Supporting Information

Mechanochemically-Flavoured Three-Way Approach for the Synthesis of K-doped Cu-Fe/ZnO-Al2O³ Catalysts for Converting CO² to Oxygenates

Boon Ying Tay,^a Charmain Kan,^a Jennet Ong,^a Shashikant U. Dighe,^{a,b} Amol M. Hengne,^{a,b} Kuo-Wei Huang,^{a,b,c} Lili Zhang,^a Roong Jien Wong,*a and Davin Tan*a,b

*a Institute of Sustainability for Chemical, Energy and Environment (ISCE²), Agency of Science, Technology and Research (A*STAR), 1 Pesek Road, Jurong Island, Singapore 627833, Republic of Singapore. E-mail: davin_tan@isce2.a-star.edu.sg; wong_roong_jien@isce2.a-star.edu.sg*

*b Institute of Materials Research and Engineering (IMRE), Agency of Science, Technology and Research (A*STAR), 2 Fusionopolis Way, Singapore 138634, Republic of Singapore.*

^c Division of Physical Sciences & Engineering, King Abdullah University of Science and Technology, Thuwal 23955-6900, Saudi Arabia.

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EXPERIMENTAL SECTION

Methods and materials

 N_a ₂CO₃, Cu(NO₃)₂, Fe(NO₃)₃, Zn(NO₃)₂, Al(NO₃)₃, CuO, Fe₂O₃, ZnO and Al₂O₃ were purchased from Sigma Aldrich, Fe₂O₃ from PenReac, K₂CO₃ from Fisher and CuO from Merck. TraceMetal™ Grade nitric acid, hydrochloric acid and hydrofluoric acid used in elemental analysis were purchased from Fisher.

Catalyst Preparation

A) Solution synthesis of **CFZA (SS1) Cu0.65-Fe0.05/Zn0.2Al0.1**

Cu_{0.65}-Fe_{0.05}/Zn_{0.2}Al_{0.1} was prepared *via* co-precipitation method. An aqueous solution of 1.2 M solution of Na₂CO₃ (125 mL) was added dropwise to 100 mL aqueous solution of stoichiometric amount of Cu(NO₃)₂, Fe(NO₃)₃, Zn(NO₃)₂ and Al(NO₃)₃ at 70 °C for 2 h and a pH of 6-7. During precipitation, the pH of the suspension was monitored constantly using a pH meter and $Na₂CO₃$ solution was added at a controlled rate to maintain the prescribed pH (6–7). The resulting precipitate was washed with 1.5 L DI water and dried for 16 h at 70 °C in oven. The dried precipitate was calcined under air flow at 5 °C/min for 4 h at 350 °C and then reduced under H₂ at 5 °C/min for 4 h at 450 °C.

B) K-promoted **KCFZA (SS1-K) Cu0.65-Fe0.05/Zn0.2Al0.1**

K2CO³ (5 wt% K) was added onto the calcined catalyst prepared in (A) *via* **incipient wetness impregnation** with an aqueous solution of K_2CO_3 . The wet mixture is then dried in an oven for 2 h at 120 °C. After drying, the solid powder is placed in a tube furnace and calcinated with an air flow at 5 °C/min for 4 h at 350 °C and then reduced under H_2 at 5 °C/min for 4 h at 450 °C to yield **SS1-K**.

Catalyst preparation *via* **mechanosynthesis**: Mechanosynthesis of **KCFZA** was carried out in a Retch MM400 mill at a frequency of 29 Hz using a 35 mL 440B stainless steel milling jar and three balls made of the same material (10 mm diameter).

BM1 – **Mechanosynthesis of solution-synthesized KCFZA:** K₂CO₃ (5 wt% K, 0.1 g) and the calcined catalyst (2.0 g) prepared from (A) was added into the 35 mL milling jar and then milled neat at a frequency of 29 Hz for 1 h following by calcination under air flow at 5 °C/min for 4 h at 350 °C and then reduction under H₂ at 5 °C/min for 4 h at 450 °C.

BM2 – Mechanosynthesis of KCFZA using metallic nitrate salt precursors: Stoichiometric amount of $Cu(NO₃)₂$, Fe(NO₃)₃, Zn(NO₃)₂, Al(NO₃)₃ and Na₂CO₃ were weighed (total weight about 4.0 g) and 1 mL of DI water (as the milling media) transferred into a 35 mL milling jar and milled at 29 Hz for 3 h. After milling, the resultant solids were washed with 500 mL DI water and dried 16 h at 70 \degree C in oven. The dried precipitate was calcined under air flow at 5 °C/min for 4 h at 350 °C and then reduced under H₂ at 5 °C/min for 4 h at 450 °C. K₂CO₃ (5 wt% K, 0.05 g) and the calcined catalyst (1.0 g) was added into a 35 mL milling jar and milled neat at a frequency of 29 Hz for 1 h following by calcination under air flow at 5 °C/min for 4 h at 350 °C and then reduction under H₂ at 5 °C/min for 4 h at 450 °C.

