

Supporting Information

Functionalization of *Shorea faguetian* Biochar using Fe₂O₃ Nanoparticles and MXene for Rapid Removal of Methyl Blue and Lead from both Single and Binary Systems

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2.1. Chemicals used for this work

MAX phase powder (Ti₃AlC₂; Jilin Technology Co.Ltd), Hydroflouric acid (HF; 40 wt%), and Ferric Chloride salt were obtained from Merk chemical Lahore, Pakistan. Anhydrous Ferric chloride salt, methyl blue, and Ammonia solution (NH₃) were obtained from Sigma Aldrich chemical Lahore, Pakistan, and *Shorea faguetian* branches were purchased from the native market of Lahore. The botanist at the Minhaj University Lahore (department of botany) certified the *Shorea faguetian*.

2.3. Characterizations

25 The X-Ray (XRD) diffractograms were acquired by Rigaku TTRAX III (Cu K α radiation). The
26 Fourier transform infrared (FTIR) was determined using Tensor27 (Bruker, Germany) to analyze
27 the variation of a functional group on the adsorbent's surface. The morphological feature and
28 elemental composition of the composite were determined using a transmission electron microscope
29 (Hitachi S3400N, Japan), scanning electron microscope (JEOL 6500F, Japan), and EDS (TM-3000
30 Hitachi). The distribution and valance of elements in composites were determined by X-ray
31 photoelectron spectroscopy (ESCALAB 250, USA). The textural features of composites were
32 determined by N₂ adsorption-desorption via Quanta chrome Autosorb 1 gas analyzer. The pore
33 volume (cm³ g⁻¹) and surface area (m² g⁻¹) of Fe₂O₃/BC/MXene composites were investigated via
34 Brunauer-Emmett-Teller (BET) and Barret-Joyner-Hallenda (BJH) approaches, respectively. By
35 using a vibrating sample magnetometer, the adsorbent's magnetic hysteresis loop was calculated
36 (VSM).

37 **2.4. Adsorption experiment**

38 Adsorption investigation was conducted in a 250 mL flask. A total of 0.2 g of Fe₂O₃/BC/MXene
39 adsorbent was dissolved in 200 mL of lead and MB solutions unless otherwise defined, and the
40 resulting mixture was stirred in a rotating shaker at 200 pm. The pH of the reaction mixture was
41 2.0-11. The sorption investigations were performed at temperatures 293, 303, and 313 K. The lead
42 and MB concentrations were 50-750 (mg/L), and the adsorption time was 1 -50 min. The sorption
43 capability and rate of lead and MB removal were determined utilizing equations 1 and 2.

$$44 \quad q_e = \left(\frac{C_o - C_e}{M} \right) V \quad \backslash * \text{MERGEFORMAT (1)}$$

$$45 \quad R = \left(\frac{C_o - C_e}{C_e} \right) \times 100 \quad \backslash * \text{MERGEFORMAT (2)}$$

46 Among them, q_e represents adsorption capability in mg g^{-1} , C_o represents lead initial lead (II) and
47 MB concentrations earlier than adsorption, R represents the remaining elimination rate (%), M
48 represents the molecular mass of composite, and V represents the molar volume of lead (II) and
49 solution in mL.

50 2.5. Isothermal study

51 The isotherm data were derived to determine the sorption capability of lead and MB using
52 composite. The experimental pieces of information were separately subjected to investigation via
53 Langmuir, Freundlich, Temkin, and Dubinin-Radushkevich models. Here, the Langmuir and
54 Freundlich isotherms, respectively, were employed to identify the monolayer and multilayer
55 sorption¹². Langmuir isotherm equation is expressed below as in eq 3

$$56 \quad q_e = \frac{q_{\max} K_L C_e}{1 + K_L C_e} \quad \backslash * \text{MERGEFORMAT (3)}$$

57 Here, q_e (mg g^{-1}) denotes the metal and dye sorption capability state of equilibrium, C_e denotes the
58 pb^{2+} ions and MB dosage at equilibrium (mg/L), q_{\max} denotes the single-layered sorption capability
59 (mg/g), and K_L denotes the Langmuir rate constant (L mg^{-1}).

60 Freundlich isotherm equation is expressed below as in eq 4.

$$61 \quad q_e = K_F C_e^n \quad \backslash * \text{MERGEFORMAT (4)}$$

62 Here, q_e/K_F (mg/g) denotes the metal sorption capability at equilibrium, C_e denotes the Pb^{+2} ions
63 and MB dye dosage at equilibrium (mg/L) and represents the Freundlich rate constant.

64 The Temkin model was utilized to measure the relationship between adsorbate and adsorbent³.

65 The determination and calculation of Temkin parameters are exhibited by equation 6.

66
$$q_e = q_s \exp(-B \epsilon^2) \quad \backslash * \text{MERGEFORMAT (5)}$$

67
$$q_e = \frac{RT}{b} \ln(AC_e) \quad \backslash * \text{MERGEFORMAT (6)}$$

68 Among them, A (L mol⁻¹) denotes the equilibrium constant associated with the highest binding
 69 energy, R (J/mol K⁻¹) denotes the gas constant, T represents the sorption temperature (K), and b
 70 represents the Temkin isotherm coefficient.

