
Supplementary Information

Treasure-Bowl Style Bifunctional Site in Cerium-Tungsten Hetero-Clusters for Superior Solar-Driven Hydrogen Production

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1. Supporting Experimental Section

1.1 Material Preparation

Nickel foam (NF, thickness: 1.5 mm, bulk density: 0.35 g cm⁻³) was purchased from Changsha Lyrun Mater. Co., Ltd. (Changsha, China). Resorcinol, dopamine (DA), formaldehyde, tetraethyl orthosilicate (TEOS), phosphomolybdic acid hydrate (H₃[P(W₃O₁₀)₄]·xH₂O, PW₁₂, AR), cerium nitrate hexahydrate (Ce(NO₃)₃·6H₂O), hydrofluoric acid (HF, AR), ethanol (C₂H₅OH, AR) and potassium hydroxide (KOH) purchased from Aladdin Co., Ltd. (Shanghai, China). Commercial Pt/C (20 wt% Pt on Vulcan XC-72R), ruthenium oxide (RuO₂, 99.9 %) and nafion (5 wt %) were purchased from Sigma-Aldrich. All chemicals were used as received without further purification and all aqueous solutions were prepared with ultrapure water (>18.25 MΩ cm⁻¹) obtained from a Millipore system.

1.2 Preparation of SiO₂ Nanospheres

In general, a precisely measured quantity of 20 mL anhydrous ethanol was combined with 4.16 g of ethyl orthosilicate (TEOS) in a 50 mL beaker labeled as beaker A. The contents were carefully stirred until a homogeneous solution was achieved. Subsequently, in a separate 100 mL beaker denoted as beaker B, a mixture composed of 30.6 g of distilled water, 20 mL of anhydrous ethanol, and 6.8 g of ammonia was prepared. This beaker was then placed on a magnetic agitator and stirred continuously. The solution from beaker A was introduced into beaker B in a gradual dropwise manner during the stirring process. The entire mixture was continuously stirred at room temperature for a duration of 6 hours to facilitate the chemical reaction. Upon completion of the reaction period, the resulting solution was separated using centrifugation at a speed of 8500 revolutions per minute. The resultant pure SiO₂ microspheres were subsequently subjected to calcination within a Muffle furnace at a temperature of

800 °C for a duration of 3 hours. Following the calcination step, the microspheres were allowed to cool naturally to room temperature.

1.3 Synthesis of WN/WC-CeO_{2-x}@PNC

In the standard synthetic procedure, 1.0 g of silica microspheres was evenly dispersed in a pre-mixed solution containing 100 mL ethanol and deionized water (water: ethanol = 7:3). Subsequently, resorcinol (0.15 g), dopamine (0.1 g), and formaldehyde (0.2 mL) were introduced individually into this solution. After 10 minutes, 0.4 mL of tetraethyl orthosilicate was added, and the mixture was maintained at a controlled temperature with continuous stirring for 14 h. Following this, 0.25 mmol of H₃[P(W₃O₁₀)₄]·xH₂O and 0.2 mmol of Ce(NO₃)₃·6H₂O were incorporated, with further agitation for an additional 10 hours. The resulting precipitate was isolated via centrifugation, followed by three washes with ultrapure water and anhydrous ethanol, concluding with overnight vacuum drying at 60 °C. The resultant product then underwent annealing under an argon atmosphere, initially at 500 °C for 30 minutes, followed by carbonization at 900 °C for 3 hours. Finally, the WN/WC-CeO_{2-x}@PNC catalyst was obtained by etching the silica microspheres with a 5 wt% hydrofluoric acid solution. In accordance with the stoichiometric ratios of metal salts, a series of composite materials were synthesized, denoted as Ce₁-W_{0.2}, Ce₁-W_{0.4}, Ce₁-W_{0.6}, Ce₁-W_{0.8} (WN/WC-CeO_{2-x}@PNC), and Ce₁-W₁.

1.4 Synthesis of WN/WC@PNC

Similar to the aforementioned synthesis of WN/WC-CeO_{2-x}@PNC, the omission of Ce(NO₃)₃·6H₂O in the procedure leads to the formation of WN/WC@PNC.

1.5 Synthesis of CeO₂

Firstly, 5 mmol Ce(NO₃)₃·6H₂O was accurately dissolved in 35 mL ultra-pure water, and then 6 g NaOH was added to it. After stirring for 30 min, the mixture was transferred to a hydrothermal reactor

with a capacity of 50 mL in polytetrafluoroethylene tank and kept at 100 °C for 24 h. After the reaction was finished, the product was separated by high speed centrifuge and washed for three times with ultra-pure water and anhydrous ethanol respectively. Finally, the sample was heated to 400 °C at a rate of 5 min/ °C and kept for 4 h, and finally CeO₂ was obtained.

