Electronic Supplementary Information (ESI)

Selective C–O bond cleavage in diphenyl ether via catalytic transfer hydrogenolysis over Ru-decorated nanocrystalline H-ZSM-5

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1. Materials

All the chemicals and materials were of AR grade, and used without further purification. The [Poly(ethylene glycol)]-block-[poly(propylene glycol)]-block-[poly(ethylene glycol)] (Pluronic®P123, $M_n = 5800$), tetraethylorthosilicate (TEOS, 98%), propyltriethoxy silane (PrTES, 97%) tetrapropylammonium hydroxide (TPAOH), sodium aluminate and ruthenium (III) chloride hydrate, and 2-propanol (IPA) were purchased from Sigma Aldrich. Sodium borohydride (98%) was purchased from Loba Chemie Pvt. Ltd. Diphenyl ether (99.89%) and other substrates were purchased from BLD pharmatech (India) Pvt. Ltd, India. The other solvents (>99%) used in this work were obtained from Merk Lifescience Private Limited, India.

2. Characterization

The powder X-ray diffraction pattern of the prepared materials was recorded on a Rigaku Miniflex III diffractometer. The diffraction intensities were measured in the 2θ range of 5-80° with a Cu k α (λ = 0.15406 nm) radiation (40 kV, 15 mA) at a scanning speed of 10 °/min. The Si/Al ratio and Ru metal loading in the prepared zeolite materials were analyzed by microwave plasma atomic emission spectroscopy (MP-AES). The analysis was carried out in a single spray chamber by injecting the samples into a stream of nitrogen plasma. The textural properties of the prepared samples were analyzed by N2-adsorption isotherms using Quantachrome autosorb-iQ₂-TPX surface area instrument. All the samples were preheated up to 300 °C for 3 h under vacuum. The specific surface area and the pore diameter estimation in the prepared catalyst were calculated using Brunauer Emmett-Teller (BET) equation in the relative pressure range of 0.05-0.3 and Barrett-Joyner-Halenda (BJH) equation, respectively. The morphological investigation of the prepared materials was recorded in scanning electron microscopy (JEOL JSM-6610LV) instrument. The transmission electron microscopy obtained the in-depth investigation of the morphology in the prepared material (FEI Tecnai G2, F30) operated at an accelerating potential of 200 kV. The elemental analysis and oxidation states of the elements present in the catalysts were examined by X-ray photoelectron spectroscopy (XPS) on PHI 5000 VersaProbeII (ULVAC- PHI, INC, Japan) operating with a microfocus (100 µm, 25 W, 15 kV) monochromatic Al-K α source (hv = 1486.6 eV) equipped with a hemispherical analyzer and a multichannel detector. The Bruker Tensor-II F-27 Fourier transform Infra-Red (FT-IR) instrument was used, and pyridine used as a probe molecule for Py FT-IR study. The total acidity (NH₃-TPD) and reducibility (H₂-TPR) of the prepared materials were examined through Temperature Programmed Desorption/Reduction experiments on a Quantachrome AutosorbiQ2-TPX, CHEMBETTM TPR/TPD instrument. For the NH3-TPD analysis, the prepared

samples were pre-treated to 300 °C at the ramp rate of 10 °C/min under He flows for 30 min. After the pre-treatment, the sample cell was cooled to 50 °C, and the NH₃ (10% in He) was adsorbed by flowing the gas for 1 h in the sample cell with a flowing rate of 10 mL/min. After adsorption, the excess or physically adsorbed NH₃-gas was removed by passing the He gas at 50 mL/min for 30 min. The amount of desorbed gas was analyzed on a thermal conductivity detector (TCD) against temperature with a heating rate of 10 °C/min in the temperature range from 50-800 °C. For the H₂-TPD analysis, H₂ gas (10% H₂ in Ar) was taken instead of NH₃ gas. The temperature-programmed reduction was performed on Quantachrome Autosorb-iQ₂-TPX, CHEMBETTM TPR/TPD instrument. During the analysis, the temperature was increased from room temperature to 800 °C with a heating rate of 5 °C/min in 10% H₂/Ar flow (30 mL/min).