71

72 **2.6. Kinetics analysis**

73 The Kinetics of adsorption of lead and MB on the Fe₂O₃/BC/MXene composite were explored in
 74 this work. The lead and MB concentrations were determined at 10, 20, 30, 40, and 50 min. The
 75 sorption rate (%) was guage via pseudo-first-order (PFO), pseudo-second-order reaction (PSO),
 76 and intra-particle diffusion (IPD), Elovich, and Bangham diffusion model defined as in eq 7, 8, 9,
 77 10, and 11, respectively.

78 PFO:

79
$$q_e - (q_e - q_t) = \ln q_e - K_1 t \quad \backslash * \text{MERGEFORMAT (7)}$$

80 PSO:

81
$$q_e = \frac{t}{q_e} + \frac{1}{K_2 q_e^2} \quad \backslash * \text{MERGEFORMAT (8)}$$

82

83 IPD

84 $q_e = K_3 t^{0.5} + C$ * MERGEFORMAT (9)

85 Elovich

86 $q_t = \frac{1}{\beta} \ln(\alpha\beta) + \frac{1}{\beta} \ln t$ * MERGEFORMAT (10)

87 Bangham diffusion model

88 $\log \log \left(\frac{C_t}{C_t - q_t M} \right) = \log \left(\frac{K_j M}{2.303 V} \right) + \alpha \log t$ * MERGEFORMAT (11)

89 Among them, q_t denotes sorption equilibrium (mg g⁻¹) at any time, and t (min) denotes sorption
 90 time. α denotes chemical sorption rate in mg g⁻¹ min⁻¹ and β represents the degree of surface area
 91 covered and activation energy in (g mg⁻¹). M expresses the concentration of the sorbent (g/L),
 92 and V defines the volume in mL. K_1 , K_2 , and K_3 denote the PFO, PSO, and ID kinetics rate
 93 constants, respectively. The K_j constants can be calculated by extracting them from the intercept
 94 and slope of the fitting plot. C denotes the constant which is connected to the thickness of the
 95 available boundary layers.

96 **2.8. Thermodynamic study**

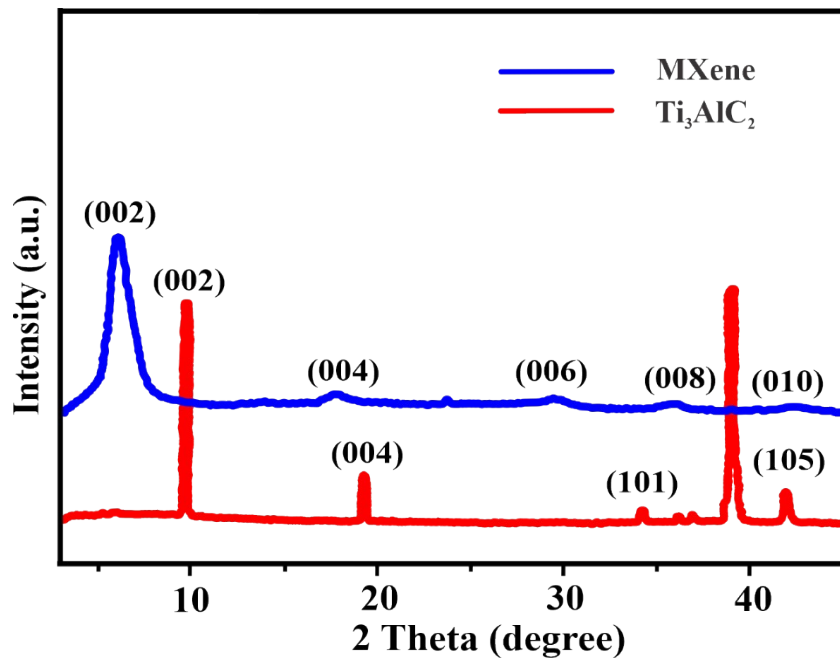
97 Each parameter of thermodynamic sorption, such as standard entropy (ΔS ; KJmol⁻¹), Gibbs free
 98 energy (ΔG ; KJmol⁻¹), and standard enthalpy (ΔH ; KJmol⁻¹), was determined via

99 $K_d = \frac{q_e}{C_e}$ * MERGEFORMAT (12)

100 $\ln K_d = -\frac{\Delta H}{RT} + \frac{\Delta S}{R}$ * MERGEFORMAT (13)

101 $\Delta G = \Delta H + T\Delta S$ * MERGEFORMAT (14)

