

Electronic Supplementary Information

Efficient Neural Network Models of Chemical Kinetics Using a Latent asinh Rate Transformation

Felix A. Döppel and Martin Votsmeier*

*martin.votsmeier@tu-darmstadt.de

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1 Linearizing Rate Expressions

$$r_j = k_{j,0} \cdot \exp\left(-\frac{E_A}{RT}\right) \cdot \prod_i c_i^{v_{i,j}} \cdot \prod_k \theta_k^{v_{k,j}} \quad (\text{S1})$$

$$\ln r_j = \ln k_{j,0} - \frac{E_A}{R} \cdot \frac{1}{T} + \sum_i v_{i,j} \cdot \ln c_i + \sum_k v_{k,j} \cdot \ln \theta_k \quad (\text{S2})$$

$$y = b + m \cdot x \quad (\text{S3})$$

2 Preferential Oxidation Mechanism

Table S1 Reactions and parameters for the PROX mechanism taken from¹ originating from²

No.	Reaction	s_0 or A_0 unitless or s^{-1}	unitless	E_A kJ/mol	$\frac{dE_A}{d\theta_H}$ kJ/mol	$\frac{dE_A}{d\theta_O}$ kJ/mol	$\frac{dE_A}{d\theta_{OH}}$ kJ/mol	$\frac{dE_A}{d\theta_{H_2O}}$ kJ/mol	$\frac{dE_A}{d\theta_{CO}}$ kJ/mol
H₂ oxidation on Pt									
R1	$H_2 + 2^* \rightleftharpoons 2H^*$	1.287×10^{-1} 7.953×10^{12}	0.8584 1.911	- 79.09	- -25.10	- 0	- 0	- 0	- 0
R2	$O_2 + 2^* \rightleftharpoons 2O^*$	5.423×10^{-1} 8.406×10^{12}	0.7656 0.9275	- 208.9	- 0	- -133.9	- 0	- 0	- 0
R3	$OH^* + ^* \rightleftharpoons O^* + H^*$	1.950×10^{12} 6.325×10^{12}	13.286 10.812	111.2 32.48	67.321 -5.820	-4.87 22.26	0 0	62.89 -41.71	0 0
R4	$H_2O^* + ^* \rightleftharpoons OH^* + H^*$	9.358×10^{12} 9.989×10^{12}	-0.3949 -0.3664	74.57 53.43	4.795 -7.757	50.33 -87.75	52.30 -52.30	-43.25 71.81	0 0
R5	$H_2O^* + O^* \rightleftharpoons 2OH^*$	4.316×10^{10} 1.700×10^{10}	0.3262 0.5285	36.74 94.32	0 0	70.10 -139.12	52.30 -52.30	-83.68 136.0	0 0
R6	$H_2O + ^* \rightleftharpoons H_2O^*$	1.084×10^{-1} 2.033×10^{12}	11.624 2.490	- 39.98	- 0	- 0	- 104.6	- -10.46	- 0
CO oxidation on Pt									
R7	$CO + ^* \rightleftharpoons CO^*$	1.000 5.659×10^{15}	0 0.3946	- 165.9	- 0	- 0	- 0	- 0	- -62.70
R8	$CO_2 + ^* \rightleftharpoons CO_2^*$	1.950×10^{-1} 3.626×10^{12}	0.2500 0.2459	- 11.60	- 0	- 0	- 0	- 0	- 0
R9	$CO_2^* + ^* \rightleftharpoons CO^* + O^*$	4.178×10^{10} 2.393×10^{11}	-0.2778 0.4558	110.4 85.42	0 0	4.27 -17.69	0 0	0 0	24.21 -38.53
Coupling reactions between CO- and H₂ oxidation									
R10	$CO_2^* + H^* \rightleftharpoons CO^* + OH^*$	8.031×10^8 1.245×10^9	-0.3259 0.8237	23.22 76.91	-6.276 6.276	60.25 -77.83	0 0	-45.56 59.04	18.12 -44.63
R11	$COOH^* + ^* \rightleftharpoons CO^* + OH^*$	8.426×10^8 1.187×10^9	0.02577 0.4719	22.66 77.46	0 0	60.25 -77.83	0 0	-45.56 59.94	18.13 -44.63
R12	$COOH^* + ^* \rightleftharpoons CO_2^* + H^*$	1.058×10^{11} 9.454×10^{10}	0.5812 -0.1098	4.975 6.079	6.276 -62.844	0 0	0 0	0 0	0 0
R13	$CO^* + H_2O^* \rightleftharpoons COOH^* + H^*$	1.103×10^{11} 9.070×10^{10}	0.4911 -0.02778	98.71 22.79	4.904 -7.657	0 0	52.30 -52.30	-5.230 5.230	-31.38 31.38
R14	$CO_2^* + OH^* \rightleftharpoons COOH^* + O^*$	5.349×10^{10} 1.870×10^{11}	0.05272 0.4515	109.5 29.70	0 0	-41.13 30.00	0 0	52.30 -52.30	0 0
R15	$CO_2^* + H_2O^* \rightleftharpoons COOH^* + OH^*$	8.642×10^{10} 1.157×10^{11}	-0.0481 0.5647	71.31 49.07	0 0	52.45 -85.62	52.30 -52.30	-44.87 70.19	0 0
R16	$CO_2^* + H^* \rightleftharpoons HCOO^* + ^*$	1.117×10^{11} 8.957×10^{10}	-0.07525 0.4218	73.49 0.00	-12.55 0	0 0	0 0	0 0	0 0
R17	$CO_2^* + OH^* \rightleftharpoons HCOO^* + O^*$	6.168×10^{10} 1.621×10^{11}	-0.3443 -0.1617	154.8 2.577	0 0	-67.47 3.657	0 0	100.2 -4.351	0 0
R18	$CO_2^* + H_2O^* \rightleftharpoons HCOO^* + OH^*$	1.022×10^{11} 9.785×10^{10}	-0.3574 0.06665	111.8 17.15	0 0	118.7 -19.40	90.99 -13.61	-98.17 16.89	0 0

