

Supplementary Information

Combined effect of Cu⁰ and oxygen vacancy in Cu-based zeolite enables highly efficient photo-Fenton-like performance for water purification

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1. Texts

Text S1. Materials.

Sodium aluminate ($\text{Al}_2\text{O}_3\cdot\text{Na}_2\text{O}$, 98%), Cetrimonium bromide (CTAB, 99%), Sodium hydroxide (NaOH, 98%), Hexamethyleneimine (HMI, 98%), Tetraethylenepentamine (TEPA, 98%), Sodium thiosulfate ($\text{Na}_2\text{S}_2\text{O}_3$, 99%) and Sodium carbonate (Na_2CO_3 , 99.8%) were purchased from Aladdin Co., Ltd.. LUDOX AS-40 colloidal silica (40 wt%), Copper (II) sulfate pentahydrate ($\text{CuSO}_4\cdot 5\text{H}_2\text{O}$, 99%), benzoquinone (BQ, 99%), L-Histidine (99%), and tert-Butanol (TBA, 99%) were purchased from Merck Co., Ltd.. Phenol (99%), 2,4-Dichlorophenol, 4-chlorophenol (Sigma-Aldrich Co., Ltd.). Hydrogen peroxide, Sulfuric acid (Sinopharm Chemical Reagent Co., Ltd.). Silver nitrate (Tianjin Tiangan Chemical Technology Development Co., Ltd.). All reagents were not purified. Deionized water was prepared by pure water meter and was used throughout the experiment.

Text S2. Characterization.

XRD patterns was recorded from 3° to 80° with nickel-filtered Cu $K\alpha$ radiation ($\lambda = 1.54 \text{ \AA}$ Rigaku, Smart Lab 9kW). Operating conditions: voltage is 45 kV, scanning rate is $10^\circ/\text{min}$. TEM was carried out using FEI Talos F200x Microscope, which operating voltage is 200kv. EDS elemental analysis was conducted using Bruker X-Flash SDD 5010. XPS was performed on Thermo SCIENTIFIC K-Alpha spectrometer (Al Kalph source). The specific surface areas were measured by a surface area analyzer (ASAP2460, Micromeritics, USA) with the Brunauer-Emmett-Teller (BET) method, and the pore size distribution was calculated using BJH calculations method. DRS spectroscopy measurement was recorded on a spectrophotometer (Agilent-Cary 5000, USA) from 200 nm to 1200 nm. FTIR spectra were recorded on a Bruker Vertex70 ($4000\text{--}400 \text{ cm}^{-1}$). EIS was measure on CHI 660E (Chenhua Co., Ltd., China). The copper leaching during the reaction was measured by an ICP-AES (Thermo Scientific, ICAP 6300 Duo) instrument.

Text S3. Analytic methods.

The degradation was monitored via high performance liquid chromatograph (Ultimate 3000, Thermo Fisher Scientific) with a DAD-300 detector, C18 Hypersil GOLD column at column chamber temperature of 35°C . The test conditions are as follows: phenol (60% H_2O , 40% methanol, flow rate:

1 mL/min, UV: 283 nm). 4-CP (30% H₂O, 70% methanol, flow rate: 1 mL/min, UV: 224 nm). 2,4-DCP (70% acetonitrile, 30% H₂O, UV: 286 nm). DCF (35% acetic acid aqueous solution (0.1%), 65% acetonitrile, UV: 274 nm). MB and RhB were detected by ultraviolet spectrophotometer.