102 Among them, K_d denotes the thermodynamic coefficient, and T denotes sorption temperature (K).

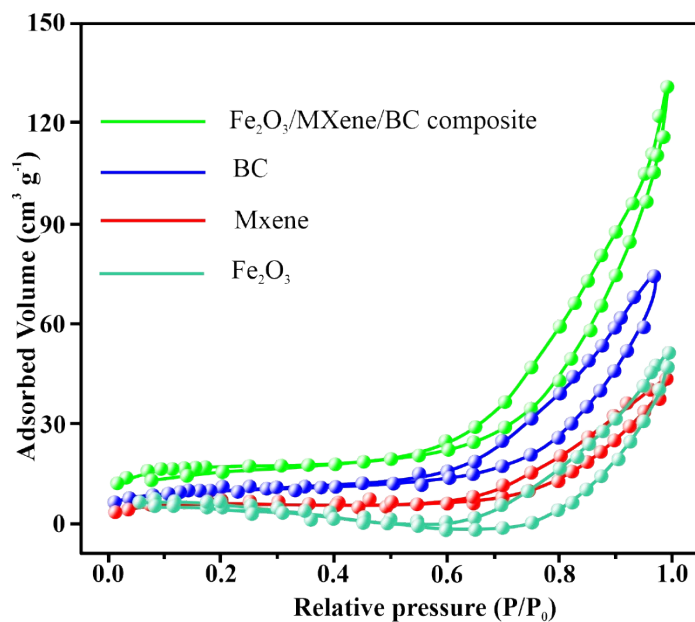


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Fig. S1: XRD spectrum of MXene and Ti_3AlC_2 phase



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Figure.S2: N_2 adsorption/desorption isotherms of $Fe_2O_3/BC/MXene$, BC, MXene, and Fe_3O_4

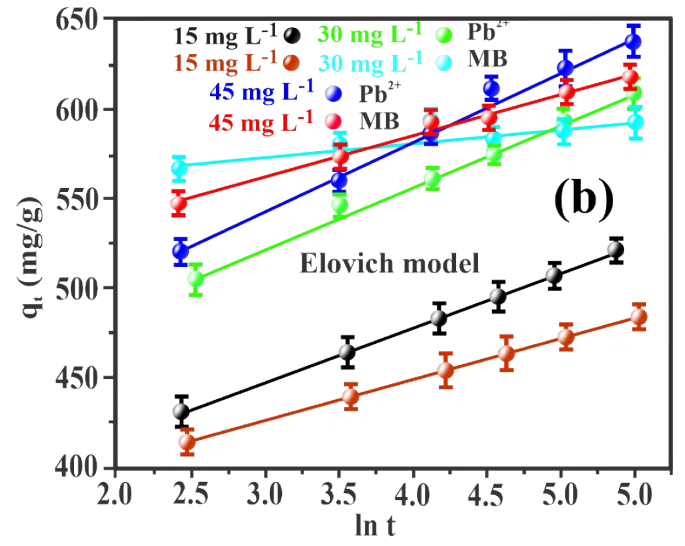
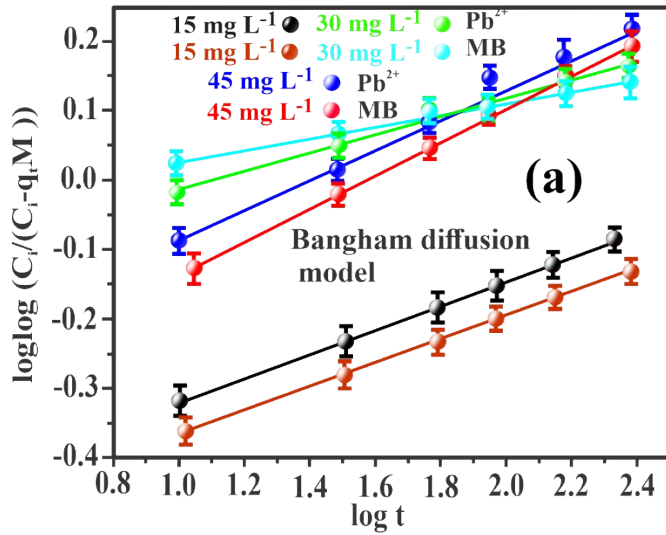


Figure.S3: Bangham diffusion (a) and Elovich kinetic model for the adsorption of Pb^{2+} and MB.

