Supporting information

Role of Zn in enhancing CO₂ hydrogenation to methanol over Zn_xZrO_y catalysts

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Section 1. SEM-EDX

Table S1. Catalysts' composition measured by SEM-EDX.

	wt.%	ZrO ₂	Zn _{0.01} ZrO _y - 500	Zn _{0.07} ZrO _y - 500	Zn _{0.19} ZrO _y - 500	Zn _{0.28} ZrO _y - 500	Zn _{0.44} ZrO _y - 500	Zn _{0.56} ZrO _y - 500	Zn _{0.19} ZrO _y - 550	Zn _{0.19} ZrO _y - 700	Zn _{0.19} ZrO _y - 800
	Zn		1.19	5.54	11.52	14.77	35.19	37.77	11.36	10.67	9.76
a*	Zr	40.46	48.44	44.25	33.35	29.53	25.94	20.56	41.25	40.11	41.42
	0	59.54	50.37	50.21	55.13	55.7	38.87	41.67	47.38	49.22	48.82
	Zn/Zr		0.02	0.13	0.35	0.50	1.36	1.84	0.28	0.27	0.24
	Zn		0.25	4.12	8.75	11.58	27.81	31.63	9.16	8.1	7.15
b*	Zr	62.21	67.98	64.6	53.55	50.43	44.83	36.64	60.7	60.79	61.89
	0	37.79	31.78	31.27	37.7	37.99	27.36	31.73	30.14	31.11	30.96
	Zn/Zr		0.00	0.06	0.16	0.23	0.62	0.86	0.15	0.13	0.12
	Zn		0.15	3.25	7.31	10.71	23.74	28.71	7.57	6.79	6.19
c*	Zr	73.17	78.27	74.81	64.58	60.3	55.08	46.73	70.13	70.5	71.08
	0	26.83	21.58	21.94	28.11	28.99	21.18	24.56	22.3	22.71	22.73
	Zn/Zr		0.00	0.04	0.11	0.18	0.43	0.61	0.11	0.10	0.09
	Zn		2.09	2.64	6.74	9.42	21.1	25.33	6.39	5.92	5.39
d*	Zr	79.82	61.8	80.1	71.21	66.79	61.31	53.28	76.14	75.87	77.15
	0	20.18	36.12	17.26	22.05	23.8	17.59	21.39	17.47	18.21	17.46
	Zn/Zr		0.03	0.03	0.09	0.14	0.34	0.48	0.08	0.08	0.07

	Atomic %	ZrO ₂	Zn _{0.01} ZrO _y - 500	Zn _{0.07} ZrO _y - 500	Zn _{0.19} ZrO _y - 500	Zn _{0.28} ZrO _y - 500	Zn _{0.44} ZrO _y - 500	Zn _{0.56} ZrO _y - 500	Zn _{0.19} ZrO _y - 550	Zn _{0.19} ZrO _y - 700	Zn _{0.19} ZrO _y - 800
	Zn		0.49	2.28	4.42	5.61	16.55	16.96	4.85	4.43	4.09
a*	Zr	10.65	14.36	13.08	9.17	8.03	8.74	6.62	12.61	11.95	12.42
	0	89.35	85.15	84.64	86.41	86.36	74.7	76.43	82.55	83.62	83.49
	Zn/Zr		0.03	0.17	0.48	0.70	1.89	2.56	0.38	0.37	0.33
	Zn		0.14	2.31	4.35	5.71	16.19	16.86	5.21	4.53	4.02
b*	Zr	22.4	27.25	25.98	19.08	17.81	18.71	14	24.74	24.37	24.91
	0	77.6	72.62	71.71	76.57	76.49	65.1	69.14	70.04	71.1	71.07
	Zn/Zr		0.01	0.09	0.23	0.32	0.87	1.20	0.21	0.19	0.16
	Zn		0.10	2.22	4.34	6.21	15.85	17.66	5.08	4.52	4.13
с*	Zr	32.35	38.84	36.59	27.48	25.07	26.36	20.6	33.74	33.66	33.96
	0	67.65	61.06	61.19	68.18	68.72	57.79	61.74	61.17	61.82	61.92
	Zn/Zr		0.00	0.06	0.16	0.25	0.60	0.86	0.15	0.13	0.12
	Zn		0.35	2.02	4.56	6.09	15.41	16.78	4.83	4.4	4.08
d*	Zr	40.97	40.03	43.96	34.51	30.98	32.09	25.3	41.23	40.37	41.88
	0	59.03	59.62	54.02	60.93	62.93	52.5	57.92	53.94	55.23	54.03
	Zn/Zr		0.01	0.05	0.13	0.20	0.48	0.66	0.12	0.11	0.10

* a, b, c, and d sets are measured at 5, 10, 15, and 20 kV electron beam energy, respectively.