In addition, EPR was used to detect the involved reaction ROS, 5,5-Dimethyl-1-pyrroline n-oxide (DMPO) was dispersed in different air-saturated methanol and aqueous dispersions. A 300 W Xe lamp ($\lambda > 400$ nm) was used as a visible-light source. In the absence of H₂O₂, a total of 100 μ L of DMPO (176.75 mM) was added into 100 μ L of the prepared degradation solution (water for \bullet OH, methyl alcohol for \bullet O₂⁻, 0.2 g/L catalyst, 10 mM H₂O₂, pH 4). Then, the mixed solution was held for 5 min under light. The solution was sucked out by a quartz capillary tube with an inner diameter of 1 mm, and the spectrum was recorded by placing the capillary tube in the EPR cavity. For comparison, H₂O₂ (10 mM) was added into solution before light irradiation to detect the different signals, and other conditions keep constant. The preparation of 2,2,6,6-tetramethyl-4-oxo-piperidine (4-oxo-TEMP) solution is the same as DMPO. 20 mg sample was placed into the sample tube and then into the ESR cavity to detect oxygen vacancy.

TOC of initial and irradiated samples were measured on Elementar TOC analyzer. For EIS test, the ITO glass coating with catalyst was used as a working electrode, and using Pt sheet and Ag/AgCl served as the counter and the reference electrode, respectively. The electrolyte solution: 0.1 M Na₂SO₄.

Text S4. DFT calculations

Gaussian09, D01 software package was used to DFT calculations¹. We used the B3LYP functional and 6-31G(d) basis (Grimme dispersion corrections, GD3BJ) to optimize the model of pollutants. Then, the singlet point energy calculations were based on the B3LYP functional and a larger 6-311G(d) basis. The Hirshfeld atomic charges, HOMO/LUMO gap, ESP and Fukui functions were achieved with the help of the Multiwfn program^{2, 3}. Fukui function has been widely used to predict reactive sites of electrophilic, nucleophilic, and radical attacking⁴.

2. Table

Table S1. Specific surface area (S_{BET}), pore size (d) and pore volume (V_t) of the samples.

sample	Structural parameters		
	$S_{\text{BET}}(\text{m}^2/\text{g})$	$d(\text{nm})$	$V_t(\text{cm}^3/\text{g})$
β -zeolite	63.2	27.99	0.41
$\text{Cu}^0@ \text{CuZ}$	133.9	14.81	0.48

Table S2 The Cu content of $\text{Cu}^0@ \text{CuZ-P}$ and $\text{Cu}^0@ \text{CuZ}$.

Catalyst	Cu^0 content (%)	Cu^+ content (%)	Cu^{2+} content (%)
$\text{Cu}^0@ \text{CuZ-p}$	33	29.8	37.2
$\text{Cu}^0@ \text{CuZ}$	42	24	34
$\text{Cu}^0@ \text{CuZ-p}$ after illumination	33.7	29.6	36.7
$\text{Cu}^0@ \text{CuZ}$ after illumination	41.1	29.5	29.4

Table S3. Degradation conditions and pollutants removal efficiency over Cu⁰@CuZ and other catalysts.