BM3 - Mechanosynthesis of KCFZA using metallic oxide precursors: Stoichiometric amount of CuO, Fe₂O₃, ZnO and Al_2O_3 were weighed (total weight about 4.0 g) and transferred into a 35 mL milling jar and milled neat at a frequency of 29 Hz for 3 h. The product was calcined under air flow at 5 °C/min for 4 h at 350 °C and then reduced under H₂ at 5 °C/min for 4 h at 450 °C. K₂CO₃ (5 wt% K, 0.05 g) was added onto the calcined catalyst (1.0 g) ball-milled neat at a frequency of 29 Hz for 1 h following by calcination under air flow at 5 °C/min for 4 h at 350 °C and then reduction under H₂ at 5 °C/min for 4 h at 450 °C.

Catalyst characterization

Powder X-ray diffraction (XRD) patterns of the calcined **KCFZA** catalysts were collected on a powder diffractometer (Bruker D8 Advance X-ray) with a Cu-K_α source (Kα=0.154nm) in the 2θ range between 20–80°. Scanning electron microscopy (SEM) was conducted using a JEOL JSM-7900F Schottky Field Emission Scanning Electron Microscope fitted with Oxford Instruments X-Max 80 EDX spectrometer. SEM Images were taken at an acceleration voltage of 10 kV while EDX analysis at an acceleration voltage of 15 kV. Samples were sputtercoated with gold, by Cressington 208HR High Resolution Sputter Coater for better conductivity. High resolution transmission electron microscopy (HRTEM) was conducted using a JEOL JEM-2200FS field emission with a highenergy electron beam operated at 200 kV. The instrument is equipped with JEOL JED-2300 Plus EDS detector for elemental analysis. Samples were prepared by drop-casting and air drying a dilute suspension of nanoparticles, after sonicating in HPLC-grade ethanol (99.8% purity), onto carbon-coated molybdenum grids. Elemental analysis of the catalysts was performed by digesting the catalysts using a Milestone ETHOS One microwave system containing 10 PTFE (polytetrafluoroethylene) Teflon digestion containers (100 mL) equipped with individual pressure safety springs and a high pressure segmented rotor (Milestone model HPR 1000/10S) with a system pressure sensor using HPR-CE-01 method in the Milestone application note, followed by analysis performed with a Varian Vista MPX CCD ICP-OES.

Catalysis

All catalytic experiments were performed using a 50 mL Parr 4792 reactor with a thermocouple attached and heated over a jacketed heater. Flow reaction was performed using a vertical tube furnace with a fixed catalyst bed. Liquid CO₂ hydrogenation products were analysed on Agilent 6890N GC with Agilent CP-Wax 52 CB capillary column (50 m x 0.25 mm x 0.5 μ m).

General procedure for CO² hydrogenation reaction.

For batch reaction: Into a 50 mL Parr reactor vessel with a magnetic stirrer bar was charged 100 mg catalyst and 10 mL water. The Parr reactor was sealed was purged 3 times with $CO₂$. Subsequently, 15 bar $CO₂$ was charged into the reactor followed by 45 bar H₂. The reaction was heated to 200 °C using a jacketed heater and was stirred for 16 h. The reaction was then cooled in an ice bath to room temperature and the gases were vented. 1 mL of the reaction mixture was filtered with a 0.45-micron syringe filter and then analysed with GC.

For continuous flow reaction, a 3/8" stainless tube was placed in a vertical furnace as the reactor. 0.5 g of catalyst was diluted in equal volume of SiC, supported on quartz wool as a fixed catalyst bed. The catalyst was first reduced with 50% H₂ at 400°C for 3 hours. Reaction gas mix (24% CO₂, 72% H₂, 4% Ar) was flowed through the catalyst at SV 2500 ml(gh)⁻¹ and at 50 bar. The CO₂ hydrogenation reaction was performed at 200 C for 16 hours. An online GC (equipped with a Thermal Conductivity Detector and Flame Ionisation Detector) was employed to analyse the reaction products.