3. Catalyst preparation

3.1 Synthesis of N-HZSM-5

Nanocrystalline zeolite (N-HZSM-5) was prepared via a reported procedure with some modification.^{S1} In a typical synthesis process, 6.355 g of TPAOH and 0.241 g of sodium aluminate (53 wt% Al₂O₃, 43 wt% Na₂O) were dissolved in 18.686 g of deionized water (DI water), and the solution was stirred for 30 min at room temperature $(25 \pm 2 \text{ °C})$ until the solution becomes clear. To this solution, 1.031 g of PrTES was added and stirred for another 5 min; after that, 9.36 g of TEOS was added. The mixed solution was stirred for another 6 h at room temperature (25 \pm 2 °C). The obtained gel mixture has a molar composition of 90TEOS/10PrTES/2.5Al₂O₃/3.3Na₂O/25TPAOH/2500H₂O. This mixed solution was transferred into a 100 mL Teflon-lined autoclave and then hydrothermally treated at 170 °C for 72 h under static conditions. The obtained white-colored material was filtered in a vacuum filtration assembly, washed with 500 mL DI water, and dried at 80 °C for 12 h. The dried material was calcined at 550 °C for 5 h at a heating rate of 2 °C/min in a muffle furnace. The ion-exchange process produced the acidic form of the material designated as N-HZSM-5 prepared by stirring with 1 M aqueous NH₄Cl solution at 80 °C for 5 h. This ion-exchange step was repeated thrice, followed by calcination at 550 °C for 5 h at a heating rate of 2 °C/min. For the comparison, conventional HZSM-5 material was synthesized using the same procedure mentioned above for the N-HZSM-5, but without adding PrTES additive.

3.2 Synthesis of Ru(x%)/N-HZSM-5

The impregnation method was used to prepare the metal NPs based catalytic materials. In a typical process, 500 mg of N-HZSM-5 was dispersed in the 50 mL of ethanol: water (2:1) system and then sonicated for 20 min. In a separate beaker, the necessary quantity of RuCl₃.3H₂O (at x = 1, 2, 3, and 5 wt.% or 10.22, 20.45, 30.67, and 51.10 mg respectively w.r.t support) was dissolved in 10 mL of water. The aqueous metal salt solution was added dropwise to the dispersed N-HZSM-5 solution under stirring and stirred for 24 h at room temperature. After the impregnation, the water evaporated at 50 °C (total evaporation time ~ 9 h). The metal salt-impregnated precursor was dried and grounded by mortar & pestle. The metal saltimpregnated precursor was reduced by the chemical reduction process. The metal saltimpregnated precursor was subjected to a chemical reduction process. In this procedure, a limited volume of NaBH₄ (30 mL) was used, with a NaBH₄ to Ru weight ratio of 15. Depending on the Ru loading (1, 2, 3, or 5 wt.%), 75, 150, 225, or 375 mg of NaBH₄ were taken. To this NaBH₄ solution, the metal salt-impregnated precursor was slowly added. Then this mixed solution was stirred for 1 h in an ice bath $(4 \pm 2 \ ^{\circ}C)$ and another 24 h at room temperature (25 \pm 2 °C). Then, reduced catalysts were washed with excess DI water and dried at 50 °C under a vacuum oven (~ 0.09 MPa) for 12 h. The reduced material is termed Ru(x%)/N-HZSM-5, where x = 1, 2, 3, and 5. The corresponding loading of the Ru NPs was further confirmed by the MP-AES analysis (Table-1). The surface area of H-ZSM-5 was 304 m²/g. The Ru content was determined to be 2.88 wt% in Ru(3%)/H-ZSM-5.

3.3 Synthesis of Ru(3%)/SBA-15

SBA-15 material was synthesized via a reported method.^{S2} In a typical process, 2g of P123 ($EO_{20}PO_{70}EO_{20}$) were dissolved in the 45 mL of HCl solution (1.6 mol/L), and then the mixture was stirred in a 40 °C water bath for 3 h. To this mixture, 4.25 g of TEOS was added and stirred for another 24 h, at 40 °C. After stirring, the mixed solution was aged for another 24 h at 100 °C. The precipitate was washed enough with water and ethanol, dried in an oven, and then calcined at 550 °C for 6 h at a 2 °C/min heating rate. The Ru(3%)/SBA-15 material was synthesized using the same method as Ru(x%)/N-HZSM-5. The surface area of SBA-15 was 698 m²/g. The Ru content was determined to be 2.89 wt% in Ru(3%)/SBA-15.