target pollutants	catalysts	reaction conditions	catalytic performance	references
phenol	FeOOH/Bi ₂ MoO ₆	pH: 3.0; catalyst: 1.0 g/L; [H ₂ O ₂]: 20 mM; C ₀ : 5 mg/L; T: 25 °C	100% removal in 3 h, $k = 1.13876 \text{ h}^{-1}$	5
phenol	Fe ₃ O ₄ -GO	pH: 5.0; catalyst: 0.25 g/L; [H ₂ O ₂]: 10 mM; C ₀ : 20 mg/L; T: 25 °C	100% removal after 120 min, $k = -$	6
phenol	FeOOH quantum dots coupled to g-C ₃ N ₄	pH: 5.0; catalyst: 4 g/L; [H ₂ O ₂]: 20 mM; C ₀ : 50 mg/L; T: 25 °C	100% removal after 90 min, $k = 0.054 \text{ min}^{-1}$	7
phenol	Cu-iminodisuccinic acid complex	pH: 7.0; catalyst: 0.02 mM; [H ₂ O ₂]: 14.7 mM; C ₀ : 50 mg/L; T: 25 °C	95% removal after 60 min, $k = -$	8
phenol	AG/Fe ₃ O ₄	pH: 7.0; catalyst: 0.5 mg/L; [H ₂ O ₂]: 250 mM; C ₀ : 40 mg/L; T: 25 °C	100% removal after 120 min, $k = 0.02083 \text{ min}^{-1}$	9
4-CP	La _{1-x} Ti _x FeO ₃	pH: 3.0; catalyst: 0.5 g/L; [H ₂ O ₂]: 3.7 mM; C ₀ : 25 mg/L; T: 25 °C	100% removal in 200 min, $k = 0.0025 \text{ min}^{-1}$	10
MB	MA-Cu-Fe@C	pH: 5; catalyst: 0.5 g/L; [H ₂ O ₂]: 32 mM; C ₀ : 50 mg/L; T: 25 °C	98.8% removal after 80 min, $k = 0.054 \text{ min}^{-1}$	11
RhB	Zn/Co-ZIFs@MIL-101(Fe)	pH: 5; catalyst: 0.2 g/L; [H ₂ O ₂]: 90 mM; C ₀ : 100 mg/L; T: 25 °C	98% removal after 3 h, $k = 1.33 \text{ h}^{-1}$	12
TC	CuFeO QDs/CNNSs	pH: 6; catalyst: 0.5 g/L; [H ₂ O ₂]: 100 mM; C ₀ : 50 mg/L; T: 25 °C	100% removal in 25 min, $k = -$	13
phenol/MB		pH: 4.0; catalyst: 0.2 g/L; [H ₂ O ₂]: 10.0 mM; C ₀ : 20 mg/L; T: 25 °C	100% removal in 20 min, $k = 0.387 \text{ min}^{-1}$	this work

3. Figures

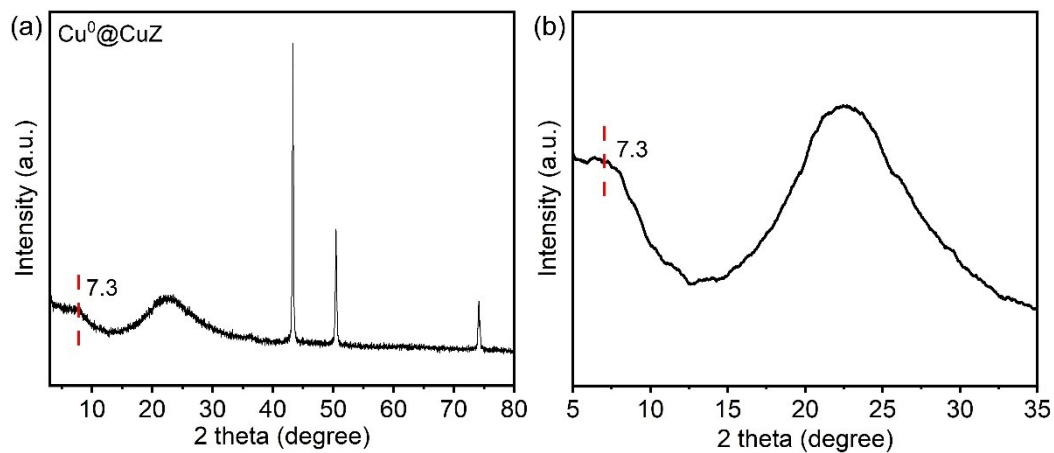


Fig. S1 (a) XRD pattern of $\text{Cu}^0@CuZ$. (b) Enlarged view of the XRD pattern of $\text{Cu}^0@CuZ$.

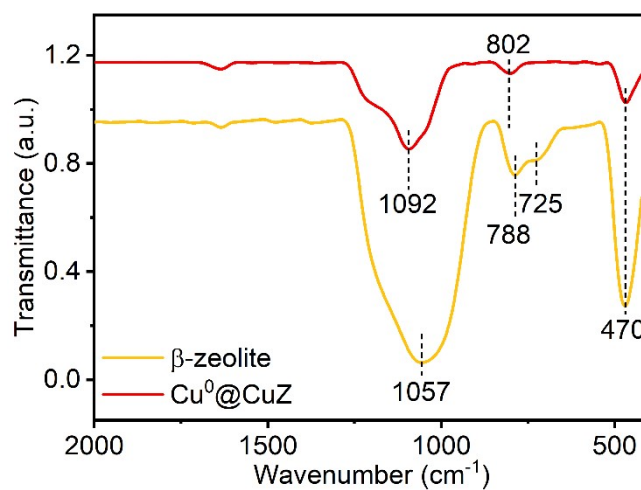


Fig. S2 FTIR spectra of samples.

