Supporting information to:

Impurity-induced Acceleration of Polymorphic Conversion via Crystalline Solid Solutions and the T-X Phase Diagrams of Salicylic acid and 3-Hydroxybenzoic acid

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Figure 1. XRPD overlay of select SA-3HBA Form I samples used in DSC analyses.

Х(ЗНВА)	DSC	Low temperature endotherm				High temperature endotherm					
	endotherms		г_	-	_		_			-	
mol		Tinset	Tonset	Tpeak	Toffset	Enthalpy	Tinset	Tonset	Tpeak	Toffset	Enthalpy
ЗА+ЗПВА		°C	°C	°C	°C	J/g	°C	°C	°C	°C	J/g
0	Ono						154.07	158.64	150 16	160.08	190 56
0	endotherm						(0.08)	(0.006)	(0.09)	(0.23)	(4 21)
	chuotherm						(0.00)	(0.000)	(0.05)	(0.23)	(1.21)
0.0031	One						152.33	158.41	158.83	160.86	178.97
	endotherm						(0.26)	(0.32)	(0.10)	(0.64)	(13.18)
0.0050	One						151.87	157.55	158.70	160.33	174.50
	endotherm						(0.57)	(0.20)	(0.09)	(0.23)	(3.49)
0.0099	Two	143.14	145.01	147.39	149.33 ¹	7.59		157.11	158.74	160.53	168.97
	partially	(0.56)	(1.08)	(0.16)	(0.66)	(4.45)		(0.80)	(0.20)	(0.02)	(10.7)
	overlapping										
	endotherms										
0.0177	Two	141.12	145.70	147.13	149.72 ¹	14.19		155.95	158.35	160.44	168.84
	partially	(0.45)	(1.11)	(0.42)	(1.52)	(6.53)		(0.88)	(0.28)	(0.39)	(8.47)
	overlapping										
	endotherms				4.40 701	40.00		450.00	457.00	150.10	100.74
0.0443	l wo	140.27	144.06	147.47	149.72	42.22		153.98	157.33	159.48	132./1
	partially	(0.14)	(0.20)	(0.22)	(1.12)	(10.97)		(0.95)	(0.90)	(0.50)	(20.71)
	overlapping										
0.0927	Two	140.10	1/2 07	1/7 22	1/0 911	99.25			155.02	157.50	01 02
0.0927	nartially	(0.10)	(0.03)	(0.09)	(0.09)	00.25 (1.55)			(0.32)	(0.22)	91.92 (5.15)
	overlanning	(0.10)	(0.03)	(0.05)	(0.05)	(1.55)			(0.52)	(0.22)	(5.15)
	endotherms										
0.1463	Two	140.50	144.33	146.50	149.40 ¹	138.06			152.50	155.27	54.78
	endotherms	(0.11)	(0.03)	(0.22)	(0.16)	(9.42)			(0.26)	(0.95)	(9.03)
	mostly	, ,	. ,	. ,	, ,	· · /			. ,	. ,	· ,
	overlapping										
0.1984	Two	140.35	144.44	146.68	149.36 ¹	156.82				154.48	38.24
	endotherms	(0.29)	(0.03)	(0.39)	(0.05)	(14.87)				(0.73)	(12.97)
	mostly										
	overlapping										
0.2378	Two	141.02	144.49	146.84	148.81 ¹	188.32				154.97	5.74
	endotherms	(0.32)	(0.02)	(0.32)	(0.22)	(8.12)				(1.49)	(5.44)
	mostly										
	overlapping								-		
0.2993	Two	140.65	144.64	146.46	149.70 ¹	183.99				160.13	11.77
	endotherms	(0.01)	(0.06)	(0.37)	(0.14)	(5.05)				(1.78)	(6.26)
	mostly										
0 2047	Тжо	140.47	144 72	146.42	140 621	171.00				167.01	26.12
0.3947	endotherms	(0.26)	(0.07)	(0.09)	(0.16)	(6 19)				(3.80)	(7.14)
	mostly	(0.20)	(0.07)	(0.05)	(0.10)	(0.15)				(3.00)	(7.11)
	overlapping										
0.4970	Two	139.61	144.66	146.05	149.58 ¹	135.75			171.72	179.64	71.79
	partially	(0.30)	(0.01)	(0.07)	(0.53)	(10.27)			(2.24)	(3.10)	(16.00)
	overlapping				. ,	. ,				. ,	. ,
	endotherms										
0.6005	Two	139.73	144.80	146.38	149.35 ¹	117.25			180.13	188.24	99.63
	partially	(0.01)	(0.01)	(0.28)	(0.11)	(4.10)			(7.58)	(6.06)	(11.92)
	overlapping										
	endotherms										

