

Electronic Supplementary Information

for

Oxidation of 1, 2-propanediol to methyl lactate over hydroxyapatite-supported Au-Cu catalysts with varying Ca/P ratios

Junying Tian ^a, Yingying Fan ^a, Tao Wei ^a, Qingxia Guo ^a, Weiguo Fang ^a, Yuanyuan Cong ^a,

Dongqiang Zhang ^a, Yongle Guo ^{a,*}

^a School of Petrochemical Technology, Lanzhou University of Technology, Lanzhou 730050, Gansu, China

^b Lanzhou Jinchuan Precious Metal Materials Co., Ltd. Lanzhou 730100, Gansu, China

* Corresponding author · E-mail: ylguo@lut.edu.cn

CAPTIONS

- Fig.S1** (a) N₂ adsorption–desorption isotherms of supports. (the Y values of different curves were displayed with different offset) (b) Barrett–Joyner–Halenda pore size distribution curves of supports with different Ca/P ratios. (c) N₂ adsorption–desorption isotherms of catalysts. (the Y values of different curves were displayed with different offset) (d) Barrett-Joyner-Halenda pore size distribution curves for catalysts with different support Ca/P ratios.....S3
- Fig.S2** The particle size results after Au-Cu/HAP-2 used.....S4

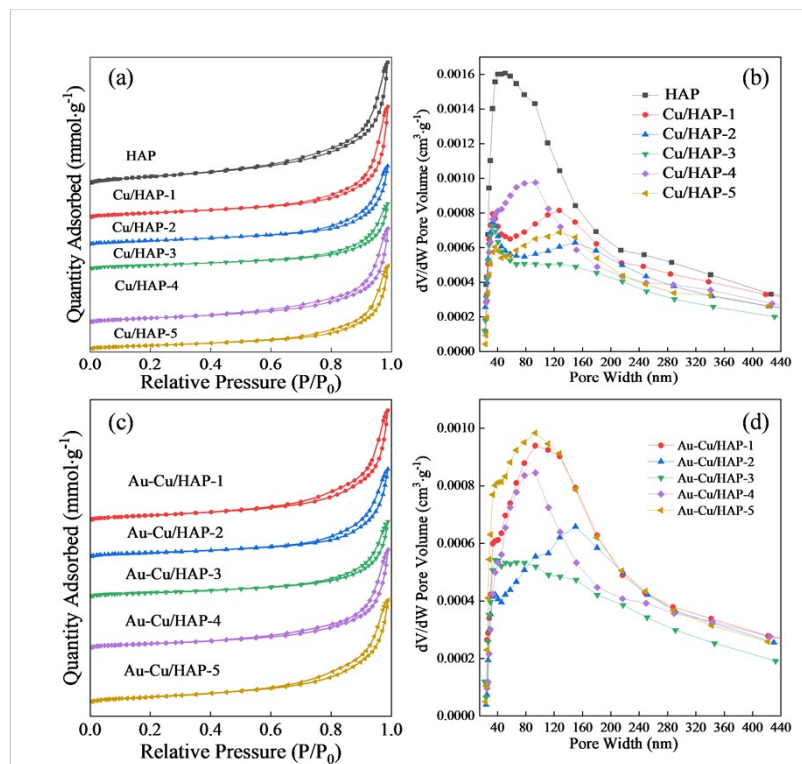


Fig. S1 (a) N₂ adsorption–desorption isotherms of supports. (the Y values of different curves were displayed with different offset) (b) Barrett–Joyner–Halenda pore size distribution curves of supports with different Ca/P ratios. (c) N₂ adsorption–desorption isotherms of catalysts. (the Y values of different curves were displayed with different offset) (d) Barrett–Joyner–Halenda pore size distribution curves for catalysts with different support Ca/P ratios.

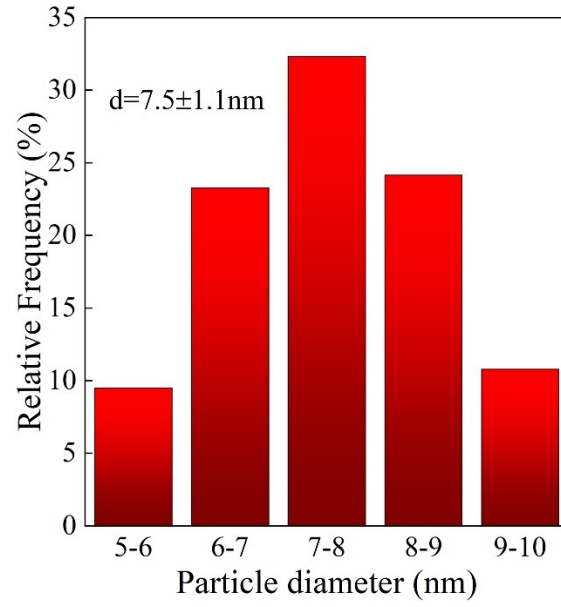


Fig. S2 The particle size results after Au-Cu/HAP-2 used