The FTIR spectrum showed that bands around 470, 725, 788, 1057 cm^{-1} were characterized to β -zeolite. By contrast, an additional band at approximately 1092 cm^{-1} was assigned to Si-O-Cu bond compared with β -zeolite¹⁴⁻¹⁶.

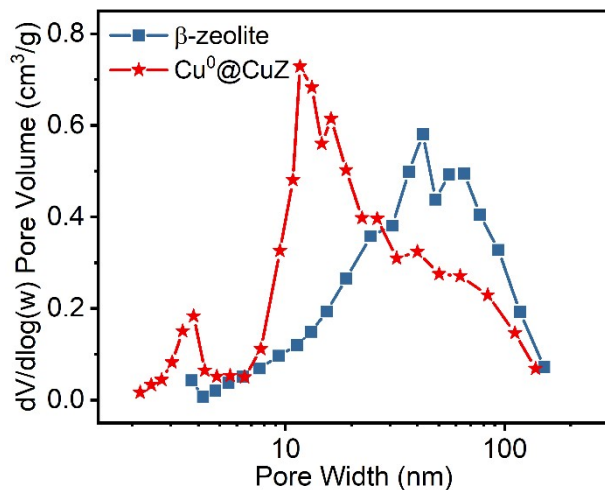


Fig. S3 Pore size distribution of $\text{Cu}^0\text{@CuZ}$ and β -zeolite.