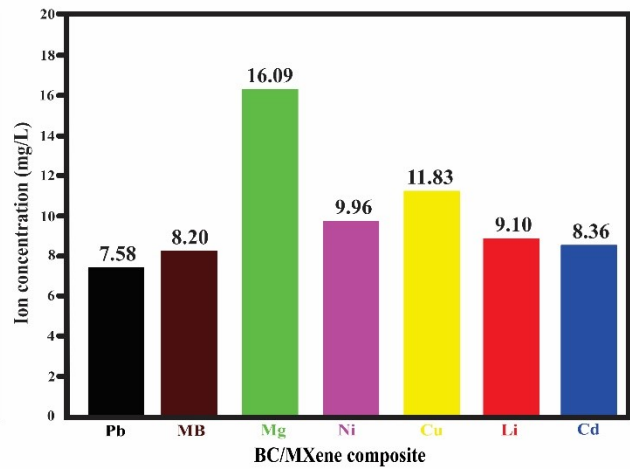
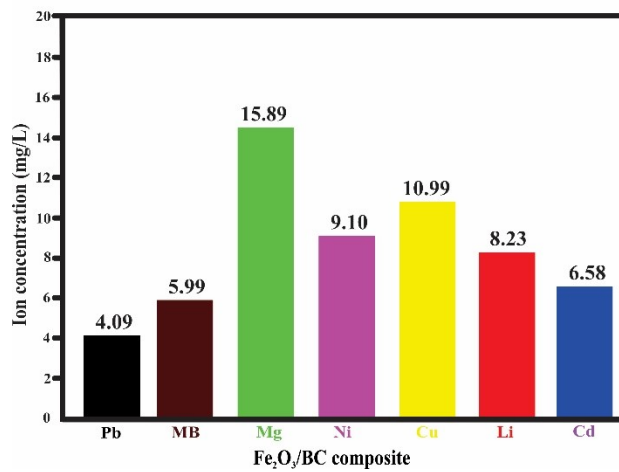
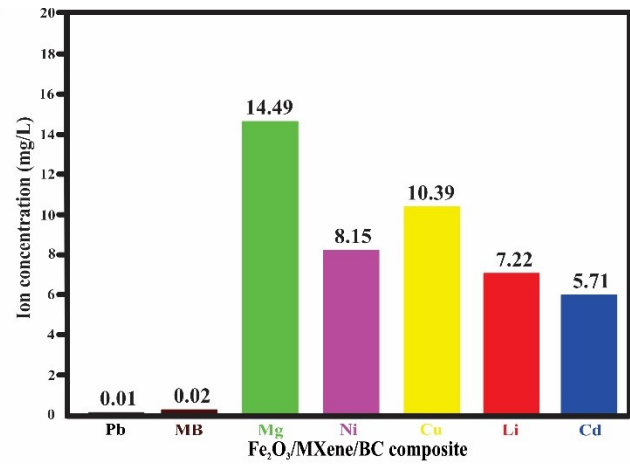
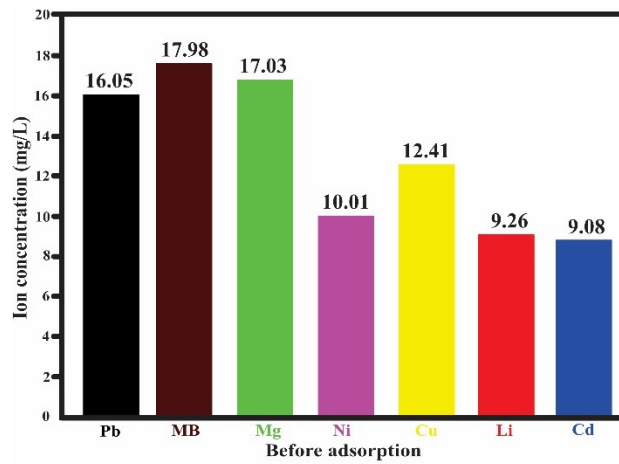
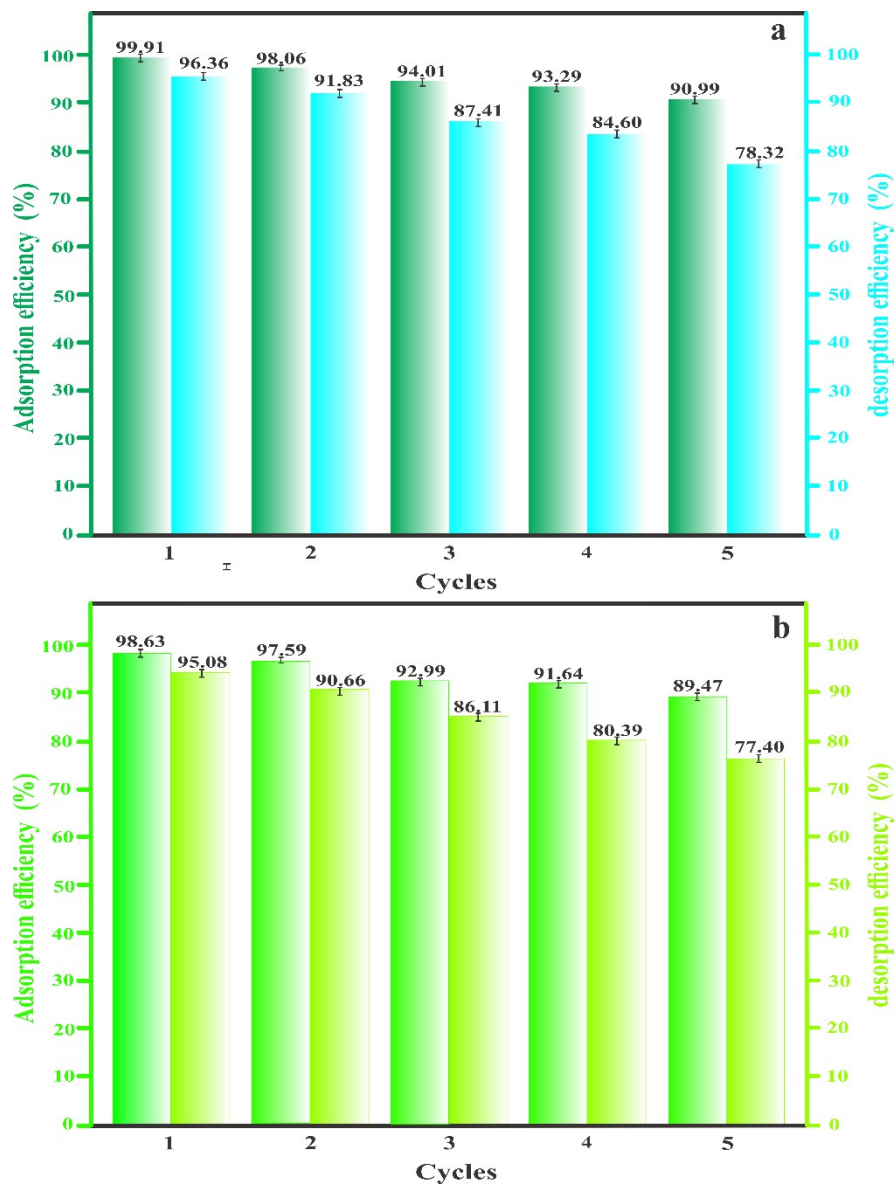


