## Electronic supporting Information

## Highly efficient cobalt catalysts promoted by CeO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> for ammonia

## decomposition

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**Fig. S1** Temperature-dependent activities of the Co-based catalysts. (a)  $CoCeO_x$  catalysts with different Co/Ce ratio; (b)  $CoCeAlO_x$  catalysts with different Ce/Al ratio; (c)  $Co_9RE_{0.5}Al_{0.5}O_x$  catalysts with different rare earth elements (Sm, Y, La, Ce); (d)  $Co_{4.5}Ni_{4.5}Ce_{0.5}Al_{0.5}O_x$  and  $Co_9Ce_{0.5}Al_{0.5}O_x$ 

To investigate the impact of component concentrations on the ammonia decomposition reaction, we assessed the reactivity of the catalysts with different mole ratios of Co, Ce and Al element. As the ratio of Co:Ce decreased (Fig. S1a), a pronounced decline in activity of the  $Co_aCe_bO_x$  catalysts occurred. Therefore, it inferred that cobalt species was the main active species for ammonia decomposition, whilst ceria acted as an assisting promoter. From Fig. S1b, it could be observed that the second round NH<sub>3</sub> conversion of  $Co_9Ce_{0.8}Al_{0.2}O_x$  decreased by approximately 9% as the mole ratio reduced from 0.5 to 0.2. This indicated the vital role of alumina in preserving stability of activity. Additionally, the catalysts obtained by replacing Ce with other rare earth elements delivered inferior activity compared to CoCeAlO<sub>x</sub>, demonstrating the unique advantages of Ce for applying in ammonia decomposition reaction (Fig. S1c). And  $Co_{4.5}Ni_{4.5}Ce_{0.5}Al_{0.5}O_x$  showed lower activity than  $Co_9Ce_{0.5}Al_{0.5}O_x$  (Fig. S1d).



Fig. S2 TEM images of the as-prepared samples. (a) CoCeO<sub>x</sub>; (b) CoAlO<sub>x</sub>; (c) CoCeAlO<sub>x</sub>; (d) Co<sub>3</sub>O<sub>4</sub>



Fig. S3 TEM images of the used samples. (a) CoCeO<sub>x</sub>; (b) CoAlO<sub>x</sub>; (c) CoCeAlO<sub>x</sub>



Fig. S4 The EDS elemental mappings of the CoCeAlO<sub>x</sub> sample after long-term stability tests



**Fig. S5** The physical properties of the catalysts. (a, c) The  $N_2$  adsorption-desorption isotherms of the as-prepared (a) and used (c) samples; (b, d) BJH pore size distributions of the as-prepared (b) and used (d) samples



Fig.S6 The Raman spectra of the samples after long-term stability tests



Fig.S7 Arrhenius plots for the catalysts (CoCeAlO<sub>x</sub>, CoCeO<sub>x</sub> and CoAlO<sub>x</sub>) in the kinetic range



Fig. S8 The Reaction orders of the  $N_2$  for CoCeAlO<sub>x</sub>, CoCeO<sub>x</sub> and CoAlO<sub>x</sub>



**Fig. S9** The desorption signals of  $H_2$  (m/z=2) in NH<sub>3</sub>-TPD over CoCeAlO<sub>x</sub>, CoCeO<sub>x</sub>, CoAlO<sub>x</sub> and Co<sub>3</sub>O<sub>4</sub> catalysts.

The  $H_2$  signal of all related samples was shown in Fig. S9. It exhibited poor data quality, causing no efficient information could be obtained. The greater capacity of CoCeAlO<sub>x</sub> for the suppression of hydrogen poisoning could be clearly concluded by the reaction order of  $H_2$  (Fig. 7b).

 Samples	Co loading (wt%)	Ce loading (wt%)	Al loading (wt%)	_
 CoCeAlO <sub>x</sub>	60.0	7.4	2.4	_
CoCeO <sub>x</sub>	58.1	13.1	_	
CoAlO <sub>x</sub>	66.6	—	5.8	

 Table S1
 The ICP-AES results of various samples.

Catalysts	Surface area (m <sup>2</sup> g <sup>-1</sup> ) <sup>a</sup>	Size of Co $_3O_4$ (nm) $^{\rm b}$	Size of CeO $_2$ (nm) $^{\rm b}$
CoCeAlO <sub>x</sub>	119.4	8.7	\
CoAlO <sub>x</sub>	83.3	15.2	١
CoCeO <sub>x</sub>	54.0	9.6	5.4
C0 <sub>3</sub> O <sub>4</sub>	46.6	17.1	١

 Table S2 Physical properties of the as-prepared samples.

a Measured by  $N_2$  adsorption-desorption experiments.

b Evaluated by XRD results using Debye-Scherrer equation.

Catalysts	Surface area (m <sup>2</sup> g <sup>-1</sup> ) <sup>a</sup>	Size of Co (nm) $^{\rm b}$	Size of CeO <sub>2</sub> (nm) $^{\rm b}$
CoCeAlO <sub>x</sub>	40.1	10.3	١
CoAlO <sub>x</sub>	30.0	15.3	١
CoCeO <sub>x</sub>	38.2	21.2	9.1
C0 <sub>3</sub> O <sub>4</sub>	5.7	32.0	١

 Table S3 Physical properties of the used samples.

a Measured by N<sub>2</sub> adsorption-desorption experiments.

b Evaluated by XRD results using Debye-Scherrer equation.

	Binding Energy (eV)		
Samples	Co <sup>3+</sup>	Co <sup>2+</sup>	Co <sup>o</sup>
CoCeAlO <sub>x</sub>	779.8, 794.8	781.5, 796.5	778.3, 793.3
CoCeO <sub>x</sub>	779.8, 794.8	781.5, 796.5	778.4, 793.4
CoAlO <sub>x</sub>	780.1, 795.1	781.8, 796.8	778.3, 793.3

Table S4 The peak center of different Co species ( $Co^{3+}$ ,  $Co^{2+}$ ,  $Co^{0}$ ) in XPS.

	Binding Energy (eV)		
Samples	Ce <sup>3+</sup>	Ce <sup>4+</sup>	
CoCeAlO <sub>x</sub>	903.9, 899.0, 885.4, 880.5	916.3, 907.3, 900.7, 897.8, 888.8, 882.2	
CoCeO <sub>x</sub>	903.9, 899.3, 885.4, 880.8	916.3, 907.6, 900.7, 897.8, 889.1, 882.2	

Table S5 The peak center of different Ce species ( $Ce^{3+}$ ,  $Ce^{4+}$ ) in XPS.

Catalysts	Co <sup>0</sup> /(Co <sup>3+</sup> +Co <sup>2+</sup> +Co <sup>0</sup> )	Ce <sup>3+</sup> /(Ce <sup>3+</sup> +Ce <sup>4+</sup> )
CoCeAlO <sub>x</sub>	19.1%	34.5%
CoAlO <sub>x</sub>	22.1%	١
CoCeO <sub>x</sub>	16.0%	27.5%

Table S6 The elements and surface composition analyzed by the XPS data of the used catalysts