

Supplementary Information for the Effect of pore size on the process of CO₂ adsorption in MIL-101, MOF-177, and UiO-66

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S1 MOF Characterization

S1.1 X-Ray Diffraction Images

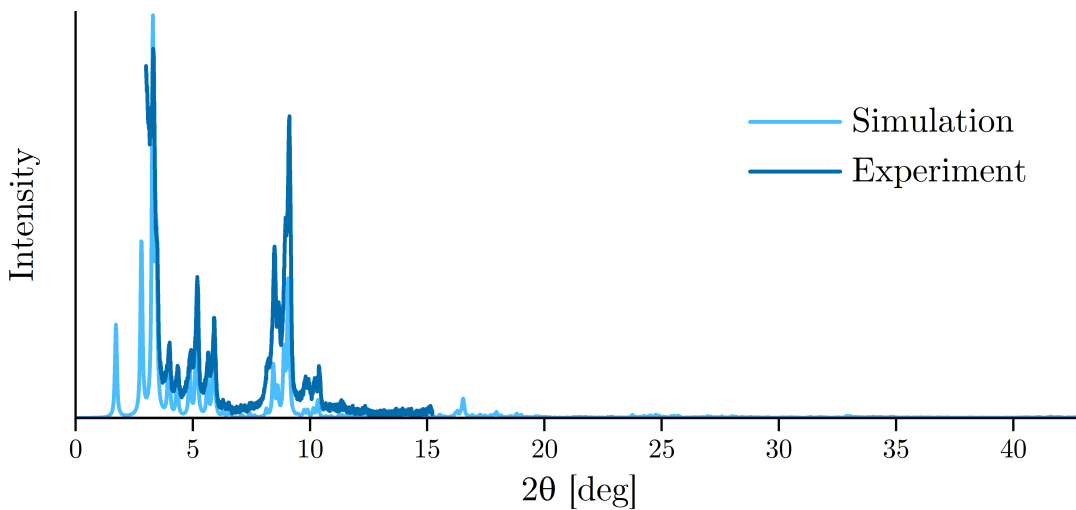


Figure S1: X-Ray diffraction data for the MIL-101 sample.

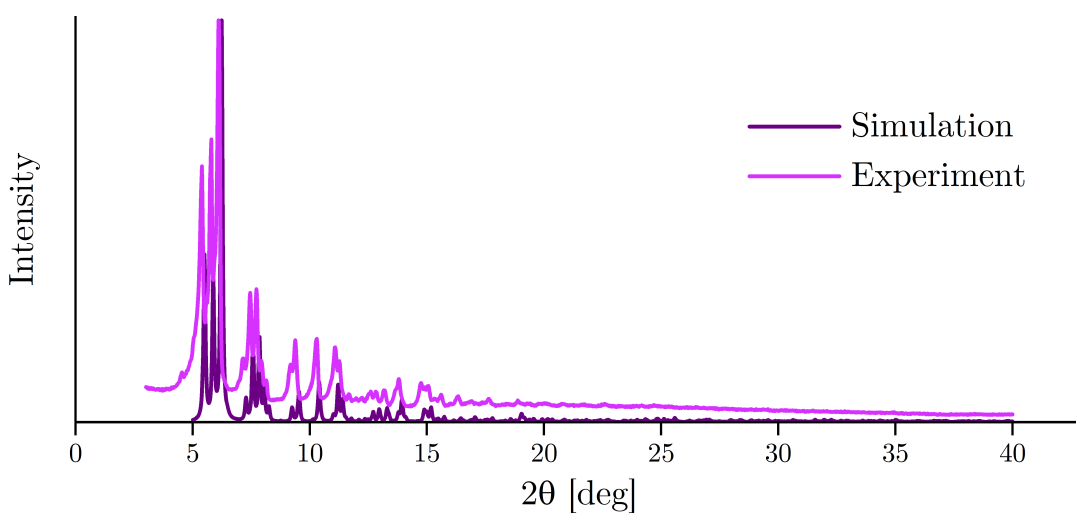


Figure S2: X-Ray diffraction data for the MOF-177 sample.

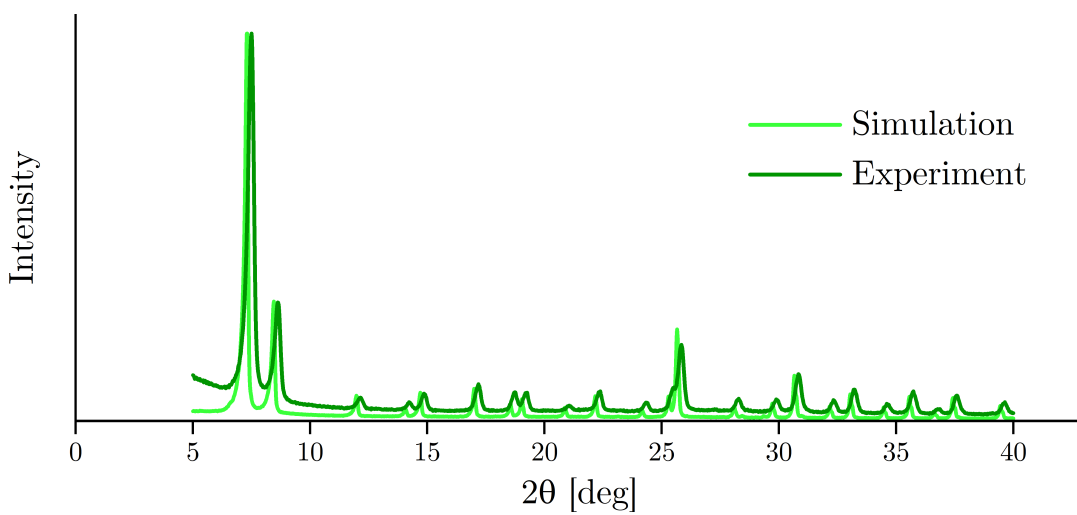


Figure S3: X-Ray diffraction data for the UiO-66 sample.

S1.2 Nitrogen Adsorption Isotherm

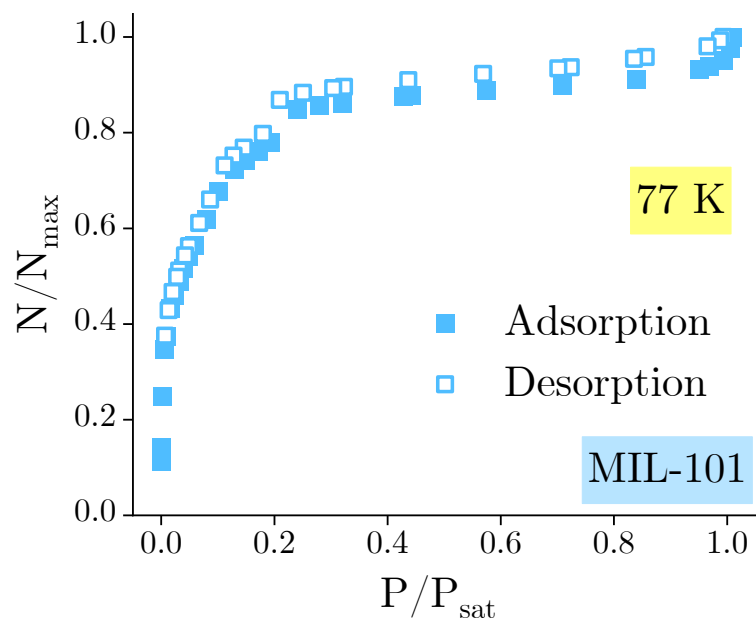


Figure S4: Nitrogen adsorption-desorption isotherm at 77 K for MIL-101.

