

Supplementary Information

Confined phase transition triggering high-performance energy storage thermo-battery

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Note S1. Theoretical analysis of the thermopower

There is a hypothetical temperature-dependent reversible redox reaction between A and B ($aA + ne^- \leftrightarrow bB$) in a thermos-electrochemical cell (TEC). The Seebeck coefficient (Se) was calculated as the ratio of the potential difference (ΔE) to temperature difference (ΔT), according to Eq. 1:^{1, 2}

$$Se = \frac{\Delta E}{\Delta T} = \frac{E_H - E_C}{T_H - T_C} \quad (1)$$

where E_H and E_C are the potential at the hot and cold sides of the sample, respectively. And T_H and T_C are the temperature at the hot and cold electrodes of TEC, respectively.

According to the Nernst equation, for above mentioned redox reaction ($aA + ne^- \leftrightarrow bB$), the equilibrium potential (E) can be expressed as:

$$E = E^0 + \frac{RT}{nF} \ln \frac{(a_A)^a}{(a_B)^b} \quad (2)$$

where E^0 is the standard potential, F is the Faraday constant, R is the ideal gas constant, a_A and a_B are the activities of species A and B, respectively. The activity (a) is defined as the product of the activity coefficient (γ) and concentration (C) ($a = \gamma \times C$).

$$E = E^0 + \frac{RT}{nF} \left[\ln \frac{(\gamma_A)^a}{(\gamma_B)^b} + \ln \frac{(C_A)^a}{(C_B)^b} \right] \quad (3)$$

According to Eq. 1, Se can be finally written as the sum of two terms:

$$Se = \frac{R}{nF\Delta T} \left[T_H \ln \frac{(\gamma_A)_H^a}{(\gamma_B)_H^b} - T_C \ln \frac{(\gamma_A)_C^a}{(\gamma_B)_C^b} \right] + \frac{R}{nF\Delta T} \left[T_H \ln \frac{(C_A)_T^a}{(C_B)_T^b} - T_C \ln \frac{(C_A)_C^a}{(C_B)_C^b} \right] \quad (4)$$

Excess free enthalpy (G^E) refers to the difference between the real solution properties and the ideal solution free enthalpy properties under the same conditions of temperature, pressure and composition ($G^E = \Delta G - \Delta G^{id}$). The G^E value is proportional to its γ .

$$G^E = RT \sum C_i \ln \gamma_i \quad (5)$$

where ΔG is the Gibbs free energy, ΔG^{id} is Gibbs free energy of ideal solution.

In general, ΔG is calculated by:

$$\Delta G = \Delta H - T\Delta S \quad (6)$$

Phase transition is characterized as a discontinuous and abrupt change in volume, solubility, or molecular conformation of a material at its transition temperature.³ The formation or dissolution of the precipitates is induced in a much narrower temperature region during a phase transition. Assuming that ΔH is constant under the temperature

region which can be estimated from isothermal titration calorimetry.^{4, 5}

$$\ln \gamma \propto -\Delta S \quad (7)$$

For the TEC containing the equal-concentration I^-/I_3^- aqueous electrolyte ($I_3^- + 2e^- \leftrightarrow 3I^-$) with a certain amount of methylcellulose (MC) under the open-circuit state, when the hot electrode temperature is below the gelation temperature of MC, both concentrations of the redox species on the hot and cold sides are equal, that is, $\Delta C = 0$. In this case, Se is only related to the entropy difference of the redox reaction. Hence, the second term of Eq. 4 can be neglected, and Se can be simplified as:

$$Se = \frac{R}{2F\Delta T} \left[T_H \ln \frac{(\gamma_{I_3^-})_H}{(\gamma_{I^-})_H^3} - T_C \ln \frac{(\gamma_{I_3^-})_C}{(\gamma_{I^-})_C^3} \right] \quad (8)$$

Here, it is worth noting that the definition of Se is defined as positive sign in this work.

When the hot electrode temperature is above the gelation temperature of MC, the hydrophobic interaction between MC and I_3^- ions leads to a substantially reduced I_3^- concentration at the hot side ($\Delta C \neq 0$).⁶ Thus, Eq. 4 is expressed as:

$$Se = -\frac{R}{2F\Delta T} \left[T_H \ln \frac{(\gamma_{I_3^-})_H}{(\gamma_{I^-})_H^3} - T_C \ln \frac{(\gamma_{I_3^-})_C}{(\gamma_{I^-})_C^3} \right] - \frac{R}{2F\Delta T} \left[T_H \ln \frac{(c_{I_3^-})_H}{(c_{I^-})_H^3} - T_C \ln \frac{(c_{I_3^-})_C}{(c_{I^-})_C^3} \right] \quad (9)$$

According to Eq. 9, the first term is considered to be dominated by difference in entropy (ΔS) between the redox anions,^{7, 8} the second term is only related to the concentrations of A and B (ΔC).

$$\frac{1}{\Delta T} \left[T_H \ln \frac{(\gamma_{I_3^-})_H}{(\gamma_{I^-})_H^3} - T_C \ln \frac{(\gamma_{I_3^-})_C}{(\gamma_{I^-})_C^3} \right] \propto \Delta S \quad (10)$$

$$\frac{1}{\Delta T} \left[T_H \ln \frac{(c_{I_3^-})_H}{(c_{I^-})_H^3} - T_C \ln \frac{(c_{I_3^-})_C}{(c_{I^-})_C^3} \right] \propto \Delta C \quad (11)$$

On the contrary, Se here has opposite sign compared to the one mentioned above Eq. 8.

