## **Electronic Supplementary Information**

## **Experimental details**

Materials characterization. Powder X-ray diffraction (XRD) tests were carried out on a Rigaku Minflex 600 Advance X-ray instrument (Cu K $\alpha$  radiation,  $\lambda = 1.5406$ Å) at a voltage of 40 kV and a current of 40 mA. A Nicolet IS50 FTIR spectrometer (Thermo Scientific) was employed to collect the Fourier transform infrared (FTIR) spectra. Field-emission scanning electron microscope (FESEM; Hitachi SU 8010) and transmission electron microscope (TEM; Philips, Tecnai 20 FEI) were used to examine the morphology and structure of the samples. The compositions of the samples were determined by energy-dispersive X-ray spectroscopy (EDS) attached to transmission electron microscope (TEM; Philips, Tecnai 20 FEI) and inductively coupled plasma emission spectrometer (iCAP7400). AC-STEM (aberrationcorrected scanning transmission electron microscopy) coupled with four energy dispersive X-ray spectroscopy detectors, were used to examine the morphology and structure of the samples on a ThermoFisher Scientific TEM (Themis Z) working at 300 kV. The HAADF collection angle of imaging was 61 to 200 mrads. X-ray photoelectron spectroscopy (XPS) analysis and Ultraviolet photoelectron spectra were carried out on a PHI Quantum 2000 XPS system with C 1s binding energy (284.6 eV) as the reference and He I excitation (21.22 eV) as the monochromatic light source. N<sub>2</sub> and CO<sub>2</sub> adsorption-desorption isotherms characterizations were conducted on a Micromeritics ASAP2020 under liquid nitrogen (77K) temperature and ice/water mixture temperature (273K), respectively.

The temperature-programmed desorption of H<sub>2</sub> (H<sub>2</sub>-TPD) and CO<sub>2</sub> (CO<sub>2</sub>-TPD) were performed using a xq-instrument TP-5080 chemisorption analyzer equipped with a TCD detector. For H<sub>2</sub>-TPD, the sample was heated from room temperature to 300 °C at a ramping rate of 10 °C min<sup>-1</sup> and held at 300 °C for 1 h, followed by cooling to 50 °C in a 10% H<sub>2</sub>/Ar mixture. After that, the carrier gas was switched to Ar to remove the weakly adsorbed H<sub>2</sub>. Then the temperature was ramping at 10 °C min<sup>-1</sup> for H<sub>2</sub> desorption. For CO<sub>2</sub>-TPD, the sample was heated from room temperature to 300 °C at a ramping rate of 10 °C min<sup>-1</sup> and held at 300 °C for 1 h, followed by cooling to 50 °C in a 10% H<sub>2</sub>/Ar mixture. After that, the carrier gas was switched to Ar to remove the weakly adsorbed H<sub>2</sub>. Then the temperature was ramping at 10 °C min<sup>-1</sup> for CO<sub>2</sub> desorption.

In-situ DRIFT spectra were carried out using a Nicolet iS50FTIR spectrometer (Thermo, U.S.A.) with a liquid-nitrogen-cooled MCT-A detector. Put about 100 mg of the sample (A mixture of 10 mg catalyst and 90 mg KBr) into the sample tank of the stainless-steel vacuum chamber with two pieces of copper mesh at the bottom and compact it. Set up the device according to the setup in the picture above, turn on the condensate water, and add liquid nitrogen toward the liquid N<sub>2</sub> added inlet. Before the experiment, the DRIFTS accessory optics were aligned and optimized. Data collection consisted of 32 scans per spectrum with a resolution of 4 cm<sup>-1</sup>. Prior to the adsorption measurement of a mixture of CO<sub>2</sub> and H<sub>2</sub> ( $V_{H_2}/V_{CO_2}/V_{He} = 72: 24:$ 4), the samples in the in-situ reaction cell were purged with Ar gas for 1 h to remove the water and gas impurities physically adsorbed on the catalyst surface. Subsequently, the reactant gas (2 mL min<sup>-1</sup> of CO<sub>2</sub> and H<sub>2</sub>, 18 mL min<sup>-1</sup> of Ar) was then introduced into the reaction chamber. The adsorption curves of CO2 at room temperature were recorded at regular intervals. After that, the background of CO<sub>2</sub> adsorption curve was deducted. Turn on the heater at a rate of 5 °C min<sup>-1</sup> to 260 °C, then deduct the background, and the changes of intermediates on the catalyst surface were recorded at regular intervals.



Fig. S1 (a) XRD pattern and (b) FESEM image of In-MIL-68 prisms.



Fig. S2 (a) HRTEM image and (b) SAED pattern of  $In_2O_3$ .