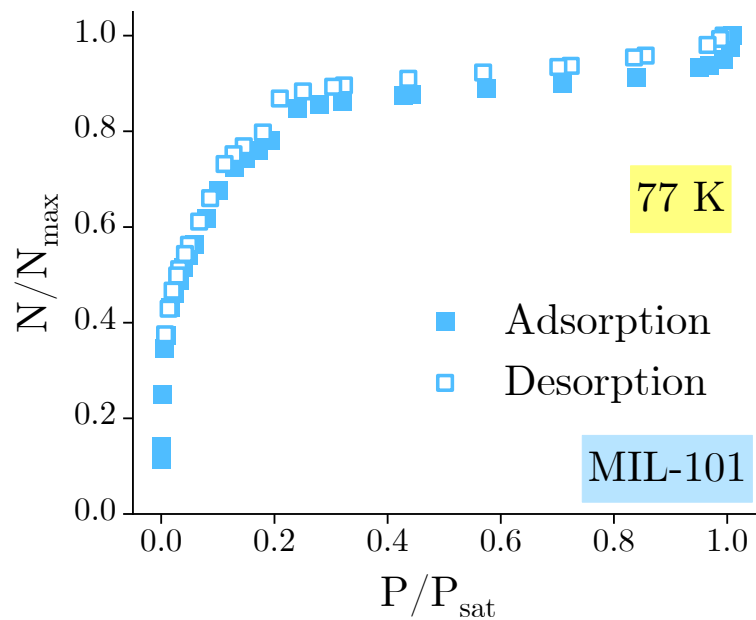


Figure S5: Nitrogen adsorption-desorption isotherm at 77 K for MOF-177.

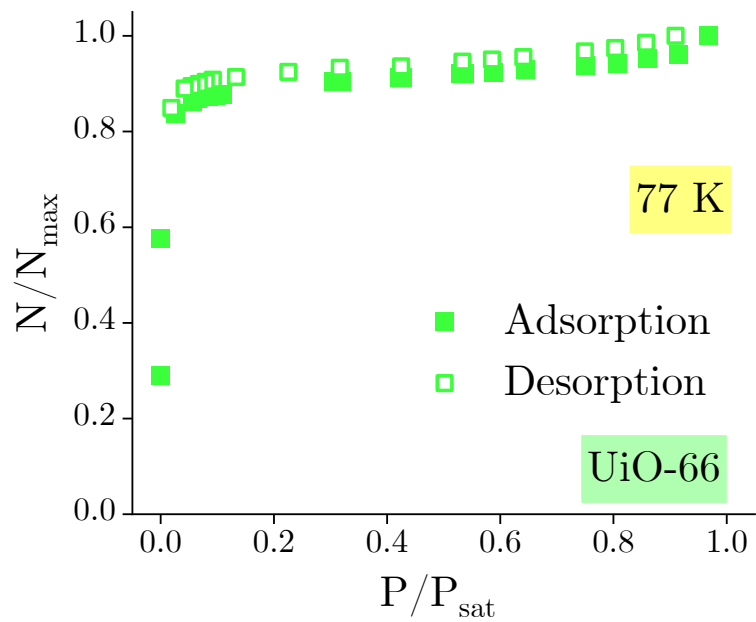


Figure S6: Nitrogen adsorption-desorption isotherm at 77 K for UiO-66.

S2 Enthalpy of Adsorption

Heat flow curves were obtained from the Calvet-type calorimeter (Microcalvet Ultra, Setaram) for the adsorption and desorption processes. The enthalpy of adsorption is calculated by integrating the heat flow curves for each pressure step.

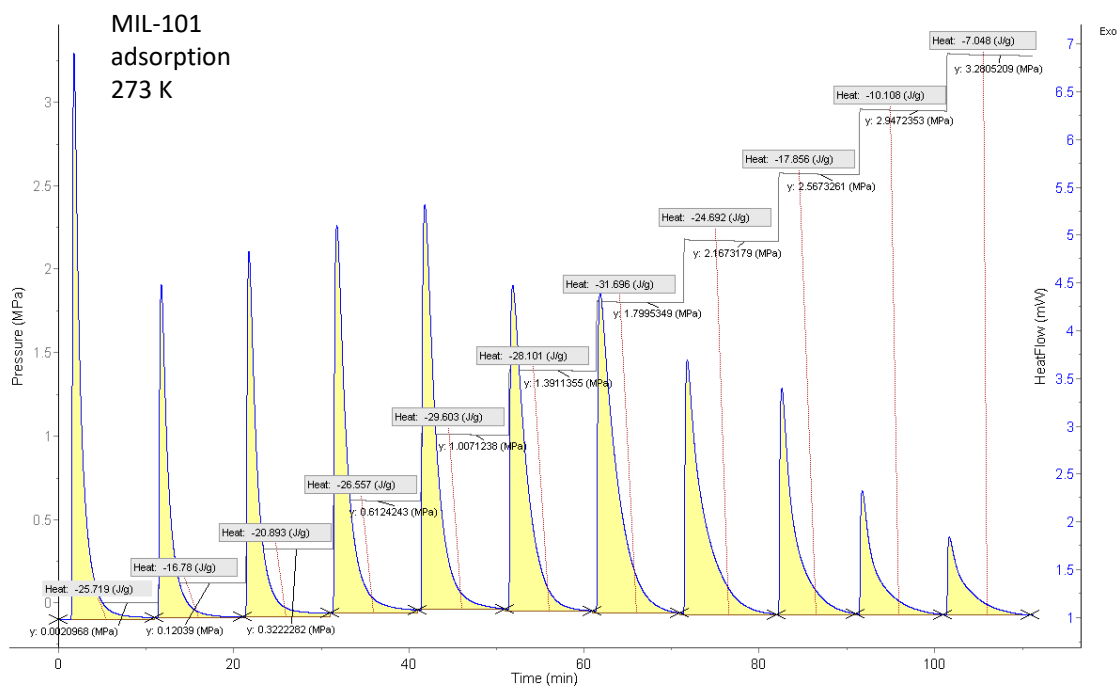


Figure S7: MIL-101 heat flow curve at 273 K during the adsorption process.