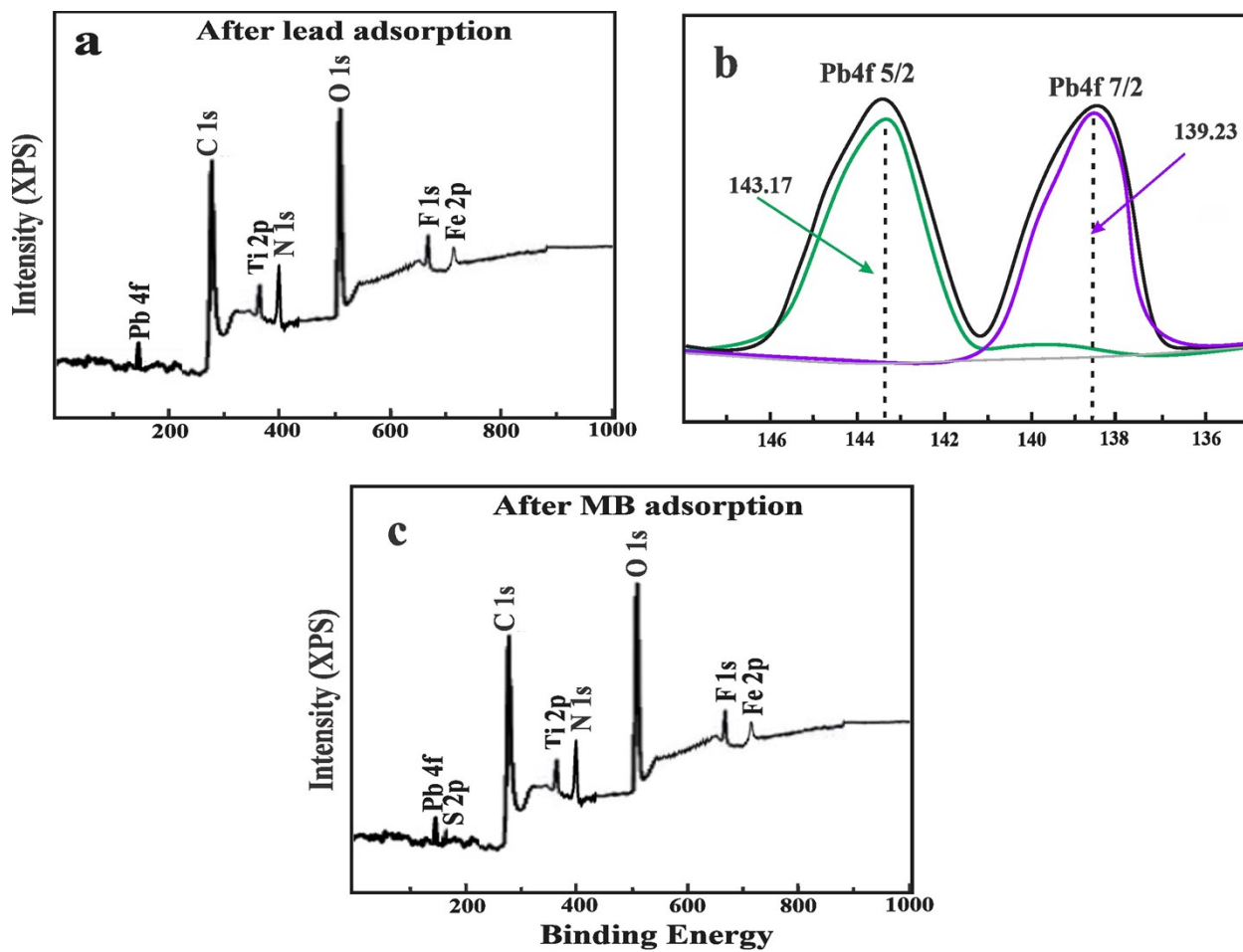
Figure.S4: Selectivity of Pb^{2+} and MB adsorption before adsorption (a), on $Fe_2O_3/BC/MXene$ (b), BC/Fe_2O_3 (c), and $BC/MXene$ (d)