Calculation regarding the formation of acetone during CTH of DPE (GC-FID data): From the Fig. S20 a and b,

The percentage of acetone formed during the 3 h of CTH of DPE = 10.078 % The amount of IPA taken in reaction mixture = 10 mL The amount of acetone formed after CTH of DPE = $10 \times \frac{10.078}{100} = 1.0078 mL$ Density of acetone (d) = $0.784 g mL^{-1} = \frac{Mass (m)}{Volume (V)}$ Mass of acetone (m) = $d \times V = 0.784 g mL^{-1} \times 1.0078 mL = 0.79011 g$ Moles of acetone formed during CTH of DPE = Mass of acetone $\times \frac{1 mole}{58.08 g}$ Moles of acetone formed during CTH of DPE = 0.79011 g $\times \frac{1 mole}{58.08 g} = 0.01360 M$ = 13.60 mmol.

Calculation for the formation of acetone during CTH process (¹H-NMR data):

From Fig. S21,

Acetone yield (%) = [(Acetone (product)i.e. area under the peaks correspond to acetone (-CH₃)protons)[/[(area under the peaks correspond to IPA (-CH₃)protons) + (Acetone (product)i.e. area under the peaks correspond to acetone (-CH₃)protons)] × 100

Acetone yield (%) =
$$\frac{0.68}{6+0.68} \times 100 = 10.17$$
 %
The amount of IPA taken in reaction mixture = 10 mL
The amount of acetone formed after CTH of DPE = $10 \times \frac{10.17}{100} = 1.017$ mL
Density of acetone (d) = $0.784 \text{ g mL}^{-1} = \frac{\text{Mass } (m)}{\text{Volume } (V)}$
Mass of acetone (m) = $d \times V = 0.784 \text{ g mL}^{-1} \times 1.017$ mL = 0.7973 g

Moles of acetone formed during CTH of DPE = Mass of acetone $\times \frac{1 \text{ mole}}{58.08 \text{ g}}$ Moles of acetone formed during CTH of DPE = 0.7973 g $\times \frac{1 \text{ mole}}{58.08 \text{ g}}$ = 0.01372 M = **13.72 mmol**. **Table S1** Assessing catalytic efficiency in the conversion of DPE using Ru/Zeolite-basedcatalysts in CTH.

S. No.	Catalyst	Reaction condition	Selectivity of HYD product (%)	Selectivity of HYD product (%) Limitations	
1	Ru/HZSM-5-OM	150 °C, 4 h, 4.0 MPa of H ₂ , 50 mg of catalyst, 1 mmol of substrate, 8 mL of water	100	Use of high pressure H ₂ gas (4.0 MPa)	S3
2	Ru/ZSM-5	reaction temperature (200 °C), WHSV (0.0867 min ⁻¹), 0.3 g catalyst, P_{H2} (4.0 MPa), H_2 flow rate (120 mL/min), guaiacol flow rate (0.026 g/min)	100	Use of high pressure H ₂ gas (4.0 MPa)	S4
3	Microporous Beta, Y, and ZSM-5 zeolites	1.0 g lignin, 0.5 g catalyst, and 100 mL ethanol, 280 °C, 6 h	-	High reaction temperature (280 °C) Lignin ethanolysis to produce the aromatic monomers not fuel range chemicals.	S5
4	Ru/H-Beta	1 mmol substrate, 0.1 g catalyst, 4 mL H ₂ O, 4.0 MPa H ₂ , temperature 140 °C	100	Use of high pressure H ₂ gas (4.0 MPa)	S6
5	Ru/HZSM-5	100 mg of DPE, 20 mL of n-hexane, 30 mg of 5% Ru/HZSM-5 catalyst, 1 MPa H ₂ , 2 h, 210 °C	100	Reaction temperature 210 °C, Use of 1 MPa H ₂ pressure, high Ru- metal loading (5 wt.%)	S7
6	Ru@H-ZSM-5	150 °C, 5.0 MPa H ₂ , phenol (2.13 mmol), catalyst (200 mg), and water (10 mL)	100	Use of high pressure H ₂ gas (4.0 MPa)	S 8
7	Ru(3%)/N- HZSM-5	DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 °C), time (3 h), and N ₂ (1 MPa)	100	Sustainable CTH process (Lower reaction temperature < 180 °C) (Alcohol as H-donor)	Present work