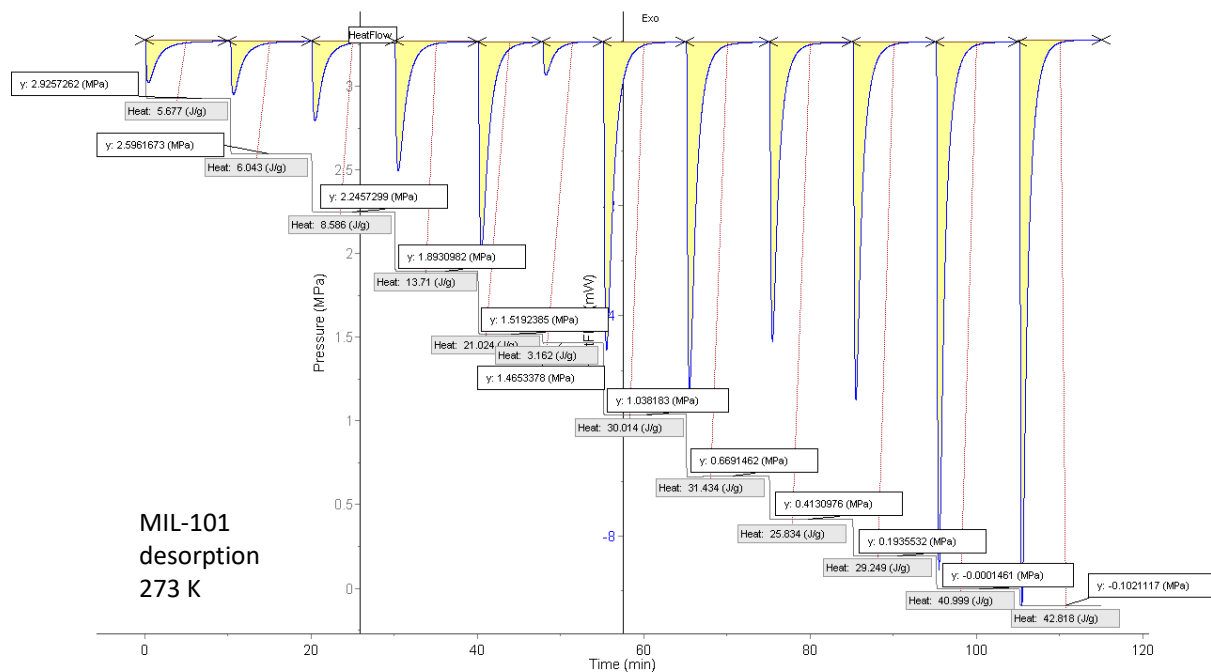


Figure S8: MIL-101 heat flow curve at 273 K during the desorption process.

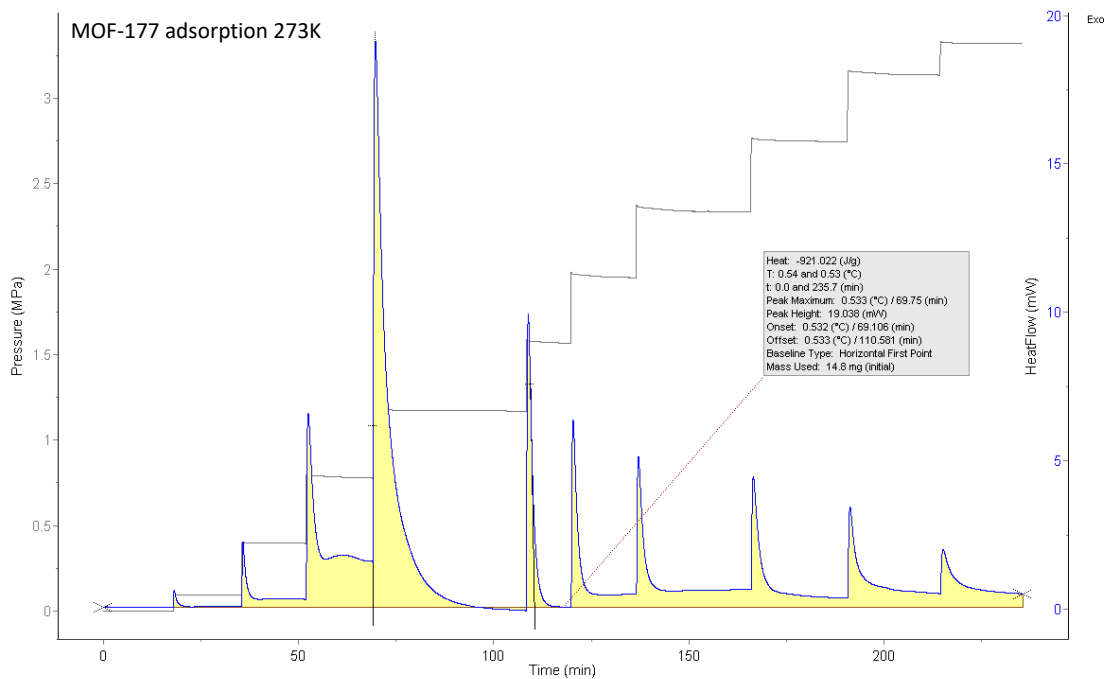


Figure S9: MOF-177 heat flow curve at 273 K during the adsorption process.

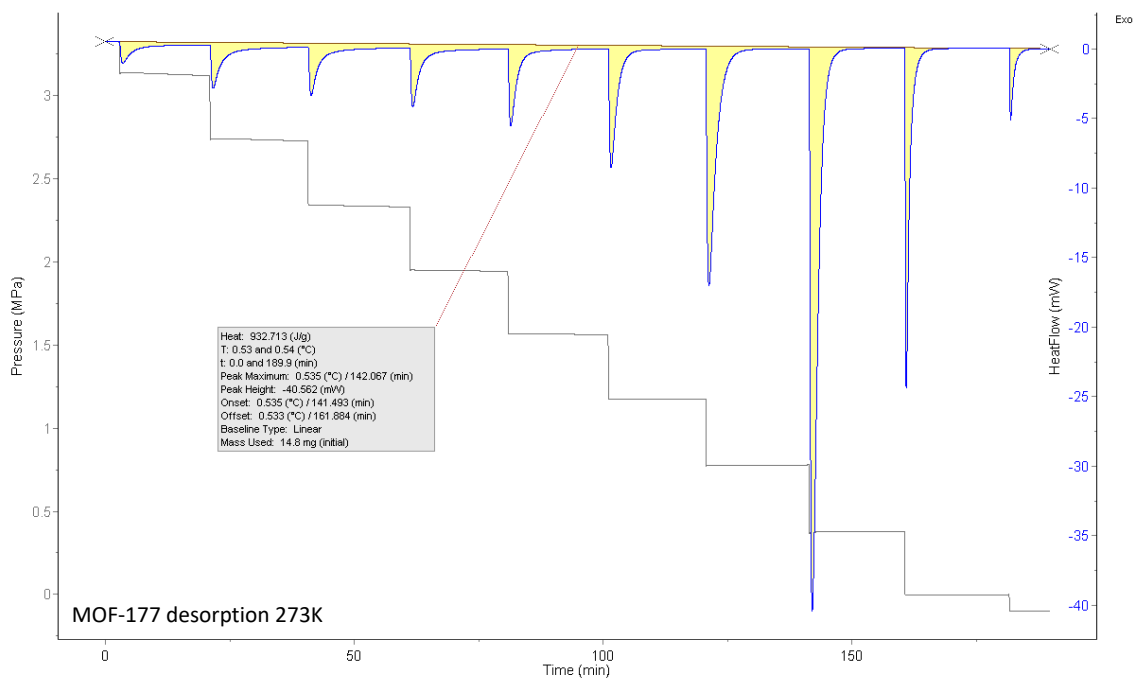


Figure S10: MOF-177 heat flow curve at 273 K during the desorption process.

