600 mg·dm ⁻³ pH 4.0 temp. 20-60°C sorbent dosage: 0.5 g	[1]
Dowex PSR-2 Dowex PSR-3	19.16 31.72	Langmuir	initial Ni(II) concentration: 100 mg·dm ⁻³ temp. 20°C contact time: 240 min sorbent dosage: 0.1 g agitation speed: 180 rpm	[2]
Lewatit TP-207	1.23	N/A	initial Ni(II) concentration: 0.395 mg·dm ⁻³ pH 6.0 contact time: 72 h sorbent dosage: 0.27 g·dm ⁻³	[3]
Lewatit AF-5	4.89	Freundlich	initial Ni(II) concentration: 100 mg·dm ⁻³ temp. 25°C contact time: 240 min sorbent dosage: 0.5 g agitation speed: 180 rpm	[4]
Lewatit MonoPlus SR-7	4.56	Freundlich	initial Ni(II) concentration: 100 mg·dm ⁻³ temp. 25°C contact time: 24 h	[5]
Lewatit MonoPlus TP-220	6.24	N/A	initial Ni(II) concentration: 100 mg·dm ⁻³ sorbent dosage: 0.5 g agitation speed: 180 rpm ambient temperature	[6]
Cliniptionite ion-exchange	3.28	Langmuir	Ni(II) concentration: 0.1–100 mg·dm ⁻³	[7]

resin			pH 7.0 sorbent dosage: 15 g·dm ⁻³ agitation speed: 250 rpm contact time: 180 min	
Modified clinoptilolite	8.90	Langmuir	initial Ni(II) concentration: 50-900 mg·dm ⁻³ pH 6.0 temp. 25°C sorbent dosage: 100 g·dm ⁻³ contact time: 300 min	[8]
Chitosan/clinoptilolite	247.0	Langmuir	initial Ni(II) concentration: 4109 mg·dm ⁻³ pH 5.0 temp. 25°C contact time: 24 h	[9]
Carboxymethyl chitosan-hemicellulose resin (CMCH)	362.3	Freundlich	initial Ni(II) concentration: 100 mg·dm ⁻³ pH 6.0 temp. 25°C contact time: 7 h	[10]
Glucan/chitosan hydrogel	184.0	Langmuir	pH 7.0 temp. 20°C contact time: 2 h sorbent dosage: 0.01 g	[11]
Oxidised carbon nanotubes	49.26	Langmuir	Ni(II) concentration: 10–200 mg·dm ⁻³ , sorbent dosage: 0.4 g·dm ⁻³ pH 6.0	[12]
Multipore activated carbons	56.90	Langmuir	pH 6.0 temp. 30°C contact time: 150 min sorbent dosage: 100 mg	[13]
Hydrophilic carbon nanoparticles over silica	13.48	Langmuir	initial Ni(II) concentration: 2.5 mg·dm ⁻³ pH 4.0 temp. 20°C	[14]

Mesoporous calcium silicate	278.35	N/A	initial Ni(II) concentration: 150 mg·dm ⁻³ pH 5.0-7.5 temp. 25°C contact time: 3 h	[15]
Acid treated montmorillonite	4.0	Langmuir	initial Ni(II) concentration: 2.04 mg·dm ⁻³ pH 6.5 temp. 25°C	[16]
Mixed layer clay	6.25	N/A	initial Ni(II) concentration: 100 mg·dm ⁻³ pH 5.6 temp. 25°C contact time: 100 min	[17]
Ball-milled South African bentonite clay	1.3	Freundlich	pH 6.0 temp. 26°C contact time: 1 h	[18]
Barley straw ash	8.25	N/A	initial Ni(II) concentration: 16 mg·dm ⁻³ pH 6.5 temp. 80°C contact time: 1.5 h	[19]
Peanut husk powder	56.82	Langmuir	initial Ni(II) concentration: 20 mg·dm ⁻³ pH 6.0 temp. 25°C sorbent dosage: 5 g·dm ⁻³	[20]
Coconut husk	404.5	N/A	initial Ni(II) concentration: 200 mg·dm ⁻³ pH 6.0 temp. 80°C contact time: 40 min sorbent dosage: 1 g	[21]
Cd-H ₄ bta MOF	120.3	Langmuir	initial Ni(II) concentration: 100 mg·dm ⁻³ temp. 25°C contact time: 30 min	[22]
Magnetic nanorods	95.42	Langmuir	initial Ni(II) concentration: 200 mg·dm ⁻³	[23]

			pH 5.5 temp. 25°C	
Magnetic graphene oxide	51.02	Langmuir	initial Ni(II) concentration: 60 mg·dm ⁻³ pH 8.0 temp. 25°C	[24]
Magnetite-Dowex 50WX4	384.0	Langmuir	initial Ni(II) concentration: 100 mg·dm ⁻³ pH 7.0 temp. 25°C	[25]
Iron oxide magnetic nanoparticles grafted on hyperbranched polyglycerol	0.45	N/A	initial Ni(II) concentration: 100 mg·dm ⁻³ pH 7.2 temp. 25°C	[26]