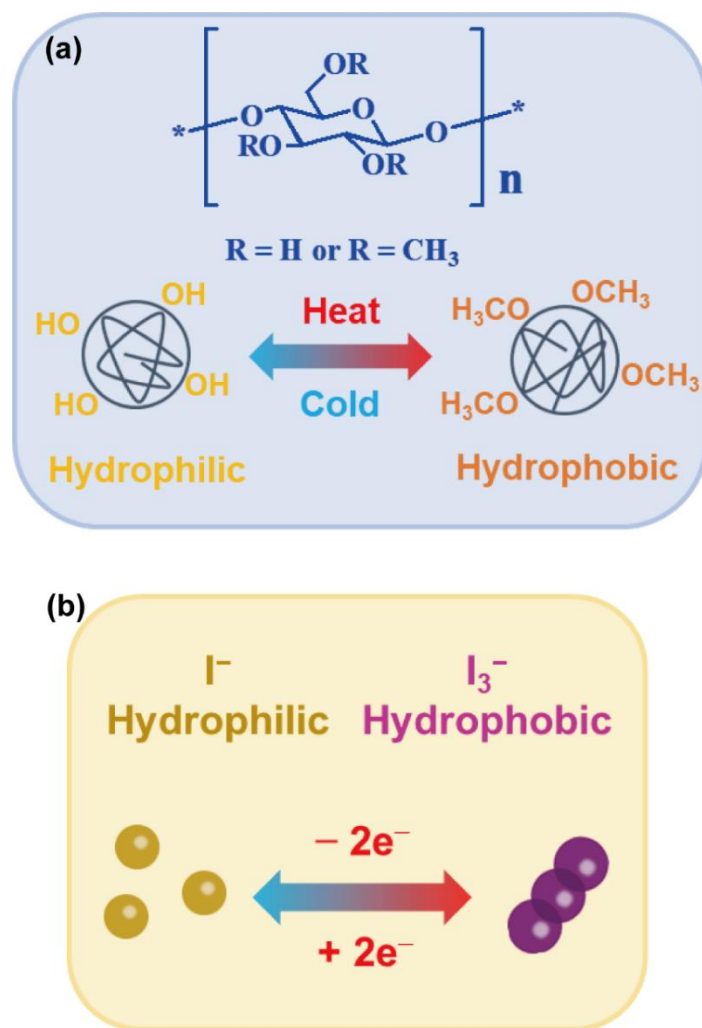


Fig. S1 The molecular structure and properties of (a) MC and (b) I^- and I_3^- ions.

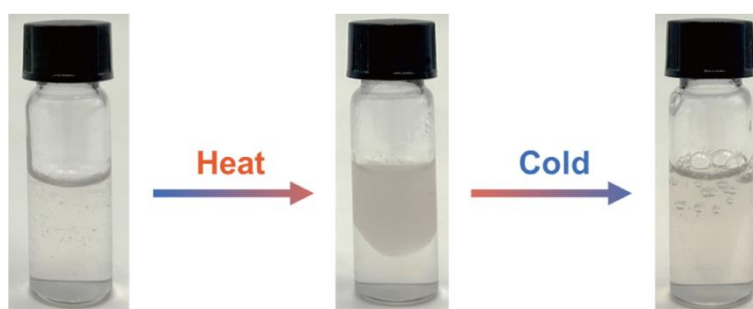


Fig. S2 Photograph of 2 wt% MC electrolyte upon heating and cooling.

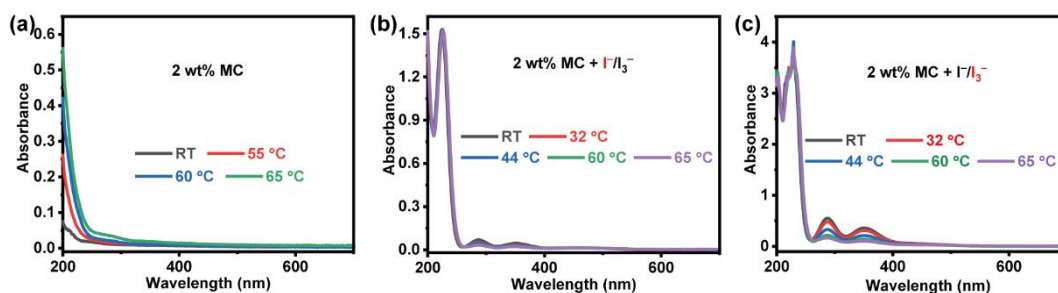


Fig. S3 UV-Vis spectra of 2 wt% MC diluted 25 times (a), 2 wt% MC + I^-/I_3^- diluted to 2×10^{-5} M (b), and 2 wt% MC + I^-/I_3^- diluted to 10^{-4} M (c) in the electrolyte at different temperatures. The peak at 225 nm is assignable to the I^- ion, and the peaks at 288 and 352 nm are assigned to I_3^- species dissolved in deionized water. This dilution concentration refers to the I^-/I_3^- solution.

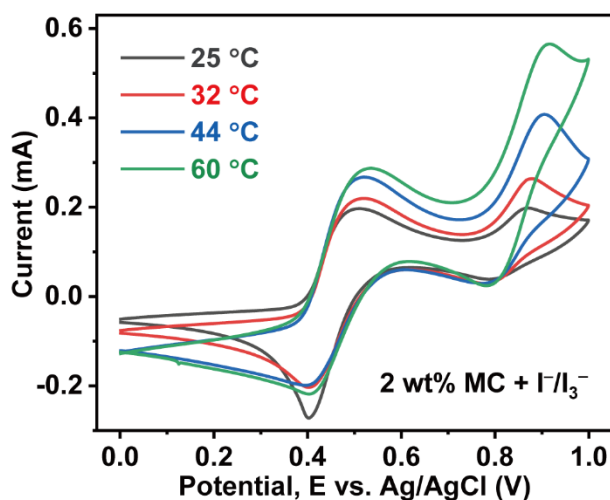


Fig. S4 CV curves of 2 wt% MC + I^-/I_3^- electrolyte with increasing temperature.

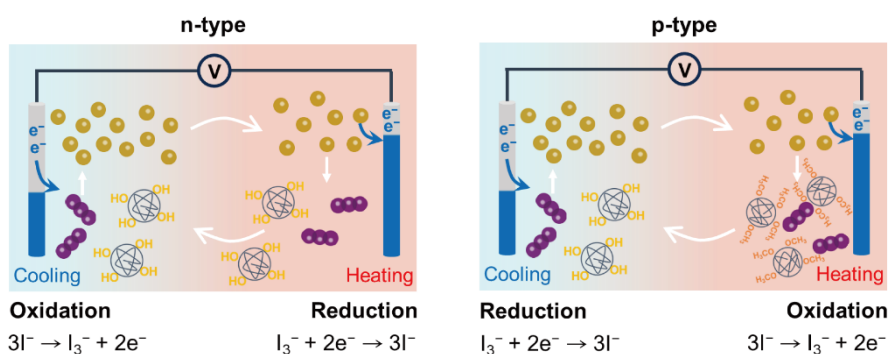


Fig. S5 Schematics of n-type TEC and p-type thermo-battery for I^-/I_3^- redox couple induced by MC.