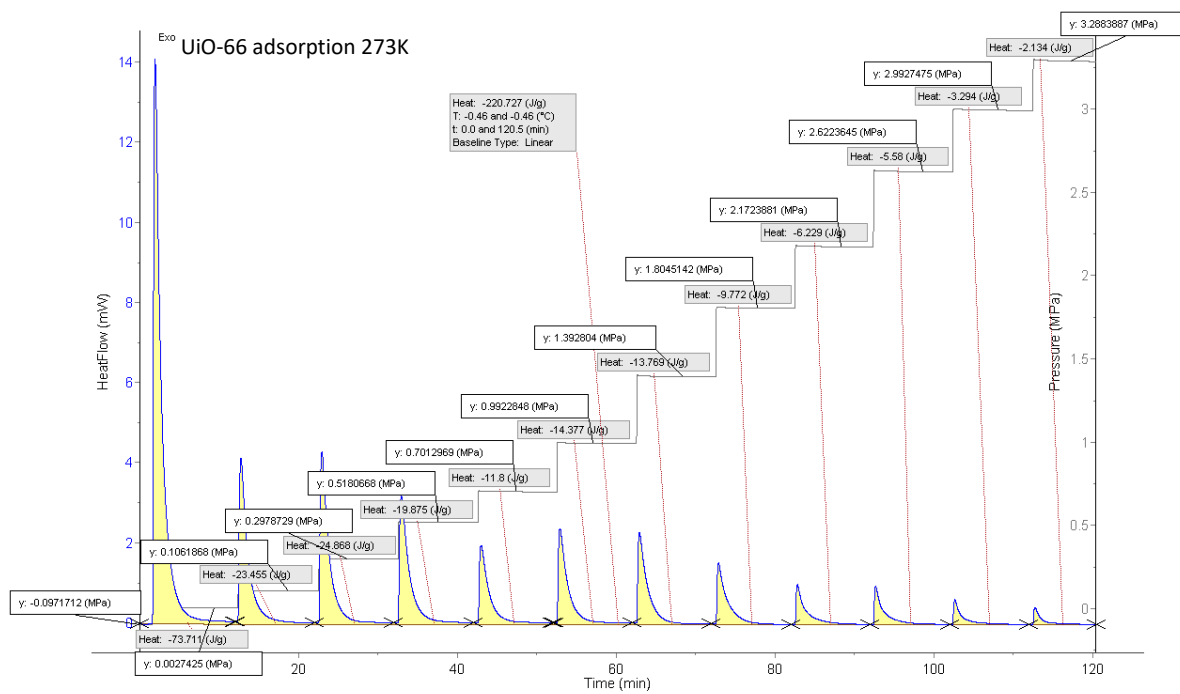


Figure S11: UiO-66 heat flow curve at 273 K during the adsorption process.

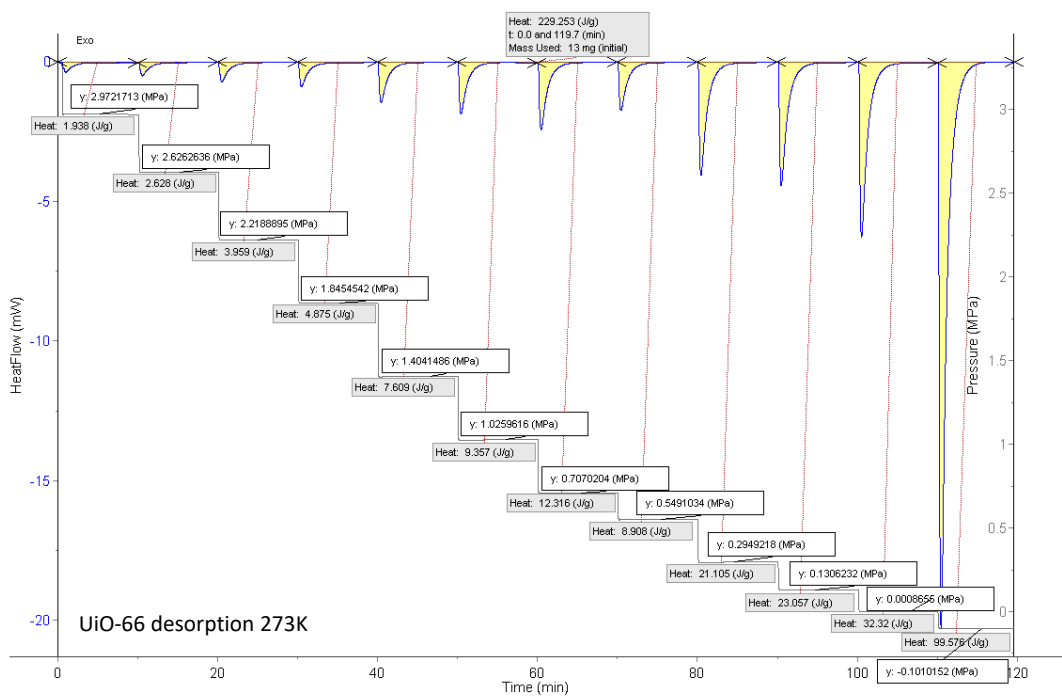


Figure S12: UiO-66 heat flow curve at 273 K during the desorption process.

S3 Grand Canonical Monte Carlo Simulation

The Lennard–Jones parameters and the grand canonical Monte Carlo (GCMC) formulation used in the simulation are given in this section.¹

S3.1 GCMC Scheme

$$U_{\text{VDW}} = 4\epsilon_{ij} \left[\left(\frac{\sigma_{ij}}{r_{ij}} \right)^{12} - \left(\frac{\sigma_{ij}}{r_{ij}} \right)^6 \right] \quad (1)$$

The mixing potential parameters are calculated using the Lorentz–Berthelot rules:

$$\epsilon_{ij} = \sqrt{\epsilon_i \epsilon_j}; \quad \sigma_{ij} = \frac{1}{2}(\sigma_i + \sigma_j) \quad (2)$$

The Coulombic interactions between charged particles are modeled using the Ewald method:

$$U_c = U^{\text{real}} + U^{\text{rec}} \quad (3)$$

where the two components of the Coulombic potential U^{real} and U^{rec} are expressed as:

$$U^{\text{real}} = \sum_{i < j} q_i q_j \frac{\text{erfc}(\alpha r_{ij})}{r_{ij}} \quad (4)$$

$$U^{\text{rec}} = \frac{2\pi}{V} \sum_{\mathbf{k} \neq 0} \frac{1}{k^2} e^{-\frac{k^2}{4\alpha^2}} \left(\left| \sum_{i=1}^N q_i \cos(\mathbf{k} \cdot \mathbf{r}_i) \right|^2 + \left| \sum_{i=1}^N q_i \sin(\mathbf{k} \cdot \mathbf{r}_i) \right|^2 \right) - \sum_i \frac{\alpha}{\sqrt{\pi}} q_i^2 \quad (5)$$

S3.2 L–J Parameters and CO₂ Model

Table T1: Lennard–Jones parameters for the MOFs¹

MOF	Element	L–J Parameters	
		ϵ [K]	σ [Å]
UiO-66	Zr	34.7221	2.7832
	O	48.1581	3.0332
	C	47.8562	3.4730
	H	7.6489	2.8464
MOF-177	Zn	62.3992	2.4616
	O	48.1581	3.0332
	C	47.8562	3.4730
	H	7.6489	2.8464
MIL-101	Cr	7.5483	2.6932
	O	48.1581	3.0332
	C	47.8562	3.4730
	F	36.4834	3.0932
	H	7.6489	2.8464

