# Study of the self-degradation performance of a passive direct methanol fuel cell with Fe-N-C catalyst

Chenjun Hou<sup>a</sup>, Weijian Yuan<sup>a,\*</sup>, Shilong Gao<sup>b</sup>, Yujun Zhang<sup>a</sup>, Yufeng Zhang<sup>a</sup>, and

Xuelin Zhang<sup>a,\*</sup>

a School of Astronautics, Harbin Institute of Technology, Harbin, China

b State Key Laboratory of Organic-Inorganic Composites, Beijing Advanced

Innovation Center for Soft Matter Science and Engineering, Beijing University of

Chemical Technology, Beijing, 100029, People's Republic of China

E-mail: ywj@hit.edu.cn (Weijian Yuan); zhangxuelin@hit.edu.cn (Xuelin Zhang)

# **Supporting Information**

# 1. Experiment

## 1.1 Chemicals

Aniline (99.0% purity) and monocyanamide (49.0% purity) were purchased from Aladdin. hydrochloric acid (HCl, 37%) was purchased from Kermel, and carbon black BP2000 was donated by Cabot Corp. Ferric chloride (FeCl<sub>3</sub>, 98% purity) and ammonium persulfate ((NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub>, 98% purity) were purchased from Alfa Aesar.

#### 1.2 Synthesis of Fe-N-C catalysts

2 ml aniline and 3 ml monocyanamide were dissolved in 80 ml 1.5 M HCl, and 0.4 g carbon black with 3 g FeCl<sub>3</sub> were dispersed in 80 ml 1.5 M HCl. The above two solutions were mixed, and then 5 g  $(NH_4)_2S_2O_8$  dissolved in 80 ml 1.5 M HCl was added. After polymerization, a heat treatment in 900 °C under N<sub>2</sub> for 1 h was conducted, and the product was pre-leached in 2 M H<sub>2</sub>SO<sub>4</sub> at 90 °C for 5 h. The pre-leached powder then underwent a second heat treatment under N<sub>2</sub> for 2.5 h and under NH<sub>3</sub> for 0.5 h in 900 °C.

#### **1.3 Characterizations**

Scanning electron microscope (SEM) was conducted to observe the morphology of prepared catalysts, and X-ray diffraction (XRD) and Raman spectroscopy were performed to analyze the physical structures and disordered degree of catalysts separately. N<sub>2</sub> adsorption/desorption test was applied to character the porous structures of catalysts, and X-ray photoelectron spectroscopy (XPS) measurement was utilized to research the chemical components of catalysts.

### **1.4 Electrochemical measurements**

The system of electrochemical measurement was composed of a glassy carbon working electrode, a platinum foil counter electrode and an Hg/Hg<sub>2</sub>SO<sub>4</sub> reference electrode. The working electrodes were prepared by coating the catalyst ink onto the surface of glassy carbon electrode. Particularly, 15 mg Fe-N-C catalyst, 525  $\mu$ L ethanol and 145  $\mu$ L Nafion solution (5%) were mixed and stirred for 30 minutes, and then, 7  $\mu$ L catalyst ink was applied onto the working electrode, making the loading of Fe-N-C catalyst 800  $\mu$ g cm<sup>-2</sup>. As a comparison, 5 mg 40% Pt/C catalyst, 1.21 mL isopropanol and 40  $\mu$ L Nafion were well mixed, and 5  $\mu$ L of catalyst ink was coated on the working electrode, making the loading of Pt 80  $\mu$ g cm<sup>-2</sup>.

