

# Supporting Information

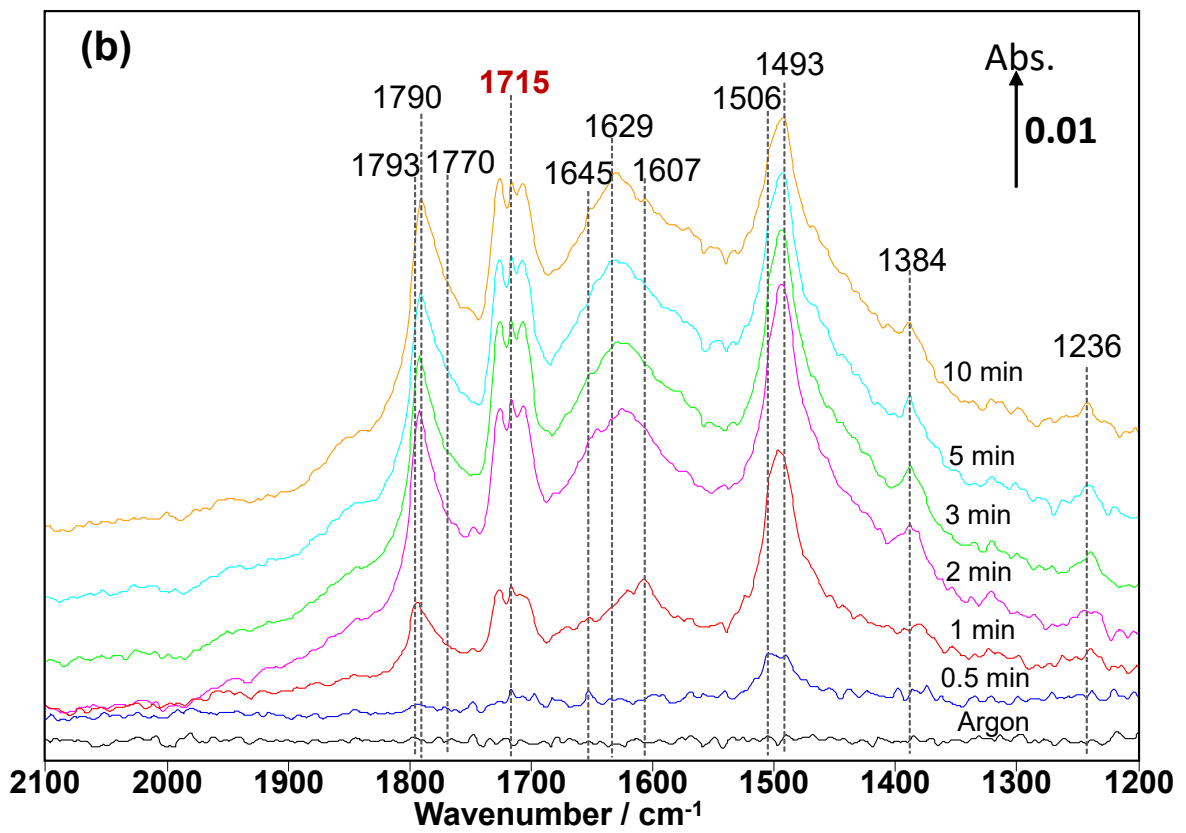
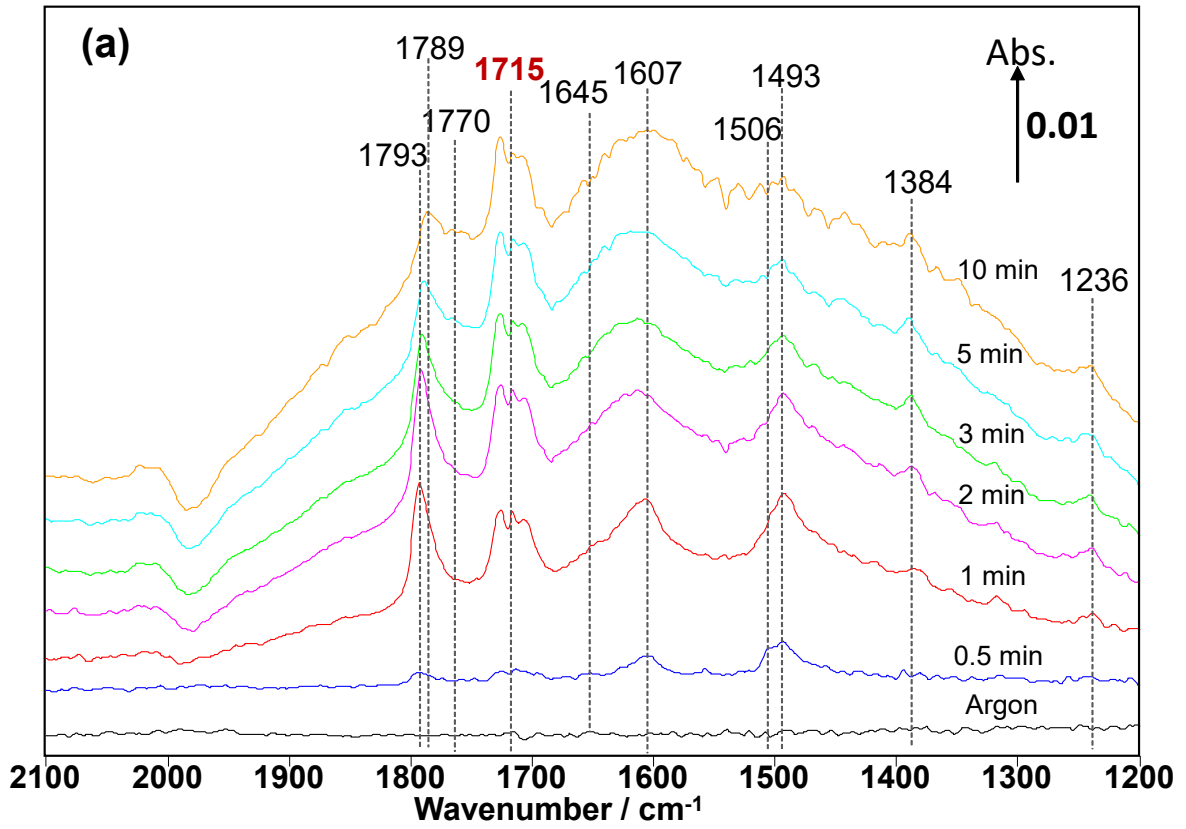
**An *in-situ* DRIFTS-MS study on elucidating the role of V  
in the selective oxidation of methacrolein to methacrylic  
acid over heteropolyacid compounds**

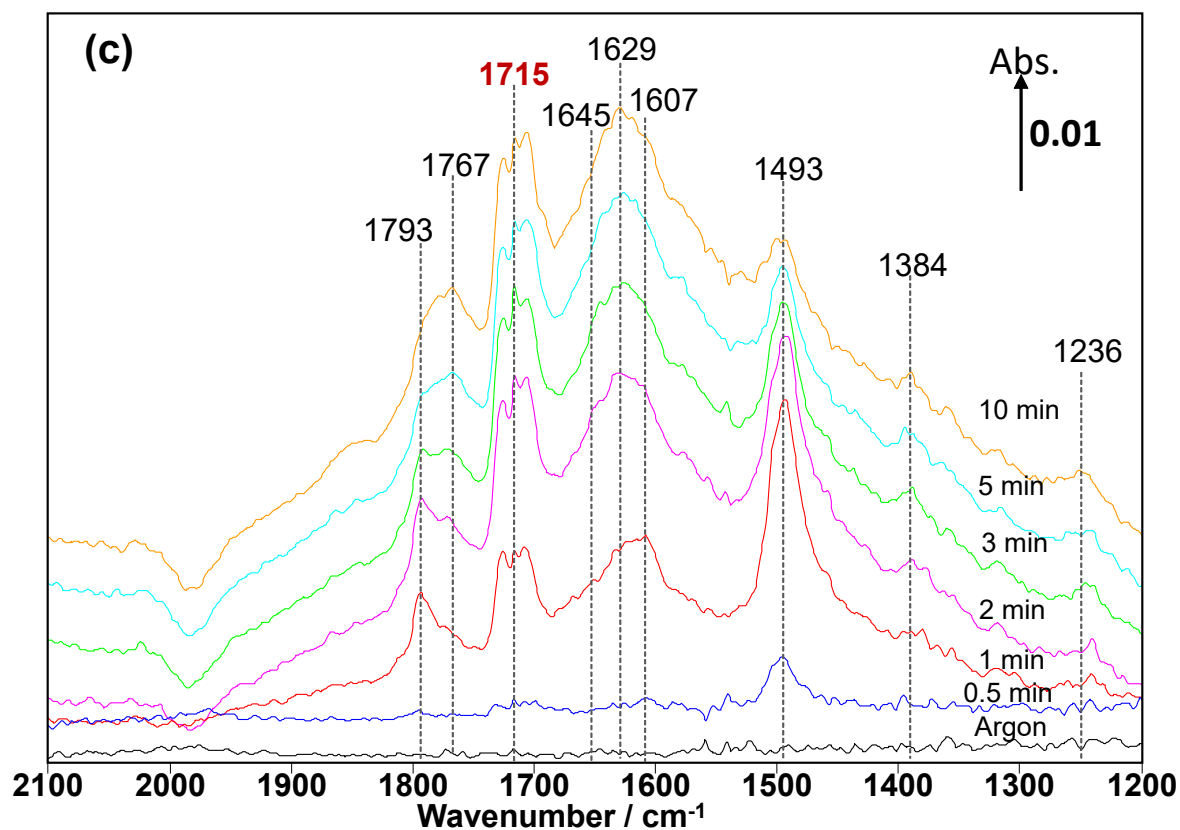
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Hardacre*<sup>a,\*</sup>**