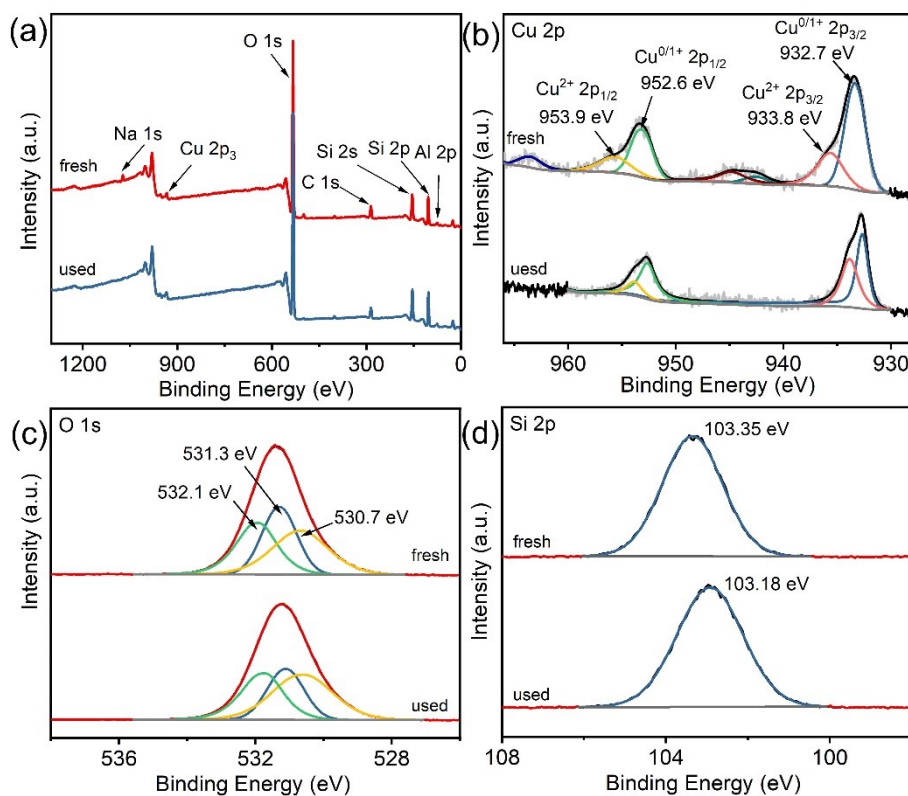


Fig. S4 (a) Wide scan XPS spectrum of $\text{Cu}^0\text{@CuZ}$. High-resolution XPS spectra of (b) Cu 2p, (c) O 1s and (d) Si 2p for $\text{Cu}^0\text{@CuZ}$.

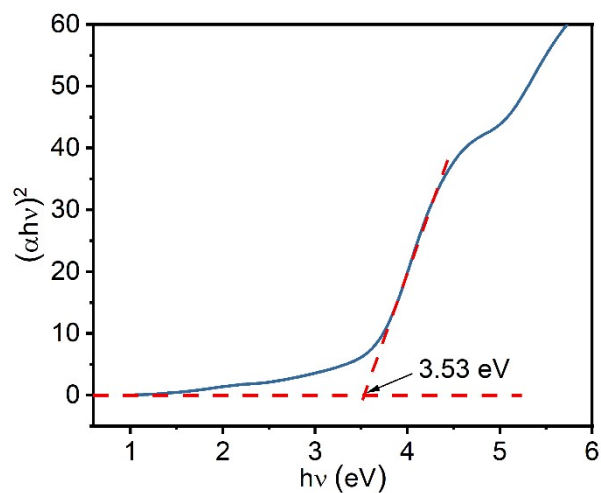


Fig. S5 Band gap values of $\text{Cu}^0\text{@CuZ-p}$.

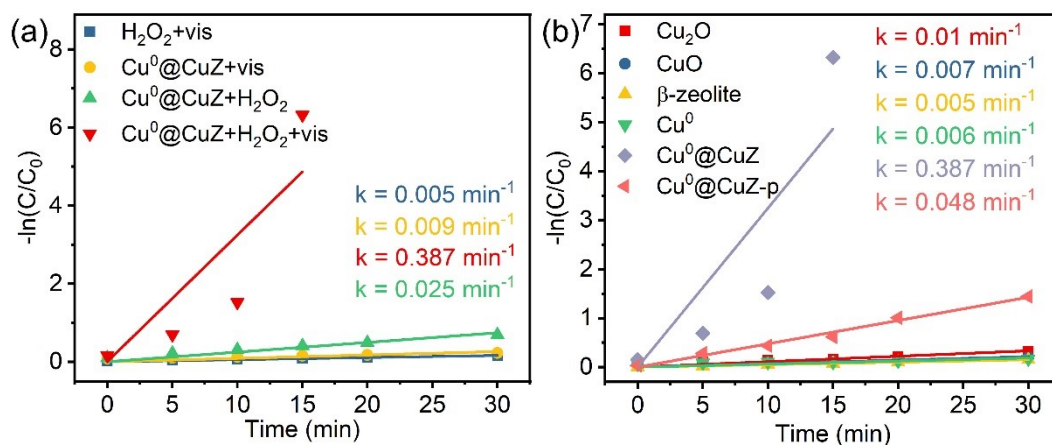


Fig. S6 (a) k values of various reaction systems. (b) k values over different catalysts in the photo-Fenton-like system.