1.6 Material Characterization

The SEM images and EDX elemental mapping were obtained with a Hitachi SU8010 scanning electron microscope (Japan). HRTEM (High resolution transmission electron microscopy), SAED (selected area electron diffraction) and STEM (scanning transmission electron microscope) were performed by Thermo Fisher Scientific Talos F200S. Powder X-ray diffraction data (XRD) pattern was recorded on a Rigaku TTRIII-18KW diffractometer operated at 40 kV voltage and 30 mA current using Cu K α radiation ($\lambda = 1.5418 \text{ \AA}$) in the range of 10 - 80°. Raman spectroscopy was recorded using a confocal Raman spectrometer (Renishaw, RM2000) that was operated using an Ar⁺ laser (532 nm wavelength) as the excitation source. The room temperature electron paramagnetic resonance spectroscopy (EPR) spectra were recorded on an X-band ($\nu_{mw} = 9.84 \text{ GHz}$) EMXmicro BRUKER spectrometer. X-ray photoelectron spectroscopy (XPS) studies were performed by means of a Thermo Fisher K-Alpha⁺ equipped with monochromatic Al K α radiation (150 W, 5 kV at 1486.6 eV). The chamber pressure for the spectrometer was kept at 10⁻⁹ Torr. The surface charge was corrected by referencing the spectra to the C 1s peak for the C-C bond at a binding energy of 284.8 eV. Raman spectra of the samples were recorded on a WITec system with a 355 nm excitation wavelength. Specific surface area and corresponding pore size distribution were quantitatively determined by measuring N₂ adsorption-desorption isotherms on a Quantachrome apparatus (Micrometrics, ASAP 2020), using the Brunauer-Emmett-Teller (BET) and Barrett-Joyner-Halenda (BJH) methods, respectively. XAS tests

were performed at the photoemission end-station at beamline BL11B of National Synchrotron Radiation Laboratory (NSRL) in Shanghai, China. XAS data extracted and analyzed using the Athena and Artemis codes. Inductively coupled plasma optical emission spectroscopy (ICP-OES, Agilent 5110) was carried out to determine the contents doped into copper in precursor, 5 mg of the sample was completely dissolved into 1 L deionized water with 5 mM HNO₃ and sonicated for 30 min for the ICP-OES test.

1.7 Electrochemical Measurements

Electrochemical measurements were performed using a conventional three-electrode configuration on a CHI 760E electrochemical workstation (CHI Instruments, Inc., Shanghai, China). A graphite rod and a reversible hydrogen electrode were used as the counter electrode and reference electrode, respectively. The catalyst ink was prepared as follows: 5 mg catalyst was suspended in a mixture containing 980 μ L water/ethanol (V:V = 1:1) and 20 μ L 5 wt% Nafion suspension, followed by 30 min sonication to form a homogeneous ink. 20 μ L of the catalyst suspension was deposited onto a carbon paper (CP) with an area of 0.5 cm \times 1.0 cm and dried at room temperature. The RuO₂ and 20 wt% Pt/C modified NF electrodes were obtained by the same method. Before the electrochemical experiments, the newly prepared 1.0 M KOH was first bubbled with high-purity Ar (for HER) or O₂ (for OER) for \approx 30 min and then the electrolyte was blanketed with an N₂/Ar or O₂ atmosphere during the entire testing process. Subsequently, CV scans were conducted in the potential window of -0.477 - 0.523 V versus RHE (for HER) or 1.023 - 2.023 V versus RHE (for OER) for several cycles until stable. Then, the linear sweep voltammetry (LSV) plots were obtained with a scan rate of 5 mV s⁻¹. All the polarization curves were corrected after iR compensation by using the equation: $E_{\text{corrected}} = E_{\text{measured}} - iR$, where i is the current and R is the uncompensated ohmic electrolyte resistance. The HER and OER cycling stability tests were conducted by the corresponding long-term CV tests (3000 cycles), after which the related LSV

curves were recorded and compared with that of their initial LSV curves. All measured potentials were referred to the reversible hydrogen electrode (RHE) using the following equation: $E(\text{RHE}) = E(\text{Hg}/\text{HgO}) + 0.059 \times \text{pH} + 0.098 \text{ V}$ and the current densities (j) were normalized by geometric surface area. For the HER, linear sweep voltammetry at a scan rate of 5 mV s^{-1} was conducted in 1 M KOH for all samples, and data were obtained with iR compensation of 90% . Electrochemical impedance spectroscopy (EIS) was carried out from 100 kHz to 0.1 Hz at the given potential with AC amplitude of 10 mV .