Energy dispersive X-ray analysis (EDX) was employed to analyze the composition of the catalyst materials. The observed loading closely corresponds to the targeted values for the Zn/Zr ratio up to 0.28, as indicated in Table S1. However, at higher loadings, the detected amount of Zn on the catalysts near the surface exceeds the nominal values. This discrepancy is likely attributed to the separation of ZnO from the mixed oxide lattice, a finding supported by X-ray diffraction (XRD) and nitrogen physisorption results. Furthermore, the zinc concentration exhibits a decreasing trend as the voltage of the measurements increases. This suggests that zinc is less incorporated in the bulk of the metal oxide, indicating a surface enrichment of Zn.

Section 2. Raman spectroscopy

The phase assignment in the XRD profiles was confirmed by Raman spectroscopy (Fig. 2). Broad bands at 273, 467, and 652 cm⁻¹ indicate the fluorite-like cubic structure ¹ for $Zn_{0.19}ZrO_{y}$ -500 and $Zn_{0.19}ZrO_{y}$ -700, with the 467 cm⁻¹ band corresponding to the Zr^{4+} -O stretch.² The band at 320 cm⁻¹ is associated with a pseudo-cubic phase, where cations maintain a cubic structure while oxygen atoms undergo tetragonal distortion.¹ Upon calcination at 800 °C, the Raman spectrum changes considerably. New peaks corresponding to characteristic bands of the monoclinic and tetragonal phases dominate, centered respectively at 185, 192, 340, 386, 480, 566, 582, 615, 645 cm⁻¹ and 227, 456, 506 cm⁻¹.¹⁻³



Section 3. N₂ physisorption

Fig. S1 N₂ adsorption-desorption isotherm of (a) Zn_xZrO_y-500 catalysts and (b) Zn_{0.19}ZrO_y-T calcined at 500, 550, 700, and 800 °C. Pore size distribution of (c) Zn_xZrO_y-500 catalysts and (d) Zn_{0.19}ZrO_y-T calcined at 500, 550, 700, and 800 °C.

Section 4. XPS

The Zr 3d spectra of ZrO_2 and $Zn_{0.19}ZrO_{y}$ -800 were deconvoluted, considering the presence of both monoclinic and tetragonal phases, with a constant FWHM of 1.84 eV. Deconvolution of $Zn_{0.07}ZrO_{y}$ -500, $Zn_{0.19}ZrO_{y}$ -500, and $Zn_{0.19}ZrO_{y}$ -700 XPS spectra with a constant FWHM of 1.84 eV revealed a peak at higher binding energies compared to the tetragonal phase, attributed to the formation of the cubic phase, and the emergence of a peak at 181.3 eV, assigned to Zn-O-Zr species. The broadening of the peaks in these samples was fitted with additional peaks at lower binding energies.

The Zn 2p spectra were deconvoluted considering the emergence of the Zn²⁺ peak at 1021.3 eV and keeping the FWHM constant at 2.0. The peak broadening at higher binding energies was fitted with a peak assigned to $Zn^{(2+\delta)^+}$ species, while the peak broadening at lower binding energies was fitted with additional peaks attributed to $Zn^{(2-\delta)^+}$ species.

		Zn	2p _{3/2}				Zr 3d _{5/2}	0 1s				
Catalyst	Zn ⁽²⁻ δ)+	Zn ²⁺	Zn-O-Zr	Zn ^{(2+δ)+}	Zr ^{(4-δ)+}	Zr-O-Zn	Zr ⁴⁺ - m	Zr ⁴⁺ - t	Zr ⁴⁺ - c	O _{sublayer}	O _{lattice}	O _{chemisor} bed surface
ZrO ₂ (t-m)					27.3%		49.0%	23.6%		23.2%	52.5%	24.4%
Zn _{0.07} Zr- 500 (c)	24.0%	46.8%	29.2%		16.1%	29.2%			54.7%	15.6%	58.7%	25.7%
Zn _{0.19} Zr- 500 (c)	38.6%	26.3%	35.1%		34.7%	35.5%			29.8%	45.2%	40.2%	14.6%
Zn _{0.19} Zr- 700 (c)	16.9%	27.1%	39.6%	16.4%	10.1%	40.9%			49.0%	16.8%	52.8%	30.3%
Zn _{0.19} Zr- 800 (t-m)	43.6%	56.4%						34.5%	65.5%	24.6%	50.4%	25.0%

Table S2. Details of the peak deconvolution of the Zn 2p, Zr 3d, and O 1s XPS spectra.