Table T2: TraPPE model parameters for CO₂²

Atom	Type	ϵ [K]	σ [Å]	q [e]
C	O=[C]=O	27.0	2.80	0.70
O	[O]=C=O	79.0	3.05	-0.35
O	O=C=[O]	79.0	3.05	-0.35

Table T3: Bond lengths for CO₂ according to TraPPE model²

Stretch	Type	Length [Å]
1–2	(O=C)=O	1.16
2–3	O=(C=O)	1.16

Table T4: Bond angles for CO₂ according to TraPPE model²

Bend	Type	θ [deg]
2-1-3	O=C=O	180

S3.3 Simulation and Experimental Results

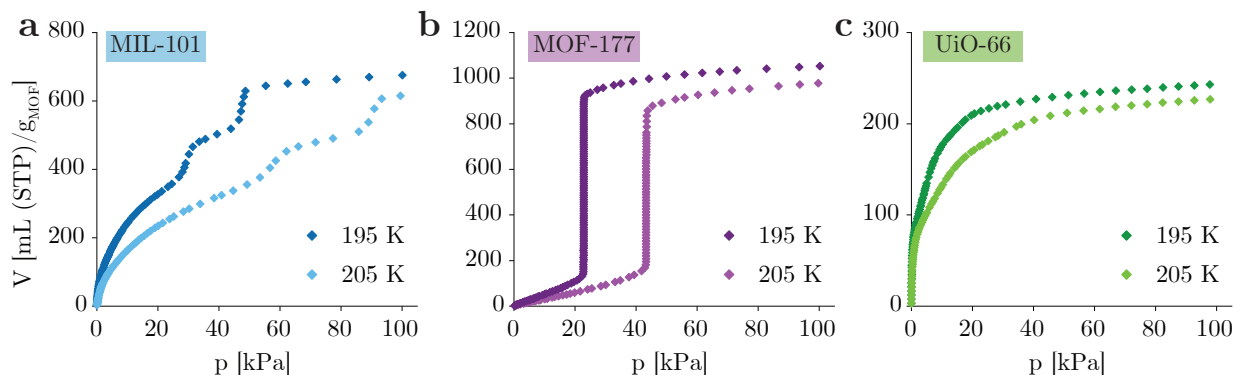


Figure S13: Experimental adsorption isotherms at 195 K and 205 K.

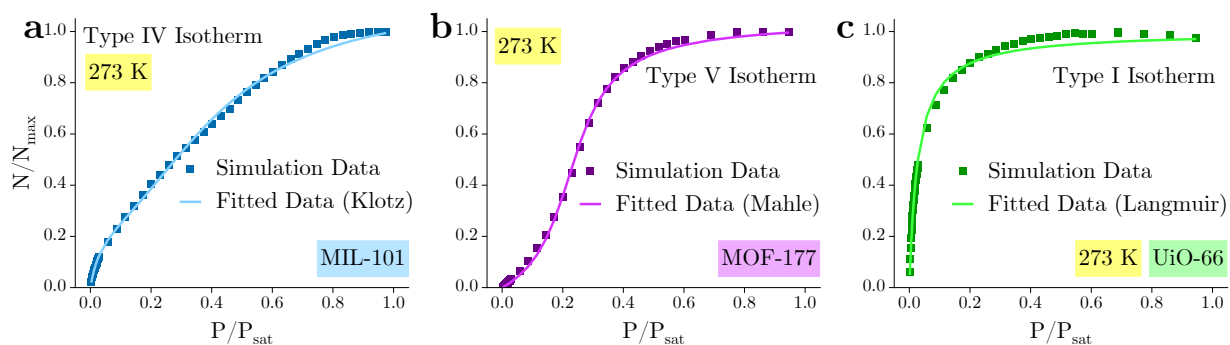


Figure S14: Adsorption isotherm obtained from the GCMC simulations at 273 K. The fitting parameters for each isotherm are listed in a later section.

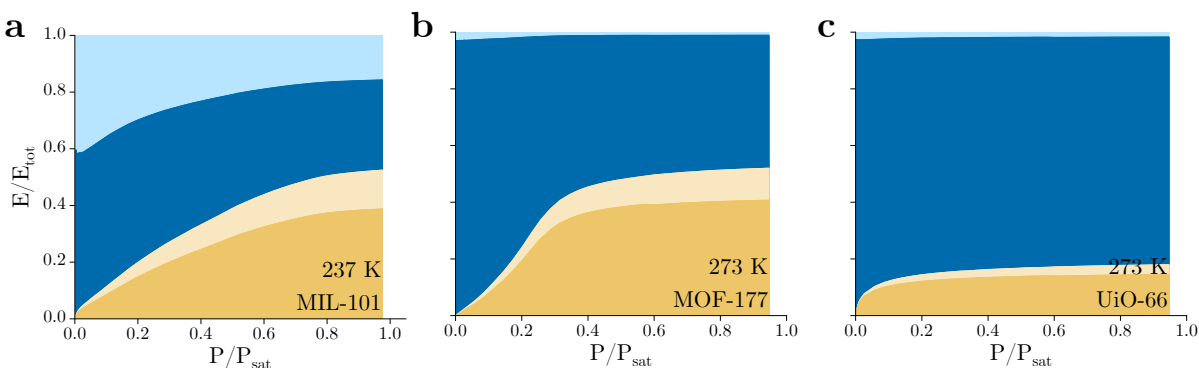


Figure S15: Interaction energy budget obtained from the GCMC simulations at 273 K.