1.8 *STH Conversion Efficiency Calculation*

For the overall water splitting system that produces hydrogen and oxygen molecules using only commercial GaAs solar power as the input, the solar-to-hydrogen conversion efficiency (*STH*) is defined as:

$$STH = \frac{\text{Chemical energy output}}{\text{Solar energy input}} = \frac{j_{op} \times A \times E_f \times FE_{H_2}}{P_s \times A} = \frac{1.23 \times j_{op}}{P_s} \times 100\%$$

Here, j_{op} represents the operating current density of the combined system, A is the effective illuminated area, E_f is the standard thermodynamic potential difference between hydrogen evolution and oxygen evolution half-reactions (1.23 V) that is corresponded to the change of Gibbs free energy of overall water splitting, FE_{H_2} is the faradic efficiency for hydrogen evolution that is assumed to be 100% and P_s is the power of solar illumination ($\text{AM } 1.5\text{G } 100 \text{ mW cm}^{-2}$).

1.9 *Theoretical calculation*

We have employed the first-principles [1,2] to perform all Spin-polarization density functional theory (DFT) calculations within the generalized gradient approximation (GGA) using the Perdew-Burke-Ernzerhof (PBE) [3] formulation. We have chosen the projected augmented wave (PAW) potentials [4,5] to describe the ionic cores and take valence electrons into account using a plane wave basis set with a kinetic energy cutoff of 450 eV . Van der Waals interactions have been considered using

the DFT-D3 method of Grimme [6,7]. The electronic energy was considered self-consistent when the energy change was smaller than 10^{-5} eV. A geometry optimization was considered convergent when the energy change was smaller than 0.02 eV \AA^{-1} . During the relaxation, the Brillouin zone with a $3 \times 3 \times 1$ Gamma centered grid was used. The 15 \AA vacuum layer was normally added to the surface to eliminate the artificial interactions between periodic images. Spin polarized calculations were performed for this calculation.

WC/WN, WC/WN-CeO₂ and WC/WN-CeO_{2-x}-Ov according to the STEM results were employed as the models to further determine the intrinsic mechanism for the excellent catalytic activity. In the vertical direction, a vacuum layer of about 15 \AA in thickness was introduced to avoid the interaction between neighboring image structures.

In all the calculations, we use $3 \times 2 \times 1$ for the Monkhorst-Pack k-point for periodic crystal structure and surface model. The convergence threshold for energy was set at 10^{-5} eV. [8] The equilibrium lattice constants were optimized with maximum stress on each atom within 0.05 eV/ \AA . In order to precisely reflect the calculations, the DFT+U corrections for 5d transition metal (W: 6 eV) were employed.[9]

The adsorption energy (ΔE_{ads}) was defined as follows:

$$E_{\text{ads}} = E_{\text{ad/sub}} - E_{\text{ad}} - E_{\text{sub}}$$

where $E_{\text{ad/sub}}$, E_{ad} and E_{sub} are the optimized adsorbate/substrate system, the adsorbate in the structure and the clean substrate respectively. Usually, a more negative E_{ads} value reflects stronger adsorption.

The free energy was calculated using the equation:

$$\Delta G = \Delta E + \Delta \text{ZPE} - \Delta \text{TS}$$

Where ΔG , ΔE , ΔZPE , and TS represented the free energy, total energy from DFT calculations, zero-point energy, and entropic contributions (T was set to be 300 K), respectively.