Table S2

Ratio of Ru^0/RuO_x calculated using a high-resolution Ru 3p XPS spectrum of Ru(3%)/N-HZSM-5.

Peaks	Binding energy	Area
$Ru^0 3p_{3/2}$	462.18 eV	11905
$Ru^0 3p_{1/2}$	484.16 eV	4901
RuO _x 3p _{3/2}	466.48 eV	4256
RuO _x 3p _{1/2}	486.78 eV	2519
$Ru^0 3p_{3/2} + Ru^0 3p_{1/2}$	Ru ⁰	16806
$RuO_x 3p_{3/2} + RuO_x 3p_{1/2}$	RuO _x	6775
	Ru ⁰ / RuO _x	2.48
	${Ru^{0}/(Ru^{0}+RuO_{x})} \times 100$	71.26%

Table S3

Ratio of Ru^0/RuO_x calculated using high-resolution Ru 3p XPS spectrum of Ru(3%)/N-HZSM-5- spent.

Peaks	Binding energy	Area
Ru ⁰ 3p _{3/2}	462.18 eV	10788
$Ru^0 3p_{1/2}$	484.16 eV	3969
RuO _x 3p _{3/2}	466.48 eV	3978
RuO _x 3p _{1/2}	486.78 eV	1558
$Ru^0 3p_{3/2} + Ru^0 3p_{1/2}$	Ru ⁰	14766
$RuO_x 3p_{3/2} + RuO_x 3p_{1/2}$	RuO _x	5536
	Ru ⁰ / RuO _x	2.66
	$\{Ru^{0}/(Ru^{0}+RuO_{x})\}\times 100$	72.73%

Table S4

The acidity measurements determined from NH₃-TPD.

S.	Catalyst	Acidity (µmol g ⁻¹) ^a					
N.	Catalyst	Weak	Medium	Strong	Total		
1	HZSM-5	40.2	9.0	-	49.2		
2	Ru(3%)/HZSM-5	40.5	14.6	-	55.1		
3	SBA-15	-	-	-	-		
4	Ru(3%)/SBA-15	6.6	26.9	-	33.5		

^aCalculated by the NH₃-TPD analysis.

Table S5

Catalytic reaction data for the control reactions and analysis of the products yield.

S. N.	Catalyst	Con. (%)	Product Yield (%)						HYD yield (%)	Aromatic yield (%)
			BEZ	CHE	PHE	СНО	CHL	CPE		
1	Ru(3%)/N -HZSM-5	50.9 ^a	6.2	14.7	8.7	4.3	16.7	0.3	36.0	14.9
2	Ru(3%)/N -HZSM-5	41.5 ^b	2.3	14.9	2.6	4.2	17.6	0.2	36.9	4.9
3	Ru(3%)/N -HZSM-5	56 ^c	7.9	18.1	9.0	1.5	19.3	0.1	39.0	16.9
4	Ru(3%)/N -HZSM-5	100 ^d	-	49.9	-	-	49.8	0.3	100	-
5	Ru(3%)/H ZSM-5	80 ^d	9.1	26.5	11.3	4.6	28.2	0.3	59.6	20.4

^aReaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (150 °C), time (3 h), and N_2 (1 MPa).

^bReaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 °C), time (1 h), and N₂ (1 MPa).

^cReaction conditions: DPE (1 mmol), dodecane (10 mL), catalyst (100 mg), temperature (170 $^{\circ}$ C), time (3 h), and H₂ (1 MPa).

^dReaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 $^{\circ}$ C), time (3 h), and N₂ (1 MPa).

