

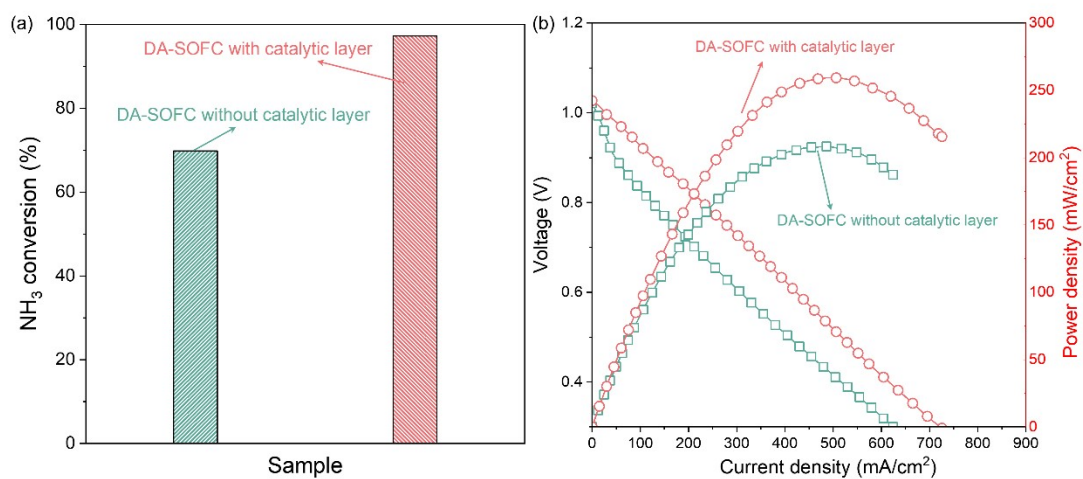
# Temperature Gradient Reduction in a Tubular Direct Ammonia Solid Oxide Fuel Cell by Fluidizing the Cathode Particles

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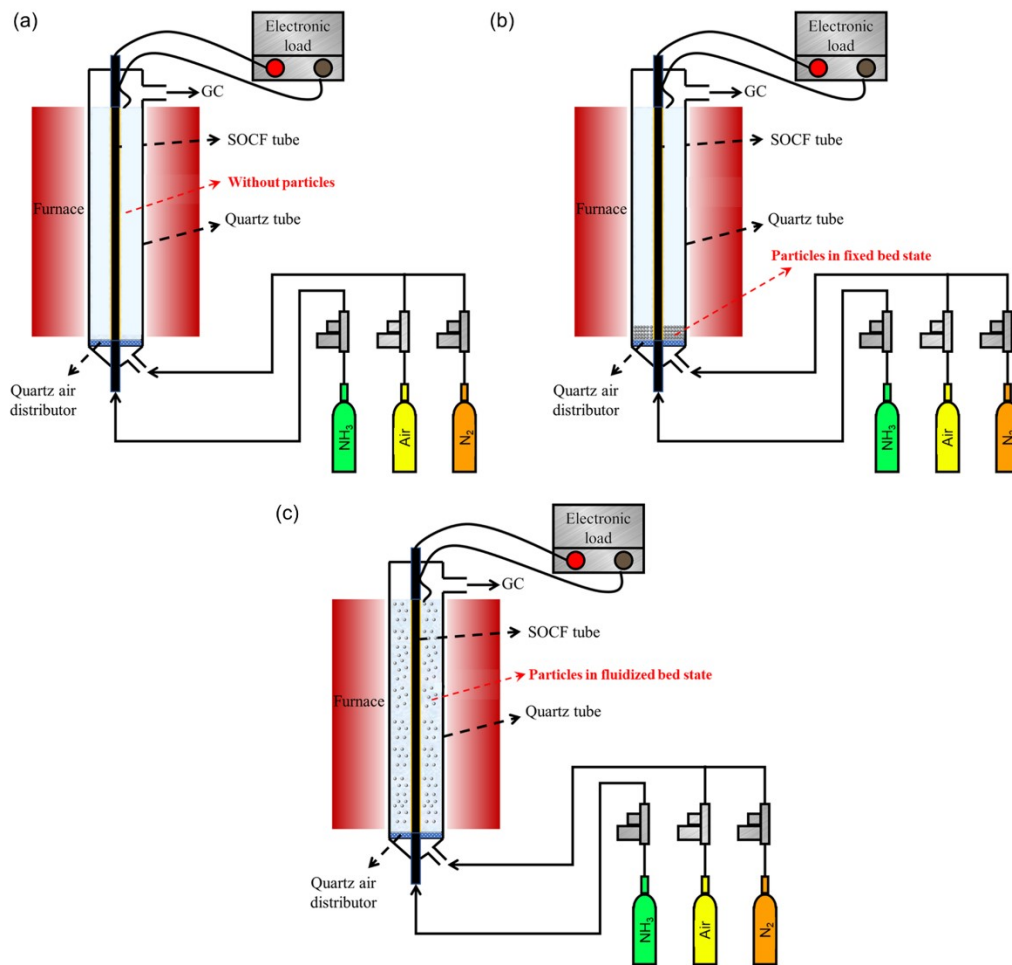
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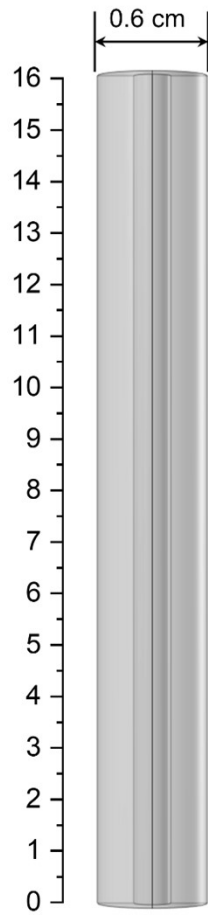
## Supporting materials