2. Supporting Figures

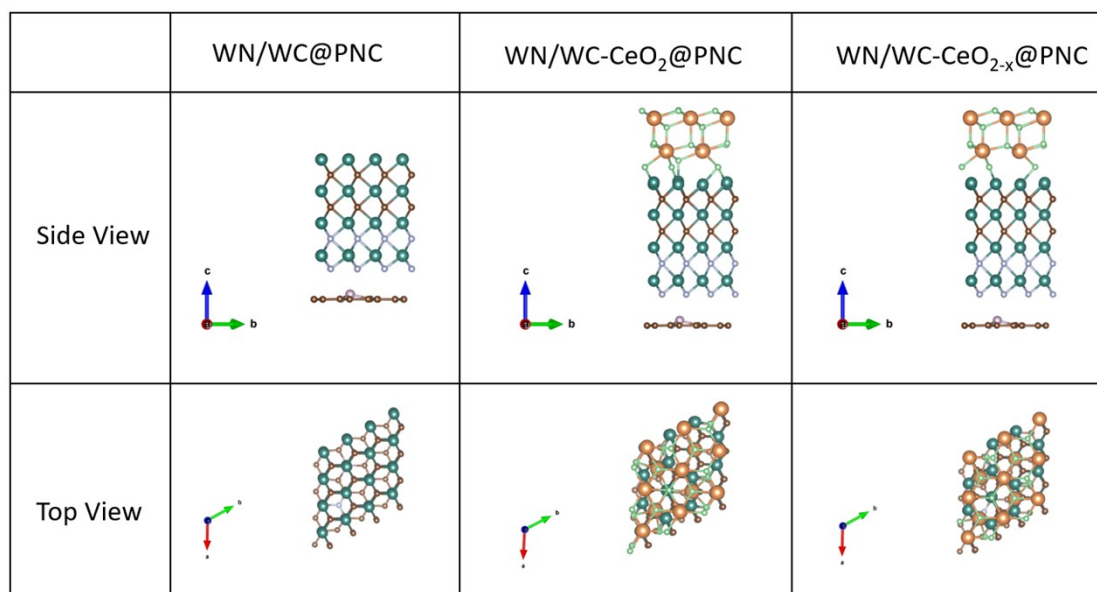


Figure S1. The optimized atomic models of WN/WC@PNC, WN/WC-CeO₂@PNC and WN/WC-CeO_{2-x}@PNC.

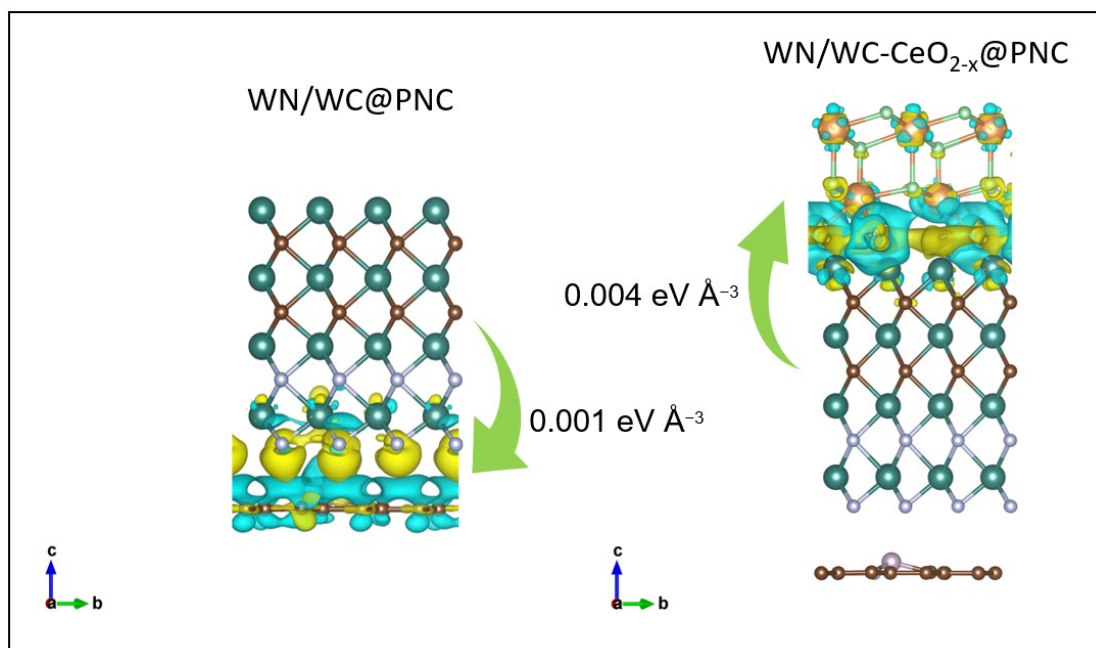


Figure S2. The charge density difference of the WN/WC@PNC and WN/WC-CeO_{2-x}@PNC.