0.7013	Two	139.77	144.25	146.19	148.51 ¹	70.88		183.38	189.24	193.74	158.78
	partially	(0.96)	(0.11)	(0.14)	(0.25)	(7.34)		(5.55)	(2.59)	(2.41)	(39.29)
	overlapping										
	endotherms										
0.8073	Two mostly	138.16	145.67	146.57	149.44 ¹	37.83		201.44	200.22	202.57	198.76
	separated	(1.52)	(2.12)	(0.20)	(0.58)	(6.59)		(0.03)	(3.42)	(2.59)	(4.61)
	endotherms										
0.8987	Two mostly	138.54	141.79	145.86	148.65 ¹	7.74		201.35	202.07	204.25	238.56
	separated	(0.79)	(2.27)	(0.97)	(0.87)	(4.05)		(0.07)	(0.11)	(0.26)	(2.63)
	endotherms										
0.9504	One						183.73	201.51	202.15	204.78	246.14
	endotherm						(0.25)	(0.27)	(0.25)	(0.37)	(3.24)
0.9601	One						186.84	201.38	202.25	204.64	244.64
	endotherm						(1.38)	(0.11)	(0.15)	(0.23)	(13.22)
0.9702	One						187.60	201.36	202.14	204.43	243.81
	endotherm						(0.70)	(0.14)	(0.14)	(0.48)	(7.16)
0.9797	One						190.95	201.41	202.09	204.23	246.09
	endotherm						(1.18)	(0.02)	(0.07)	(0.11)	(5.68)
0.9905	One						182.37	201.24	202.05	203.98	247.55
	endotherm						(1.71)	(0.07)	(0.12)	(0.32)	(5.92)
1.000	One						194.51	201.40	202.11	204.22	248.94
	endotherm						(0.69)	(0.03)	(0.13)	(0.44)	(3.77)

1 Mid-point between endotherms is used as an approximation of the baseline offset temperature of the low-temperature endotherm. This separation also provides the calculation of the enthalpy of both the low- and high-temperature endotherms, when possible.



Figure 2. XRPD overlay of select SA-3HBA Form II samples used in DSC analyses prepared via evaporative crystallization from MeOH.