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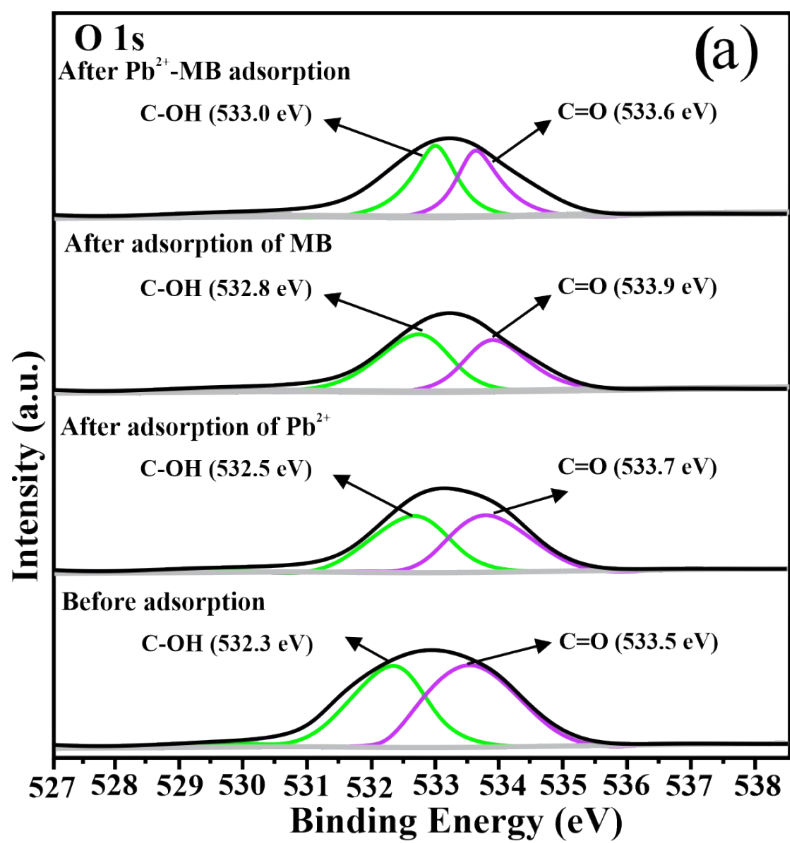
Figure.S5: Reusability of Fe₂O₃/BC/MXene composite for sorption of Pb²⁺ (a) and MB (b)