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Manchester, Manchester M13 9PL, U.K.*

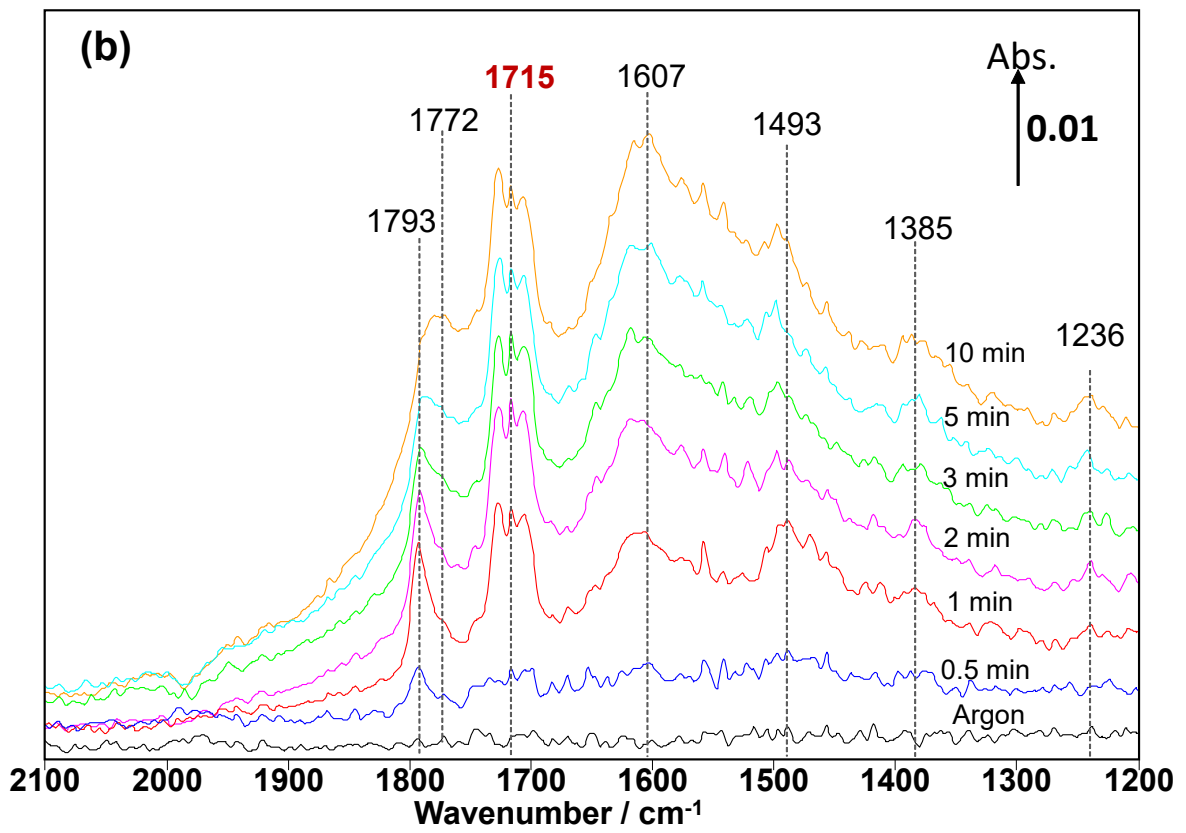
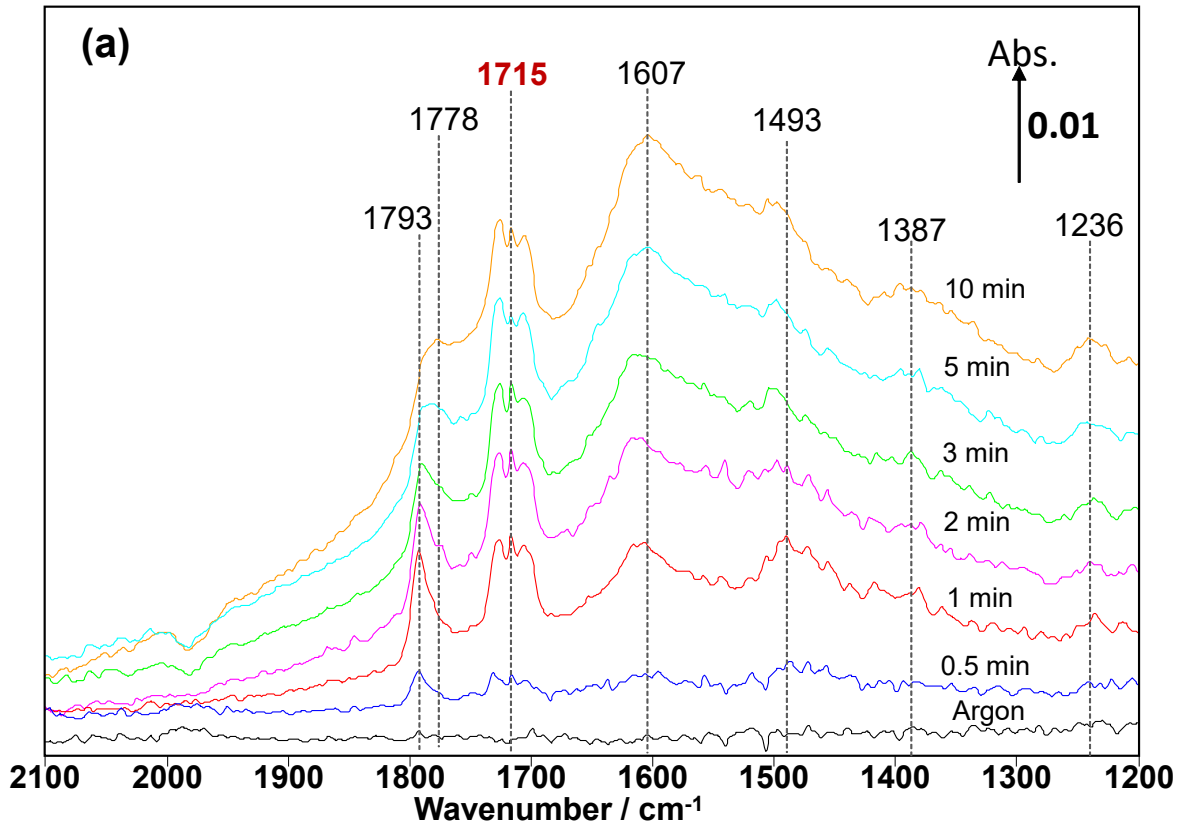
<sup>b</sup> *MMA Group, Monomers & Catalysts Laboratory, Mitsubishi Chemical Corporation, 20-1  
Miyuki-cho, Otake-shi, Hiroshima 739-0693, Japan.*