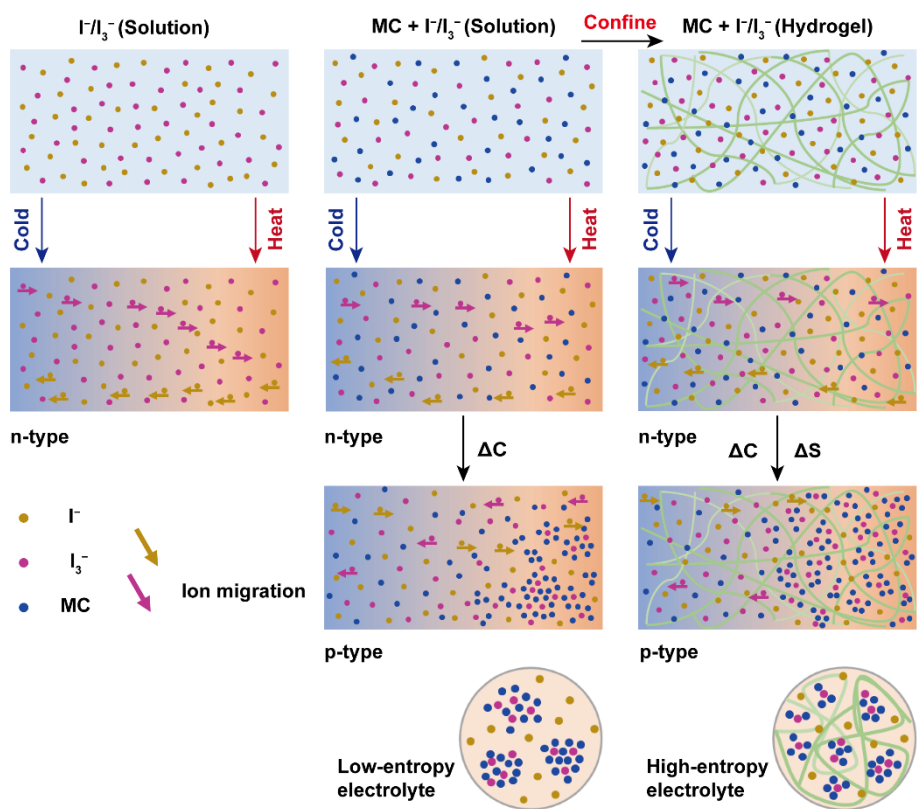


Fig. S6 Design concept of thermo-batteries and schematic of enhanced thermopower. Low-entropy electrolyte refer to the electrolyte system with a weak solvation interaction between the I_3^- ions and H_2O . In contrast, high-entropy electrolyte refers to the electrolyte system with a strong solvation interaction between I_3^- ions and H_2O , which has smaller ion clusters.

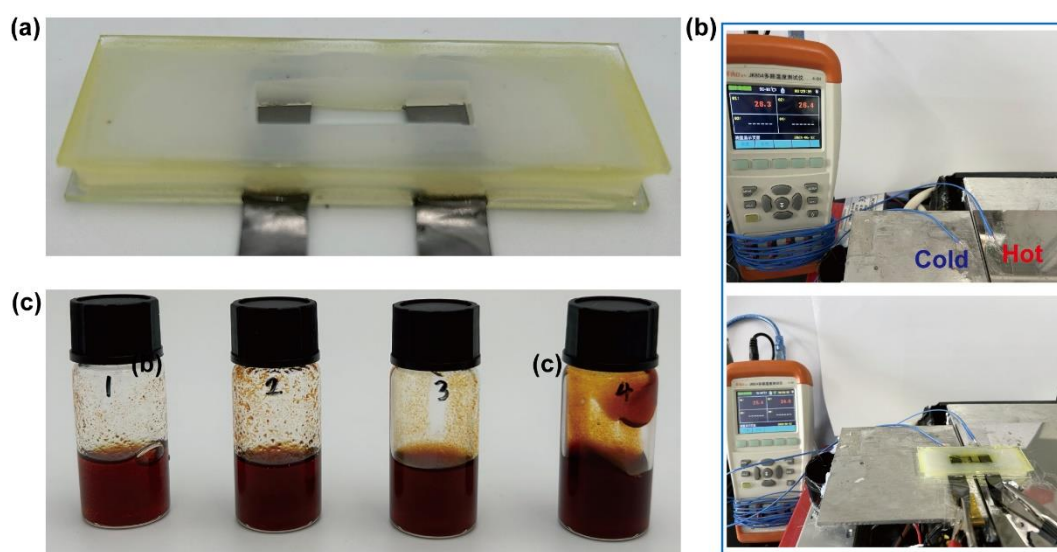


Fig. S7 (a) Experimental setup for characterizing the thermopower and power

generation performance. (b) The photos of the home-made equipment. (c) Photograph of x wt% MC + I^-/I_3^- electrolytes (x = 1, 2, 3, 4) from left to right. The electrolytes become more viscous with the increase of MC content.

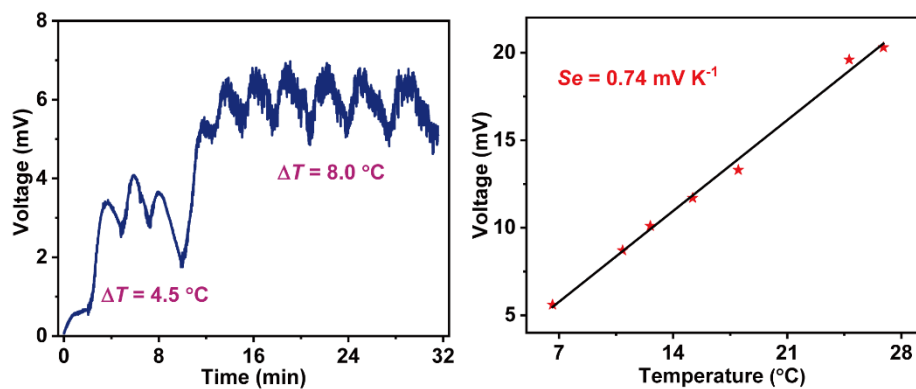


Fig. S8 Recorded open-circuit voltage over time and Se of the thermocell with I^-/I_3^- electrolyte.