Fig. S3 In MNN Auger spectra of In<sub>2</sub>O<sub>3</sub>, Pt/In<sub>2</sub>O<sub>3</sub> and Pt@In<sub>2</sub>O<sub>3</sub>.



Fig. S4 CO<sub>2</sub> hydrogenation performance of  $In_2O_3$ ,  $Pt_{0.7}@In_2O_3$ ,  $Pt_{6.4}@In_2O_3$  and  $Pt@In_2O_3$ .



**Fig. S5** (a) Product evolution rates and (b) methanol selectivity of  $In_2O_3$ , Pt/In<sub>2</sub>O<sub>3</sub> and Pt@In<sub>2</sub>O<sub>3</sub> at different reaction temperatures.



Fig. S6 Long-time catalytic activity of Pt@In<sub>2</sub>O<sub>3</sub>.



Fig. S7 SEM images of Pt@In<sub>2</sub>O<sub>3</sub> after reaction.



Fig. S8 XRD patterns of Pt@In<sub>2</sub>O<sub>3</sub> before and after reaction.



**Fig. S9** (a) In 3d, (b) O 1s, (c) Pt 4f XPS spectra and (d) In MNN Auger spectra of  $Pt@In_2O_3$  before and after the  $CO_2$  hydrogenation reaction.



Fig. S10 (a,b) TEM images and (c) EDX maps of Pt@In<sub>2</sub>O<sub>3</sub> after reaction.



Fig. S11 (a,b) TEM images and (c) EDX maps of Pt/In<sub>2</sub>O<sub>3</sub> after reaction.



Fig. S12  $N_2$  sorption isotherms and BET surface area of  $Pt/In_2O_3$  (a) before and (b) after reaction.



Fig. S13  $N_2$  sorption isotherms and BET surface area of  $Pt@In_2O_3$  (a) before and (b) after reaction.



Fig. S14 *In-situ* DRIFT spectra of (a)  $Pt@In_2O_3$  and (b)  $Pt/In_2O_3$  under different  $CO_2$  adsorption times at 25 °C.



**Fig. S15** *In-situ* DRIFT spectra of (a)  $Pt@In_2O_3$  and (b)  $Pt/In_2O_3$  collected at 260 °C for different reaction times in CO<sub>2</sub>-saturated atmosphere.



**Fig. S16** *In-situ* DRIFT spectra of  $Pt/In_2O_3$  collected at 260 °C for different reaction times in CO<sub>2</sub>-saturated atmosphere.



Fig. S17 Schematic illustration of methanol production from  $CO_2$  hydrogenation involving CO as the intermediate over the  $Pt@In_2O_3$  catalyst

Catalysts	Pressure (MPa)	Temperature (°C)	Selectivity (%)	Yiled rate (mmol g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup> )	Ref.
Pt@In <sub>2</sub> O <sub>3</sub>	3	260	73	29.0	This work
Pt/In <sub>2</sub> O <sub>3</sub>	2	300	56	15.1	1
Pt/In <sub>2</sub> O <sub>3</sub>	5	300	53	16.9	2
Rh/In <sub>2</sub> O <sub>3</sub>	5	300	56	17.0	3
Au/In <sub>2</sub> O <sub>3</sub>	5	300	68	14.7	4
Ni/In <sub>2</sub> O <sub>3</sub>	5	300	54	17.2	5
Pd-P/In <sub>2</sub> O <sub>3</sub>	5	300	72	27.6	6
Pd/In <sub>2</sub> O <sub>3</sub> -CP	5	280	75	19.1	7
h-In <sub>2</sub> O <sub>3</sub> /Pd	3	295	72.4	16.6	8
Pd@In <sub>2</sub> O <sub>3</sub>	3	295	81.1	13.4	9
Pd/In <sub>2</sub> O <sub>3</sub> /SBA-15	5	260	84	11.0	10
h-In <sub>2</sub> O <sub>3</sub>	5	340	78	9.5	11
In <sub>2</sub> O <sub>3</sub> /ZrO <sub>2</sub>	5	300	99.5	9.2	12

Table S1. The CH<sub>3</sub>OH generation rate of  $Pt@In_2O_3$  in comparative with those of other catalysts in similar  $In_2O_3$ -based catalysts.

**Table S2.** The content of Pt in each sample determined by ICP-OES.

Sample	Pt content (wt.%)		
Pt <sub>0.7</sub> @In <sub>2</sub> O <sub>3</sub>	0.7		
Pt@In <sub>2</sub> O <sub>3</sub>	1.6		
Pt <sub>6.4</sub> @In <sub>2</sub> O <sub>3</sub>	6.4		
Pt/In <sub>2</sub> O <sub>3</sub>	1.6		

## **Supplementary References**

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