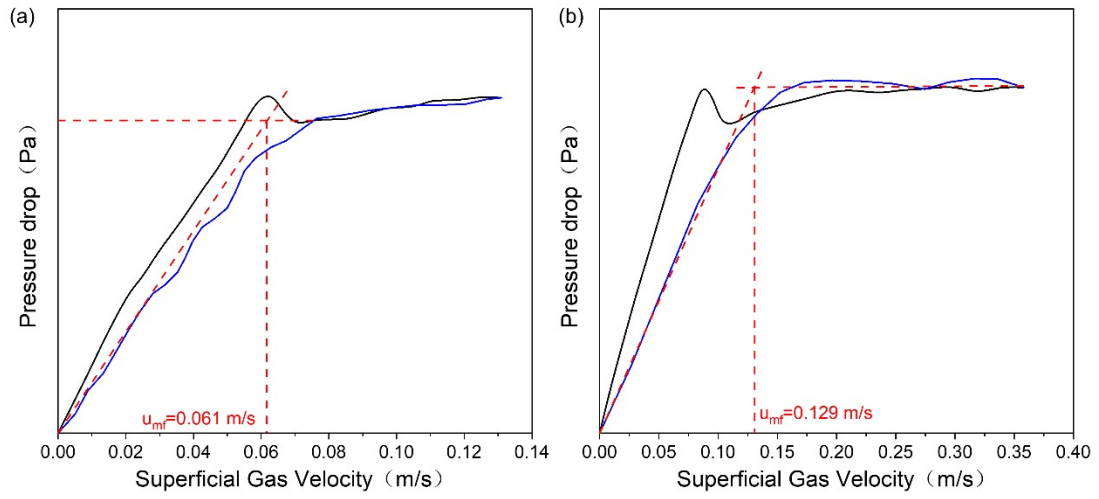
**Fig. S1.** (a) NH<sub>3</sub> decomposition and (b) *I-V-P* profiles of DA-SOFC with and without catalytic layer.



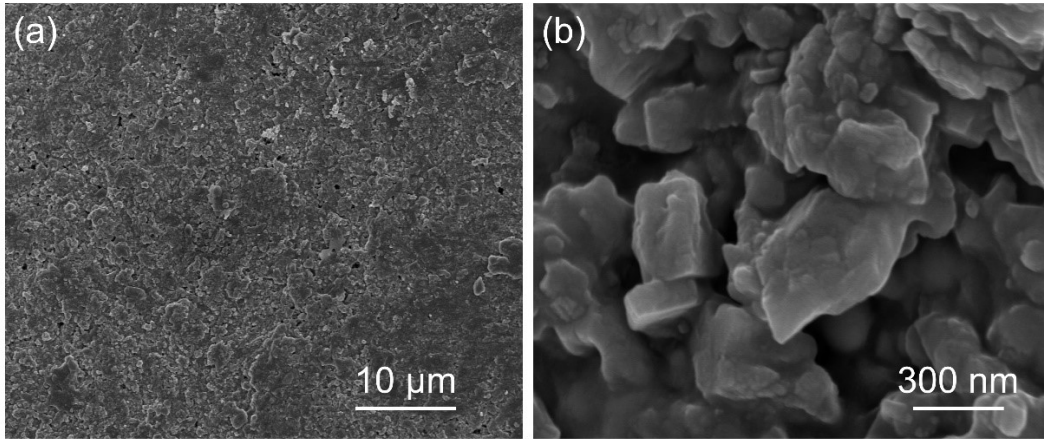
**Fig. S2.** Schematic illustration of the three configurations. (a) DA-SOFC/N, (b) DA-SOFC/FB, and (c) DA-SOFC/FL



**Fig. S3.** Schematic of the numerical model.



**Fig. S4.** Pressure drops versus superficial velocity for the particles with the size of (a) 242  $\mu\text{m}$  and (b) 350  $\mu\text{m}$  to determine the critical fluidized velocity ( $u_{mf}$ ).



**Fig. S5.** SEM images of the cathode layer for DA-SOFC/FL after 200 hours

**Table S1. Configuration of the tubular SOFC**

Layers	Composition	Thickness ( $\mu\text{m}$ )	Diameter (mm)	Elastic modulus (GPa)	Thermal expansion coefficient ( $/^{\circ}\text{C}$ )
Anode	Ni/YSZ	620	6	200	$11.5 \cdot 10^{-6}$
Electrolyte	YSZ	5.91	6	200	$10.0 \cdot 10^{-6}$
Cathode	LSCF/YSZ	8.38	6	95	$17.0 \cdot 10^{-6}$

**Table S2.** Parameters of the DA-SOFC used in the modelling

Parameter	Dimension
Inner diameter	6 mm
Anode thickness	620 $\mu\text{m}$
Electrolyte thickness	5.9 $\mu\text{m}$
Cathode thickness	8.4 $\mu\text{m}$
Cell length	16 cm
Anode permeability	1e-10 $\text{m}^2$
Cathode permeability	1e-10 $\text{m}^2$
Temperature	750 $^{\circ}\text{C}$
Anode thermal conductivity	11 (W/m/K)
Electrolyte thermal conductivity	2.7 (W/m/K)
Cathode thermal conductivity	6 (W/m/K)
Anode specific heat	450 (J/kg/K)
Electrolyte specific heat	470 (J/kg/K)
Cathode specific heat	430 (J/kg/K)
Porosity	0.35
Anode inlet composition	Pure Ammonia
Anode inlet composition	Air
Reference diffusivity	3.16e-8 $\text{m}^2/\text{s}$