Table 2. DSC summary for SA-3HBA Form II

Х(ЗНВА)	DSC endotherms	Low temperature endotherm					High temperature endotherm				
mol		T _{inset}	Tonset	T_{peak}	T _{offset}	Enthalpy	T _{inset}	Tonset	T_{peak}	Toffset	Enthalpy
3HBA/mol											
ЗА+ЗПВА		°C	°C	°C	°C	J/g	°C	°C	°C	°C	J/g
0	One						154.07	158.64	159.16	160.98	189.56
	endotherm						(0.08)	(0.006)	(0.09)	(0.23)	(4.21)
0.0038	One						152.60	158.06	159.13	161.09	185.24
0.0062	One						154.04	158.01	158.85	160.85	184.04
0.0002	endotherm						(0.51)	(0.22)	(0.12)	(0.20)	(6.26)
0.0079	One						152.59	157.74	158.81	160.93	180.93
	endotherm						(0.28)	(0.11)	(0.16)	(0.24)	(1.96)
0.0103	Two	141.72	142.71	144.12	145.88	1.50	149.41	157.27	158.89	160.63	171.06
	separated endotherms	(0.41)	(0.08)	(0.06)	(0.39)	(0.38)	(0.36)	(0.34)	(0.09)	(0.22)	(9.7)
0.0307	Two	140.28	143.50	144.63	146.50 ¹	13.56		154.31	157.66	159.72	162.64
	partially	(0.24)	(0.12)	(0.02)	(0.28)	(0.47)		(0.06)	(0.14)	(0.25)	(5.19)
	overlapping endotherms										
0.0508	Two	139.11	143.41	144.76	146.54 ¹	31.30		152.63	156.53	158.67	146.43
	partially	(0.11)	(0.10)	(0.01)	(0.24)	(2.31)		(0.25)	(0.18)	(0.23)	(2.99)
	overlapping										
	endotherms				1						
0.0699	Two	138.45	143.52	144.80	146.88 ¹	49.12		150.92	155.47	158.18	129.74
	partially	(0.42)	(0.04)	(0.03)	(0.07)	(6.83)		(1.45)	(0.38)	(0.24)	(2.87)
	endotherms										
0.0959	Two	138.66	142.18	144.78	147.14 ¹	67.36		150.87	154.66	157.27	112.64
	partially	(0.53)	(0.02)	(0.08)	(0.07)	(2.24)		(2.16)	(0.31)	(0.62)	(5.16)
	overlapping										
	endotherms										
0.2012	Two	137.48	142.22	144.59		152.40				152.64	35.88
	endotherms	(0.56)	(0.02)	(0.04)		(0.45)				(1.22)	(3.40)
	overlapping										
0.2489	Two	138.18	142.19	144.05		173.28				151.98	17.22
	endotherms	(0.19)	(0.02)	(0.23)		(2.16)				(1.64)	(0.35)
	mostly										
	overlapping										
0.3050	Two	137.90	142.44	143.92		178.83	Not acce	ssible due	to form tr	ansformat	ion
	endotherms	(0.30)	(0.20)	(0.17)		(5.37)					
	mostly										
0 3952	Тууо	137 48	142 30	143 80		170 72	Not acce	ssible due	to form tr	ansformat	ion
0.5552	endotherms	(0.95)	(0.03)	(0.20)		(3.37)					
	mostly	. ,	. ,	. ,		. ,					
	overlapping										
0.4889	Two	138.83	142.24	144.12	146.53 ¹	140.28	Not acce	ssible due	to form tr	ansformat	ion
	partially	(1.03)	(0.04)	(0.20)	(0.28)	(6.02)					
	overlapping										
	endotherms										
	exotherm										

0.6004	Two	138.77	142.04	143.77	145.98	103.71	Not accessible due to form transformation
	partially	(0.18)	(0.04)	(0.15)	(0.29)	(2.69)	
	overlapping						
	endotherms						
	and one						
	exotherm						
0.7028	Two	138.47	141.98	143.38	145.62	69.12	Not accessible due to form transformation
	partially	(0.25)	(0.09)	(0.09)	(0.34)	(4.32)	
	overlapping						
	endotherms						
	and one						
	exotherm						
0.8126	Two	137.30	141.65	143.18	145.19	49.83	Not accessible due to form transformation
	partially	(0.13)	(0.04)	(0.12)	(0.27)	(3.75)	
	overlapping						
	endotherms						
	and one						
	exotherm						
0.9016	Two mostly	136.04	140.86	142.60	144.42	18.83	Not accessible due to form transformation
	separated	(0.95)	(0.12)	(0.11)	(0.37)	(2.80)	
	endotherms						
	and one						
	exotherm						
0.9513	Two	134.94	139.76	141.99	144.11	8.1	Not accessible due to form transformation
	separated	(1.13)	(0.10)	(0.08)	(0.49)	(0.78)	
	endotherms						
	and one						
	exotherm						
0.9754	Two	134.07	135.95	139.61	142.81	3.30	Not accessible due to form transformation
	separated	(0.97)	(2.34)	(1.45)	(0.24)	(0.23)	
	endotherms						
	and one						
	exotherm						
0.9904	One						Not accessible due to form transformation
	endotherm						
1.000	One						Not accessible due to form transformation
	endotherm						

1 Mid-point between endotherms is used as an approximation of the baseline offset temperature of the low-temperature endotherm. This separation also provides the calculation of the enthalpy of both the low- and high-temperature endotherms, when possible.