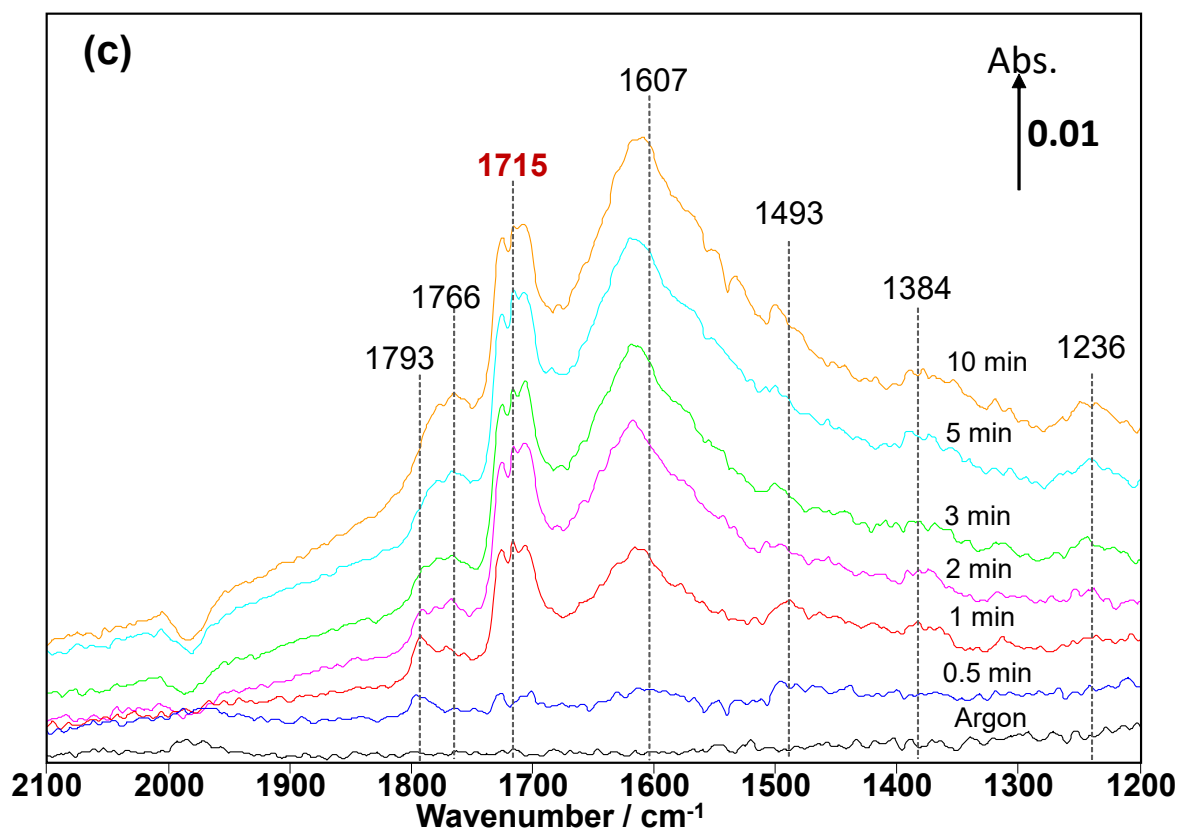
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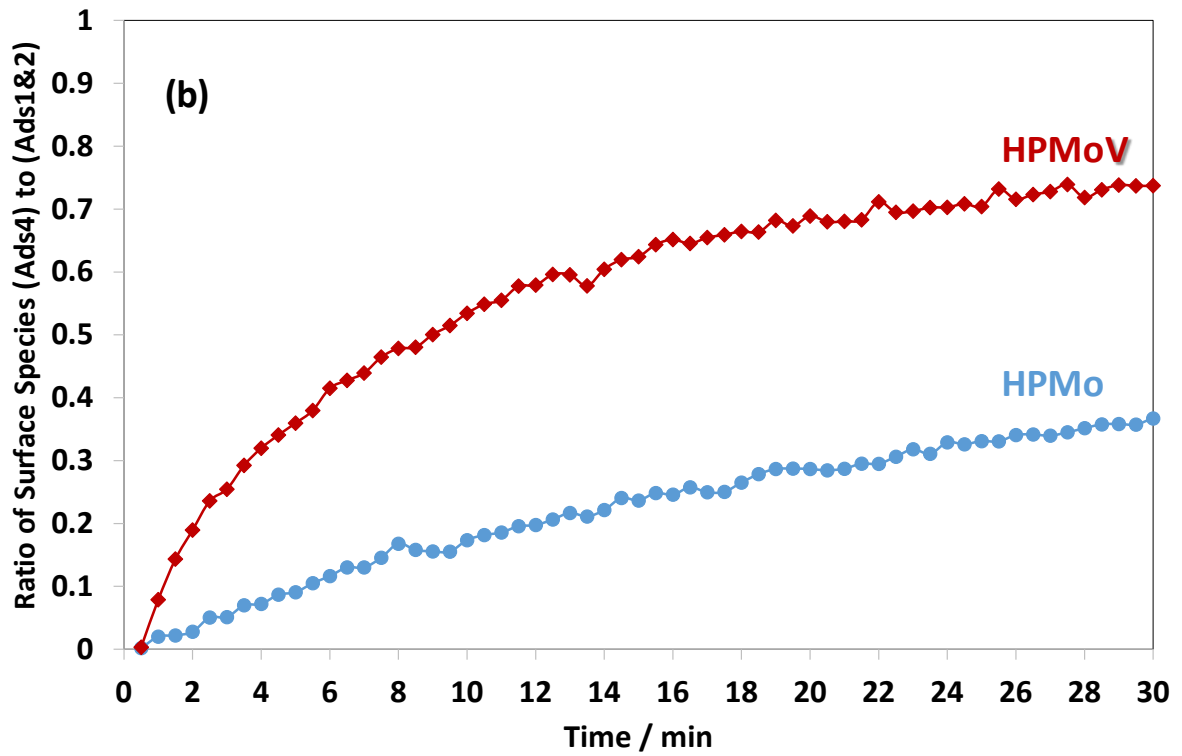
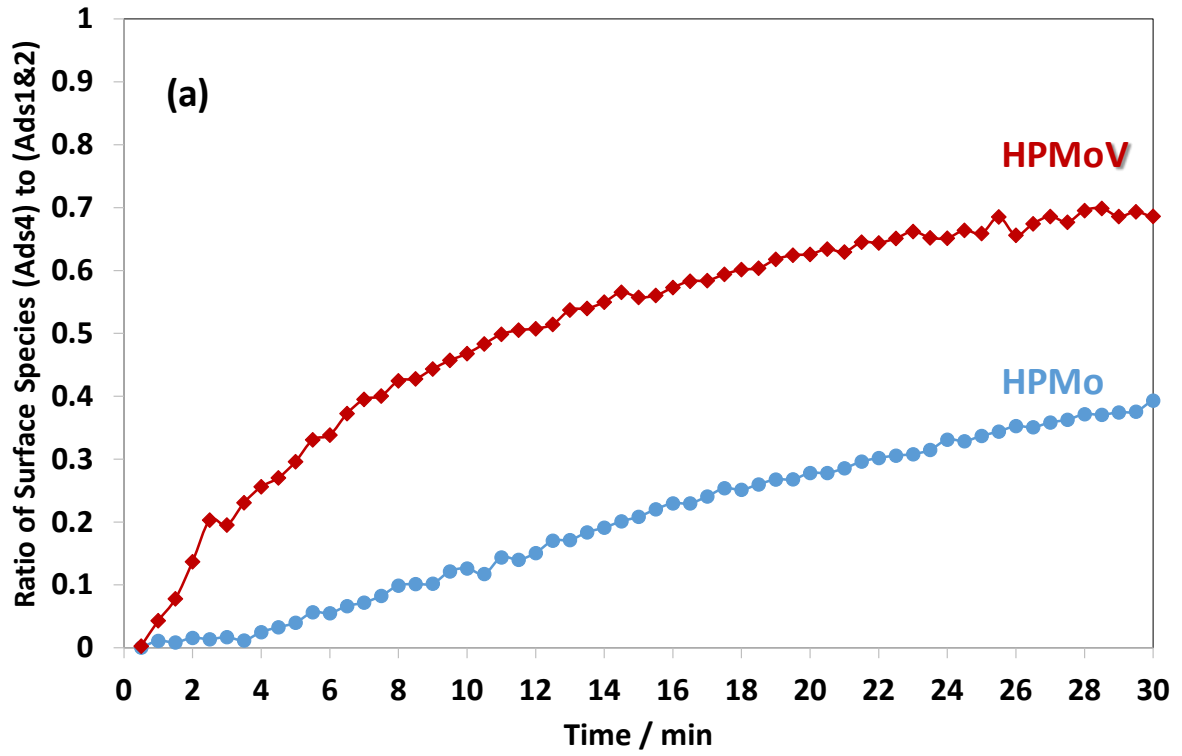


