

## Supplementary Information

### Selective CO<sub>2</sub> electroreduction to formate over Cu-based catalyst in S<sup>2-</sup>- containing electrolyte

Shuyu Liang<sup>1,2,#</sup>, Ziyi Fang<sup>1,2,#</sup>, Chaoran Yang<sup>1,2</sup>, Qiang Wang<sup>1,2,\*</sup>

<sup>1</sup>College of Environmental Science and Engineering, Beijing Forestry University,  
Beijing 100083, China

<sup>2</sup>State Key Laboratory of Efficient Production of Forest Resources, Beijing Forestry  
University, Beijing 100083, China

<sup>#</sup>Equal contribution

\*Email: [qiangwang@bjfu.edu.cn](mailto:qiangwang@bjfu.edu.cn) (Q. Wang)

## **Experimental Section**

### **Materials**

Copper chloride dihydrate ( $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$ , 99.99%), ascorbic acid ( $\text{C}_6\text{H}_8\text{O}_6$ , 99%), potassium sulfide ( $\text{K}_2\text{S}$ , 99%), and formic acid ( $\text{HCOOH}$ , 99%) were purchased from Aladdin Reagent Co., Ltd. (Shanghai, China). Sodium hydroxide ( $\text{NaOH}$ , 96%), potassium bicarbonate ( $\text{KHCO}_3$ , 99.7%), potassium hydroxide ( $\text{KOH}$ , 85%), and anhydrous ethanol ( $\text{C}_2\text{H}_5\text{OH}$ , 99.99%) were purchased from Beijing Innokai Technology Co., LTD. (Beijing, China). Nafion (5%) is purchased from Shanghai Sanshik Industrial Co., Ltd. (Shanghai, China).

### **Synthesis of $\text{Cu}_2\text{O}$**

$\text{Cu}_2\text{O}$  nanocube was synthesized by a previously reported ligand-free method with slight modification. 10 mL of 0.1 M  $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$  solution was added to 400 mL of deionized water, then 30 mL of 0.2 M  $\text{NaOH}$  solution was added to the solution to form a blue flocculent precipitate. After stirring for 5 min, 20 mL of 0.1 M ascorbic acid solution was added dropwise to the solution described above and further stirred for 1 hour. The solution was then washed several times with ethanol and water and finally dried in a vacuum oven.

For the catalyst ink preparation, 5 mg of the as-prepared catalyst was mixed with 1.0 mL ethanol and 20  $\mu\text{L}$  5 wt.% Nafion solution, and then ultrasonicated for at least 30 min. Then, 56  $\mu\text{L}$  of the ink was slowly drop-casted on the glassy carbon electrode with a diameter of 6 mm to obtain a catalyst loading of 1  $\text{mg cm}^{-2}$ .

### **Characterizations**

The morphology of the samples were characterized by field emission scanning electron microscopy (FESEM, SU8010) and transmission electron microscopy (TEM, FEI Talos F200S, operated at 200 kV). High-angle annular dark field scanning transmission electron microscopy (HAADF-STEM) and energy dispersive X-ray spectroscopy (EDX) were carried out on a FEI Talos F200S microscope. The crystal structure of the catalysts was analyzed by X-ray diffraction (XRD, Shimadzu-7000) equipped with Cu K $\alpha$  radiation. The surface composition of the samples was determined by X-ray photoelectron spectroscopy (XPS, Thermo Scientific ESCALAB 250Xi). All spectra of the sample were calibrated to the C 1s binding energy at 284.8 eV. XPS depth profiles were obtained by etching using an Ar ion beam.

### **Electrochemical measurements and product analysis**

The electrochemical measurements were performed in a commercial H-type cell separated by a Nafion 117 membrane. A Pt mesh and an Ag/AgCl electrode were used as the counter electrode and the reference electrode, respectively. The linear sweep voltammetry (LSV) tests were performed in CO<sub>2</sub>-saturated 0.1 M KHCO<sub>3</sub> electrolyte containing different concentrations of K<sub>2</sub>S (0, 0.01, 0.05, 0.25 mM) at a scan rate of 20 mV s<sup>-1</sup> in a potential range from 0 to -2.0 V vs. RHE. Constant electrolysis was performed at the potential window from -1.0 to -1.4 V vs. RHE (no IR correction) in the H-type cell.