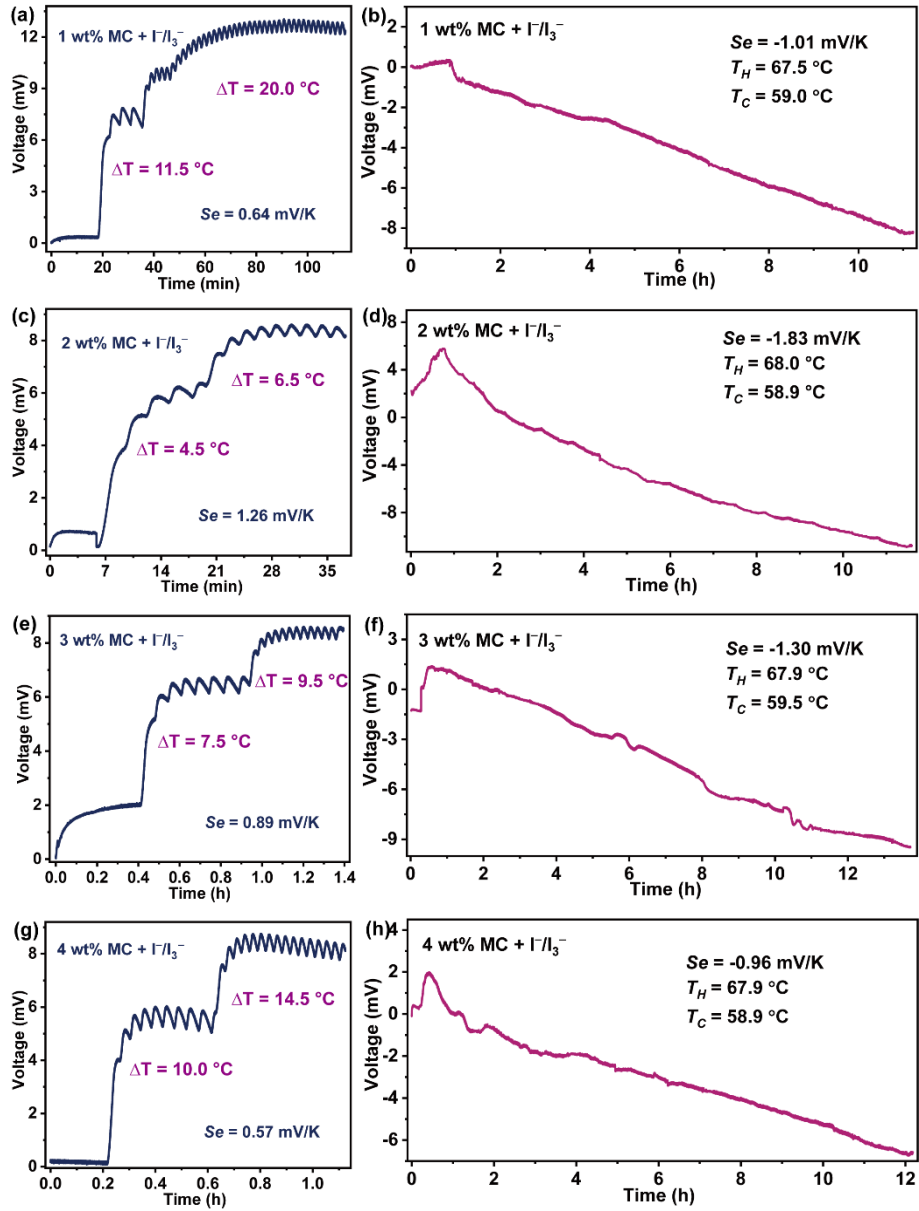


Fig. S9 Recorded open-circuit voltages for (a) 1, (c) 2, (e) 3, and (g) 4 wt% MC + Γ/I_3^- electrolytes of n-type thermocells and for (b) 1, (d) 2, (f) 3, and (h) 4 wt% MC + Γ/I_3^- electrolytes of p-type thermo-batteries. And T_H is held at room temperature for n-type thermocell.

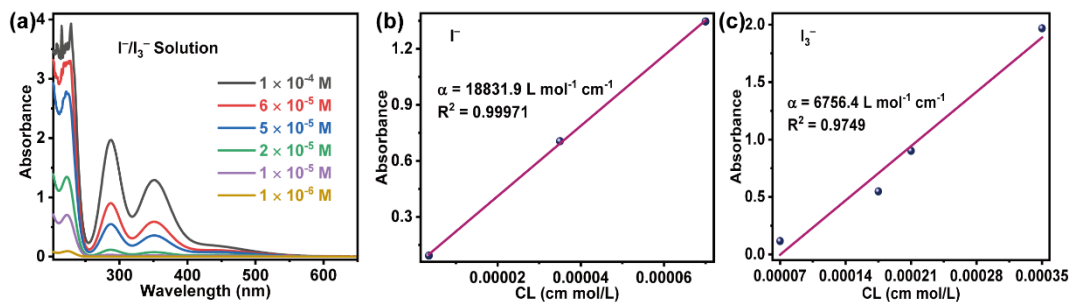


Fig. S10 (a) UV-Vis spectra of I^-/I_3^- solutions with a series of concentration gradients. The fitting of molar extinction coefficient of (b) I^- at 225 nm, and (c) I_3^- at 288 nm based on the absorbance at different concentrations. The thickness of the solution is 3 cm in the cuvette.