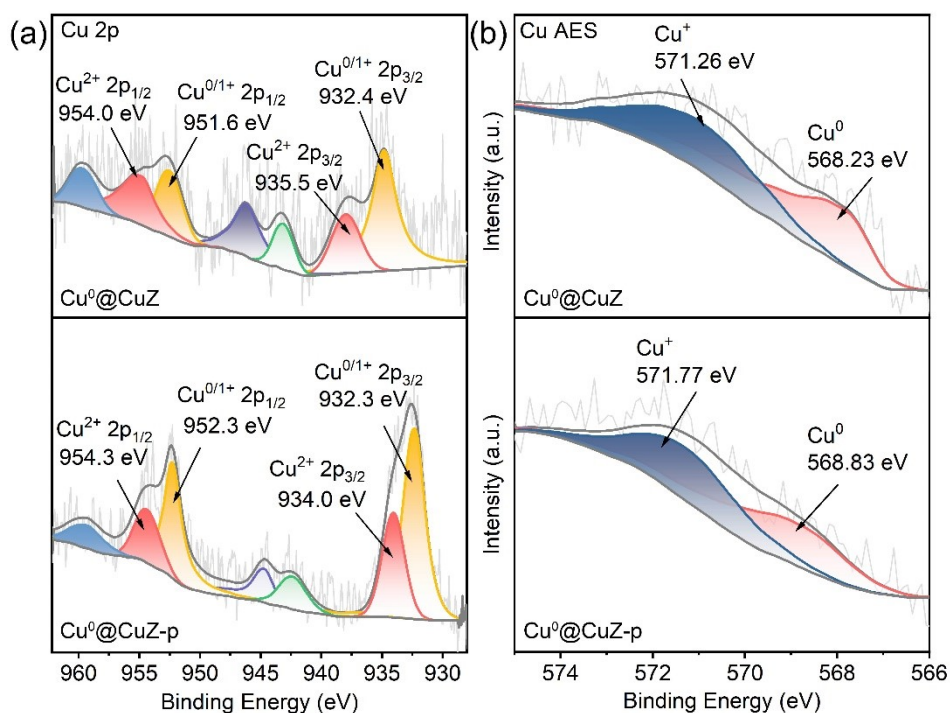


Fig. S7 The high-resolution XPS of Cu 2p and Cu AES spectrum of $\text{Cu}^0@CuZ$ and $\text{Cu}^0@CuZ-p$ after 30 min illumination.

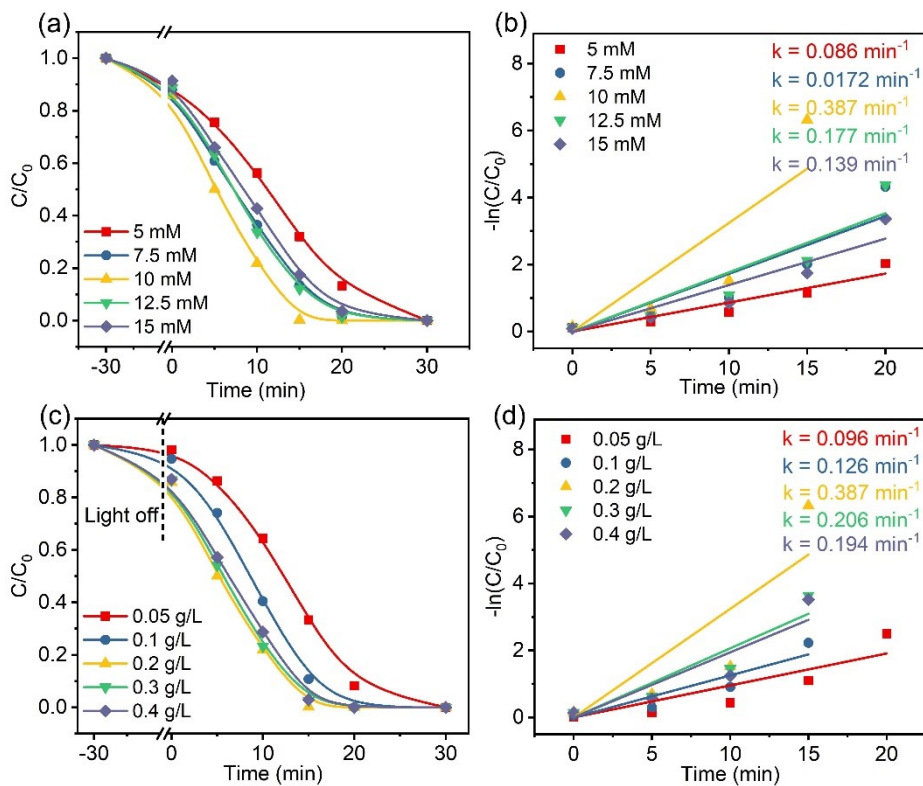


Fig. S8 Effects of (a) H_2O_2 concentration and (b) corresponding k value on phenol removal over $\text{Cu}^0@CuZ$. (c) catalyst dosage and (d) corresponding k value on phenol removal over $\text{Cu}^0@CuZ$.