Electron transfer numbers can be calculated according to the Koutecky-Levich (K-L) equation, which can be expressed as:

$$1/j = 1/j_k + 1/j_d = 1/j_k + 1/(0.62nFD^{2/3}v^{-1/6}C\omega^{1/2})$$
(1)

where *j* is the total current density,  $j_k$  is the kinetic current density and  $j_d$  is the diffusion limiting current density. K-L equation relates the liming current density measured in RDE tests and the number of electron transfer (*n*), the rotation speed ( $\omega$ ) and other parameters including *F*, the Faraday constant (96485 C mol<sup>-1</sup>); *D*, the diffusion coefficient of oxygen (1.93\*10<sup>-5</sup> cm<sup>2</sup> s<sup>-1</sup>); *v*, the electrolyte kinematic viscosity (1\*10<sup>-2</sup> cm<sup>2</sup> s<sup>-1</sup>); and *C*, the bulk oxygen concentration (1.26\*10<sup>-3</sup> mol dm<sup>-3</sup>). For rotating ring disk electrode (RRDE) test, the ring potential was kept as 1.2 V vs RHE, and the H2O2 yield was calculated according to the Equation (2):

$$\%H_{2}O_{2} = 100 \cdot \frac{\frac{2I_{r}}{N}}{I_{d} + \frac{I_{r}}{N}}$$
(2)

where:  $I_{d}$ ,  $I_{r}$  and N represent the disk current, the ring current and the ring collection

efficiency (0.37). RRDE tests were performed under 1600 rpm at 10 mV s<sup>-1</sup>.

# 2. Figures



Fig. S1 Polarization curves of Pt/C based DMFC at 60 °C.



Fig. S2 Discharging curve of a DMFC with a constant current density of 100 mA cm<sup>-2</sup>
within 12 hours (a); Polarization curves of a DMFC before and after the stability test
(b). The working temperature is 60 °C and the methanol concentration is 3 M.



Fig. S3 Polarization curves of Pt/C based DMFC after stationary over several days.

The concentration of supplied methanol is 3 M and the temperature is 60 °C.



Fig. S4 Pore size contribution curve of prepared Fe-N-C catalyst



Fig. S5 LSV curves of catalysts tested in O<sub>2</sub>-satuarated 0.1M HClO<sub>4</sub>.



Fig. S6 Koutecky-Levich plots of Fe-N-C tested in O2-satuarated 0.1 M HClO4



Fig. S7 H<sub>2</sub>O<sub>2</sub> yield of the prepared Fe-N-C catalyst in O<sub>2</sub>-satuarated 0.1 M HClO<sub>4</sub>



Fig. S8 I-t curves of Pt/C catalyst and Fe-N-C catalyst tested in O<sub>2</sub>-satuarated 0.1 M

HClO<sub>4</sub> at 0.5 V vs RHE.



Fig. S9 SCV curves of Fe-N-C based electrode tested in  $O_2$ -satuarated 0.1M HClO<sub>4</sub>

with the addition of methanol.