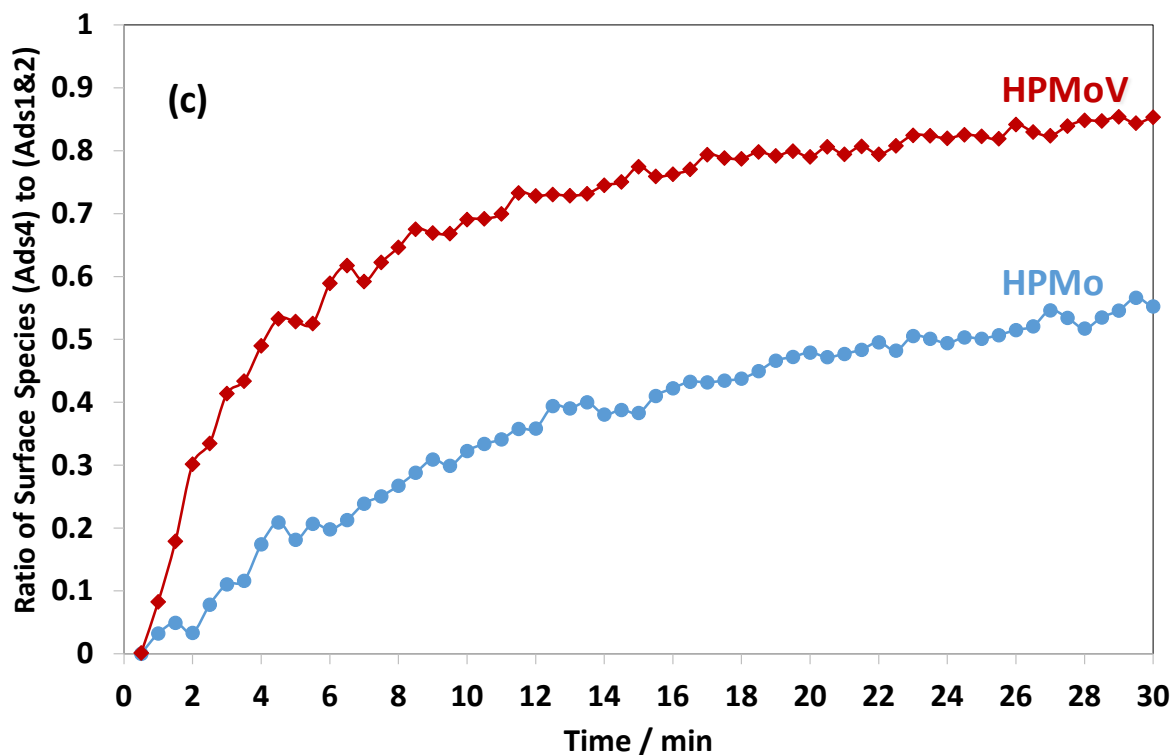
**Figure S1** Changes in *in-situ* DRIFT spectra recorded at 320 °C over **HPMo** catalyst within 10 min under MAL (a), MAL+O<sub>2</sub> (b), and MAL+O<sub>2</sub>+H<sub>2</sub>O (c). Gas feed is composed of 3500 ppm MAL (when added), 7000 ppm O<sub>2</sub> (when added), 7000 ppm H<sub>2</sub>O (when added), and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.



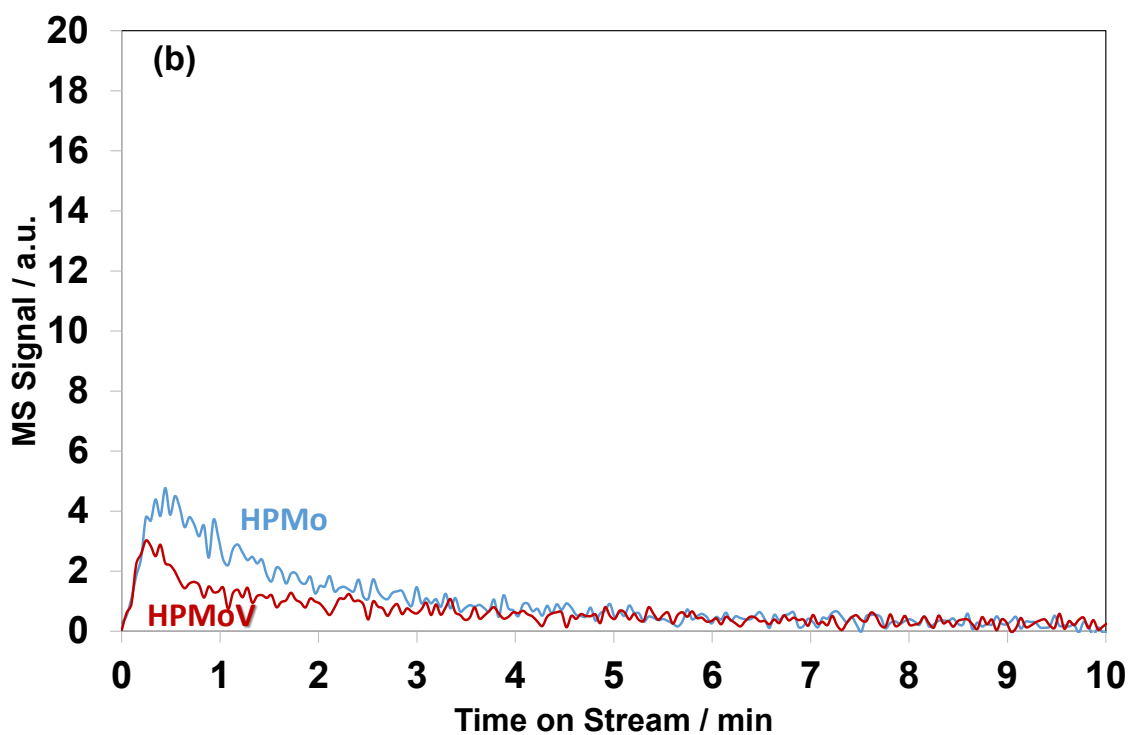
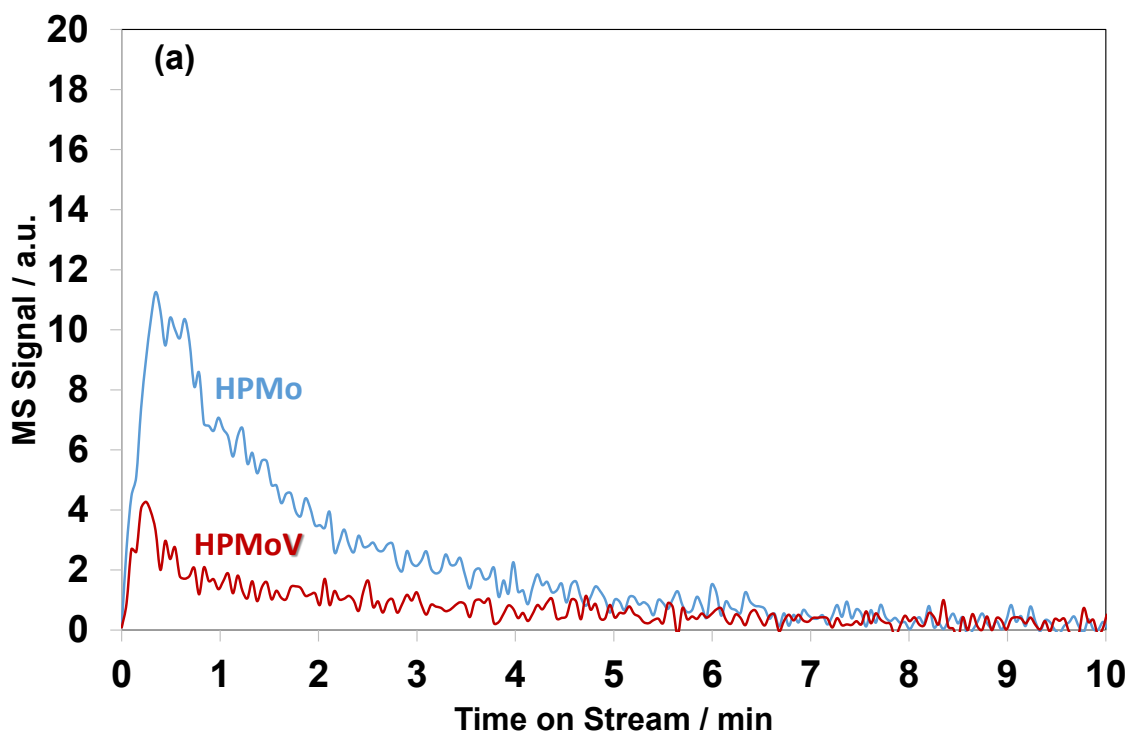


**Figure S2** Changes in *in-situ* DRIFT spectra recorded at 320 °C over **HPMoV** catalyst within 10 min under MAL (a), MAL+O<sub>2</sub> (b), and MAL+O<sub>2</sub>+H<sub>2</sub>O (c). Gas feed is composed of 3500 ppm MAL (when added), 7000 ppm O<sub>2</sub> (when added), 7000 ppm H<sub>2</sub>O (when added), and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.