S. N.	Substrate	Conversion (%) ^a	Product (yield (%))
1	Benzene ^b	100	Cyclohexane (100)
2	Phenol ^b	100	Cyclohexane (2.8), Cyclohexanol (97.2)
3	Toluene ^c	<2	Methylcyclohexane (100)
4	Ethylbenzene ^c	22.3	Ethylcyclohexane (100)

Table S6 Controlled CTH reactions with different substrates.

^aReaction conditions: Substrate (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 $^{\circ}$ C), and N₂ (1 MPa).

^bTime 2 h.

^cTime 3 h.

Table S7 Comparative catalytic activity for the CTH of DPE with the reported catalysts.

Ent ry	Catalyst	H-Donor	Reaction conditions (Temperature/T ime/Pressure))	DPE Conv. (%)	Product Sele. (%)		Yield (%)		Ref.
					HYD	Aromatic	HYD	Aromatic	
			00.00/101/	100	Sele.	Sele.	Yield	Yield	G 0
1	RANEY Ni	2- propanol	80 °C/12 h/-	100	52	48	-	-	S9
2	Ni/Al ₂ O ₃ -650	2-	150 °C/5 h/1	100	-	-	100	100	S10
	C	propanoi	MPa(IN ₂)						
3	20% Ni/CNT	2- propanol	240 °C/2/-	100	-	-	CHE (88) CHL (82)	-	S11
4	Pt/C	ethanol– water- mixture	300 °C/12h/0.1 MPa (N ₂)	100	-	100	-	-	S12
5	Ru/hydroxya patite	2- propanol	150 °C/10 h/-	100	-	-	73.7	26.3	S13
6	Au ₁ Pd ₁ /CeO ₂	НСООН	180 °C/ 24 h/-	100	-	100	-	-	S14
7	Ru(3%)/N- HZSM-5	2- propanol	170 °C/ 3h/1 MPa (N ₂)	100	100	-	100	-	This work

Table S8

Ru contents in Ru(3%)/N-HZSM-5 catalyst.

Catalyst	Ru metal loading weight (%)
Ru(3%)/N-HZSM-5	2.94
Ru(3%)/N-HZSM-5-spent ^a	2.92

^aRu content after five recycling experiment.



Fig. S1 Calibration plots of (a) diphenyl ether, (b) cyclohexane, and (c) cyclohexanol.



Fig. S2 PXRD patterns of the (a) HZSM-5 and Ru(3%)/HZSM-5, (b) SBA-15 and Ru(3%)/SBA-15.



Fig. S3 FT-IR spectra of the HZSM-5 and SBA-15.



Fig. S4 SEM images of the (a, b) N-HZSM-5, and (c, d) Ru(3%)/N-HZSM-5.



Fig. S5 (a) TEM image and (b) size distribution of Ru NPs in Ru(3%)/N-HZSM-5.



Fig. S6 EDAX spectrum of Ru(3%)/N-HZSM-5 catalyst.



Fig. S7 FT-IR spectra of N-HZSM-5 support, Py-IR spectra of N-HZSM-5 and Ru(3%)/N-HZSM-5 catalyst.



Fig. S8 H₂-TPR profiles of (a) Ru(x%)/N-HZSM-5 (where x = 1, 3, 5) and (b) Ru(3%)/HZSM-5 catalyst.



Fig. S9 GC-MS chromatogram of CTH of DPE after 3 h (at 100% conversion) (Reaction conditions: DPE (1 mmol), Ru(3%)/N-HZSM-5 (100 mg), IPA (10 mL), N_2 (10 bar), Temperature (170 °C), Time (3 h) internal standard (n-dodecane).



Fig. S10 (a) Influence of N₂-pressure [Reaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 °C), and time (3 h)] and (b) solvent [Reaction conditions: DPE (1 mmol), solvent (10 mL), catalyst (100 mg), temperature (170 °C), time (3 h), and N₂ (1 MPa)] in the CTH of DPE over Ru(3%)/N-HZSM-5.