3 Ammonia Oxidation Mechanism

Table S2 shows all 15 reversible reactions of the ammonia oxidation mechanism considered in this work, the activation energy E_A associated with the forward direction and the energy difference ΔE of the reaction. Table S3 lists all non-imaginary frequencies ν of the initial- and transition states. Values have to be multiplied by the elementary charge e and divided by Planck's constant h to convert to the unit Hz. Sticking coefficients of all adsorption reactions are assumed to be one.

Table S2 All 15 reversible ammonia oxidation reactions, the activation energy E_A associated with the forward direction and the energy difference ΔE of the reaction

Reaction	$E_A / \text{J mol}^{-1}$	$\Delta E / \text{J mol}^{-1}$
$\text{O}_2 + 2^* \rightleftharpoons 2\text{O}^*$	0	-238 319
$\text{NH}_3 + ^* \rightleftharpoons \text{NH}_3^*$	0	-66 575
$\text{NH}_3^* + \text{O}^* \rightleftharpoons \text{NH}_2^* + \text{OH}^*$	67 540	39 559
$\text{NH}_2^* + \text{O}^* \rightleftharpoons \text{NH}^* + \text{OH}^*$	78 153	-14 473
$\text{NH}^* + \text{O}^* \rightleftharpoons \text{N}^* + \text{OH}^*$	154 377	31 840
$\text{NH}_3^* + \text{OH}^* \rightleftharpoons \text{NH}_2^* + \text{H}_2\text{O}^*$	33 770	-13 508
$\text{NH}_2^* + \text{OH}^* \rightleftharpoons \text{NH}^* + \text{H}_2\text{O}^*$	965	-67 540
$\text{NH}^* + \text{OH}^* \rightleftharpoons \text{N}^* + \text{H}_2\text{O}^*$	39 559	-22 192
$2\text{OH}^* \rightleftharpoons \text{O}^* + \text{H}_2\text{O}^*$	0	-53 067
$\text{H}_2\text{O}^* \rightleftharpoons \text{H}_2\text{O} + ^*$	18 332	18 332
$2\text{N}^* \rightleftharpoons \text{N}_2 + 2^*$	244 108	-52 102
$\text{N}^* + \text{O}^* \rightleftharpoons \text{NO}^* + ^*$	213 233	3859
$\text{NO}^* \rightleftharpoons \text{NO} + ^*$	184 287	184 287
$\text{N}^* + \text{NO}^* \rightleftharpoons \text{N}_2\text{O}^* + ^*$	164 990	89 731
$\text{N}_2\text{O}^* \rightleftharpoons \text{N}_2\text{O} + ^*$	0	-2895

Table S3 A list of all non-imaginary frequencies ν of the initial states IS and transition states TS