Fig. S2 Effect of calcination temperature on surface Zn/Zr ratio (from XPS).

The O 1s spectra are presented in Fig. S3, revealing spectral contributions at approximately 529-530 eV with two shoulders at lower and higher binding energies. The peaks observed at binding energies of 529-530 eV are identified as lattice oxygen ions (O^{2-}). In contrast, the peak at higher binding energy is attributed to weakly charged surface chemisorbed oxygen species, such as surface hydroxyl groups or oxygen vacancies.⁴ The peak at lower binding energy (527.6 eV) can be assigned to physically adsorbed oxygen species⁵ or oxygen atoms that are in subsurface layers (due to differences in their

chemical environment). The relative percentage of each oxygen component is summarized in Table S2. After Zn addition, the peaks shift to higher binding energies, representing the binding energy of O atoms in different crystal phases of ZrO_2 . The emergence of low-energy O 1s species at 526.4 eV likely arises from the charge transfer between the neighboring O^{2-} , Zn^{2+} , and Zr^{4+} species ⁶ due to the formation of a mixed metal oxide.^{5,7} Increasing the Zn/Zr ratio to 0.19 raises the ratio of low energy O 1s peaks while increasing the calcination temperature enhances the binding energy of the O 1s species.



Fig. S3 Deconvoluted XPS spectra of O 1s in ZrO_2 (t + m), $Zn_{0.07}ZrO_{y}$ -500 (c), $Zn_{0.19}ZrO_{y}$ -500 (c), $Zn_{0.19}ZrO_{y}$ -700 (c), and $Zn_{0.19}ZrO_{y}$ -800 (t + m).

Section 5. CO₂-TPD

Table S3. Peak deconvolution of CO₂-TPD profiles.

		Peak 1	Peak 2	Peak 3	Total basicity
	T °C	122	347	412	
ZnO	CO ₂ (µmol g ⁻¹)	0.54	0.22	0.83	1.59
	CO ₂ (µmol m ⁻²)	0.02	0.01	0.03	0.05
	Т°С	104	159	280	
ZrO ₂ -500	CO ₂ (µmol g ⁻¹)	3.29	3.84	6.83	13.96
	CO ₂ (µmol m ⁻²)	0.12	0.14	0.26	0.52
	Т°С	101	153	264	
Zn _{0.01} ZrO _y -500	CO ₂ (µmol g ⁻¹)	3.44	3.81	8.91	16.17
	CO ₂ (µmol m ⁻²)	0.13	0.14	0.34	0.61
	Т°С	109	160	250	
Zn _{0.07} ZrO _y -500	CO ₂ (µmol g ⁻¹)	5.68	4.92	12.71	23.31
	CO ₂ (µmol m ⁻²)	0.16	0.14	0.35	0.65
	Т°С	107	154	231	
Zn _{0.19} ZrO _y -500	CO ₂ (µmol g ⁻¹)	6.55	5.03	14.75	26.33
	CO ₂ (µmol m ⁻²)	0.21	0.16	0.47	0.84
	Т°С	113	162	248	
Zn _{0.28} ZrO _y -500	CO ₂ (µmol g ⁻¹)	9.46	8.43	26.60	44.48
	CO ₂ (µmol m ⁻²)	0.33	0.29	0.92	1.54
	Т°С	96	140	208	
Zn _{0.44} ZrO _y -500	CO ₂ (µmol g ⁻¹)	1.24	0.72	3.37	5.32
	CO ₂ (µmol m ⁻²)	0.07	0.04	0.19	0.30
	Т°С	112	162	260	
Zn _{0.56} ZrO _y -500	CO₂ (µmol g⁻¹)	0.94	0.91	1.91	3.76
	CO ₂ (µmol m ⁻²)	0.07	0.07	0.15	0.29
	Т°С	104	148	235	
Zn _{0.19} ZrO _y -550	CO ₂ (µmol g ⁻¹)	6.41	4.25	16.20	26.86
	CO ₂ (µmol m ⁻²)	0.19	0.13	0.48	0.79
	Т°С	104	151	263	
Zn _{0.19} ZrO _y -700	CO ₂ (µmol g ⁻¹)	8.64	7.57	21.68	37.88
	CO ₂ (µmol m ⁻²)	0.94	0.82	2.36	4.12
	Т°С	120	187	271	
Zn _{0.19} ZrO _y -800	CO ₂ (µmol g ⁻¹)	0.99	0.82	0.82	2.64
	CO_2 (µmol m ⁻²)	0.90	0.75	0.75	2.40