Fig. S11 Kinetic plots for the CTH of DPE (a) relationship between DPE conversion and reaction time, (b) relationship between $-\ln(1-x)$ and reaction time, and (c) relationship between ln k and 1/Temperature (1/T). [Reaction condition: DPE (1 mmol), Ru(3%)/N-HZSM-5 (100 mg), IPA (10 mL), N₂ (10 bar)]



Fig. S12 Kinetic plots for the CTH of DPE (a) relationship between DPE conversion and reaction time, (b) relationship between $-\ln(1-x)$ and reaction time, and (c) relationship between ln k and 1/Temperature (1/T). [Reaction condition: DPE (1 mmol), Ru(1%)/N-HZSM-5 (100 mg), IPA (10 mL), N₂ (10 bar)]



Fig. S13 Kinetic plots for the CTH of DPE (a) relationship between DPE conversion and reaction time, (b) relationship between $-\ln(1-x)$ and reaction time, and (c) relationship between ln k and 1/Temperature (1/T). [Reaction condition: DPE (1 mmol), Ru(3%)/HZSM-5 (100 mg), IPA (10 mL), N₂ (10 bar)]



Fig. 14 Thermograms of the fresh and spent Ru(3%)/N-HZSM-5 catalyst.





Fig. S15 SEM images (a, b, and c) of the Ru(3%)/N-HZSM-5-spent.



Fig. S16 (a) TEM images, (b, c, d and e) HR-TEM images at different magnifications (illustrating the Ru (101) lattice fringes), (f) the region selected for elemental mapping, and elemental mapping for (g) combined Ru, Al, Si, O, (h) Si, (i) Al, (j) O (k) Ru elements in the Ru(3%)/N-HZSM-5-spent.



Fig. S17 (a) TEM image and (b) Ru NPs size distribution of the Ru(3%)/N-HZSM-5-spent catalyst.



Fig. S18 EDAX spectrum of the Ru(3%)/N-HZSM-5-spent catalyst.



Fig. S19 GC-TCD chromatogram showing the gas phase GC chromatogram from the IPA mediated CTH of DPE. Reaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 °C), time (3 h) and N₂ (1 MPa). GC instrument information: The reaction mixture was analyzed by gas chromatography (GC) (Shimadzu 2010 Plus; SH-Rt®-Q-BOND; capillary column: SH; $30m \times 0.32mm$ ID $\times 10\mu m$ df) equipped with thermal conductivity detector (TCD) detector. Oven Temperature: 36 °C (hold 6 min), Nitrogen, Constant Flow @ 1.20 mL/min.



Fig. S20 (a) Calibration data for the assessment of the acetone formation during the catalytic process, (b) GC-FID chromatogram showing the liquid phase from the IPA mediated CTH of DPE. Reaction conditions: DPE (1 mmol), IPA (10 mL), catalyst (100 mg), temperature (170 °C), time (3 h) and N₂ (1 MPa). GC instrument information: The reaction mixture was analyzed by gas chromatography (GC) (Shimadzu 2010 Plus; Rxi-624 Sil MS; capillary column: Restek; $30m \times 0.32mm$ ID $\times 1.8\mu m$ df) equipped with flame ionization (FID) detector. Oven Temperature: 35 °C (hold 13 min) to 225 °C @ 30 °C/min (hold 7 min), Nitrogen, Constant Flow @ 0.80 mL/min.



Fig. S21 (a) ¹H NMR spectra recorded before reaction, (b) ¹H NMR spectra recorded after reaction demonstrating the acetone formation.



Fig. S22. (a) the IPA and DPE conversion and products selectivity during the course of the reaction. (b) Gas chromatogram (TCD) of gaseous phase in the CTH of DPE during the course of reaction (Shimadzu 2010 Plus; SH-Rt®-Q-BOND; capillary column: SH; $30m \times 0.32mm$ ID × 10µm df).



Fig. S23 Poisoning test with pyridine in the CTH of DPE over Ru(3%)/N-HZSM-5.



Fig. S24 GC-MS chromatogram of CTH of phenol after 1 h (at 60% conversion) [Reaction conditions: phenol (1 mmol), Ru(3%)/N-HZSM-5 (100 mg), IPA (10 mL), N_2 (10 bar), Temperature (170 °C), Time (1 h)].



Scheme S1 Proposed mechanism for the CTH of DPE over Ru(3%)/SBA-15.

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