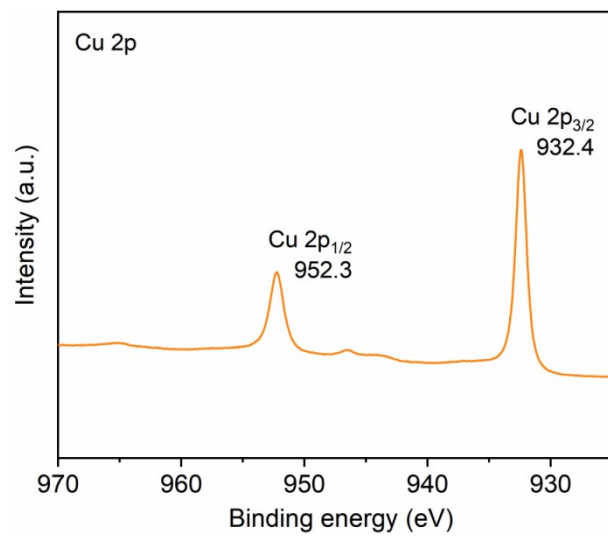
The flow cell is composed of three chambers: gas, catholyte and anolyte chambers. The catalyst ink was dropped onto a gas diffusion layer (GDL, AvCarb GDS2230) with a catalyst loading of 0.5 mg cm<sup>-2</sup> to obtain the gas diffusion electrode (GDE). The

Ag/AgCl and Pt foil were used as the reference electrode and anode, respectively. A Nafion 117 membrane was employed to separate the catholyte from the anolyte chamber. In the flow cell, 1 M KOH was selected as electrolyte and a series of amounts of 50 mM K<sub>2</sub>S was added to reach the concentration of 0.00, 0.05, 0.25, 1.00 and 2.50 mM. CO<sub>2</sub> was flowed into the gas chamber behind the GDE at a rate of 20 mL min<sup>-1</sup>, and it can diffuse through the gas diffusion electrode to the surface of the catalyst and form a three-phase interface with the electrolyte. Constant electrolysis was performed at the current density window from -50 to -200 mA cm<sup>-2</sup> in the flow cell.

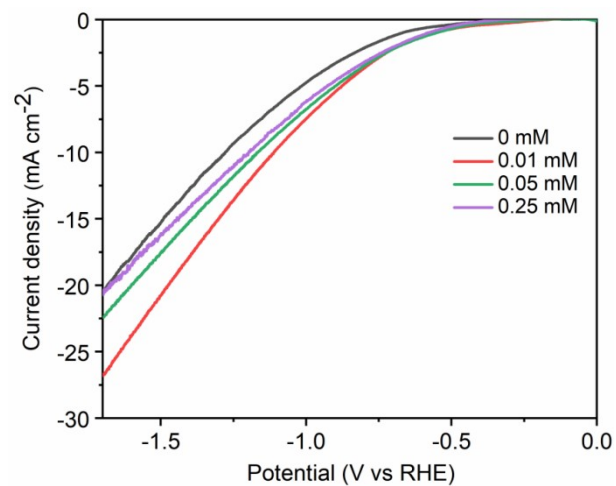
The gas products were quantified by online gas chromatography (Shimadzu GC-2014C). A thermal conductivity detector (TCD) was employed to determine H<sub>2</sub>, and a flame ionization detector (FID) was used to determine CO, CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub>. The liquid product of formic acid/formate was determined by High-Performance Liquid Chromatography (HPLC, Shimadzu). The Faradaic efficiency (FE) was calculated through Eq. (1), where Q<sub>total</sub> is the total charge passed during electrolysis (C), N<sub>i</sub> is the number of moles for the target product (mol), n is the number of electrons transferred (e.g., 2 for CO), and F is the Faraday constant (96485 C mol<sup>-1</sup>).

$$FE = \frac{N_i \times n \times F}{Q_{total}} \times 100\% \quad (1)$$

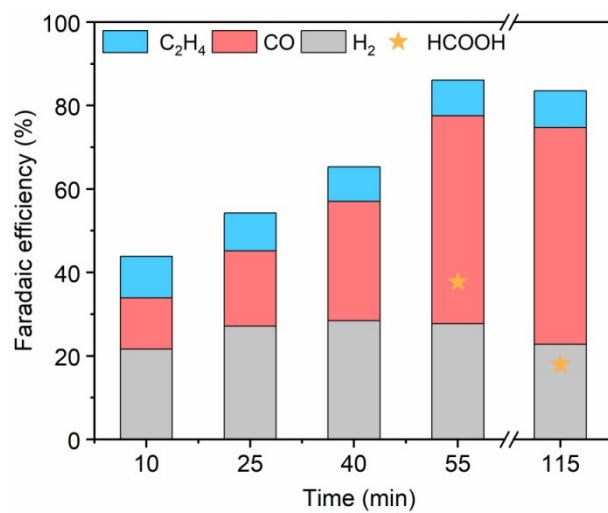
**Fig. S1.** The HAADF-STEM image and the corresponding energy dispersive X-ray spectroscopy (EDX) elemental mappings of Cu<sub>2</sub>O.