Fig. S4 Deconvolution of CO_2 -TPD profiles of (a) Zn_xZrO_y -500 catalysts and (b) $Zn_{0.19}ZrO_y$ -T calcined at 500, 550, 700, and 800 °C, and (c) ZnO. (Black full lines: measured data, dotted lines: deconvoluted data, and orange dash line: envelope)

Section 6. DRIFTS



Fig. S5 Evolution of surface species during CO₂ adsorption on ZrO₂ and Zn_{0.19}ZrO_y at 325 °C and 10 bar over 40 minutes.

Table S4. Comparison of Zn _x ZrO _y catalysts' performance in literature.										
Catalyst	T, °C	P, bar	GHSV, ml g ⁻¹ h ⁻¹	H ₂ :CO ₂	CO₂ conversion, %	Methanol selectivity, %	Methanol STY, g g _{cat} -1 h-1	reference		
$Zn_{0.19}ZrO_{\gamma}$	325	45	21000	3	4	82	0.20	This study		
20%ZnO-ZrO ₂	320	20	24000	4	4	82	0.20	1		
Zn _{0.2} ZrO _x	320	50	24000	4	4	86	0.24	2		
13%ZnZrO _x	320	20	24000	3	4	85	0.23	3		
13%ZnO-ZrO ₂	320	50	24000	3	10	86	0.50	4		
ZnZr25	325	10	3600	3	8	40	0.04	5		
15%ZnZr	300	40	12000	3	3	85	0.11	6		
13%ZnZrO _x	320	50	24000	4	7	83	0.25	7		
ZnO/ZrO ₂ -F *	320	30	24000	4	6	74	0.30	8		
ZnZrO _x	330	45	10800	3	6	78	0.18	9		
25%ZnZrO _x	350	30	4000	3	12	86	0.15	10		

Section 7. Zn_xZrO_v in literature

*hollow nano-frame

Section 8. Catalyst stability

The stability of the $Zn_{0.19}ZrO_y$ -500 catalyst was assessed in CO_2 hydrogenation (Fig. S6). The effect of reaction temperature was studied by increasing the temperature from 350 °C to 400 °C, maintaining each temperature for 4 hours, and then decreasing the temperature back to 350 °C to determine if the same activity could be obtained. The result shows that the catalyst remains stable under these reaction conditions.



Fig. S6 Stability test of $Zn_{0.19}ZrO_{y}$ -500 in CO₂ hydrogenation to methanol at 45 bar, H₂:CO₂:Ar=3:1:1, and GHSV= 21000 Nml g_{cat}^{-1} h⁻¹.



Section 9. Parameters correlation

Fig. S7 Effect of (a) surface area on CO₂ conversion and (b) pore volume on methanol selectivity at 350 °C, 45 bar, H₂:CO₂:Ar=3:1:1, and GHSV= 21000 Nml g_{cat} ⁻¹ h⁻¹ (blue colour: pure cubic-phase, grey colour: cubic-phase + h-ZnO, and orange colour: the rest of the samples).

Fig. S8 reveals the negative effect of ZnO formation on catalyst performance within the cubic-phase samples.



Fig. S8 Comparison of the performance of the cubic-phase catalysts at 350 °C, 45 bar, H_2 :CO₂:Ar=3:1:1, and GHSV= 21000 Nml g_{cat} ⁻¹ h⁻¹.

The amount of CO_2 adsorption correlates with the surface Zn/Zr ratio (Fig. S9a). However, the increasing surface ratio of Zn/Zr and the consequently increased CO_2 adsorption do not directly relate to the methanol formation rate. Methanol formation peaks at a narrow Zn/Zr ratio of 0.18-0.22 and an adsorbed CO_2 range of 23.3-26.3 µmol g⁻¹ (Fig. S9a and b).



Fig. S9 Effect of surface Zn/Zr ratio on (a) CO₂ adsorption capacity, and (b) methanol formation at 350 °C, 45 bar, H₂:CO₂:Ar=3:1:1, and GHSV= 21000 Nml $g_{cat}^{-1} h^{-1}$.

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