X(3HBA)	T _{inset}	T _{onset}	T _{peak}	T _{offset}	Enthalpy of
					exotherm
mol	°C	°C	°C	°C	J/g
3HBA/mol					
SA+3HBA					
0.4889	156.64	158.50	161.60	165.33	15.1
	(1.39)	(0.93)	(0.77)	(0.71)	(1.12)
0.6004	154.37	156.09	158.94	161.6	7.69
	(0.17)	(0.18)	(0.17)	(0.27)	(0.72)
0.7028	154.76	160.73	164.02	168.71	11.32
	(2.82)	(0.25)	(0.27)	(2.09)	(1.07)
0.8126	153.27	158.05	162.39	167.10	10.26
	(0.63)	(0.31)	(0.19)	(0.37)	(1.11)
0.9016	158.33	160.50	164.98	170.32	6.21
	(1.47)	(0.93)	(0.95)	(0.37)	(2.62)
0.9513	161.18	163.11	167.76	171.99	2.47
	(1.39)	(2.05)	(2.19)	(1.78)	(0.19)
0.9754	154.59	156.23	160.43	165.55	2.43
	(3.02)	(3.62)	(2.57)	(2.43)	(0.92)
0.9904	145.73	147.64	152.78	159.36	1.83
	(2.00)	(2.01)	(0.98)	(0.77)	(0.38)
1.000	142.21	143.41	150.40	159.36	3.17
	(2.20)	(1.57)	(0.74)	(2.31)	(0.31)

Table 3. DSC summary for SA-3HBA Form II: Exothermic transition from Form II (or βII) to Form I (or βI) of 3HBA

Table 4. Solid-Liquid Equilibria (SLE) summary of SA-3HBA Form I in 40 w% MeOH in H2O at 25°C

Solid	Liquid	Solid	Conc. of	Conc. of	X(SA)	X(3HBA)	X(solvent)
phase			SA	3HBA			
	w% or	w% or	mg SA/g	mg	mmol	mmol	mol
	mol%	mol%	solvent	3HBA/g	SA/(mol	3HBA/(m	solvent/(mol
	3HBA in	3HBA in		solvent	total)	ol total)	total)
	SA	SA					
SA	0.00%	0.00%	23.37	0.00	3.6813	0.0000	0.9963
α	18.25%	0.04%	26.81	5.99	4.2173	0.9416	0.9948
α	26.67%	0.08%	27.63	10.04	4.3423	1.5788	0.9941

α	37.37%	0.09%	29.52	17.61	4.6327	2.7639	0.9926
α	40.57%	0.13%	29.78	20.33	4.6723	3.1897	0.9921
α	55.26%	0.26%	34.06	42.06	5.3211	6.5720	0.9881
α	60.84%	0.39%	39.53	61.41	6.1523	9.5570	0.9843
α	65.38%	0.45%	43.14	81.46	6.6895	12.6310	0.9807
α+βΙ	69.47%	0.65%	51.83	117.96	7.9809	18.1642	0.9739
α+βΙ	70.27%	48.72%	52.21	123.39	8.0317	18.9833	0.9730
α+βΙ	69.64%	78.71%	53.47	122.65	8.2254	18.8676	0.9729
α+βΙ	70.35%	91.47%	52.15	123.72	8.0221	19.0337	0.9729
βι	79.26%	99.58%	29.48	112.63	4.5586	17.4181	0.9780
βι	77.79%	99.59%	32.93	115.38	5.0883	17.8253	0.9771
βι	85.36%	99.70%	18.60	108.40	2.8825	16.8022	0.9803
βι	87.84%	99.79%	14.53	104.99	2.2547	16.2929	0.9815
βι	85.06%	99.80%	19.31	109.87	2.9914	17.0254	0.9800
βι	94.51%	99.85%	6.17	106.17	0.9581	16.4948	0.9825
βι	96.94%	99.93%	3.16	100.18	0.4924	15.5864	0.9839
3HBA, Form I	100%	100%	0.00	98.36	0.0000	15.3148	0.9847

Table 5. Solid-Liquid Equilibria (SLE) summary of SA-3HBA Form II in 40 w% MeOH in H2O at 25°C