As depicted in Figs. S6a-b, the phenol removal efficiency increased from 87% to 100% when H_2O_2 concentration raised from 5 to 10 mM, and the k value of $\text{Cu}^0@\text{CuZ}$ markedly increased from 0.086 to 0.387 min^{-1} , which was due to the increasing concentration of H_2O_2 can produce more $\bullet\text{OH}$ for phenol removal. However, both the removal efficiency and the k value decreased as the H_2O_2 concentration further increased to 15 mM, which is due to the fact that the excessive H_2O_2 could be a scavenger for $\bullet\text{OH}$ (An 2023). Therefore, 10 mM H_2O_2 was selected as the optimum reaction parameters. The catalyst dosage influence on phenol removal efficiency was exhibited in Figs. S6c-d. When the $\text{Cu}^0@\text{CuZ}$ dosage was greater than 0.1 g/L, 100% phenol removal efficiency was achieved. Notably, the k value increased from 0.096 to 0.387 min^{-1} with an increase in catalyst dosage from 0.05 to 0.2 g/L, which is owing to that the higher catalyst dosage produces the more H_2O_2 activation sites to generate more $\bullet\text{OH}$, leading to the good phenol removal efficiency. Nevertheless, with further increasing of $\text{Cu}^0@\text{CuZ}$ dosage from 0.2 to 0.4 g/L led the k value decreased. This is mainly attributed to that the superfluous catalysts could reduce the solution transmittance, resulting in light scattering, and the sum total of photons eventually reaching the surface of catalyst would be reduced.

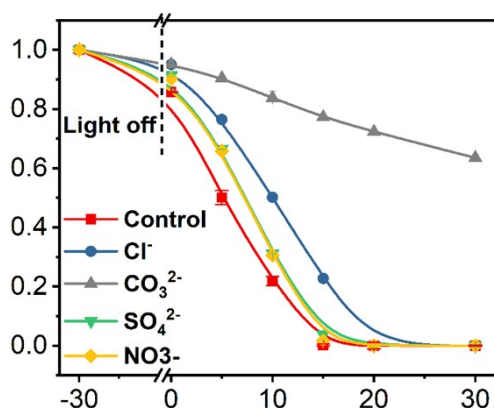
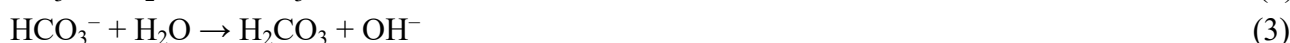


Fig. S9 Effects of coexisting anions on phenol removal efficiency over $\text{Cu}^0@\text{CuZ}$.

The addition of CO_3^{2-} inhibited the phenol removal efficiency by 63%. The reasons for the decrease are as follows: CO_3^{2-} , as trapping agent for $\bullet\text{OH}$, would react with $\bullet\text{OH}$ to generate $\bullet\text{CO}_3^-$ with weak oxidation ability; CO_3^{2-} in the water bodies can easily form HCO_3^- , OH^- , and H_2CO_3 , leading to an increase in reaction system pH value (Eqs. 1–3), and the catalytic activity of the $\text{Cu}^0@\text{CuZ}$ would be hindered.



