## Steering Competitive N<sub>2</sub> and CO Adsorption toward Efficient Urea Production with the Confined Dual Site

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## **Complement to Computational Detail**

The calculated lattice constants for the single site catalyst are a = 12.78 Å, b = 12.30 Å, and the vacuum space was set to be 15 Å in the *c* direction to minimize the interaction between periodic images. The dual site catalyst was placed into a 20 Å cubic box for optimization. The 3×3×1 Monkhorst-Pack and the 1×1×1 Gamma-centered k-point meshes were used to sample the Brillouin zone for the single site catalyst and dual site catalyst, respectively.

The adsorption energy ( $E_{ads}$ ) was calculated based on the equation:  $E_{ads} = E_{total} - E_{substrate} - E_{adsorbate}$ , where  $E_{total}$ ,  $E_{substrate}$  and  $E_{adsorbate}$  represent the total energies of the systems containing the substrate and adsorbate, the substrate, and the adsorbate, respectively. According to this definition, a more negative adsorption energy indicates a stronger interaction.

The Boltzmann function was used to evaluate the distribution of N2 and CO on the

active sites, which is defined as  $f_{dis} = 1/(1 + \exp\left\{-\frac{\delta G}{k_B T}\right\}) \times 100\%$ , where  $\delta G$  is the free energy difference between N<sub>2</sub> and CO adsorption,  $k_B$  is Boltzmann constant, and *T* is the room temperature of 298.15 K.

The Gibbs reaction free energy change ( $\Delta G$ ) of each elementary step was calculated by using the computational hydrogen electrode (CHE) model proposed by Nørskov *et al.*<sup>1</sup> The chemical potential of the proton-electron pair in aqueous solution is related to that of one-half of the chemical potential of an isolated hydrogen molecule. Based on this model, the  $\Delta G$  value can be obtained by the formula:  $\Delta G = \Delta E + \Delta ZPE$  $- T\Delta S + \Delta G_{pH} + eU$ , where  $\Delta E$  is the reaction energy of reactant and product species adsorbed on the catalyst directly obtained from DFT computations;  $\Delta ZPE$  and  $\Delta S$  are the changes between the adsorbed species and the gas phase molecules in zero-point energies and entropy at 298.15 K, which can be calculated from the vibrational frequencies.  $\Delta G_{pH}$  is the free energy correction of pH, and can be calculated by:  $\Delta G_{pH} = k_BT \times pH \times \ln 10$ . Notably, the pH value was set to be zero in this work for simplicity; U was the applied potential.

Single site	Adsorption	Ti	V	Cr	Mn	Fe	Со	Ni	Mo	Ru	Rh
	CO(v)	-2.10	-1.89	-1.15	-1.00	-1.45	-0.86	-0.16	-2.91	-2.77	-1.01
TMN <sub>4</sub>	$N_2(v)$	-1.68	-1.38	-0.45	-0.19	-0.43	-0.15	-0.16	-1.97	-1.34	-0.21
	$N_2(h)$	-1.68	-0.82	#	#	0.46	#	#	-1.88	-0.47	#
	CO(v)	-2.45	-1.85	-1.49	-1.24	-1.60	-1.56	-0.28	-3.52	-3.10	-1.89
TMN <sub>3</sub> C <sub>1</sub>	$N_2(v)$	-2.10	-1.31	-0.94	-0.42	-0.54	-0.61	-0.15	-2.64	-1.82	-0.66
	$N_2(h)$	-2.01	-1.29	#	-0.01	-0.04	#	#	-2.68	-1.13	#
	CO(v)	-2.55	-1.84	-1.85	-1.26	-1.54	-1.78	-0.70	-3.07	-3.46	-2.53
TMN <sub>2</sub> C <sub>2</sub>	$N_2(v)$	-2.19	-1.43	-1.26	-0.53	-0.43	-0.72	-0.17	-2.31	-2.20	-1.20
	$N_2(h)$	#	-1.21	-0.67	#	#	#	#	-2.07	-1.61	#
TMN <sub>1</sub> C <sub>3</sub>	CO(v)	-2.77	-2.23	-1.75	-1.34	-1.49	-1.94	-1.00	-3.46	-3.08	-2.59
	$N_2(v)$	-2.49	-1.76	-1.26	-0.79	-0.51	-0.74	-0.24	-2.84	-2.04	-1.61
	$N_2(h)$	#	-1.53	#	#	#	#	#	#	-1.64	-1.21