S3.4 Pore-filling Process

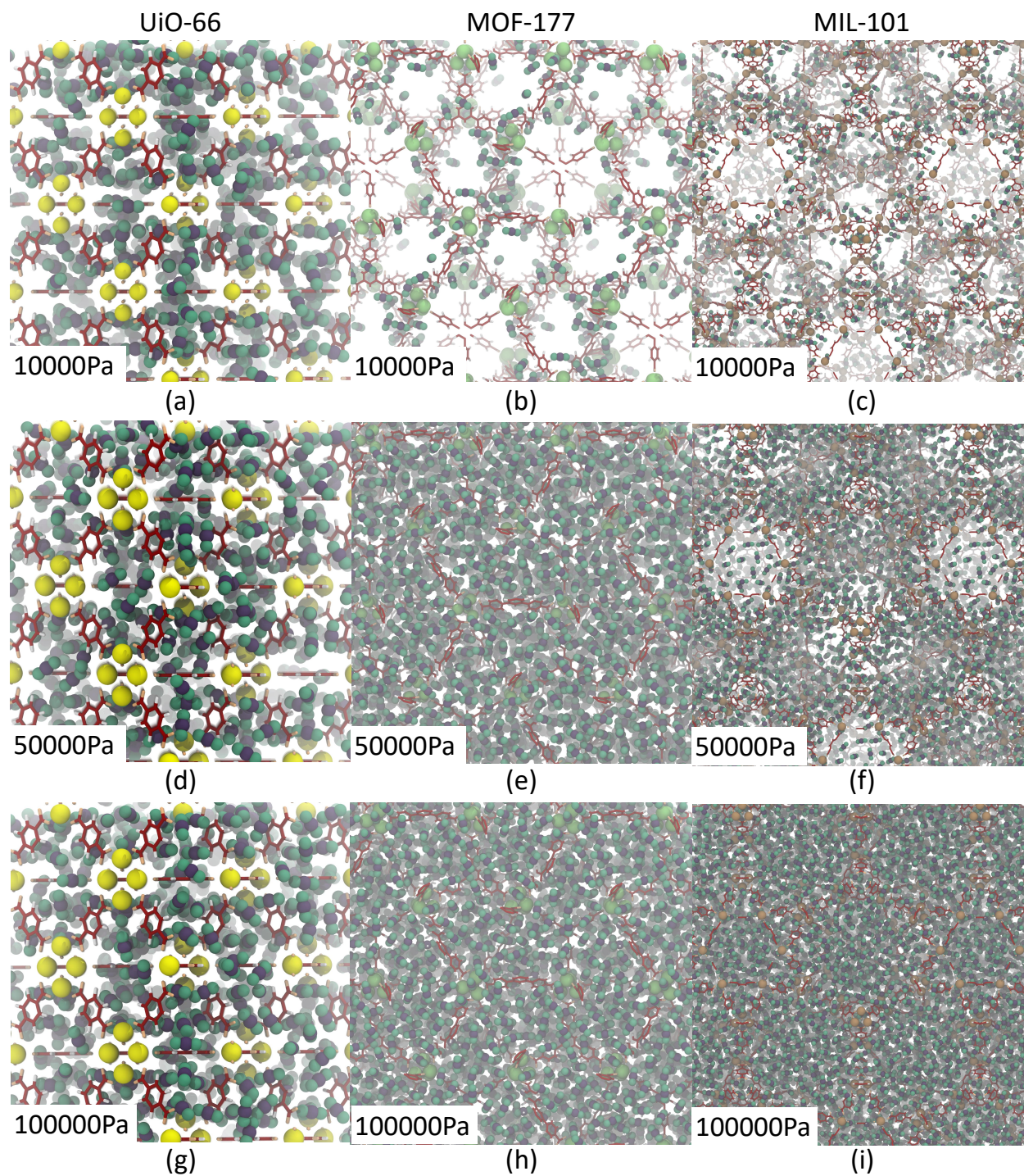


Figure S16: Pore-filling process.

S3.5 Isotherm Fitting

The type IV isotherms are modeled using Klotz theory,^{3,4} as given by

$$\frac{N}{N_{max}} = \frac{Cq(1 - (1 + m)q^m + mq^{m+1})}{(1 - q)(1 + (C - 1)q - Cq^{m+1})} \quad (6)$$

where,

$$q = \frac{Kp}{p_{sat}} = KP^* \quad (7)$$

The m , C , and K are the fitting parameters valued at 4.8192 ± 0.16159 , 13.0442 ± 1.61476 , and 2.3236 ± 0.05718 , respectively, with an R-square value of 0.99787.

The isotherm is modeled using a form given by Mahle⁵ as

$$\frac{N}{N_{max}} = \frac{1}{D} \left(\tan^{-1} \left(\frac{P^* - A}{B} \right) - \tan^{-1} \left(\frac{-A}{B} \right) \right) \quad (8)$$

where D is,

$$D = \tan^{-1} \left(\frac{1 - A}{B} \right) - \tan^{-1} \left(\frac{-A}{B} \right) \quad (9)$$

The fitting parameters in Eq. 8 are $A = 0.22275 \pm 0.00199$ and $B = -0.10738 \pm 0.00294$ with an R-square value of 0.99904. The Type I adsorption mechanism can be modeled using single-site Langmuir theory as

$$\frac{N}{N_{max}} = \frac{bP^*}{1 + bP^*} \quad (10)$$

The fitting parameter is $b = 35.24596 \pm 0.84979$, with an R-square value of 0.99382.

S4 UiO-n Family

As discussed in the main manuscript, to eliminate the effect of coulombic interaction we perform a similar analysis on the MOFs UiO-66, UiO-67, and UiO-68. The obtained results are plotted in this section. The adsorption isotherms change from Type I to Type V as

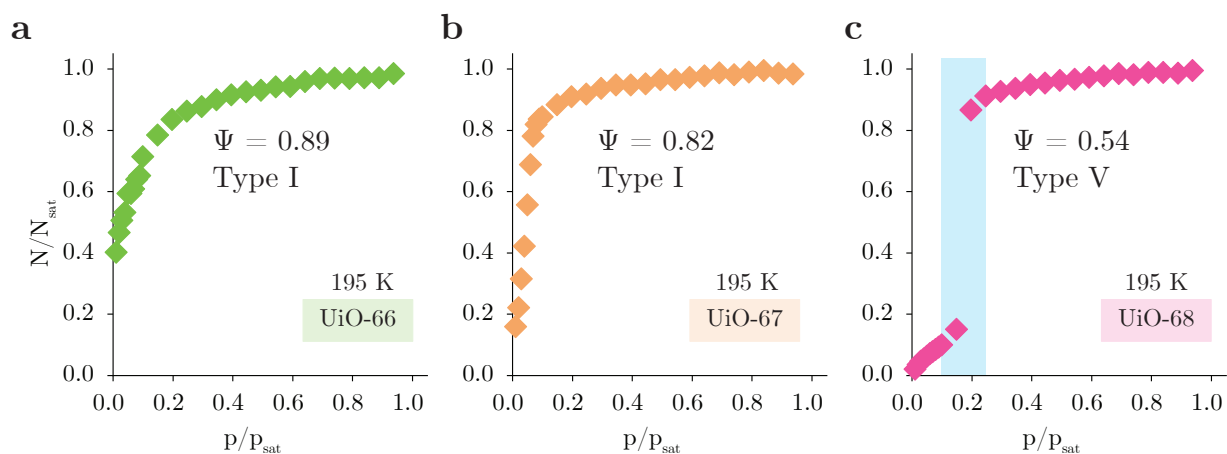


Figure S17: **CO₂ adsorption isotherms for the UiO-family at 195 K**

a UiO-66: Type I adsorption isotherm, **b** UiO-67: Type I adsorption isotherm, **c** UiO-68: Type V adsorption isotherm

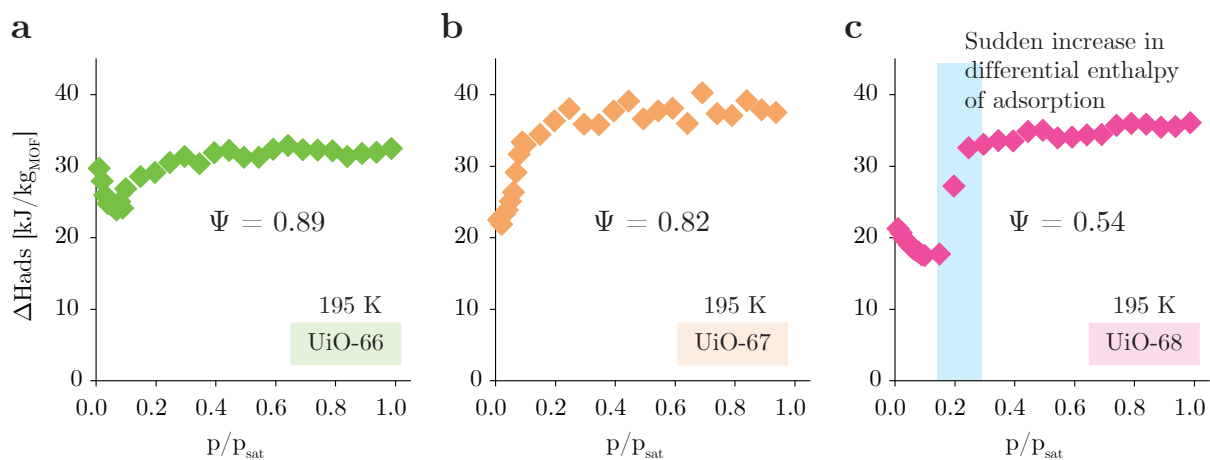


Figure S18: **Differential enthalpy of adsorption as a function of relative pressure**
a UiO-66, **b** UiO-67, **c** UiO-68

the pore size is increased. UiO-66 with a 6 Å pore has a type I adsorption isotherm (Fig. S17a), UiO-67 with a 9 Å pore has a type I adsorption isotherm (Fig. S17b), and finally