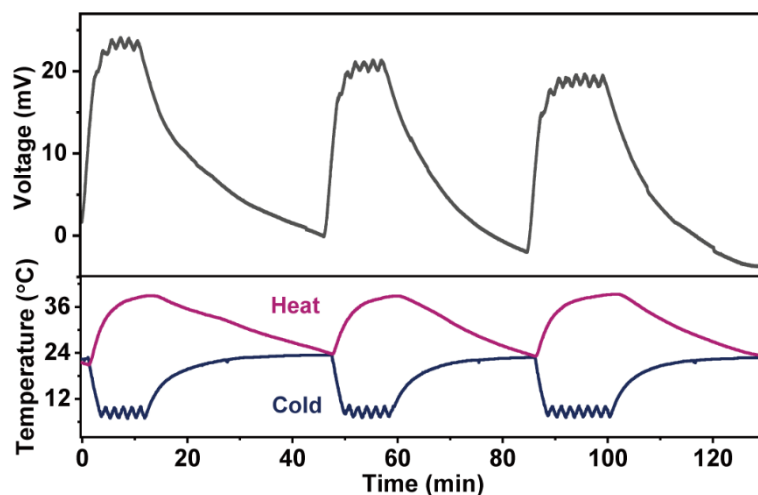


Fig. S11 The open-circuit voltage-time curves of I^-/I_3^- electrolyte with and without temperature difference.

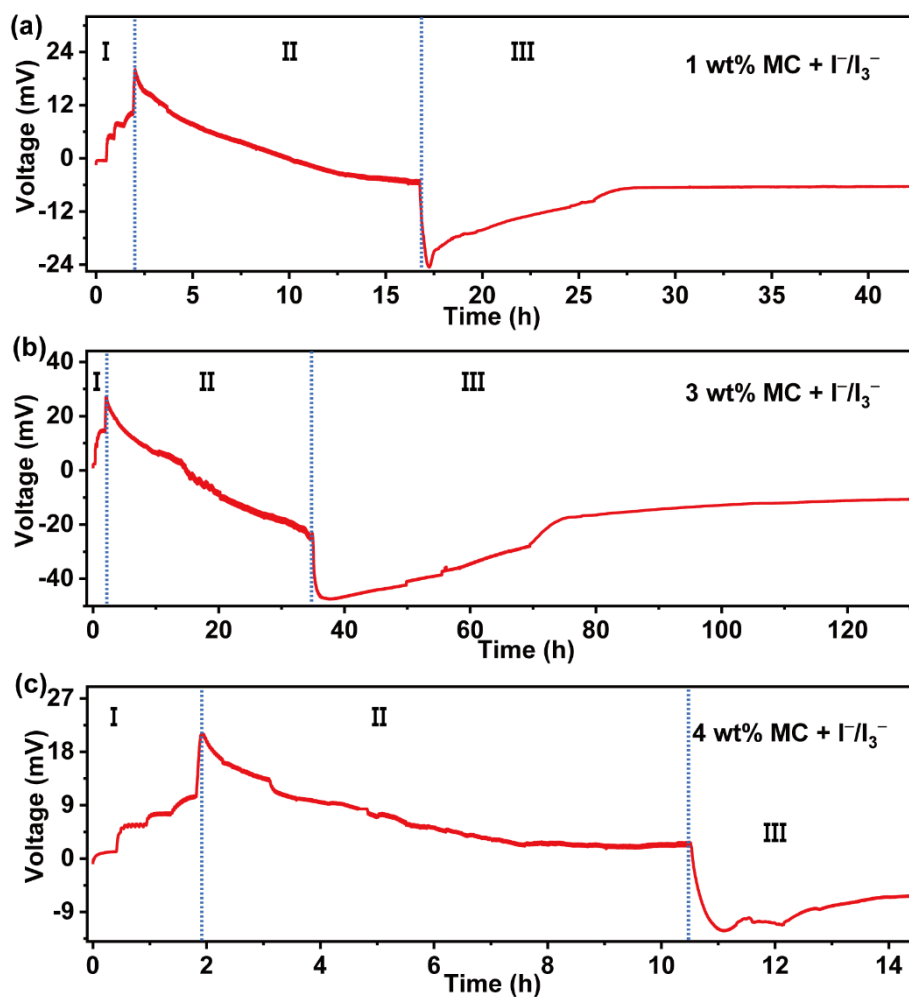


Fig. S12 Recorded open-circuit voltages for (a) 1, (b) 3 and (c) 4 wt% MC + I⁻/I₃⁻ electrolytes during charging and self-discharging (I: $T_H < 56$ °C, n-type; II: $T_H > 56$ °C, p-type; III: $\Delta T = 0$ °C, the V_{OC} decreases slowly), The cold electrode temperature is held at 15 °C.

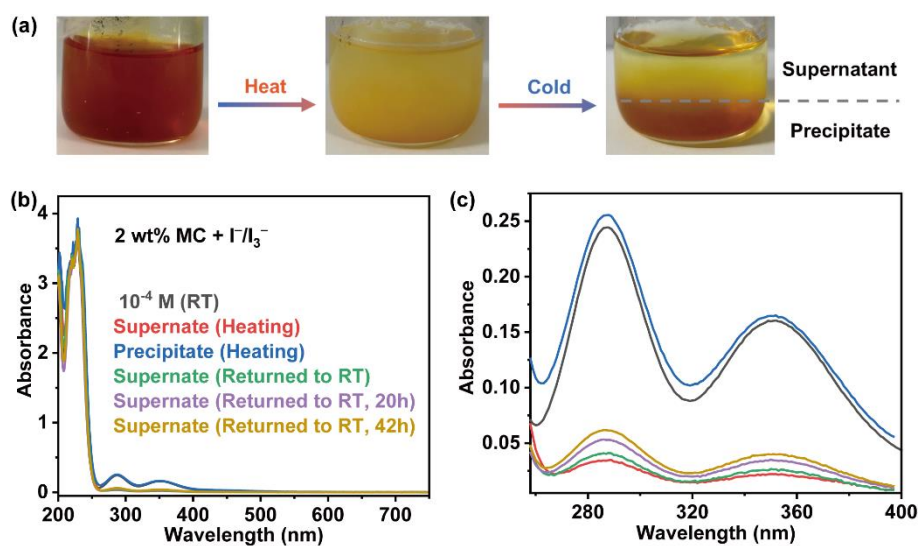


Fig. S13 (a) Photographs of 2 wt% MC + I^-/I_3^- electrolyte under different temperatures, and the schematic showing the change of MC from the hydrophobic to hydrophilic state upon heating and cooling. (b) UV-Vis spectra of the 2 wt% MC + I^-/I_3^- electrolytes with different treatment conditions, and magnified UV-Vis spectra (c) of wavelengths from 258 to 400 nm.