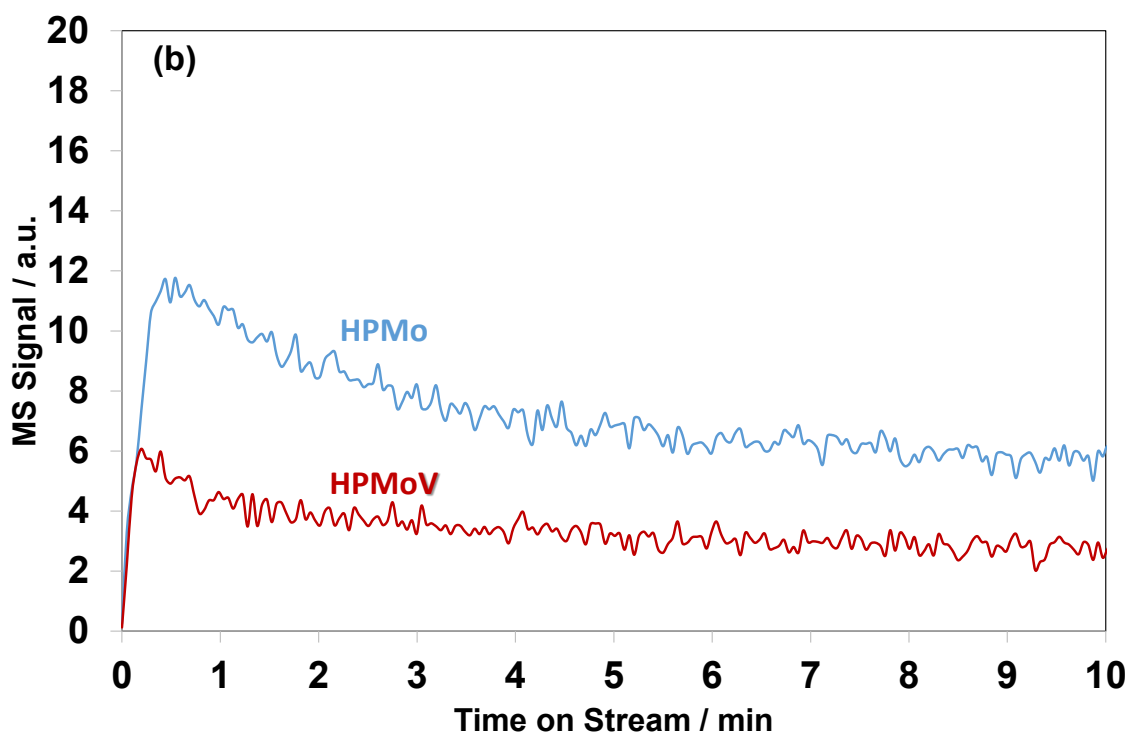
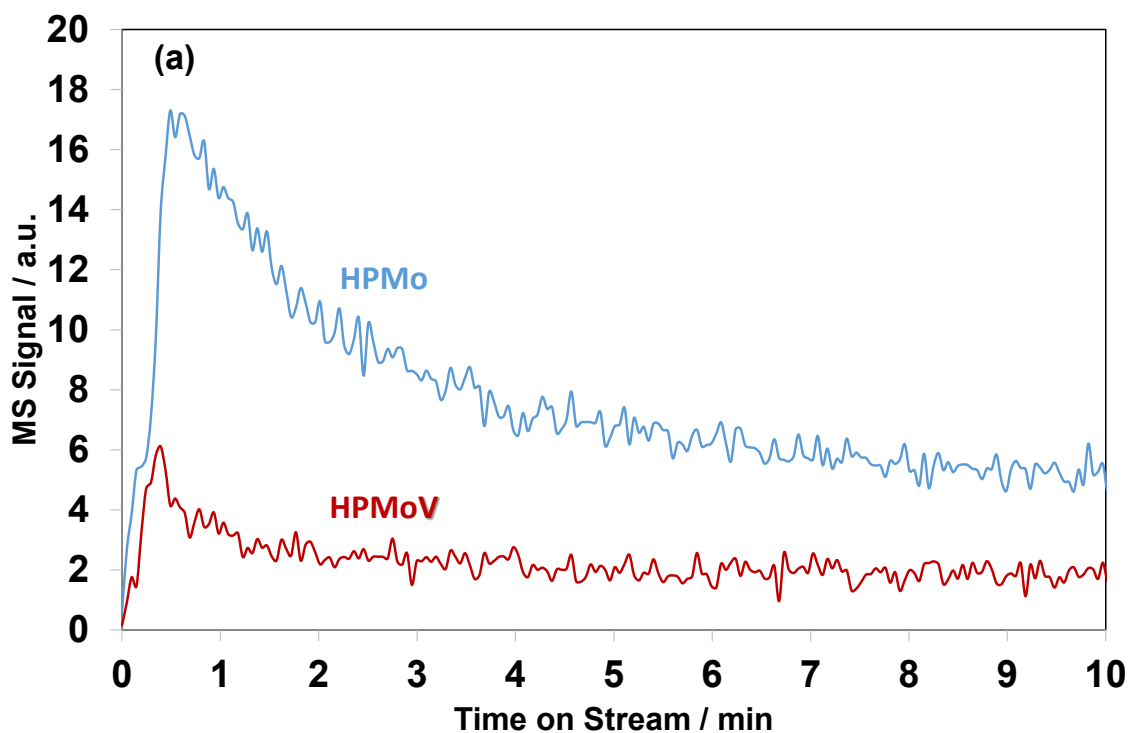


**Figure S3** Changes in ratio of monodentate methacrylate adsorbed species (**Ads4**) in the IR range of  $1780 - 1760 \text{ cm}^{-1}$  to lactone-type adsorbed species (**Ads1** and **Ads2**) in the IR range of  $1800 - 1780 \text{ cm}^{-1}$  as a function of time on stream at  $320 \text{ }^\circ\text{C}$  over HPMo and HPMoV catalysts under MAL (**a**), MAL+O<sub>2</sub> (**b**), and MAL+O<sub>2</sub>+H<sub>2</sub>O (**c**) reaction conditions. Gas feed is composed of 3500 ppm MAL (when added), 7000 ppm O<sub>2</sub> (when added), 7000 ppm H<sub>2</sub>O (when added), and Ar balance and the total flow rate is  $100 \text{ cm}^3 \text{ min}^{-1}$ .