Table S2. Kinetic models and equilibrium isotherms used in this work

Models	Form of equation	Parameters	Reference
Pseudo-first-order equation (PFO)	$\log(q_{\text{exp}} - q_t) = \log(q_1) - \left(\frac{k_1}{2.303}\right) \cdot t$ (1)	q_1 (mmol g ⁻¹) k_1 (min ⁻¹)	[27,28]
Pseudo-second-order equation (PSO)	$\frac{t}{q_t} = \frac{1}{k_2 q_2^2} + \frac{t}{q_2}$ (2)	q_2 (mmol g ⁻¹) k_2 (g mmol ⁻¹ min ⁻¹)	[28,29]
Intraparticle diffusion model (IPD)	$q_t = k_{IPD} \cdot t^{0.5} + B$ (3)	B (mmol g ⁻¹) k_{IPD} (mmol g ⁻¹ min ^{-0.5})	[28,30]
Liquid film diffusion model (LFD)	$\ln(1 - F) = -k_{LFD} \cdot t$ (4)	$F = q_t/q_e$ (-) k_{LFD} (min ⁻¹)	[31,32]
Langmuir isotherm	$q_e = \frac{q_L \cdot k_L \cdot c_e}{1 + k_L \cdot c_e}$ (5)	q_L (mmol g ⁻¹) k_L (dm ³ mmol ⁻¹)	[33,34]
Freundlich isotherm	$q_e = k_F \cdot c_e^{1/n}$ (6)	$1/n$ (-) k_F ((dm ³) ^{1/n} mmol ^(1-1/n) g ⁻¹)	[34,35]

where:

- B parameter related to the thickness of the boundary layer (mmol g⁻¹)
- c_e equilibrium concentration of Ni(II) (mmol dm⁻³)
- F fractional attainment of equilibrium (-)
- k_1 rate constant of the PFO model (min⁻¹)
- k_2 rate constant of the PSO model (g mmol⁻¹ min⁻¹)
- k_F Freundlich constant indicative of the relative adsorption capacity of the adsorbent ((dm³)^{1/n} mmol^(1-1/n) g⁻¹)
- k_{IPD} intraparticle diffusion rate constant (mmol g⁻¹ min⁻¹)
- k_L Langmuir constant related to the energy of adsorption (dm³ mmol⁻¹)

k_{LFD}	liquid film diffusion rate constant (min^{-1})
n	Freundlich equation exponent (-)
q_{exp}	amount of adsorbed Ni(II) obtained experimentally (mmol g^{-1})
q_1	adsorption capacity of Ni(II) for PFO model (mmol g^{-1})
q_2	adsorption capacity of Ni(II) for PSO model (mmol g^{-1})
q_e	amount of Ni(II) adsorbed at equilibrium (mmol g^{-1})
q_L	maximum adsorption capacity in the Langmuir model (mmol g^{-1})
q_t	amount of Ni(II) adsorbed at time t (mmol g^{-1})
t	time (min)
T	temperature (K)