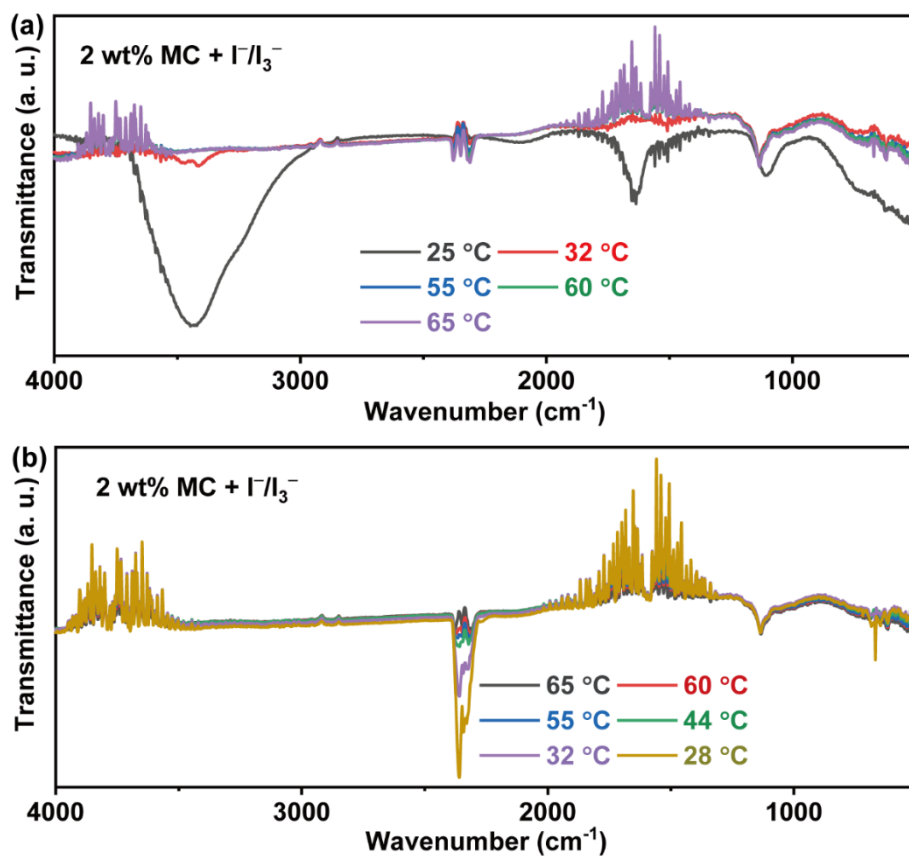


Fig. S14 FTIR spectra about 2 wt% MC + I^-/I_3^- electrolyte solution in a closed heating (a) and cooling (b) cycle.

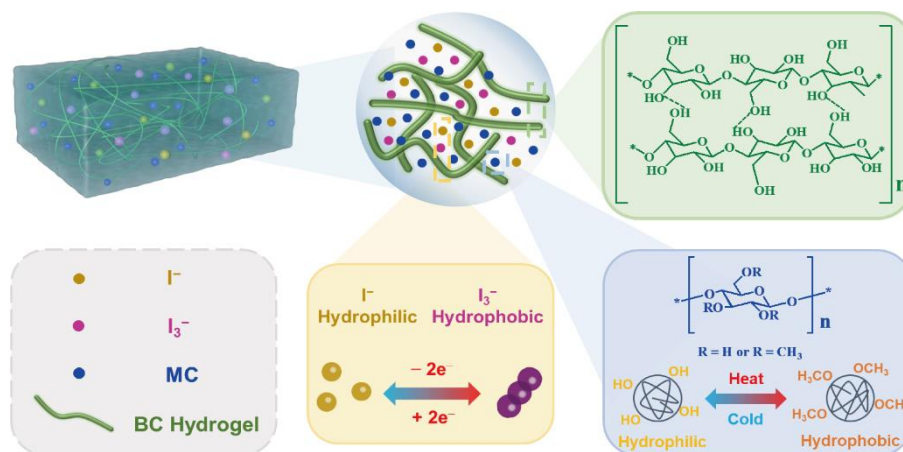


Fig. S15 Components of BC hydrogel-based 2 wt% MC + I^-/I_3^- electrolyte.

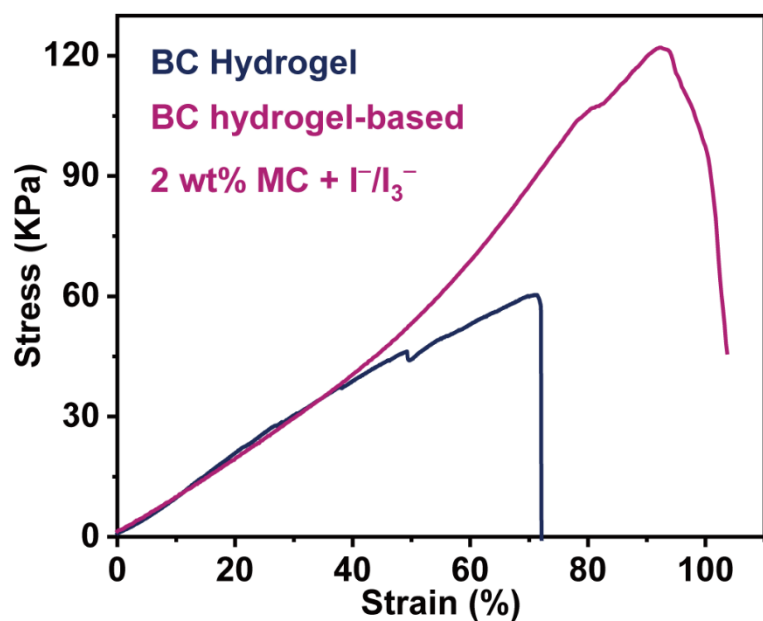


Fig. S16 Tensile stress-strain curves of BC hydrogel and BC hydrogel-based 2 wt% MC + I⁻/I₃⁻ electrolyte, respectively.