**Table S1.** The detailed calculated adsorption energies of CO and  $N_2$  via vertical (v) and horizontal (h) mode on the designed single site catalysts. The unit is eV and the symbol # indicates unstable or physical adsorption.

**Table S2.** The detailed calculated adsorption energies of CO and  $N_2$  on the confined dual site catalysts. The unit is eV and the symbol # indicates unstable catalyst with severe deformation during the structural relaxation.

Dual site	adsorption	Ti	V	Cr	Mn	Fe	Со	Ni	Mo	Ru	Rh
	СО	-2.26	-2.00	-0.79	-1.03	-1.32	-0.61	-0.22	-2.83	-2.13	-0.58
I IVIIN4	$N_2$	-2.18	-2.62	-0.44	-0.21	-0.31	0.08	-0.24	-2.77	-1.25	-0.23
	СО	-1.90	-1.67	-1.02	-1.15	-1.49	-1.12	-0.30	-3.43	-2.22	-1.25
TMIN <sub>3</sub> C <sub>1</sub>	$N_2$	-1.78	-1.89	-0.80	-0.37	-0.53	-0.46	-0.27	-3.25	-1.53	0.22
TMN <sub>2</sub> C <sub>2</sub>	СО	-1.65	-1.91	-1.47	-1.12	-1.55	-1.51	-0.30	#	-3.22	#
	$N_2$	-1.39	-2.09	-1.70	-0.26	-0.44	-0.70	-0.25	#	-2.40	#
TMN <sub>1</sub> C <sub>3</sub>	CO	-1.43	-1.69	-0.76	-0.93	-1.05	-1.45	-1.15	#	#	#
	$N_2$	-1.02	-1.49	-0.82	-0.46	-0.51	-0.82	-0.25	#	#	#

**Table S3.** The detailed calculated information about adsorption energy difference ( $\Delta E$ ), zero-point energy (ZPE), entropy change (T $\Delta$ S) at 298.15 K, adsorption free energy ( $\Delta G_{ads}$ ), and adsorption free energy difference ( $\Delta G$ ) over eight dual site catalysts. The unit is eV.

Dual site	TiN <sub>4</sub>	VN <sub>4</sub>	MoN <sub>4</sub>	TiN <sub>3</sub> C <sub>1</sub>	VN <sub>3</sub> C <sub>1</sub>	VN <sub>2</sub> C <sub>2</sub>	CrN <sub>2</sub> C <sub>2</sub>	CrN <sub>1</sub> C <sub>3</sub>
$\Delta E = E_{ads}(N_2) - E_{ads}(CO)$	0.09	-0.62	0.06	0.12	-0.23	-0.18	-0.23	-0.07
$ZPE(N_2)$	0.21	0.22	0.21	0.20	0.21	0.21	0.22	0.21
ZPE(CO)	0.19	0.20	0.25	0.17	0.20	0.21	0.20	0.21
$T\Delta S(N_2)$	0.10	0.08	0.09	0.10	0.08	0.08	0.08	0.09
$T\Delta S(CO)$	0.09	0.10	0.08	0.13	0.10	0.08	0.10	0.09
$\Delta G_{ads}(N_2)$	-1.63	-2.05	-2.21	-1.25	-1.34	-1.53	-1.13	-0.27
$\Delta G_{ads}(CO)$	-1.70	-1.45	-2.20	-1.41	-1.12	-1.33	-0.92	-0.18
$\Delta G = G_{ads}(N_2) - G_{ads}(CO)$	0.07	-0.60	-0.01	0.16	-0.22	-0.21	-0.20	-0.09

Note that for the values of energy difference ( $\Delta E$  and  $\Delta G$ ), there is a small and negligible error, showing the reliable data in Figure 2 for evaluating the competitive adsorption. A more negative value of energy difference ( $\Delta E$  and  $\Delta G$ ) indicates a stronger N<sub>2</sub> adsorption than CO.

