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Supporting Information:

Selective hydrogenation of high concentration acetylene over the well-defined

crystalline sites of Pd1Cu1 and Pd1Cu3

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Figure S1. TEM images and EDS elemental mapping of the unsupported nanoparticles: (a-e) Pd₁Cu₁(NS) and (f-j) Pd₁Cu₃(NS).



Figure S2. TG profiles of the as-synthesized nanoparticles without calcination treatment.



Figure S3. XRD patterns of the PdCu/SiO₂(WI) catalysts.

Table S1. XRD peak deconvolution results of the PdCu/SiO₂(WI) catalysts.

	Alloy phases		Cu	
	Peak position	Area %	Peak position	Area %
$Pd_1Cu_1/SiO_2(WI)$	$41.4 (Pd_1Cu_1)$	43.0	43.3	57.0
$Pd_1Cu_3/SiO_2(WI)$	42.3 (Pd ₁ Cu ₃)	23.0	43.3	77.0



Figure S4. CuLMM Auger spectra of the reduced catalysts.



Figure S5. Acetylene conversion as a function of reaction temperature.

Catalyst	Temperature (°C)	Conversion (%)	C ₂ H ₄ selectivity (%)	TOF/Pd loading (S ⁻¹)	TOF/ surface site (S ⁻¹)	ln(TOF)/Pd loading (S ⁻¹)	ln(TOF)/ surface site (S ⁻¹)
Pd/SiO ₂ (WI)	22.7	19.2	47.8	0.1	10.5	-1.9	2.3
	26.3	25.0	47.3	0.2	13.7	-1.7	2.6
	31.3	33.2	48.4	0.3	18.2	-1.4	2.9
	32.3	35.2	47.4	0.3	19.2	-1.3	3.0
Pd ₁ Cu ₁ /SiO ₂ (WI)	23.9	7.5	50.2	0.06	2.1	-2.8	0.7
	33.4	11.4	50.8	0.09	3.2	-2.4	1.2
	43.4	18.5	50.3	0.1	5.2	-1.9	1.6
	53.6	28.3	49.7	0.2	7.9	-1.5	2.1
Pd ₁ Cu ₃ /SiO ₂ (WI)	38.2	4.4	50.7	0.03	1.6	-3.4	0.5
	48.2	8.2	49.5	0.06	2.9	-2.8	1.1
	58.8	14.3	50.8	0.1	5.1	-2.2	1.6
	68.9	23.5	49.5	0.2	8.4	-1.7	2.1
Pd/SiO ₂ (NS)	29.3	10.5	51.3	0.2	8.4	-1.6	2.1
	34.4	13.4	50.4	0.3	10.7	-1.4	2.4
	43.9	20.3	51.7	0.4	16.2	-0.9	2.8
	49.1	26.9	50.2	0.5	21.5	-0.7	3.1
Pd ₁ Cu ₁ /SiO ₂ (NS)	28.8	6.1	53.9	0.1	6.2	-2.4	1.8
	38.5	10.7	51.7	0.2	10.8	-1.8	2.4
	45.1	16.2	50.1	0.3	16.3	-1.4	2.8
	55	27.3	50.2	0.4	27.6	-0.9	3.3
Pd ₁ Cu ₃ /SiO ₂ (NS)	28.6	3.9	50.8	0.04	2.0	-3.3	0.7
	38.3	7.8	44.2	0.08	4.0	-2.6	1.4
	48.5	16.0	41.4	0.2	8.1	-1.9	2.1
	53.9	22.1	41.8	0.2	11.2	-1.5	2.4

Table S2. Ethylene selectivity, TOFs and ln(TOFs) (based on Pd loading and surface site normalization) for different catalysts at low conversions.



Figure S6. Selectivity of (a) ethylene, (b) ethane, (c) oligomer at the different temperature in acetylene hydrogenation.



Figure S7. The 1,3-butadiene selectivity over different catalysts with (a) conversion and (b) temperature.



Figure S8. Ethylene yield for different catalysts at different reaction temperature.

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	H^{*}	$C_2H_2^*$	${\rm C_2H_3}^*$	${\rm C_2H_4}^*$	$C_2H_5^*$	${\rm C_2H_6}^*$
Pd (111)			.66			916
$E_{\rm ads}$ /eV	-2.82	-1.40	-2.37	-0.77	-1.54	1.09
Pd ₁ Cu ₁ (111)		38	3	8		00
$E_{\rm ads}$ /eV	-2.68	-0.78	-2.06	-0.59	-1.56	-0.33
Pd ₁ Cu ₃ (111)			a contraction	8	.81	
$E_{\rm ads}$ /eV	-2.45	-0.50	-1.85	-0.47	-0.98	-0.24

Table S3. The optimized adsorption patterns of the reaction intermediates on Pd (111), Pd₁Cu₁(111), Pd₁Cu₃ (111) surface.



Figure S9. The reaction transition states on Pd(111).



Figure S10. The reaction transition states on $Pd_1Cu_1(111)$.



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