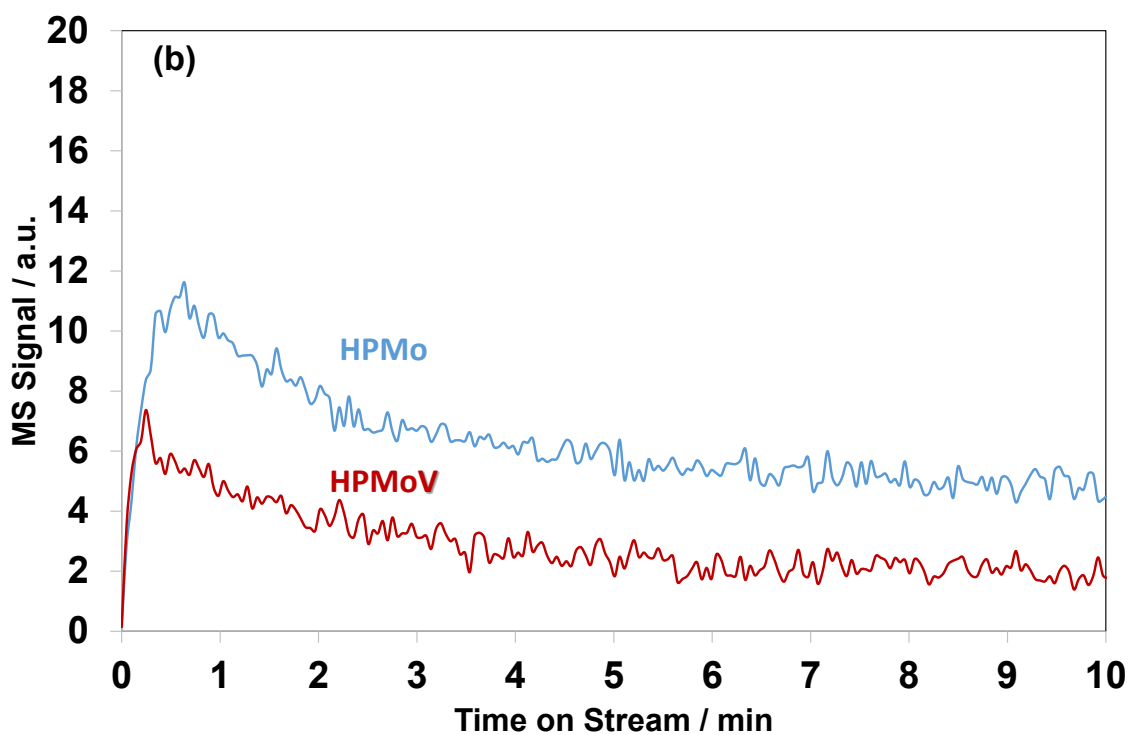
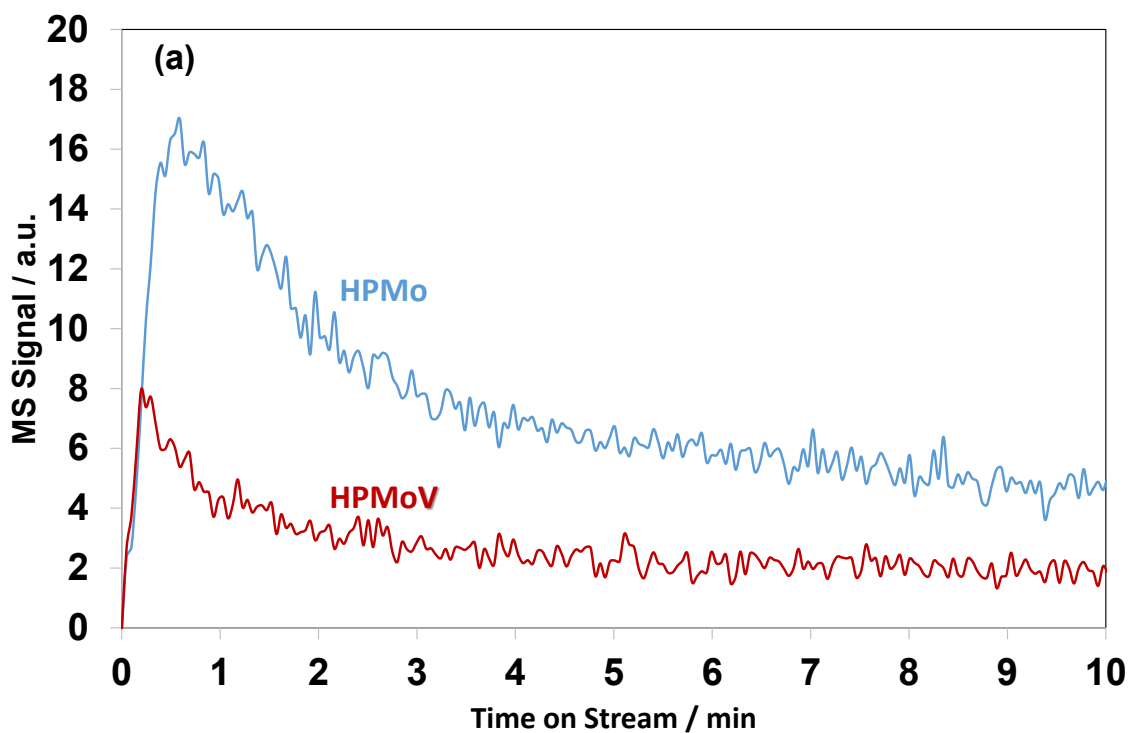


**Figure S4** Comparison of the evolution of CO (a) and CO<sub>2</sub> (b) formation as a function of time on stream at 320 °C over H<sub>3</sub>PMoO<sub>12</sub>O<sub>40</sub> (HPMo) and H<sub>4</sub>PMoO<sub>11</sub>VO<sub>40</sub> (HPMoV) under MAL adsorption. Gas feed is composed of 3500 ppm MAL and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.

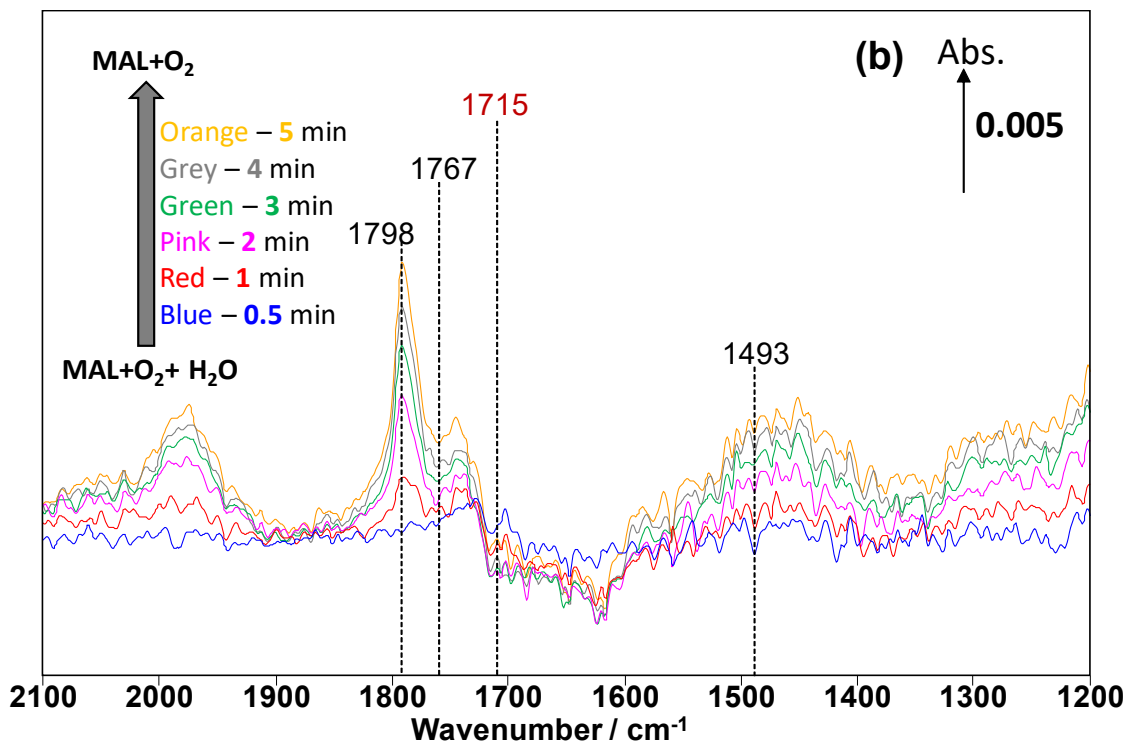
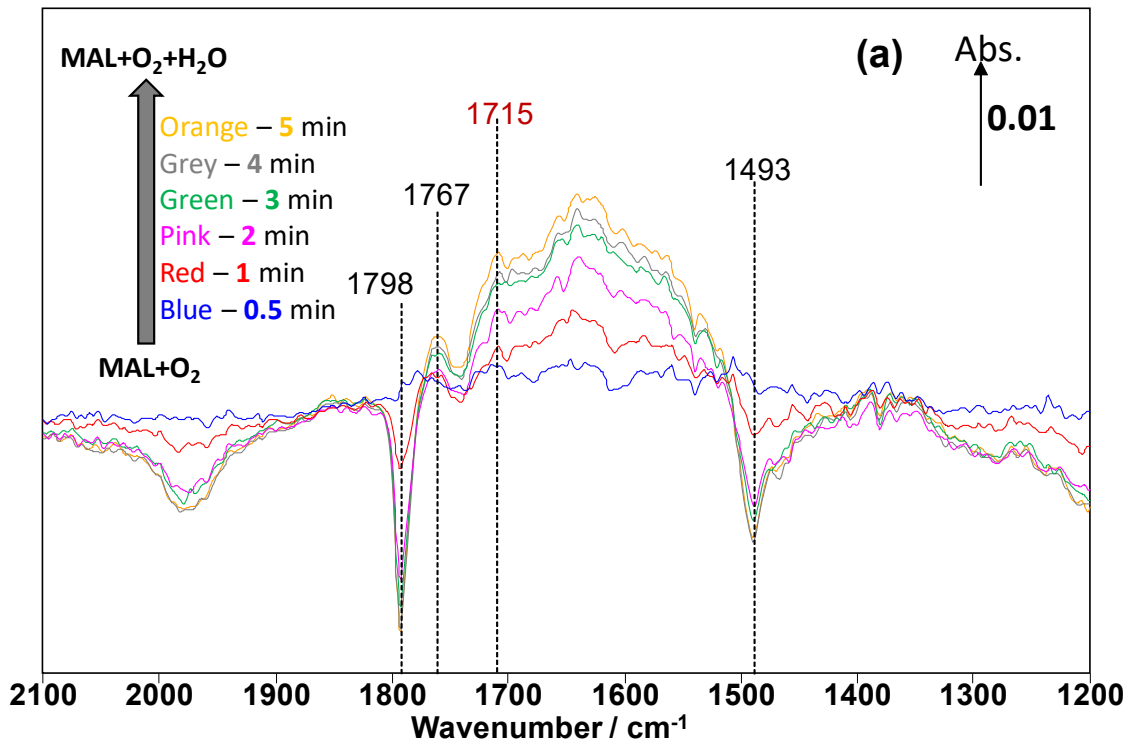