UiO-68 with a 15 Å pore has a Type V adsorption isotherm (Fig. S17c). This shows the capillary condensation of CO₂ does not take place in the case of UiO-66 and UiO-67 (the gradual increase in the number density of the adsorbate). Whereas in the case of UiO-68, an abrupt increase is seen (see the blue shaded region in Fig. S17c), which corresponds to capillary condensation.⁶ Similar trends can be observed from the differential enthalpy of adsorption as a function of relative pressure (see Fig. S18). The energy budget for the UiO-

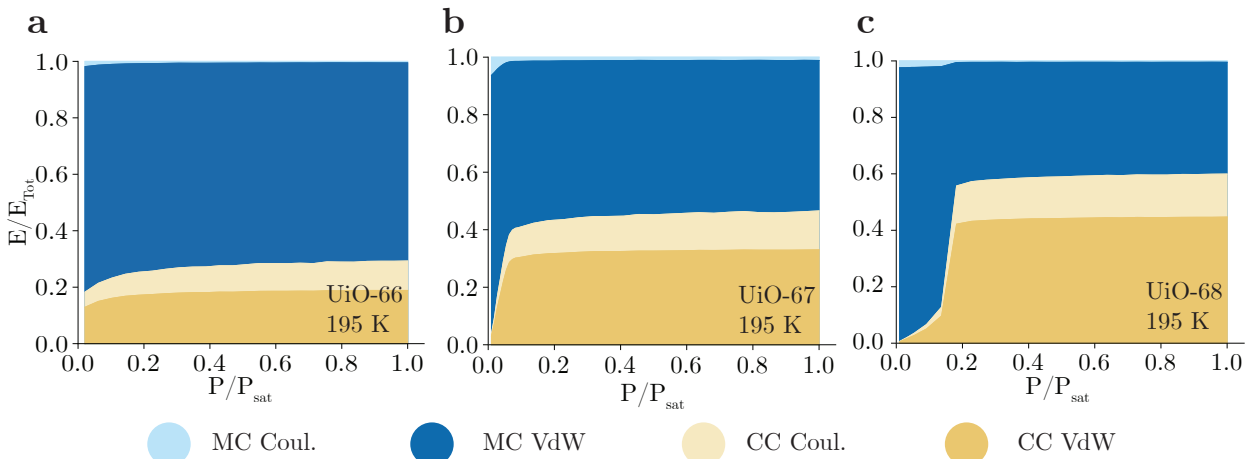


Figure S19: **Interaction energy budget for UiO-family**
a UiO-66, **b** UiO-67, **c** UiO-68

family is shown in Fig. S19. In all three cases, the MC coulombic interaction is infinitesimal. The contributions of inter-molecular interactions increase with increasing pore diameter, suggesting a higher number of molecules are adsorbed. Additionally, the ratio of MC - CC interactions increases drastically in the UiO-68 case around $p/p_0 \approx 0.2$ suggesting phase change inside the pore (capillary condensation). Finally, in Fig. S20, radial distribution functions are shown at different relative pressures. Fig. S20a, S20b, and S20c show the distribution of CO₂ around the central metal atom (Zr) in each case. For UiO-66, the center of the pore is the primary adsorption site as discussed in the main manuscript. Whereas in the case of UiO-67 and UiO-68 the primary adsorption site is near the metal atom at low pressure and shifts towards the center of the pore as the pressure increases. Fig. S20d, S20e, and S20f show the radial distribution function of the adsorbed CO₂ around adsorbed

CO₂. It is interesting to note that in all three cases, the RDF shows a “solid-like” structure. This might correspond to “capillary freezing” as the bulk CO₂ shows sublimation properties at 195 K. However, further investigation to understand the phase of adsorbed CO₂ inside UiO-family pores is needed.

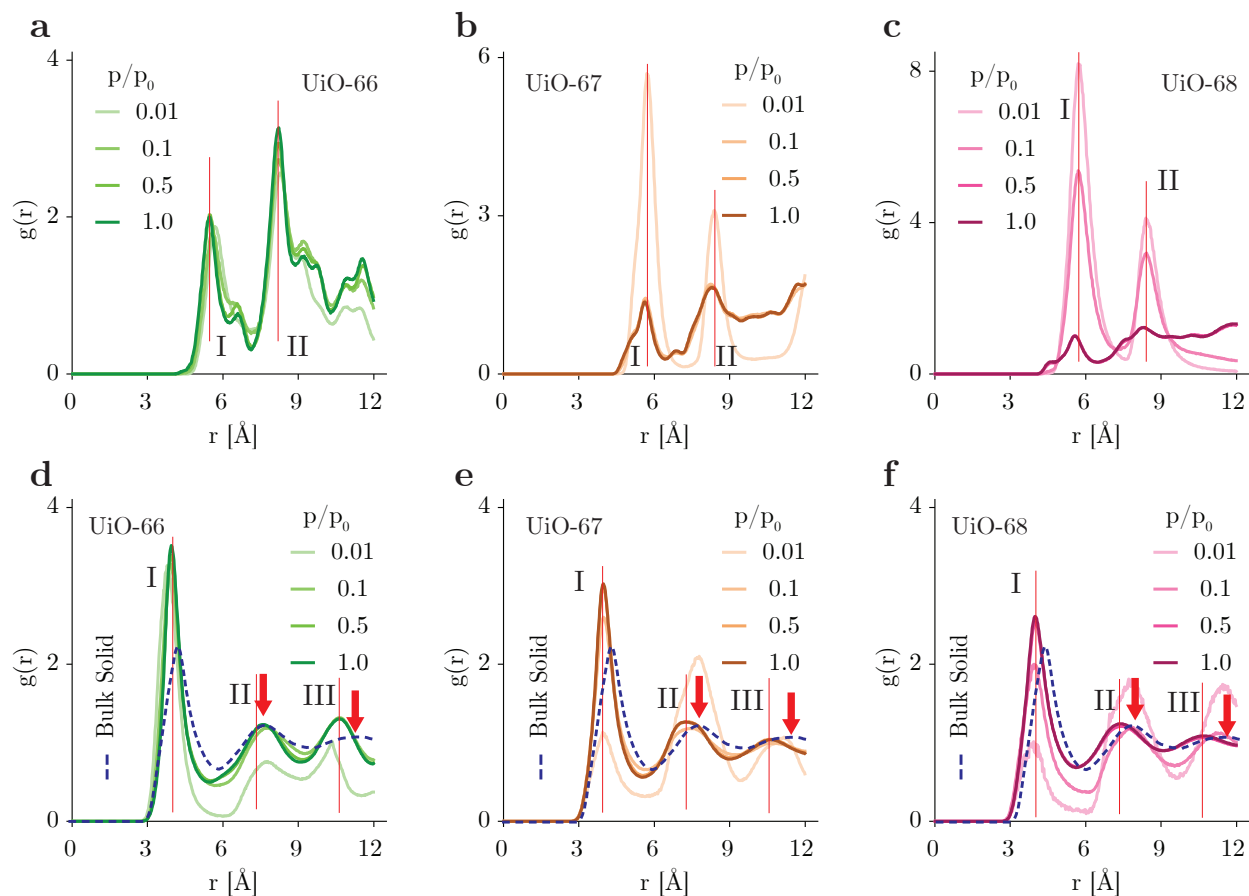


Figure S20: **Radial distribution functions**

RDF of adsorbed CO₂ around the central metal atom Zr in **a** UiO-66, **b** UiO-67, and **c** UiO-68