Solid	Liquid	Solid	Conc. of	Conc. of	X(SA)	Х(ЗНВА)	X(solvent)
phase	w% or mol% 3HBA in SA	w% or mol% 3HBA in SA	mg SA/g solvent	mg 3HBA/g solvent	mmol SA/(mol total)	mmol 3HBA/(m ol total)	mol solvent/(mol total)
SA	0.00%	0.00%	23.37	0.00	3.6813	0.0000	0.9963
α	18.25%	0.04%	26.81	5.99	4.2173	0.9416	0.9948
α	26.67%	0.08%	27.63	10.04	4.3423	1.5788	0.9941
α	37.37%	0.09%	29.52	17.61	4.6327	2.7639	0.9926
α	40.57%	0.13%	29.78	20.33	4.6723	3.1897	0.9921
α	55.26%	0.26%	34.06	42.06	5.3211	6.5720	0.9881
α	60.84%	0.39%	39.53	61.41	6.1523	9.5570	0.9843
α	65.38%	0.45%	43.14	81.46	6.6895	12.6310	0.9807
α+βΙΙ	73.37%	9.21%	60.17	165.79	9.1853	25.3108	0.9655
α+βΙΙ	72.92%	40.33%	60.31	162.41	9.2120	24.8068	0.9660
α+βΙΙ	72.58%	58.11%	62.02	164.14	9.4682	25.0573	0.9655
βΙΙ	80.93%	99.68%	35.59	150.99	5.4658	23.1907	0.9713
βΙΙ	86.61%	99.73%	22.53	145.77	3.4707	22.4509	0.9741
βΙΙ	87.77%	99.81%	19.89	142.76	3.0654	22.0069	0.9749
βΙΙ	93.04%	99.82%	10.32	137.85	1.5943	21.2985	0.9771
3HBA, Form II	100.00%	100.00%	0.00	130.54	0.0000	20.2229	0.9798



Figure 3. Reference spectra for 3HBA Form I and II. Peak area between 1685 and 1705 cm⁻¹ were used as reference to monitor polymorphic conversion rate



Figure 4. Example of changes in Raman spectra during a form conversion (wavelength: 1800 – 1500 cm⁻¹)

Thermodynamic Modelling via NRTL

Fitting the Liquid BIPs $\Delta g_{12}^{L,\pi}$ and $\Delta g_{21}^{L,\pi}$

As mentioned in the text, for the liquid-state NRTL BIPs of 3-hydroxybenzoic acid (1) and salicylic acid (2), Δg_{12}^L and Δg_{21}^L were not expressed as functions of temperature due to the sparsity of solid-liquid equilibrium melt data (i.e., the SSLE data at the eutectic temperature). As also explained in the text, the Δg_{12}^L and Δg_{21}^L were treated separately for the equilibria involving β I and β II. Hence, we can succinctly denote the two different parameter sets as $\{\Delta g_{12}^{L,\pi}, \Delta g_{21}^{L,\pi}\}$, where π denotes the β -phase (I or II) involved in the phase equilibria.

As performed in our earlier study [Wang, Y. Ricci, F., Nordstrom, F.L., Terminal crystalline solid solutions and T-X phase diagram of salicylic acid – 4-hydroxybenzoic acid, Phys. Chem. Chem. Phys, 2024, 26, 3069.], a more in-depth study $\Delta g_{12}^{L,\pi}$ and $\Delta g_{21}^{L,\pi}$ was performed to assess the degeneracy of the liquid parameters with respect to the SSLE criteria which must be satisfied simultaneously:

$$\left\{\gamma_{i}^{\alpha}x_{i}^{\alpha}f_{i}^{S}/f_{i}^{L}=\gamma_{i}^{L}x_{i}^{L}=\gamma_{i}^{\beta\pi}x_{i}^{\beta\pi}f_{i}^{S}/f_{i}^{L}\right\}_{i=1,2}$$
(S1)

Numerically, the regression procedure requires determination of the parameters $\Delta g_{12}^{L,\pi}$ and $\Delta g_{21}^{L,\pi}$ to calculate γ_i^L (provided known values of Δg_{12}^S and Δg_{21}^S , which we obtained from regressing the solvus data to the T-dependent expressions described in the text, and hence known values of γ_i^S). This was done by driving the objective function shown below to zero:

$$OF = \sum_{i=1}^{2} (\gamma_{i}^{\alpha} x_{i}^{\alpha} f_{i}^{S} / f_{i}^{L} - \gamma_{i}^{L} x_{i}^{L})^{2} + (\gamma_{i}^{\beta\pi} x_{i}^{\beta\pi} f_{i}^{S} / f_{i}^{L} - \gamma_{i}^{L} x_{i}^{L})^{2}$$
(S2)