Cathode	Anode	Reactant	Reactant Performance		
$5.0 \text{ mg/cm}^2$	4.0mg/cm <sup>2</sup>	3M CH <sub>3</sub> OH 1mL/min	80°C		
50% Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$130 \text{ mW/cm}^2$	1	
$2.5 \text{mg/cm}^2$	$1.0 \text{ mg/cm}^2$	2M CH <sub>3</sub> OH 1mL/min	90°C	2	
50% Nafion	Pt/C	O <sub>2</sub> ,200 mL/min	$20 \text{ mW/cm}^2$		
$4.5 \text{ mg/cm}^2$	$1.0 \text{ mg/cm}^2$	10M CH <sub>3</sub> OH2mL/min	90°C	3	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$48 \text{ mW/cm}^2$		
$2.5 \text{ mg/cm}^2$	$2.5 \text{ mg/cm}^2$	5M CH <sub>3</sub> OH 2mL/min	110°C	4	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	11.2 mW/cm <sup>2</sup>		
$4.0 \text{ mg/cm}^2$	$1.0 \text{ mg/cm}^2$	2M CH <sub>3</sub> OH 2mL/min	90°C	5	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$10.5 \text{ mW/cm}^2$		
$3.0 \text{ mg/cm}^2$	$1.0 \text{ mg/cm}^2$	10M CH <sub>3</sub> OH 2mL/min	90°C	6	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$22 \text{ mW/cm}^2$		
$7.4 \text{ mg/cm}^2$	$1.0 \text{ mg/cm}^2$	10M CH <sub>3</sub> OH 2mL/min	90°C	7	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$30 \text{ mW/cm}^2$	,	
$5.0 \text{ mg/cm}^2$	$2.0 \text{ mg/cm}^2$	1M CH <sub>3</sub> OH 2mL/min	80°C	8	
66.7%Nafion	PtRu/C	O <sub>2</sub> ,400 mL/min	$32 \text{ mW/cm}^2$		
4.0mg/cm <sup>2</sup>	$1.5 \text{ mg/cm}^2$	2M CH <sub>3</sub> OH 20mL/min	50°C	9	
25%Nafion	PtRu/C	O <sub>2</sub> ,500 mL/min	$20.9 \text{ mW/cm}^2$		
$4.0 \text{ mg/cm}^2$	$4.0 \text{ mg/cm}^2$	10M CH <sub>3</sub> OH 2mL/min	90°C	10	
45%Nafion	PtRu/C	O <sub>2</sub> ,100 mL/min	$60 \text{ mW/cm}^2$		
$5.0 \text{ mg/cm}^2$	$2.0 \text{ mg/cm}^2$	5M CH <sub>3</sub> OH 10mL/min	20°C	11	
50%Nafion	PtRu/C	O <sub>2</sub> ,25 mL/min	$6 \text{ mW/cm}^2$		
$4.0 \text{ mg/cm}^2$	$2.7 \text{ mg/cm}^2$	0.5M CH <sub>3</sub> OH 1.8mL/min	75°C	12	
45%Nafion	PtRu/C	Air,500 mL/min	$58 \text{ mW/cm}^2$		
$5.0 \text{ mg/cm}^2$	$2.0 \text{ mg/cm}^2$	1M CH <sub>3</sub> OH 2.5mL/min	70°C	13	
50%Nafion	PtRu/C	Air,100 mL/min	14.9 mW/cm <sup>2</sup>		
$4.0 \text{ mg/cm}^2$	$4.0 \text{ mg/cm}^2$	2M CH <sub>3</sub> OH	60°C	14	
45%Nafion	PtRu/C	Air-breathing	19.48 mW/cm <sup>2</sup>		
$5.0 \text{ mg/cm}^2$	$4.0 \text{ mg/cm}^2$	1M CH <sub>3</sub> OH	30°C	15	
50%Nafion	PtRu/C	Air-breathing	11.72 mW/cm <sup>2</sup>	10	
8.0 mg/cm <sup>2</sup>	4.0 mg/cm <sup>2</sup>	<b>3M CH<sub>3</sub>OH</b>	60°C	This	
45%Nafion	PtRu/C	Air-breathing	28.85 mW/cm <sup>2</sup>	Work	

Fe-N-C based cathode catalyst

P <sub>max</sub> @Fe-N-C	P <sub>max</sub> @Pt/C	Tem.	P <sub>max</sub> @Fe-N-C/ P <sub>max</sub> @Pt/C	Ref.
6.5 mW/cm <sup>2</sup>	11.1 mW/cm <sup>2</sup>	30°C	58.6%	7
22.6 mW/cm <sup>2</sup>	30.9mW/cm <sup>2</sup>	90°C	73.1%	16
19.6 mW/cm <sup>2</sup>	30.9mW/cm <sup>2</sup>	90°C	63.4%	2
38.47 mW/cm <sup>2</sup>	60 mW/cm <sup>2</sup>	70°C	64.1%	17
71 mW/cm <sup>2</sup>	$115 \text{ mW/cm}^2$	80°C	61.7%	18
19.48 mW/cm <sup>2</sup>	33.95mW/cm <sup>2</sup>	60°C	57.4%	14
58 mW/cm <sup>2</sup>	120 mW/cm <sup>2</sup>	60°C	48.3%	12
21.5 mW/cm <sup>2</sup>	115 mW/cm <sup>2</sup>	70°C	18.7%	19
28.85 mW/cm <sup>2</sup>	34.94 mW/cm <sup>2</sup>	60°C	82.6%	This Work