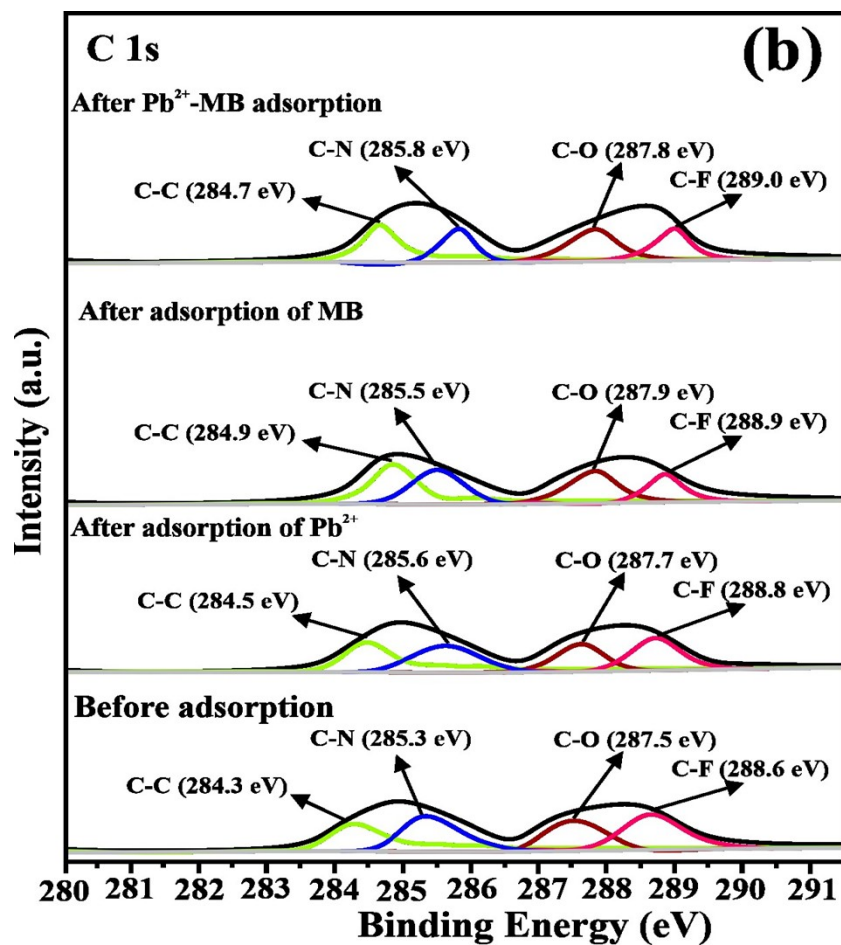
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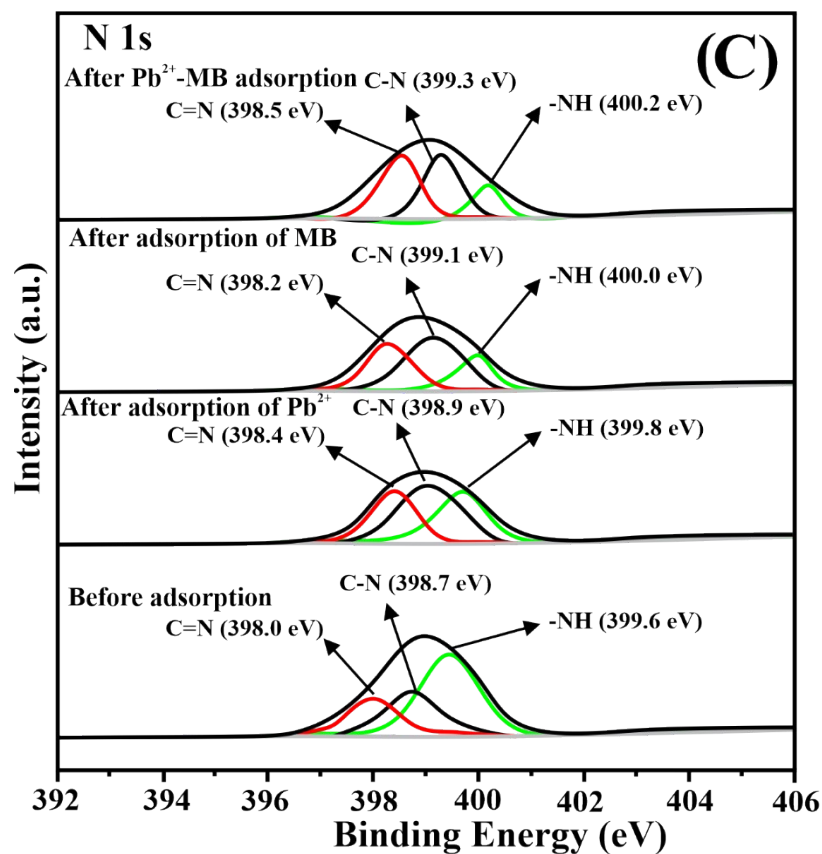
Figure.S6: XPS survey patterns of Fe₂O₃/BC/MXene composite after adsorption of lead (a-b) and MB (c)



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121 Figure.S7: O 1 s XPS spectra before adsorption and after adsorption of Pb^{2+} , MB, and Pb^{2+} -MB (a). C 1 s XPS spectra
 122 before adsorption and after adsorption of Pb^{2+} , MB, and Pb^{2+} -MB (b). N 1 s XPS spectra before adsorption and after
 123 adsorption of Pb^{2+} , MB, and Pb^{2+} -MB (c).

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Table.S1: PFO, PSO, Elovich, and Bangham kinetic models' parameters

Kinetic models used	Lead concentrations (mg L ⁻¹)	Variables or Parameters				
		$\ln(q_e - q_t)$	K_1	R^2	χ^2	SSE
Lead (II)						
PFO	15	0.237	0.935	0.8950	4.768	8.587
	30	7.905	1.035	0.9326	9.250	16.025
	45	8.091	1.650	0.8791	15.255	22.291

MB						
PFO	15	0.203	0.713	0.8521	2.396	3.985
	30	4.369	0.906	0.9183	6.575	8.577
	45	8.091	1.650	0.8791	13.951	15.368
Lead (II)						
PSO	15	181.088	0.999	1.000	0.425	0.789
	30	179.631	0.073	0.999	0.634	0.923
	45	66.476	0.059	0.999	0.991	0.992
MB						
PSO	15	180.233	0.917	0.997	0.163	0.130
	30	153.891	0.063	0.993	0.149	0.228
	45	47.568	0.031	0.993	0.173	0.421
Lead (II)						
Elovich		β_{EI}	α_{EI}	R^2	χ^2	SSE
	15	0.1327	1.831×10^{28}	0.996	9.816	10.990
	30	0.0635	4.608×10^9	0.980	26.558	14.584
	45	0.0356	2.97×10^5	0.926	44.002	59.287
MB						

Elovich		β_{EI}	α_{EI}	R^2	χ^2	SSE
	15	0.1067	1.531×10^{25}	0.981	8.367	10.058
	30	0.0425	3.256×10^7	0.973	24.458	35.583
	45	0.0219	1.95×10^4	0.918	21.781	31.177
Lead (II)						
Bangham		K_j	α	R^2	χ^2	SSE
	15	523.65	0.0739	0.969	7.905	11.208
	30	613.51	0.3215	0.921	28.318	39.986
	45	640.83	0.0751	0.955	55.258	68.828
MB						
Bangham						
	15	460.39	0.0522	0.952	5.571	8.890
	30	593.85	0.2293	0.939	19.507	22.515
	45	624.47	0.0425	0.946	25.879	31.025