Species	Type	ν / V
NH_3^*	IS	0.4320 0.4319 0.4152 0.1936 0.1934 0.1342 0.0820 0.0819 0.0458 0.0150 0.0149
NH_2^*	IS	0.4327 0.4189 0.1800 0.0969 0.0954 0.0825 0.0595 0.0436 0.0269
NH^*	IS	0.4242 0.0994 0.0992 0.0665 0.0588 0.0587
N^*	IS	0.0612 0.0612 0.0612
N_2O^*	IS	0.2980 0.1614 0.0541 0.0540 0.0225 0.0150 0.0149 0.0033
NO^*	IS	0.1924 0.0512 0.0511 0.0388 0.0187 0.0184
H_2O^*	IS	0.4578 0.4448 0.1919 0.0635 0.0573 0.0167 0.0122 0.0114
OH^*	IS	0.4391 0.0930 0.0896 0.0466 0.0244 0.0225
O^*	IS	0.0558 0.0454 0.0453
*	IS	-
$\text{NH}_3\text{-O}$	TS	0.4379 0.4262 0.3916 0.1802 0.1211 0.1125 0.0810 0.0685 0.0641 0.0588 0.0418 0.0316 0.0201 0.0137
$\text{NH}_2\text{-O}$	TS	0.4129 0.1870 0.1610 0.1155 0.1045 0.0786 0.0669 0.0576 0.0458 0.0332 0.0272
NH-O	TS	0.2167 0.1402 0.0776 0.0656 0.0569 0.0523 0.0355 0.0298
$\text{NH}_3\text{-OH}$	TS	0.4564 0.4366 0.4309 0.4057 0.1952 0.1826 0.1033 0.0825 0.0671 0.0638 0.0426 0.0333 0.0270 0.0201 0.0143 0.0088 0.0065
$\text{NH}_2\text{-OH}$	TS	0.4623 0.4009 0.3930 0.1915 0.1032 0.0995 0.0750 0.0607 0.0569 0.0502 0.0460 0.0197 0.0178 0.0113
NH-OH	TS	0.4531 0.2032 0.1503 0.1021 0.0783 0.0637 0.0626 0.0563 0.0448 0.0306 0.0198
OH-OH	TS	0.4549 0.1881 0.1673 0.1026 0.0799 0.0709 0.0632 0.0534 0.0368 0.0231 0.0180
N-N	TS	0.0716 0.0702 0.0537 0.0474 0.0228
N-O	TS	0.0722 0.0613 0.0525 0.0299 0.0287
N-NO	TS	0.2166 0.0731 0.0574 0.0515 0.0367 0.0339 0.0159 0.0060

4 Training Times

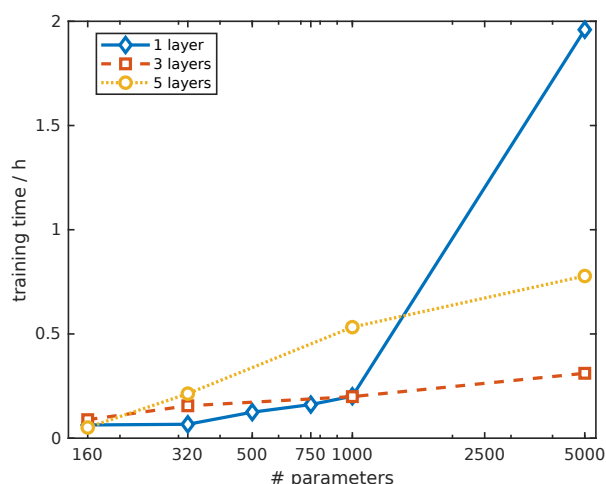


Figure S1 Median training times of the neural networks predicting CO source terms with the latent hyperbolic sine transformation strategy. Measured using three threads of a Intel® Xeon® Platinum 9242 Processor each.

5 Comparing Relative Error and MATE

So far, we applied the inverse hyperbolic sine transformation in a latent way. To investigate the effects of the latent approach, we also applied the inverse hyperbolic sine transformation in the conventional way. This means data are transformed in a preprocessing step and the transformed values are used as targets to be learned by a conventional neural network. As shown in table S4, the conventional approach leads to relative prediction errors above 1000%, while the latent approach achieves 15%. This can be attributed to the fact that instead of the relative error, the conventional approach minimizes an error measure defined in terms of the transformed values $\text{asinh}(\hat{s})$ which we call MATE. This error measure, however, is not relevant for reactor simulations.