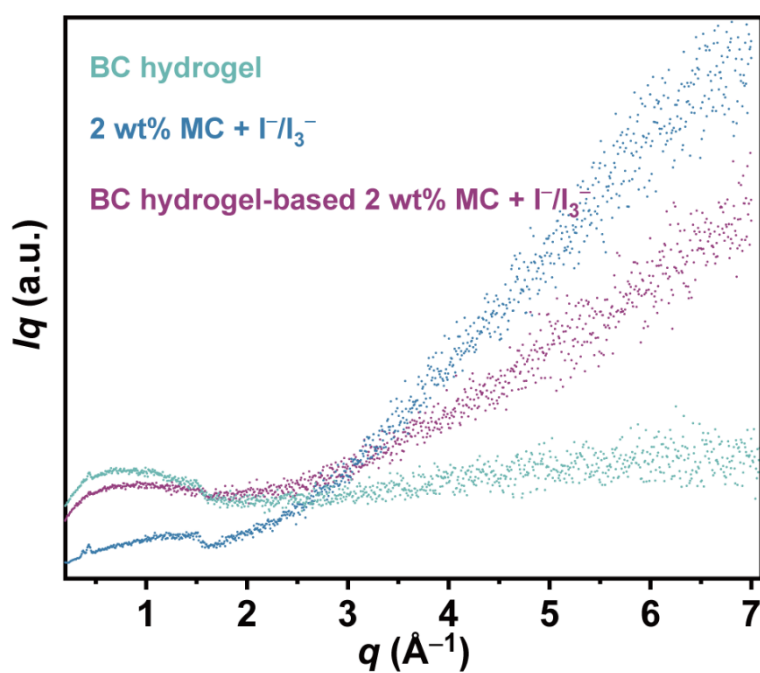


Fig. S17 Representative SAXS profiles of BC hydrogel, 2 wt% MC + I⁻/I₃⁻ and BC hydrogel-based 2 wt% MC + I⁻/I₃⁻ electrolytes under 60 °C, respectively.

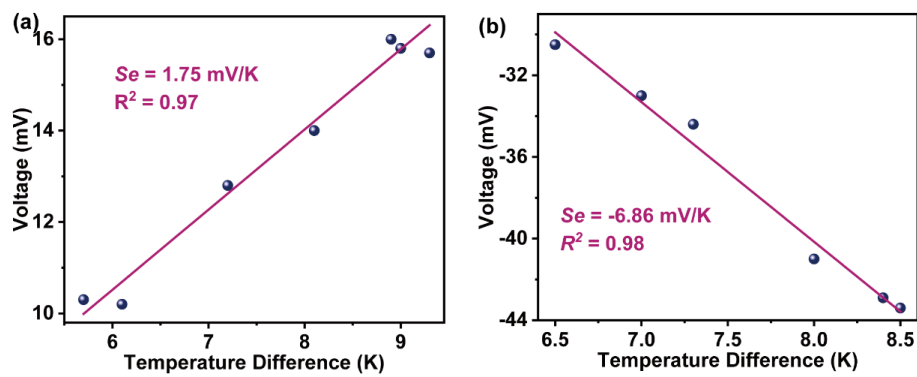


Fig. S18 Se for n-type thermocell (a) and p-type thermo-battery (b) with BC hydrogel-based 2 wt% MC + Γ/I_3^- electrolyte, respectively.

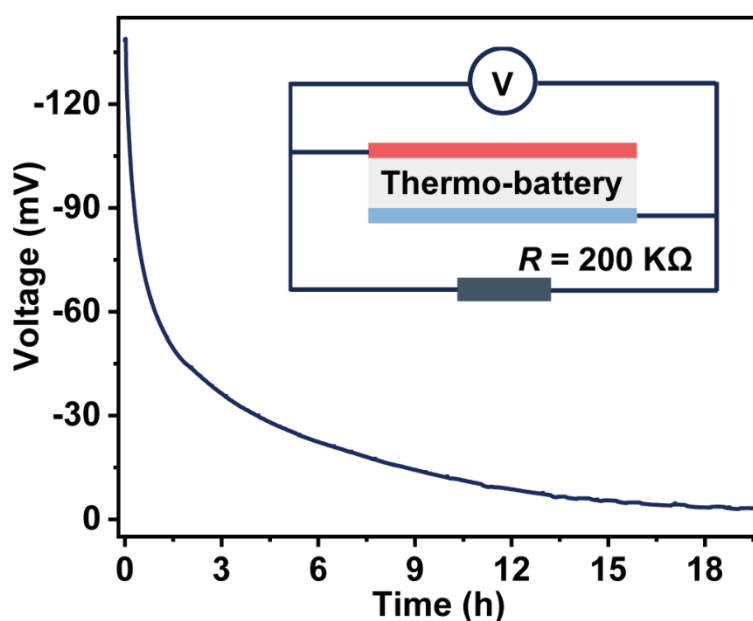


Figure S19. The open-circuit voltage of the continuous discharge process at the external resistor $R = 200 \text{ k}\Omega$ and $\Delta T = 0 \text{ }^\circ\text{C}$. The inset shows the measurement circuit.

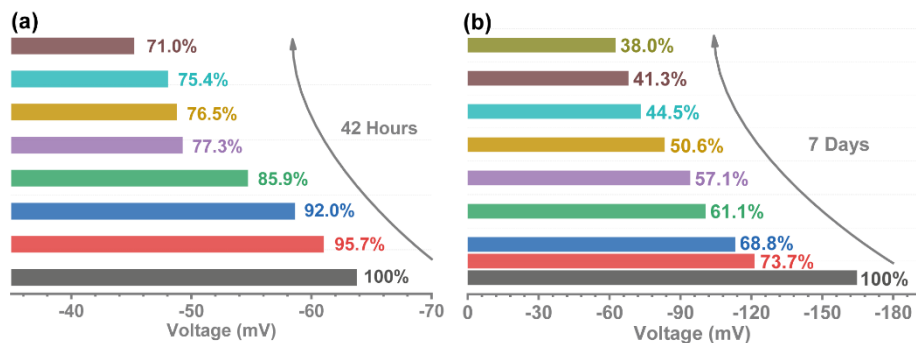


Fig. S20 (a) The V_{OC} attenuation of 2 wt% MC + I⁻/I₃⁻ electrolytes during self-discharging process. The self-discharge time is successively 0, 6, 12, 18, 24, 30, 36 and 42 hours from bottom to top. (b) The V_{OC} attenuation of BC hydrogel-based 2 wt% MC + I⁻/I₃⁻ electrolytes during self-discharging process. The self-discharge time is successively 0, 0.5, 1, 2, 3, 4, 5, 6 and 7 days from bottom to top.