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Table .S2: The fitting parameters of IPD

Adsorbent cons (mg L⁻¹)	R^2	C (mg/g)	K (mg/g-min^{0.5})
Lead (II)			

	1R ²	2R ²	3R ²	C ₁	C ₂	C ₃	K ₁	K ₂	K ₃
15 mg L ⁻¹	1.0	0.81	0.76	9.65	8.67	7.36	0.39	0.27	0.22
30 mg L ⁻¹	1.0	0.96	0.61	15.32	9.90	8.06	0.35	0.19	0.15
45 mg L ⁻¹	1.0	0.98	0.59	16.43	10.76	9.62	0.29	0.14	0.07
MB									
15 mg L ⁻¹	1.0	0.79	0.70	8.19	7.39	5.03	0.37	0.30	0.24
30 mg L ⁻¹	1.0	0.93	0.57	13.61	11.31	8.61	0.36	0.15	0.13
45 mg L ⁻¹	1.0	0.96	0.49	14.90	10.69	6.62	0.29	0.11	0.09

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Table.S3: Adsorption isotherm parameters of Pb²⁺ and MB adsorption time on Fe₂O₃/BC/Mxene

Isothermal model	Para meters	293 K	303 K	313K
Lead (II)				
Langmuir	q _{m exp} (mg g ⁻¹)	1003	625	325
	q _{m cal} (mg g ⁻¹)	992.76	623.37	319.06
	K _L	0.065	0.041	0.033
	R ²	0.999	0.997	0.995
	χ ²	1.18	2.07	4.62
	SSE	3.06	4.25	5.51
	MB			
Langmuir	q _{m exp} (mg g ⁻¹)	995	565	300

	$q_{m \text{ cal}} (\text{mg g}^{-1})$	899.03	562.91	296.88
	K_L	0.055	0.036	0.017
	R^2	0.998	0.996	0.993
	χ^2	2.72	3.68	6.90
	SSE	4.81	6.37	8.02
Lead (II)				
Freundlich				
	$K_{F \text{ exp}} (\text{mg g}^{-1})$	820	626	419
	$K_{F \text{ cal}} (\text{mg g}^{-1})$	809.41	600.05	401.99
	n	3.68	3.39	3.27
	R^2	0.853	0.846	0.839
	χ^2	7.27	13.00	25.68
	SSE	10.21	19.68	31.01
MB				
Freundlich				
	$K_{F \text{ exp}} (\text{mg g}^{-1})$	805	515	320
	$K_{F \text{ cal}} (\text{mg g}^{-1})$	791.74	507.61	311.54
	n	3.55	3.31	2.99
	R^2	0.816	0.879	0.799
	χ^2	11.62	15.85	39.25

	SSE	14.33	21.84	45.39
Lead (II)				
Temkin				
	K_T	783.09	608.58	497.69
	B	0.856	0.456	0.409
	R^2	0.975	0.859	0.921
	χ^2	19.56	27.35	44.28
	SSE	33.45	56.24	70.69
MB				
Temkin				
	K_T	701.04	553.18	398.99
	B	0.789	0.398	0.307
	R^2	0.935	0.813	0.889
	χ^2	25.17	38.69	51.28
	SSE	33.45	56.24	70.69

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Table.S4: Thermodynamic parameters of Pb^{2+} and MB adsorption on $Fe_2O_3/BC/MXene$

Temperature (K)	$\Delta G(KJ mol^{-1})$	$\Delta H(KJ mol^{-1}K^{-1})$	$\Delta S(K mol^{-1})$
Lead (II)			
393 K	-8.362	-39.319	-0.110

303 K	-5.395		
313 K	-3.287		
MB			
393 K	-6.929	-25.179	-0.103
303 K	4.081		
313 K	-2.731		

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132 **Table.S5: Selectivity parameters of Pb²⁺ and MB adsorption on Fe₂O₃/BC/MXene, BC/Fe₂O₃ (c), and BC/MXene**

Heavy metals ion	Fe ₂ O ₃ /BC/MXene composite		BC/Fe ₂ O ₃ .		BC/MXene	
	K _d (mL g ⁻¹)	K	K _d (mL g ⁻¹)	K	K _d (mL g ⁻¹)	K
Pb (II)	19303.88	-	743.50	-	355.89	-
MB	16976.03	-	556.81	-	237.59	-
Mg (II)	80.43	230.8	80.39	11.28	32.02	54.80
Ni(I)	298.6	51.01	389.87	3.99	177.15	89.63
Cu (II)	3.75	6127.85	40.62	19.36	23.50	75.38
Cd (II)	176.09	100.21	7.52	141.73	85.38	133.90
Li (I)	19.51	985.67	41.52	23.63	102.61	3.63

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134 **References**

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