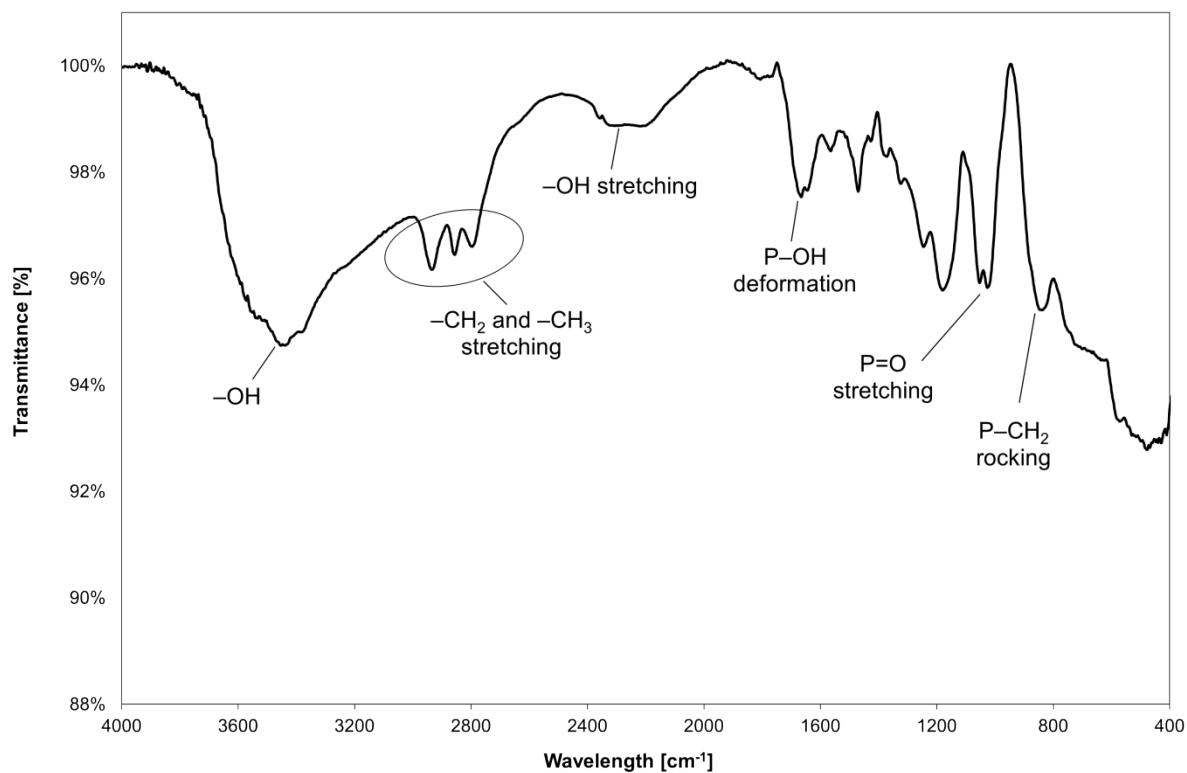


Fig. S1. FTIR spectrum of the obtained amino-hypophosphite polyampholyte with signal assignment (based on [36-38]).

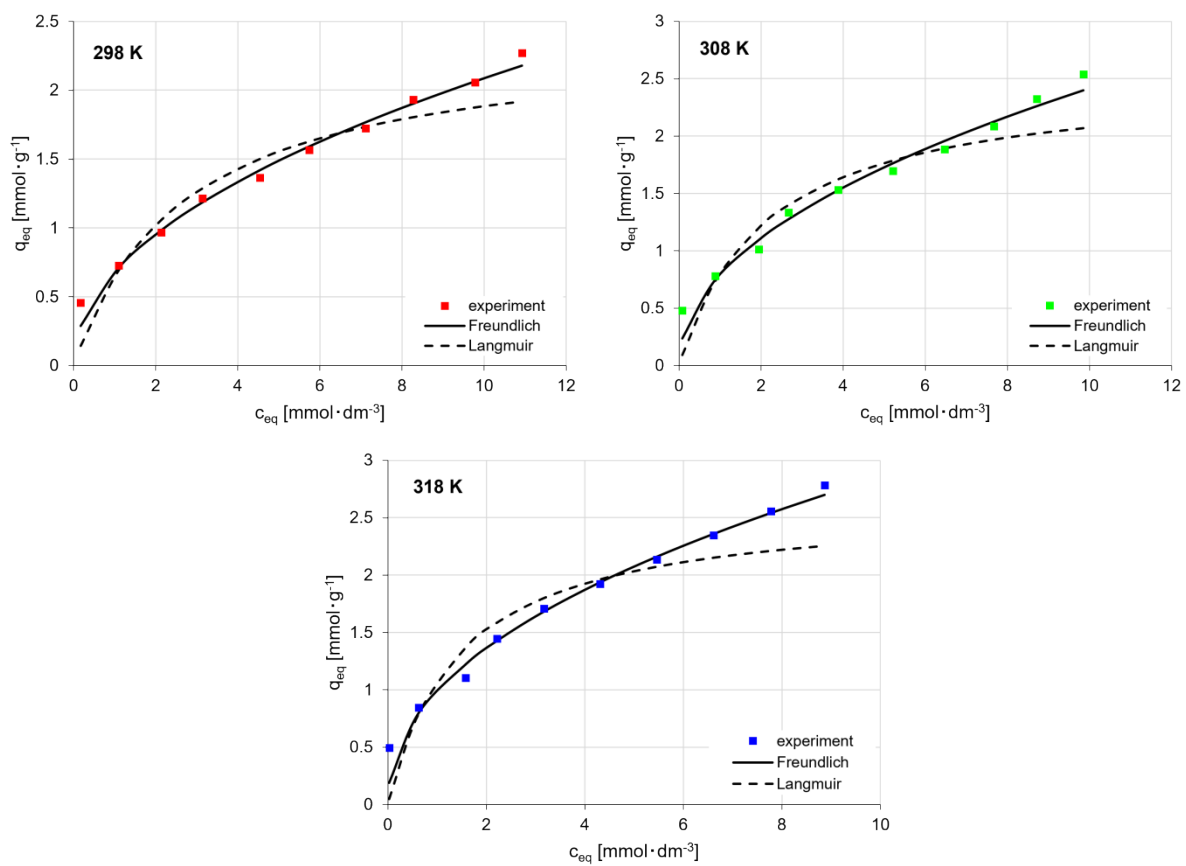


Fig. S2. Sorption isotherms of the obtained amino-hypophosphite polyampholyte for removal of Ni(II) in different temperature. Simulation by Freundlich and Langmuir models.

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