Distribution (%)	$D_s$ -Ti $N_4$	D <sub>S</sub> -VN <sub>4</sub>	D <sub>s</sub> -MoN <sub>4</sub>	D <sub>s</sub> -TiN <sub>3</sub> C <sub>1</sub>
N <sub>2</sub> adsorption	5.83	100.00	61.24	0.19
CO adsorption	94.17	0.00	38.76	99.81
Distribution (%)	$D_{s}$ - $VN_{3}C_{1}$	$D_s$ - $VN_2C_2$	$D_s$ - $CrN_2C_2$	$D_{s}$ - $CrN_{1}C_{3}$
N <sub>2</sub> adsorption	99.98	99.97	99.96	97.12
CO adsorption	0.02	0.03	0.04	2.88

**Table S4.** The calculated data of adsorption distributions of CO and  $N_2$  molecules over eight dual site catalysts.

ICOHP	TM-N	ТМ-С	ТМ-О
D <sub>S</sub> -VN <sub>4</sub>	-3.04	-3.07	-1.65
$D_{s}$ - $VN_{3}C_{1}$	-2.63	-3.07	-1.73
$D_s$ - $VN_2C_2$	-2.90	-2.94	-1.68
$D_s$ - $CrN_2C_2$	-2.86	-2.68	-0.94
$D_{s}$ - $CrN_{1}C_{3}$	-2.68	-2.90	-1.31

**Table S5.** The calculated ICOHP values of TM–N, TM–C and TM–O bonds over five dual site catalysts.

**Table S6.** The calculated N affinity on the single site catalysts and the adsorption energy difference ( $\Delta E = E_{ads}(N_2)-E_{ads}(CO)$ ). The unit is eV and the symbol # indicates unstable catalyst with severe deformation during the structural relaxation. A more negative value of N binding represents a stronger TM–N interaction and a more negative value of  $\Delta E$  indicates a stronger N<sub>2</sub> adsorption than CO.

	transition metal	Ti	V	Cr	Mn	Fe	Co	Ni	Mo	Ru	Rh
	N binding (single site)	0.07	-0.59	-0.04	0.48	1.65	2.81	4.28	-2.49	-0.41	2.51
TMN <sub>4</sub>	$\Delta E$ (single site)	0.42	0.50	0.70	0.81	1.02	0.71	0.00	0.94	1.43	0.80
	$\Delta E$ (dual site)	0.09	-0.62	0.35	0.82	1.00	0.68	-0.03	0.06	0.88	0.36
	N binding (single site)	0.22	-0.70	-0.28	0.47	0.85	2.44	3.80	-2.40	-1.42	1.84
TMN <sub>3</sub> C <sub>1</sub>	$\Delta E$ (single site)	0.35	0.54	0.55	0.83	1.06	0.95	0.12	0.88	1.29	1.23
	$\Delta E$ (dual site)	0.12	-0.23	0.22	0.78	0.96	0.67	0.03	-0.04	0.69	1.47
	N binding (single site)	0.45	-0.53	-0.52	0.37	0.51	1.91	3.64	-1.98	-1.92	0.76
TMN <sub>3</sub> C <sub>1</sub>	$\Delta E$ (single site)	0.37	0.40	0.58	0.73	1.11	1.06	0.53	0.77	1.27	1.33
	$\Delta E$ (dual site)	0.27	-0.18	-0.23	0.87	1.11	0.81	0.05	#	0.83	#
	N binding (single site)	0.86	-0.11	-0.29	-0.01	0.20	1.15	3.20	-2.30	-1.78	0.21
TMN <sub>3</sub> C <sub>1</sub>	$\Delta E$ (single site)	0.28	0.47	0.49	0.55	0.98	1.20	0.76	0.62	1.04	0.98
	$\Delta E$ (dual site)	0.41	0.21	-0.19	0.47	0.54	0.63	0.90	#	#	#

Note that there are some TM sites showing weaker N binding (e.g., dual RhN<sub>4</sub>) still present efficient improvement via dual site strategy. This may be due to the confinement introduced by the dual site catalyst that constrains the adsorption behavior of CO, making it unable to adsorb on the one-sided active site in an optimal orbital overlapping manner.