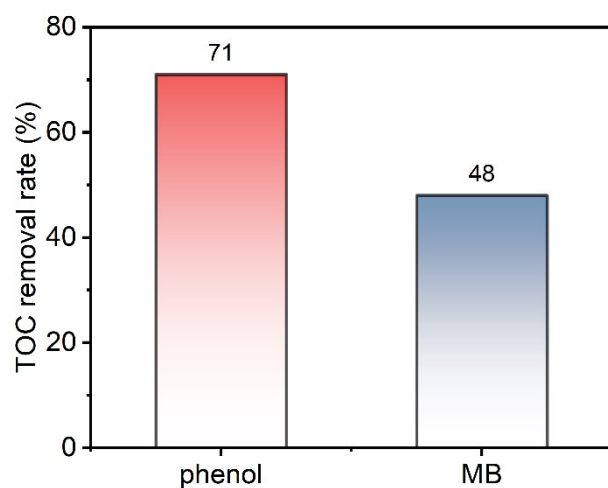


Fig. S10 The TOC removal rate of phenol and MB over $\text{Cu}^0\text{@CuZ}$ in photo-Fenton-like system within 90 min.

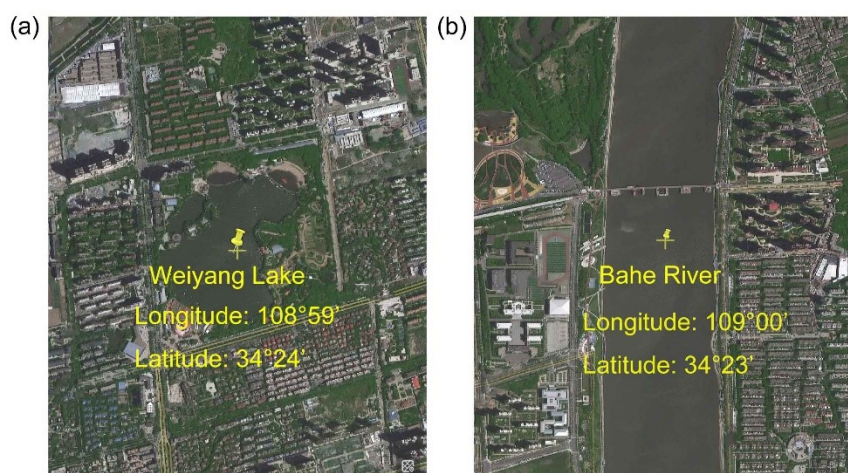


Fig. S11 (a) Lake water and (b) river water intake point.

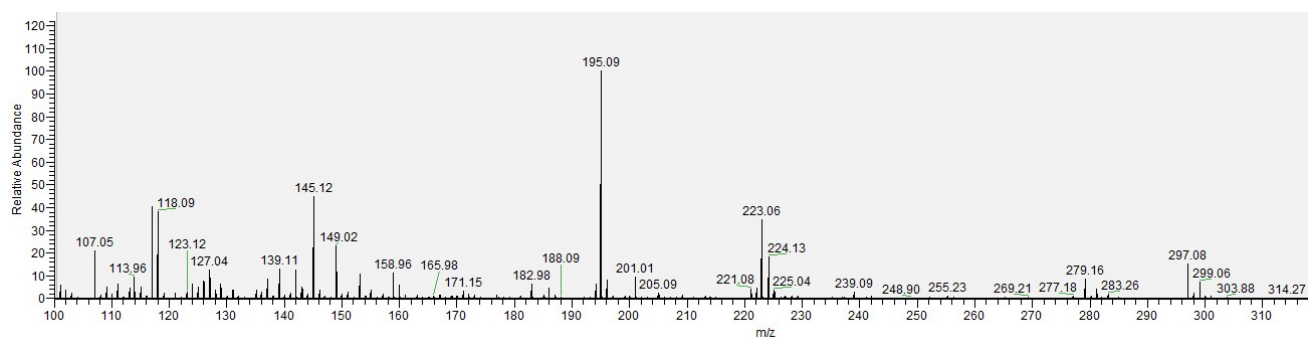


Fig. S12 Mass spectrum peak obtained from the DCF degradation over Cu^0/CuZ after 10 min irradiation.

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