Because there are only two regression parameters in the above equation ($\Delta g_{12}^{L,\pi}$ and $\Delta g_{21}^{L,\pi}$), one can easily visualize how the OF varies with the parameter values. Contour plots showing this functional dependency for both the β I and β II systems are illustrated below. These contour plots were used to locate the approximate minimum of the OF, and the corresponding approximate values of $\Delta g_{12}^{L,\pi}$ and $\Delta g_{21}^{L,\pi}$ were used as initial guesses in the regression algorithm.



Figure 5. Objective function at SSLE (α - β I-L), with varying values of $\Delta g_{12}^{L,l}$ and $\Delta g_{21}^{L,l}$. The right pane shows a zoomed view, with the data cursor showing the approximate location of the minimum.



Figure 6. Objective function at SSLE (α - β II-L), with varying values of $\Delta g_{12}^{L,II}$ and $\Delta g_{21}^{L,II}$. The right pane shows a zoomed view, with the data cursor showing the approximate location of the minimum.

We also note that it was attempted to predict the α - β II T-X phase diagram using the Δg_{12}^L and Δg_{21}^L values regressed to the α - β I data (e.g., $\{\Delta g_{12}^{L,l}, \Delta g_{21}^{L,l}\}$); however, the predicted eutectic composition was in significant error. A potentially more accurate approach for using only one set of $\{\Delta g_{12}^L, \Delta g_{21}^L\}$ would be to regress these two parameters to both the α - β I and α - β II phase equilibria simultaneously.

NRTL Parameter Values

The regressed NRTL BIP values are provided below. We note once again that the non-randomness parameters (α_{ij}) were all taken as 0.2 for both the solid and liquid state models. We reiterate that the liquid state BIPS for components 1 and 2 { $\Delta g_{12}^{L,l}, \Delta g_{21}^{L,l}$ } and { $\Delta g_{12}^{L,l}, \Delta g_{21}^{L,l}$ } were regressed to SSLE data in the 1-2 system (i.e., with respect to the two solid solutions in equilibrium with the eutectic melt). The other liquid state BIPs involving the solvent (e.g., $\Delta g_{13}^{L,l}$, etc...) were regressed to the solubility data in 40 w% MeOH in H₂O, where this fixed-composition binary solvent mixture was treated as a pseudo pure solvent.

$C_{12}^{S,I} = 18185.8959 \text{ J/mol}$
$d_{12}^{S,I}$ = -32.149 J/mol-K
$c_{21}^{S,I}$ = -3747.1294 J/mol
$d_{21}^{S,I} = 41.4138 \text{ J/mol-K}$
$c_{12}^{S,II} = 11139.8254 \text{ J/mol}$
$d_{12}^{S,II}$ = -6.839 J/mol-K
$c_{21}^{S,II} = -453.2698 \text{ J/mol}$
$d_{21}^{S,II} = 28.9163 \text{ J/mol-K}$

Table	6.	NRTL	Solid	State	BIPs
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$\Delta g_{12}^{L,I}$	-5230.7972 J/mol
$\Delta g^{L,I}_{21}$	11619.6266 J/mol
$\Delta g_{13}^{L,I}$	19762.0553 J/mol
$\Delta g^{L,I}_{31}$	-6585.69442 J/mol
$\Delta g^{L,I}_{23}$	-4161.09328 J/mol
$\Delta g^{L,I}_{32}$	11119.0683 J/mol
$\Delta g_{12}^{L,II}$	-3002.0537 J/mol
$\Delta g_{21}^{L,II}$	6858.9432 J/mol
$\Delta g_{13}^{L,II}$	-9017.86118 J/mol
$\Delta g^{L,II}_{31}$	17803.6867 J/mol
$\Delta g_{23}^{L,II}$	-7094.86151 J/mol
$\Delta g^{L,II}_{32}$	18299.0624 J/mol

Table 7. NRTL Liquid State BIPs