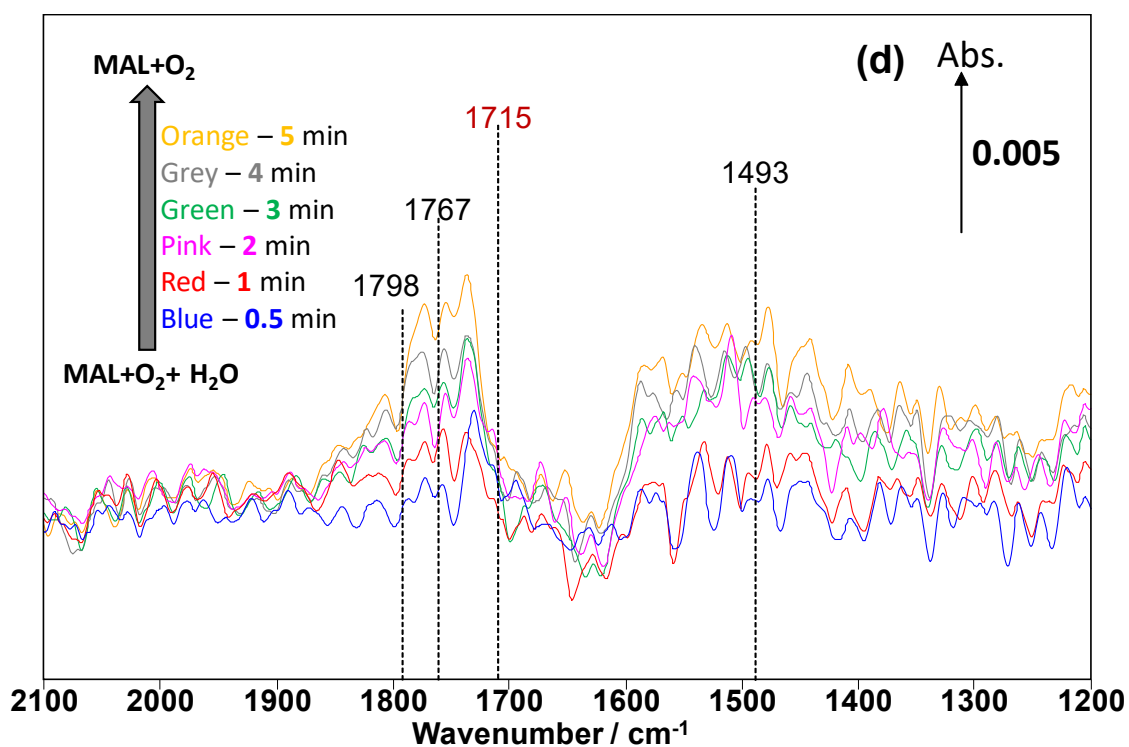
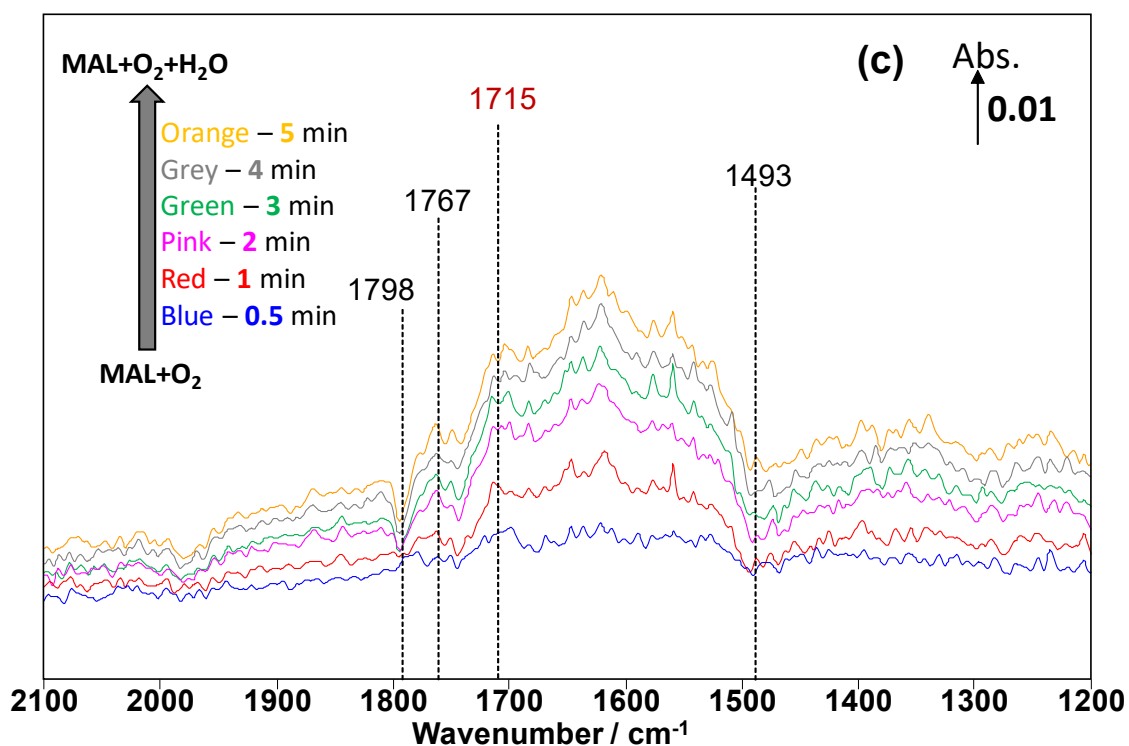


**Figure S5** Comparison of the evolution of CO (a) and CO<sub>2</sub> (b) formation at 320 °C as a function of time on stream over H<sub>3</sub>PMoO<sub>12</sub>O<sub>40</sub> (HPMo) and H<sub>4</sub>PMoO<sub>11</sub>VO<sub>40</sub> (HPMoV) under **MAL+O<sub>2</sub>** reaction. Gas feed is composed of 3500 ppm MAL, 7000 ppm O<sub>2</sub>, and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.