Table S4 Prediction errors of lightweight neural networks with 40 nodes in a single hidden layer (≈ 320 parameters) modeling the CO source terms \hat{s} with two different approaches: Latent transformation minimizes the relative error during training resulting in an average accuracy of 15%. Conventional transformation minimizes the error of transformed values MATE instead.¹ Therefore, its predictions are two orders of magnitude less accurate, as measured by the relative error. Because MATE is not a relevant measure for the application in reactor simulations, the slightly better MATE score of the conventional approach poses no considerable advantage over the latent approach. The equations show how the errors are computed using the neural network predictions h

error measure	equation	latent (this work)	conventional
relative error	$\left \frac{\hat{s} - h(\hat{s})}{\hat{s}} \right $	15 %	>1000 %
MATE	$ \text{asinh}(\hat{s}) - h(\text{asinh}(\hat{s})) $	120 %	110 %

Figure S2 shows the relative error and the mean absolute transformed error MATE as a function of the predicted value. The exact value is arbitrarily chosen to be one. Both error measures share the same minimum and show similar asymptotic behavior for underestimations. Because of the logarithmic x-axis, the relative error grows exponentially for overestimations while MATE grows linearly. This leads to much more significant overestimations occurring in models trained with the conventional transformation approach as opposed to the latent approach.

¹Actually, both approaches minimize the root mean square of the term shown in the respective equation, not the mean absolute which is reported in table S4. As the root mean square is more sensitive to outliers it is well suited for model training but not an intuitive indicator of the model quality.

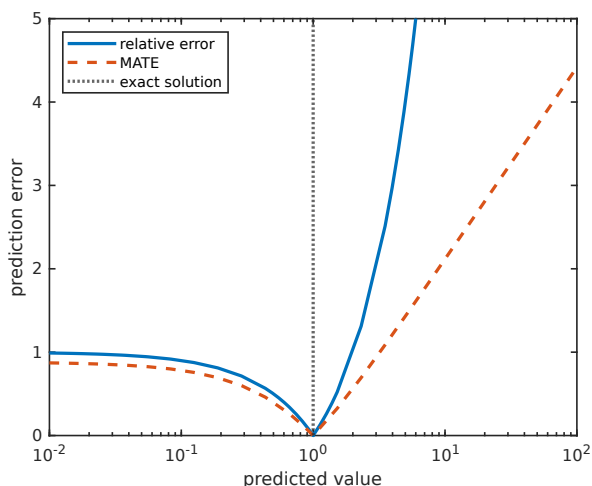


Figure S2 Comparison between the relative error and the mean absolute transformed error MATE (y-axis) for different predicted values (x-axis) assuming an exact solution of one.

6 Comparing Conventional and Latent Transformation Results

Figure S3 shows the prediction accuracy gain when using latent inverse hyperbolic sine transformation instead of the conventional approach modeling steady state CO source terms from test case one. The numbers shown are computed by dividing the relative prediction error obtained with the conventional approach by the error of the latent approach.

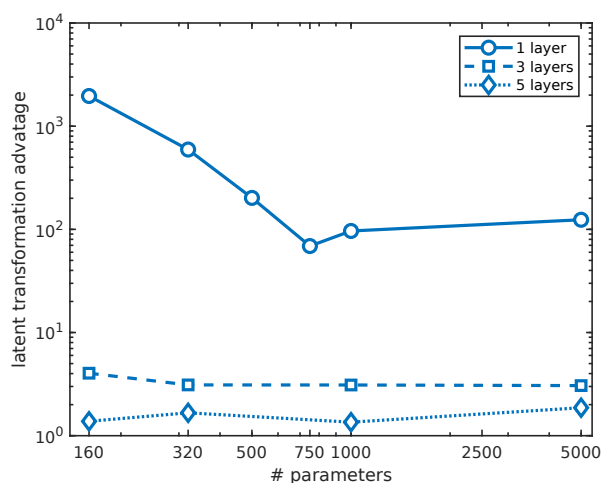


Figure S3 The accuracy gain of latent over conventional data transformation is shown as the quotient between relative prediction errors of models with identical complexity modeling steady state CO source terms. Results are shown for different numbers of hidden layers as a function of the number of model parameters.

7 Inference Time

Source term prediction time t_{predict} for 100 000 reaction conditions is averaged over 1000 runs with the models used for the preferential oxidation plug-flow reactor simulations. Results are shown in table S5 using an AMD Ryzen 7 5800X CPU and a GEFORCE RTX 3070 GPU. Computing the exact solution on the same machine takes 800 s resulting in a speed-up of 45 700 on the CPU and 95 200 on the GPU.