Fig. S21 Photograph of a device module containing 5 units in series.

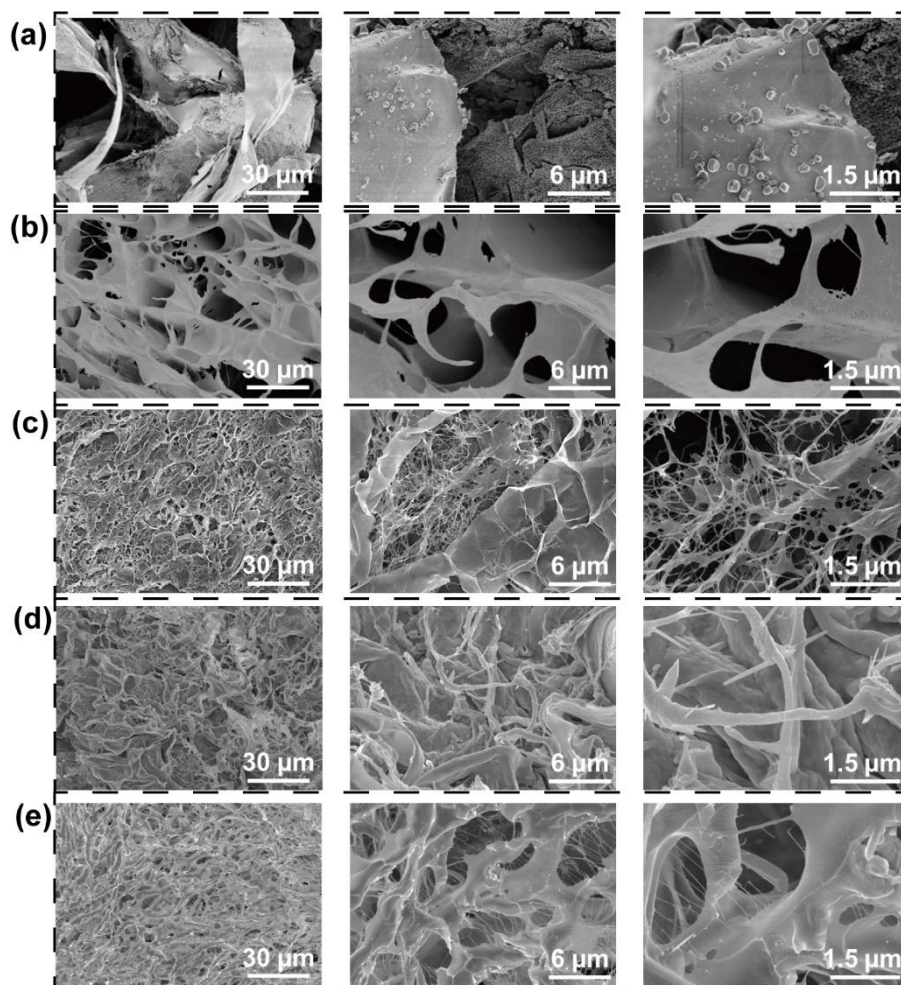


Fig. S22 Morphology characterization of 2 wt% MC + Γ/I_3^- electrolyte with RT (b) and heat (c), BC hydrogel (d), and BC hydrogel-based 2 wt% MC + Γ/I_3^- electrolyte under RT (e) and heating (f) at different magnifications.

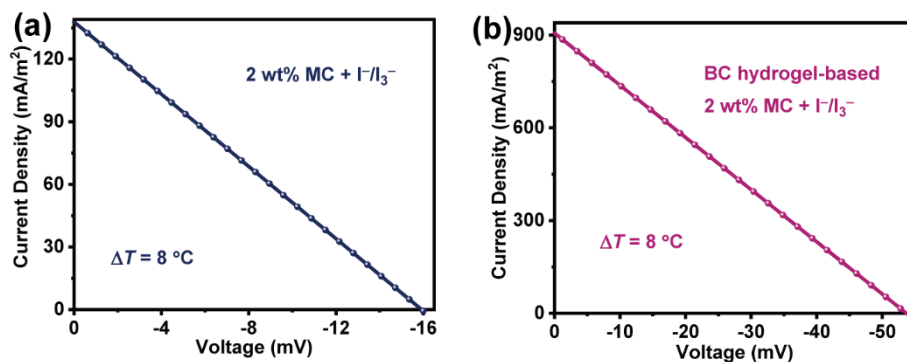


Fig. S23 The output voltage-current density curve of p-type thermo-battery without (a) and with (b) BC hydrogel for 2 wt% MC + Γ/I_3^- electrolyte under $\Delta T = 8^\circ C$. The cold electrode temperature is fixed at $58^\circ C$.

Table S1. When the hot electrode temperature is below/above the gelation temperature of MC, the reactions at hot and cold electrodes.

n-type	Hot electrode	$I_3^- + 2e^- \rightarrow 3I^-$
	Cold electrode	$3I^- \rightarrow I_3^- + 2e^-$
p-type	Hot electrode	$3I^- \rightarrow I_3^- + 2e^-$
	Cold electrode	$I_3^- + 2e^- \rightarrow 3I^-$

Table S2. Comparison of Se values in this work with those reported for I^-/I_3^- based thermocells in the literature.

Redox Couple	State	Hydrophobic Matrix	n/p-type	Se (mV/K)	References
I^-/I_3^-	Liquid	--	n	0.71	6
	Liquid	α -cyclodextrins	n	1.45	5
	Liquid	Starch	n	1.50	9
	Liquid	Poly (N-isopropylacrylamide)	n	0.71	10
			p	-1.91	
	Liquid	Poly (N-isopropylacrylamide)	n	0.71	11
			p	-1.19	
	Liquid	Methylcellulose	n	1.32	6
			p	-1.48	
	Liquid	Methylcellulose	n	1.26	This work
			p	-1.83	
	BC	Methylcellulose	n	1.75	
Hydrogel		p	-6.84		

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