Table S2 Summary of the performance of the PEM-based DMFC with Fe-N-C and

Pt/C cathode catalysts

## **Reference:**

- Y.-C. Wang, L. Huang, P. Zhang, Y.-T. Qiu, T. Sheng, Z.-Y. Zhou, G. Wang, J.-G. Liu, M. Rauf, Z.-Q. Gu, W.-T. Wu and S.-G. Sun, *ACS Energy Letters*, 2017, 2, 645-650.
- L. Osmieri, R. Escudero-Cid, A. H. A. Monteverde Videla, P. Ocón and S. Specchia, *Applied Catalysis B: Environmental*, 2017, 201, 253-265.
- D. Sebastián, A. Serov, K. Artyushkova, J. Gordon, P. Atanassov, A. S. Aricò and V. Baglio, *ChemSusChem*, 2016, 9, 1986-1995.
- A. H. A. Monteverde Videla, D. Sebastián, N. S. Vasile, L. Osmieri, A. S. Aricò,
   V. Baglio and S. Specchia, *Int. J. Hydrogen Energy*, 2016, 41, 22605-22618.
- 5. C. Lo Vecchio, A. Aricò and V. Baglio, *Materials*, 2018, 11.
- D. Sebastián, A. Serov, K. Artyushkova, P. Atanassov, A. S. Aricò and V. Baglio, *J. Power Sources*, 2016, **319**, 235-246.
- 7. D. Sebastián, V. Baglio, A. S. Aricò, A. Serov and P. Atanassov, *Applied Catalysis B: Environmental*, 2016, **182**, 297-305.
- 8. J. C. Park and C. H. Choi, J. Power Sources, 2017, **358**, 76-84.
- Y. Hu, J. Zhu, Q. Lv, C. Liu, Q. Li and W. Xing, *Electrochim. Acta*, 2015, 155, 335-340.
- D. Sebastián, A. Serov, I. Matanovic, K. Artyushkova, P. Atanassov, A. S. Aricò and V. Baglio, *Nano Energy*, 2017, 34, 195-204.
- S. Baranton, C. Coutanceau, J. M. Léger, C. Roux and P. Capron, *Electrochim. Acta*, 2005, **51**, 517-525.

- 12. Q. Li, T. Wang, D. Havas, H. Zhang, P. Xu, J. Han, J. Cho and G. Wu, *Advanced Science*, 2016, **3**.
- R. Mei, J. Xi, L. Ma, L. An, F. Wang, H. Sun, Z. Luo and Q. Wu, *J. Electrochem.* Soc., 2017, 164, F1556-F1565.
- X. Zhang, C. Hou, W. Yuan, C. Deng, F. Ji, L. Tian, G. Lin, H. Deng and Y. Zhang, *Fuel Cells*, 2022, 23, 42-50.
- J. Xi, F. Wang, R. Mei, Z. Gong, X. Fan, H. Yang, L. An, Q. Wu and Z. Luo, *RSC Advances*, 2016, 6, 90797-90805.
- L. Osmieri, R. Escudero-Cid, M. Armandi, A. H. A. Monteverde Videla, J. L. García Fierro, P. Ocón and S. Specchia, *Applied Catalysis B: Environmental*, 2017, 205, 637-653.
- L. Cao, W. Yang, H. Zou, S. Chen and Z. Liu, J. Inorg. Organomet. Polym. Mater., 2019, 29, 1886-1894.
- X. Xu, X. Zhang, Z. Xia, R. Sun, J. Wang, Q. Jiang, S. Yu, S. Wang and G. Sun, ACS Appl. Mater. Interfaces, 2021, 13, 16279-16288.
- E. Giordano, E. Berretti, L. Capozzoli, A. Lavacchi, M. Muhyuddin, C. Santoro,
   I. Gatto, A. Zaffora and M. Santamaria, *J. Power Sources*, 2023, 563.