Table S5 Neural network prediction times t_{predict} for 100 000 reaction conditions averaged over 1000 measurements with the same models as used for the preferential oxidation plug-flow reactor simulations

Hardware	$t_{\text{predict}}(\text{O}_2) / \text{ms}$	$t_{\text{predict}}(\text{CO}) / \text{ms}$
CPU: AMD Ryzen 7 5800X	5.5	12
GPU: GEFORCE RTX 3070	3.0	5.4

8 Comparing to our Previous Work Using Mechanistic Insights

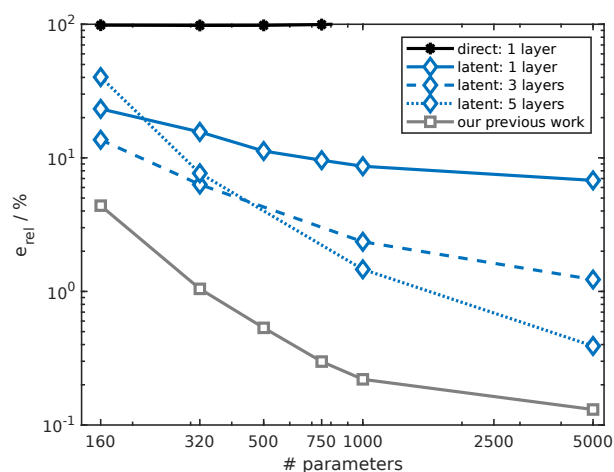
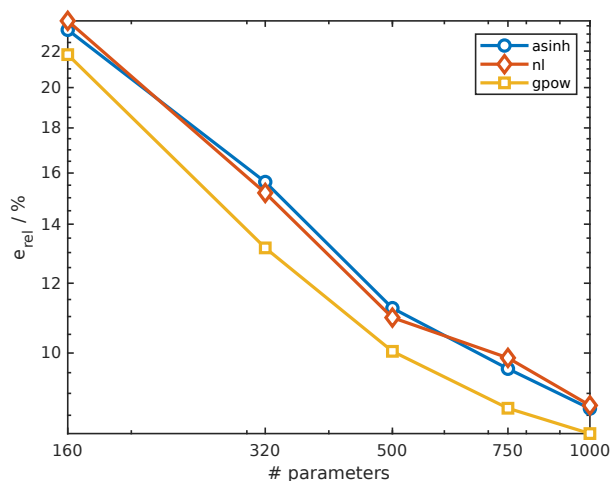
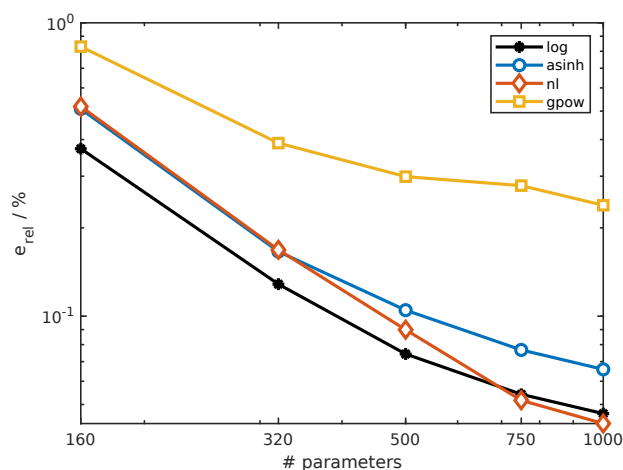


Figure S4 Relative prediction error of CO source terms dependent of the total number of learnable parameters in a neural network compared between different modeling strategies. Our previous work¹ performs best but requires a reaction path analysis and therefore cannot be used with experimental data or highly complex computational models.

9 Alternatives to the Hyperbolic Sine



(a) ... CO source terms.



(b) ... O₂ source terms.

Figure S5 Comparing the prediction accuracy of different transformation functions as a function of trainable model parameters in a single hidden layer for ...

References

- [1] F. A. Döppel and M. Votsmeier, *Chemical Engineering Science*, 2022, **262**, 117964.
- [2] W. Hauptmann, M. Votsmeier, H. Vogel and D. G. Vlachos, *Applied Catalysis A: General*, 2011, **397**, 174–182.