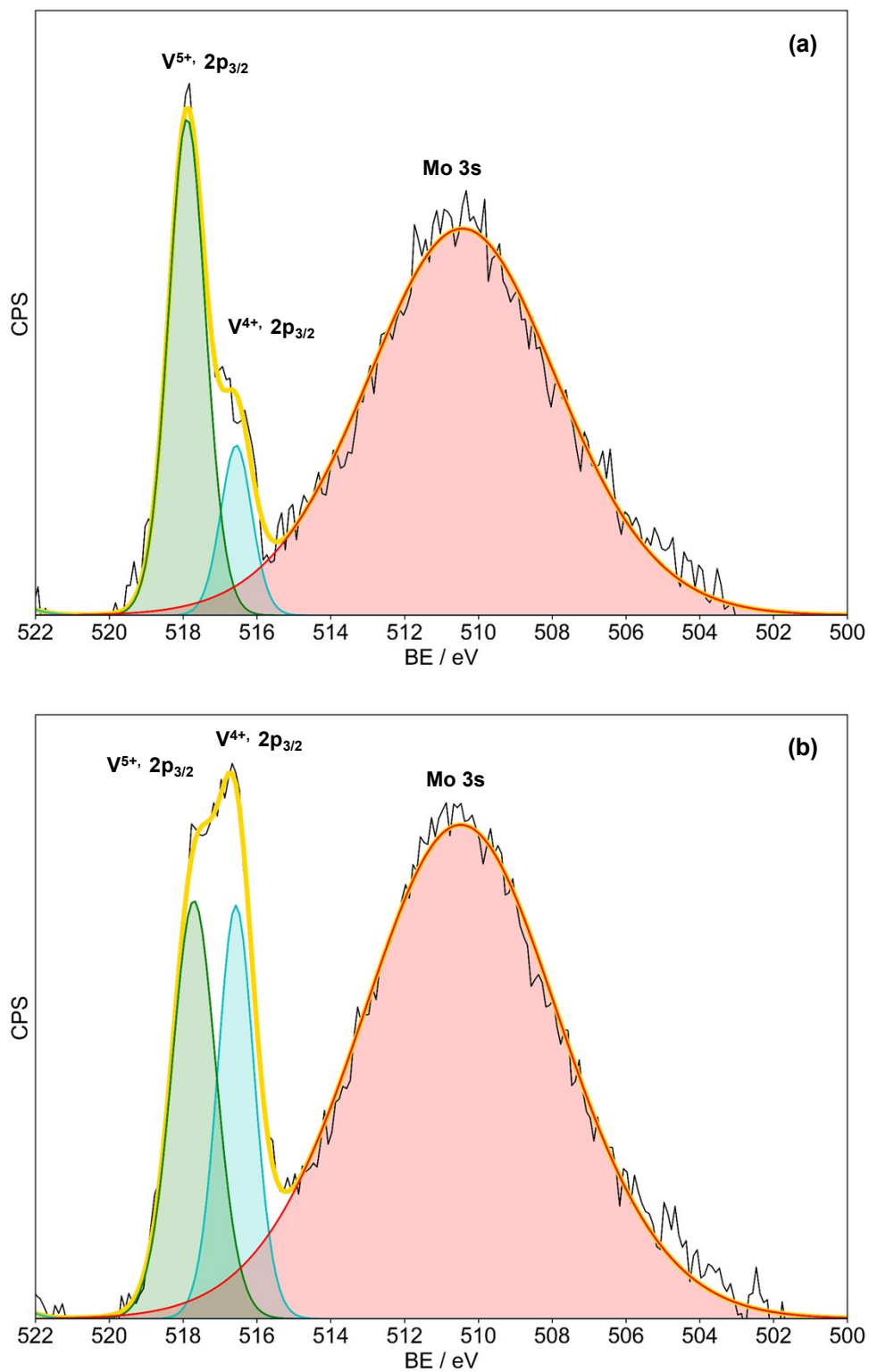


**Figure S6** Comparison of the evolution of CO (a) and CO<sub>2</sub> (b) formation at 320 °C as a function of time on stream over H<sub>3</sub>PMoO<sub>12</sub>O<sub>40</sub> (HPMo) and H<sub>4</sub>PMoO<sub>11</sub>VO<sub>40</sub> (HPMoV) under MAL+O<sub>2</sub>+H<sub>2</sub>O reaction. Gas feed is composed of 3500 ppm MAL, 7000 ppm O<sub>2</sub>, 7000 ppm H<sub>2</sub>O and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.

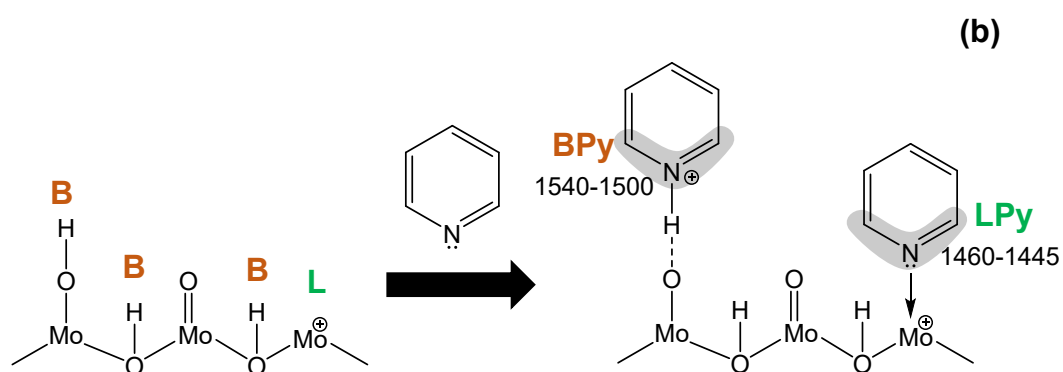
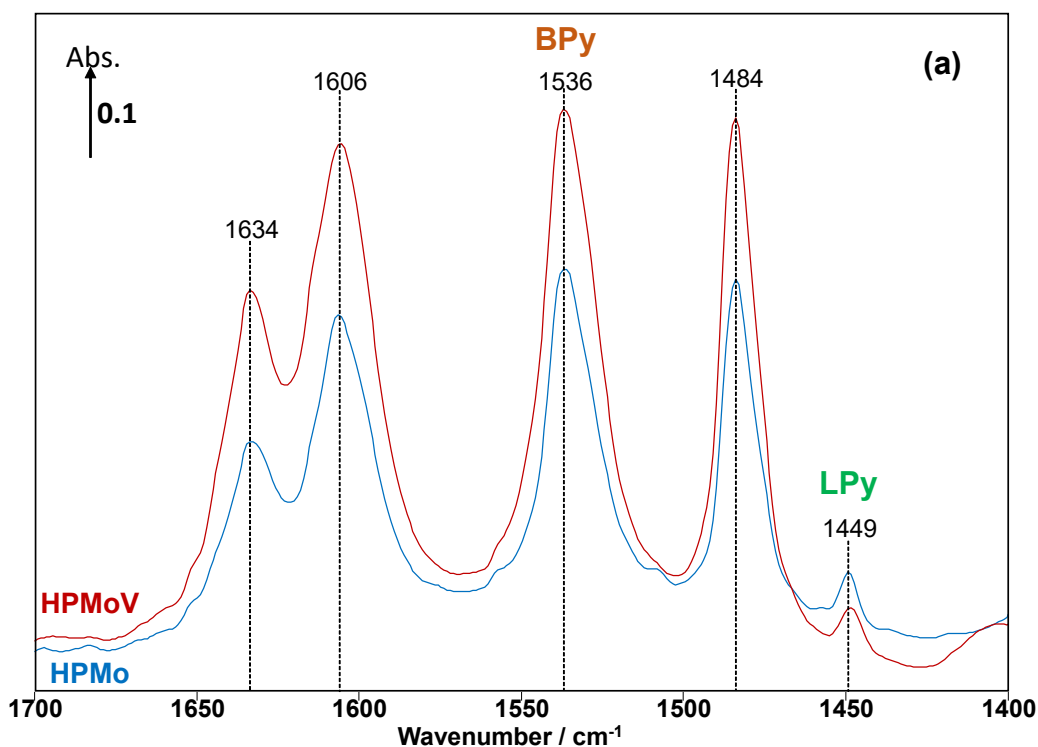




**Figure S7** Changes in *difference* DRIFT spectra ( $2100 - 1200 \text{ cm}^{-1}$ ) corresponding to the formation of MAA formation shown in Figure 3 as a function of time on stream over HPMo (a, b) and HPMoV (c,d) catalysts at  $320 \text{ }^\circ\text{C}$  during the 2<sup>nd</sup> cycle of switches of  $\text{H}_2\text{O}$  in and out of  $\text{MAL} + \text{O}_2$  gas feed. Gas feed is composed of 3500 ppm MAL, 7000 ppm  $\text{O}_2$ , 7000 ppm  $\text{H}_2\text{O}$  (when added), and Ar balance and the total flow rate is  $100 \text{ cm}^3 \text{ min}^{-1}$ .



**Figure S8** Comparison of V 2p<sub>3/2</sub> XPS spectra of H<sub>4</sub>PMoO<sub>11</sub>VO<sub>40</sub> (HPMoV) catalyst before (a) and after (b) MAL+O<sub>2</sub>+H<sub>2</sub>O reaction at 320 °C for 60 min. Gas feed is composed of 3500 ppm MAL, 7000 ppm O<sub>2</sub>, 7000 ppm H<sub>2</sub>O and Ar balance and the total flow rate is 100 cm<sup>3</sup> min<sup>-1</sup>.



**Figure S9** Comparison of *in-situ* DRIFT spectra of pyridine adsorption at 320 °C (a) at 10 min under Ar purge after pyridine adsorption at 30 °C for 60 min over  $\text{H}_3\text{PMoO}_{12}\text{O}_{40}$  (HPMo) and  $\text{H}_4\text{PMoO}_{11}\text{VO}_{40}$  (HPMoV) and the schematic representation of acid sites of heteropoly acids (b). Adsorption feed is composed of 3500 ppm pyridine and Ar balance and the total flow rate is  $100 \text{ cm}^3 \text{ min}^{-1}$ .