SUPPORTING INFORMATION

SEM Micrograph/ SEM-EDX elemental mapping

Supp. Info. 1. SEM micrographs of solution synthesized Cu-Fe/Zn/Al (**SS1**) catalyst, 1k magnification (left), 10k magnification (middle) and 50k magnification (right).

Supp. Info. 2. SEM micrographs of K-doped Cu-Fe/Zn/Al catalyst *via* wet impregnation **(SS1-K)**, 1k magnification (left), 10k magnification (middle) and 50k magnification (right).

Supp. Info. 3. SEM micrographs of K-doped Cu-Fe/Zn/Al (K**CFZA**) catalyst *via* mechanosynthesis (**BM1**), 1k magnification (left), 10k magnification (middle) and 50k magnification (right).

Supp. Info. 4. SEM micrographs of K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst using metallic nitrate salt precursors (**BM2**), 1k magnification (left), 10k magnification (middle) and 50k magnification (right).

Supp. Info. 5. SEM micrographs of K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst using metallic oxide precursors (**BM3**), 1k magnification (left), 10k magnification (middle) and 50k magnification (right).

Supp. Info. 6.(A) SEM-EDX elemental mapping of solution synthesized Cu-Fe/Zn/Al **(SS1)** catalyst, (B) elemental composition of solution synthesized Cu-Fe/Zn/Al **(SS1)** catalyst.

(B)

(B)

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Supp. Info. 8.(A) SEM-EDX elemental mapping of K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst via ball milling (**BM1**), (B) elemental composition of K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst via ball milling (**BM1**).

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Supp. Info. 10.(A) SEM-EDX elemental mapping K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst using metallic oxide precursors (**BM3**), (B) elemental composition of K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst using metallic oxide precursors (**BM3**).

HR-TEM Micrograph/ TEM-EDX elemental mapping

Supp. Info. 11. (A) TEM micrographs of K-doped Cu-Fe/Zn/Al catalyst *via* wet impregnation **(SS1-K)**, (B) lattice d-spacing of the observed CuO, ZnO, $Fe₂O₃$ particles in the sample.

TEM shows areas containing lattice d-spacing for Cu, ZnO and $Fe₂O₃$ zones in close proximity for particles of **SS1-K**. Such multi-metallic zones could have promoted the formation of EtOH and higher alcohols.

Supp. Info. 12.TEM-EDX elemental mapping K-doped Cu-Fe/Zn/Al (**KCFZA**) catalyst using metallic nitrate salt precursors (**SS1-K**). Brightness for images of Fe, Al and K have been increased by 65% and sharpness reduced by 30%.

Supp. Info. 13. TEM-EDX elemental mapping K-doped Cu-Fe/Zn/Al **(KCFZA)** catalyst using metallic oxide precursors **(BM3)**. Brightness for images of Fe, Al and K have been increased by 65% and sharpness reduced by 30%.

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	ß	2θ (°)	D (nm)
SS ₁	0.3728	43.1	22.9
$SS1-K$	0.2256	43.2	37.9
BM1	0.2137	43.2	40.0
BM ₂	0.2256	43.2	37.9
BM ₃	0.1741	43.3	49.1

Supp. Info. 16. Crystallite size estimation of the five catalysts based on PXRD.

Supp. Info. 17. XRD analysis of **BM3**.

Energy Calculation Data

The energy consumption for each method is based on the duration and relative power output of each equipment: Hotplate (825 W, max. temp. 300 °C), drying oven (1250 W, max. temp. 300 °C), tube furnace (3000 W, max. temp. 1200 °C) and ball mill (165 W, max. 30 Hz).

*Assuming density of the liquid washings waste, which includes solution of unreacted carbonate and nitrate salts, is same as water (1 g/mL). **Without considering energy consumed for calcination and reduction. ***E-factor is calculated by the (total mass of waste) / (total mass of product); the lower the magnitude of E-factor, the greener the process.

Supp. Info. 18. Energy calculations on the various methods of synthesizing **KCFZA**.

Fixed Bed Reaction Data

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ICP-OES analysis

Supp. Info. 20. ICP-OES analysis of the five catalysts in the study.

AUTHOR CONTRIBUTIONS

B. Y. Tay, C. Kan and D. Tan designed and synthesised the catalysts and conducted the batch reactor experiments. J. Ong, R. J. Wong and D. Tan conducted the fixed bed reactor experiments. B. Y. Tay and D. Tan drafted the manuscript. B. Y. Tay, C. Kan, R. J. Wong and D. Tan characterized the catalysts and analysed the results. S. Dighe and A. Hengne contributed to the discussions of GC results. K. W. Huang and L. Zhang contributed to the discussions and editing of the manuscript.