**Fig. S2.** Cu 2p XPS spectrum of Cu<sub>2</sub>O.

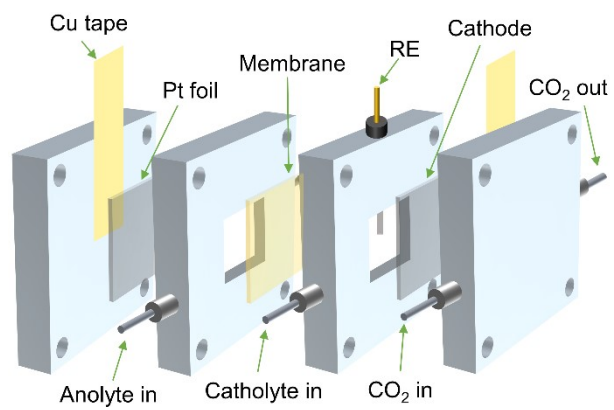


**Fig. S3.** LSV curves of Cu<sub>2</sub>O in CO<sub>2</sub>-saturated electrolytes containing different concentrations of K<sub>2</sub>S.

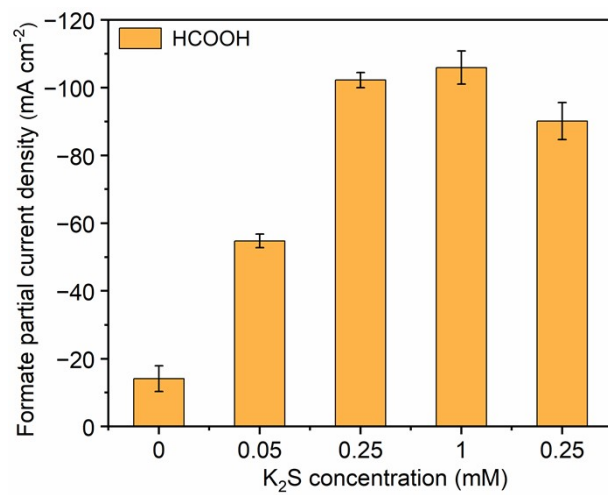


**Fig. S4.** The products' FE of Cu<sub>2</sub>O/Cu<sub>x</sub>S along with the reaction time.

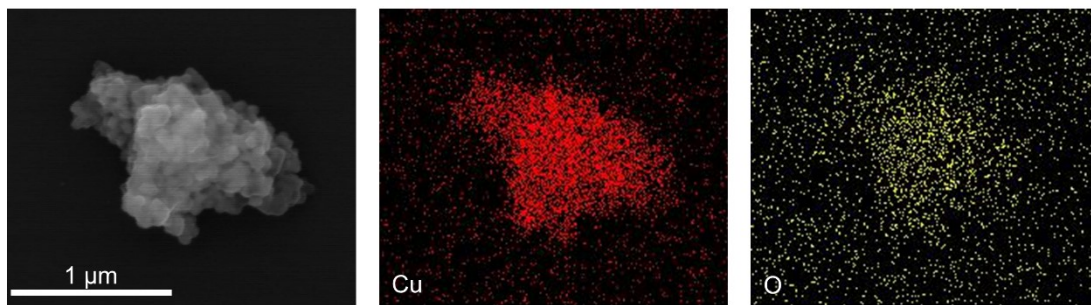




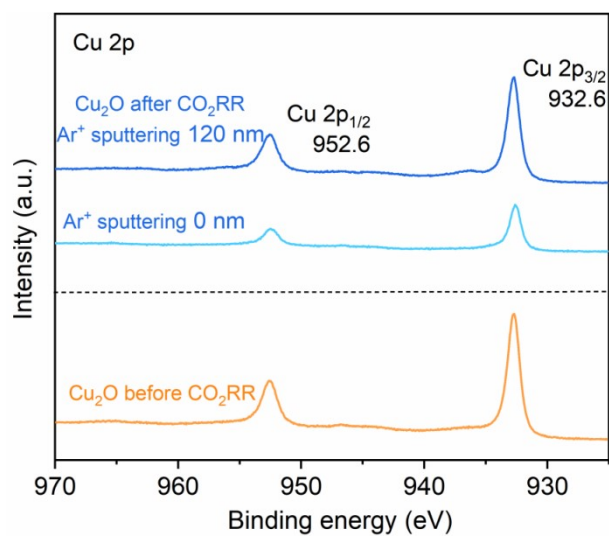
**Fig. S5.** Schematic illustration of the flow cell configuration.