RDF of CO₂-CO₂ adsorbed in **d** UiO-66, **e** UiO-67, and **f** UiO-68

S5 Additional MOFs

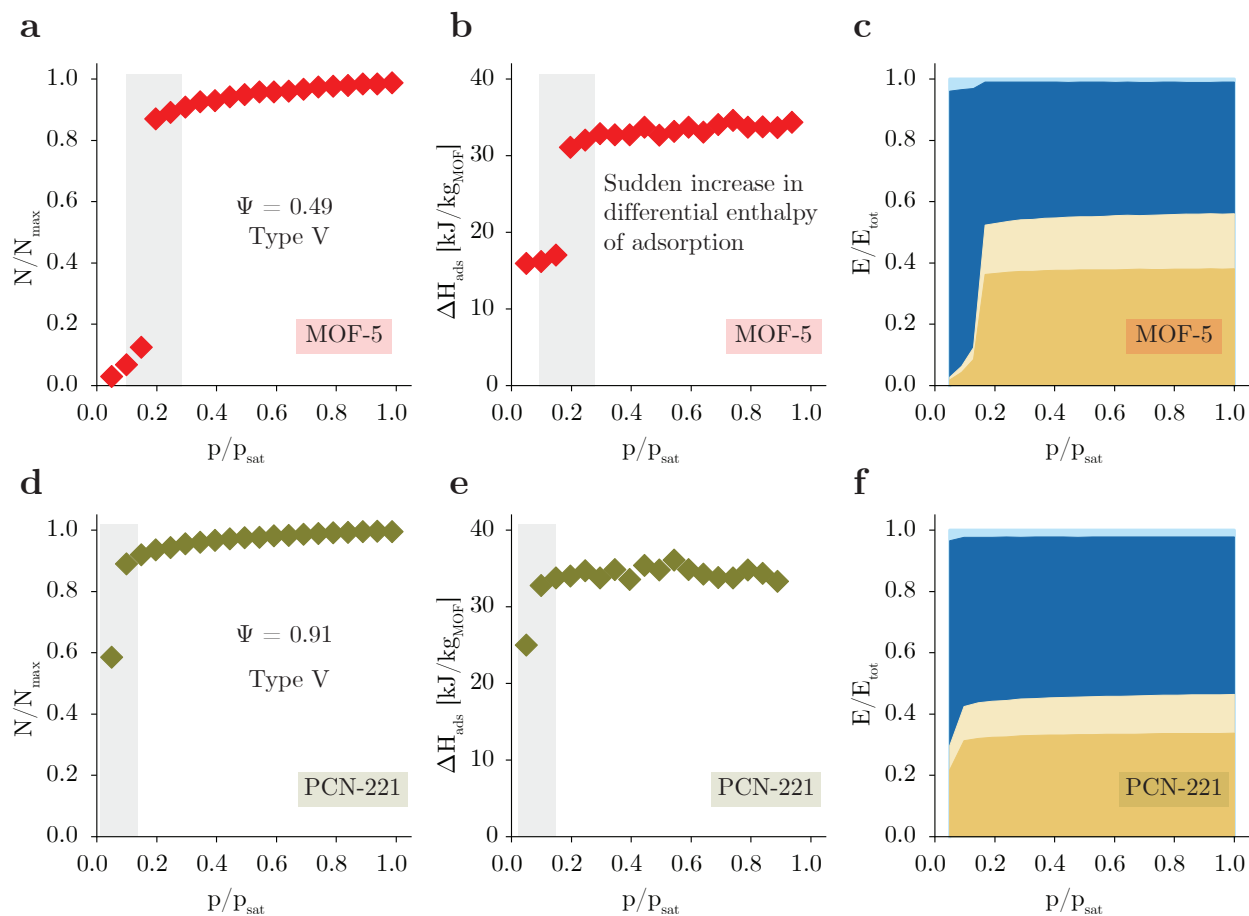


Figure S21: **Additional MOFs studied**

MOF-5: **a** Adsorption isotherm, **b** Differential enthalpy of adsorption, **c** Interaction energy budget

PCN-221: **a** Adsorption isotherm, **b** Differential enthalpy of adsorption, **c** Interaction energy budget

To understand the effect of pore structure on the adsorption characteristics we investigated CO₂ adsorption in MOF-5 which has all the other parameters (central metal atom, pore-size) similar to MOF-177. However, the structures of pores in each case are different. The results obtained are shown in Fig. S21a, Fig. S21b, and Fig. S21c. It can be observed that, despite different pore structures, different central metal atoms, and charge distribution the adsorption isotherms of MOF-177 (see Fig. ??c), UiO-68 (see Fig. S17c), and MOF-5 (see Fig. S21a) are similar to each other, as the confinement parameter for each

all three MOFs lie within 0.4 and 0.6 (see Fig. ??b). This shows the consistency of the one-dimensional model. However, in the case of PCN-221 where there are two metal sites (Cu and Zr), the adsorption isotherm is still type V despite the confinement parameter being greater than Ψ_{crit} ($\Psi = 0.91$) (see Figs. S21d, e, and f)

References

- (1) Rappé, A. K.; Casewit, C. J.; Colwell, K.; Goddard III, W. A.; Skiff, W. M. UFF, a full periodic table force field for molecular mechanics and molecular dynamics simulations. *Journal of the American chemical society* **1992**, *114*, 10024–10035.
- (2) Potoff, J. J.; Siepmann, J. I. Vapor–liquid equilibria of mixtures containing alkanes, carbon dioxide, and nitrogen. *AIChE journal* **2001**, *47*, 1676–1682.
- (3) Klotz, I. M.; Walker, F. M.; Pivan, R. B. The binding of organic ions by proteins1. *Journal of the American Chemical Society* **1946**, *68*, 1486–1490.
- (4) Buttersack, C. Modeling of type IV and V sigmoidal adsorption isotherms. *Physical Chemistry Chemical Physics* **2019**, *21*, 5614–5626.
- (5) Mahle, J. J. An adsorption equilibrium model for Type 5 isotherms. *Carbon* **2002**, *40*, 2753–2759.
- (6) Zsigmondy, R. Über die Struktur des Gels der Kieselsäure. Theorie der Entwässerung. *Zeitschrift für anorganische Chemie* **1911**, *71*, 356–377.