**Figure S1.** The detailed atomic structures of single TM atom embedded in graphene with different coordination.

Note that for the  $TMN_2C_2$  complexes, there are two possible configurations (i.e., orthoand para-doping). After testing, the ortho-configuration (as shown in the above Figure) is more energetically stable. Therefore, this configuration is employed herein, including single site or dual site catalysts in the main text.



Figure S2. The detailed atomic structures of confined dual TM site.



Figure S3. The calculated adsorption energy of  $N_2$  and CO molecules on the para-TMN<sub>2</sub>C<sub>2</sub> moiety with isolated single site and confined dual site. The black dashed line represents the equivalent adsorption, and above the line is the N<sub>2</sub>-dominated adsorption region.

(%) 100-	N <sub>2</sub> dominant	O D <sub>S</sub> -VN <sub>4</sub>			O D <sub>S</sub> -VN <sub>3</sub> C <sub>1</sub>	O D <sub>S</sub> -VN <sub>2</sub> C <sub>2</sub>	$\bigcirc$ D <sub>s</sub> -CrN <sub>2</sub> C <sub>2</sub>	D <sub>s</sub> -CrN <sub>1</sub> C <sub>3</sub>
stributio			D <sub>s</sub> -MoN <sub>4</sub>					-
tion dis								-
Adsorp 100-	D <sub>S</sub> -TiN <sub>4</sub>			D <sub>s</sub> -TiN <sub>3</sub> C <sub>1</sub>				CO dominant

Figure S4. The calculated adsorption distribution of CO and  $N_2$  molecules over eight dual-site catalysts.



Figure S5. Spin charge density of N<sub>2</sub> adsorption and CO adsorption, where the isosurface value was set to be 0.009 e Å<sup>-3</sup> on (A)  $D_s$ -VN<sub>3</sub>C<sub>1</sub>, (B)  $D_s$ -VN<sub>2</sub>C<sub>2</sub>, (C)  $D_s$ -CrN<sub>2</sub>C<sub>2</sub>, and (D)  $D_s$ -CrN<sub>1</sub>C<sub>3</sub>.



Figure S6. The calculated charge transfer on adsorbed  $N_2$  and CO molecules on five single site catalysts.



Figure S7. The atomic structures of \*NCON and  $N_2H$  intermediates over five dual site catalysts.



**Figure S8.** The calculated energy change ( $\Delta E$ ) from an adsorbed N<sub>2</sub> molecule (N<sub>2</sub><sup>\*</sup>) to two isolated N atoms (2N<sup>\*</sup>) over five candidates, and the atomic structure of two isolated N atoms adsorbed on D<sub>S</sub>-VN<sub>4</sub> was given below as an example. The  $\Delta E$  is defined as  $\Delta E = E(2N^*) - E(N_2^*)$ , where  $E(2N^*)$  and  $E(N_2^*)$  are the calculated total energies of two isolated N atoms and an adsorbed N<sub>2</sub> molecule, respectively.

D <sub>S</sub> -VN <sub>4</sub>	Initial state	Transition state	Final state
*NCON formation		¥.	Y.

Figure S9. The atomic structures of initial, transition and final states in the kinetic pathway of C–N coupling on the designed  $D_S$ -VN<sub>4</sub> catalyst.



Figure S10. The atomic structures of the adsorption of two H atom on the designed  $D_{S}$ -VN<sub>4</sub> catalyst.

## References

1 J. K. Nørskov, J. Rossmeisl, A. Logadottir, L. Lindqvist, J. R. Kitchin, T. Bligaard and H. Jonsson, *J. Phys. Chem. B*, 2004, **108**, 17886-17892.