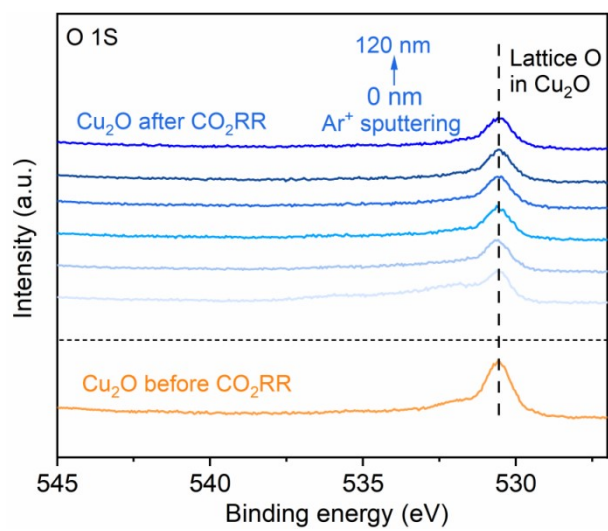
**Fig. S6.** Formate partial current density for Cu<sub>2</sub>O catalysts in electrolytes containing different concentrations of K<sub>2</sub>S at -150 mA cm<sup>-2</sup>.



**Fig. S7.** The SEM image and the corresponding energy dispersive X-ray spectroscopy (EDX) elemental mappings of  $\text{Cu}_2\text{O}$  after  $\text{CO}_2$  RR.



**Fig. S8.** Cu 2p XPS spectrum of Cu<sub>2</sub>O before and after CO<sub>2</sub>RR in the electrolyte containing K<sub>2</sub>S.



**Fig. S9.** O 1s spectrum of Cu<sub>2</sub>O before and after CO<sub>2</sub>RR in the electrolyte containing

K<sub>2</sub>S.

**Table. S1.** Performance comparison of Cu-based catalysts for CO<sub>2</sub> electroreduction to formate.

Catalyst	Electrolyte	Potential V vs. RHE	J <sub>formate</sub> (mA cm <sup>-2</sup> )	Formate FE (%)
Cu <sub>2</sub> O (H-type cell) This work	0.1 M KHCO <sub>3</sub> + 0.05 mM K <sub>2</sub> S	-1.2	8.3	74
Cu <sub>2</sub> O (Flow cell) This work	1 M KOH+1 mM K <sub>2</sub> S	/	105.9	70.6
Commercial Cu <sub>2</sub> S <sup>1</sup>	0.1 M KHCO <sub>3</sub>	-0.86	~3.6	~36
CuS <sup>2</sup>	0.1 M KHCO <sub>3</sub>	-0.6	1.5	98 (keep decreasing from 98% to 40% during 8 h)
5% PTFE Cu array <sup>3</sup>	0.1 M KHCO <sub>3</sub>	-0.7	2.3	41
Cu <sub>2</sub> S NSs/C <sup>4</sup> (H-type cell)	0.1 M KHCO <sub>3</sub>	-1.2	8.9	71.4
Cu <sub>2</sub> S NSs/C <sup>4</sup> (Flow cell)	0.1 M KHCO <sub>3</sub>	/	205	82
S-doped Cu/Cu foil <sup>5</sup>	0.1 M KHCO <sub>3</sub>	-0.8	10.7	75
CuS 811 (H-type cell) <sup>6</sup>	0.1 M KHCO <sub>3</sub>	-1.0	~7.5	92
CuS 811 (flow cell) <sup>6</sup>	1 M KOH	/	172	86
Cu <sub>2</sub> O/CuS <sup>7</sup>	0.1 M KHCO <sub>3</sub>	-0.9 V	15.3	67.6
S3-Cu <sub>2</sub> O-70 <sup>8</sup>	0.1 M KHCO <sub>3</sub>	-0.9 V	260 (flow cell)	90
Cu nanoflower <sup>9</sup>	0.1 M KHCO <sub>3</sub>	-1.6	9	50
CuS/N <sub>x</sub> S-rGO <sup>10</sup>	0.5 M KHCO <sub>3</sub>	-0.63	~4.8	82
AC-CuS <sub>x</sub> <sup>11</sup>	0.1 M KHCO <sub>3</sub>	-0.9	9	75
L-S CuS <sub>x</sub> <sup>12</sup>	0.1 M KHCO <sub>3</sub>	-0.9	~10	80
CuS/BM <sup>13</sup>	0.5 M KHCO <sub>3</sub>	-0.7	75	67.8

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