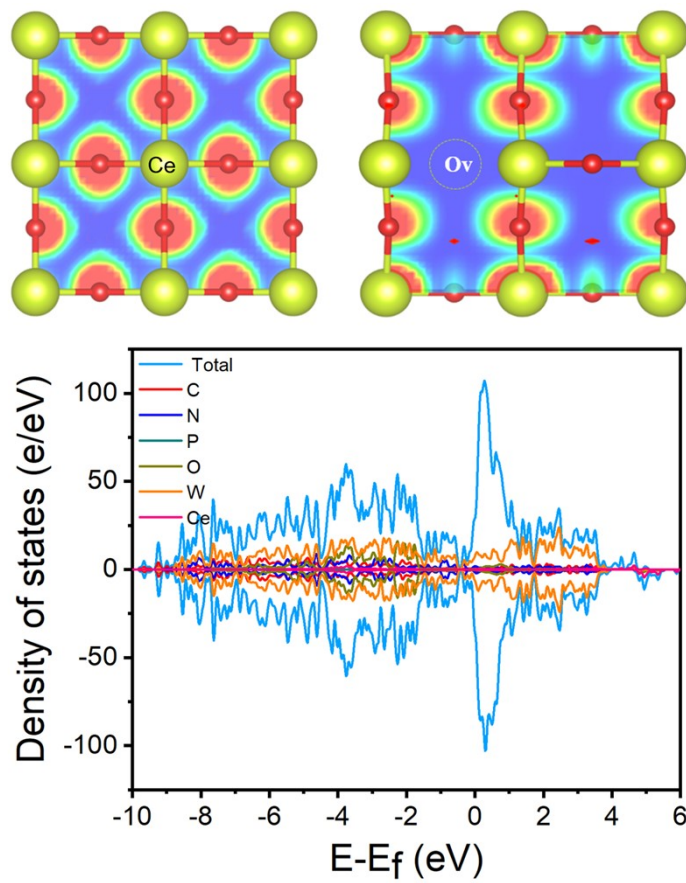


Figure S3. Density of states of WN/WC-CeO₂@PNC.

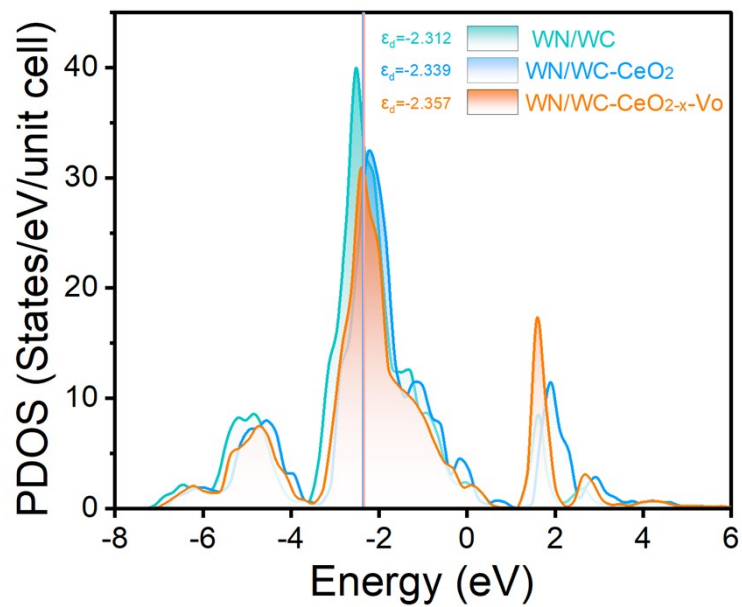


Figure S4. *d*-band centers for WN/WC, WN/WC-CeO₂, and WN/WC-CeO_{2-x}-O_v.

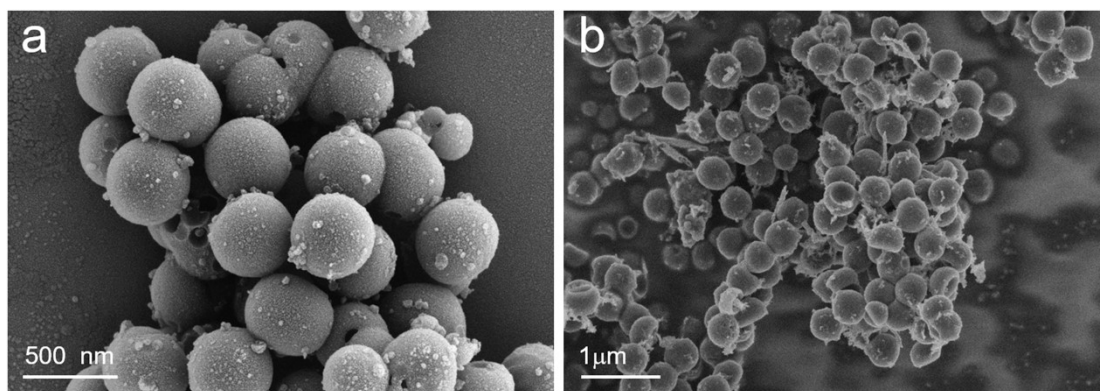


Figure S5. SEM images of (a) $\text{SiO}_2@\text{Ce-PW}_{12}@\text{RF/SiO}_2$ and (b) $\text{SiO}_2@\text{WN/WC-CeO}_{2-x}@\text{PNC}$.

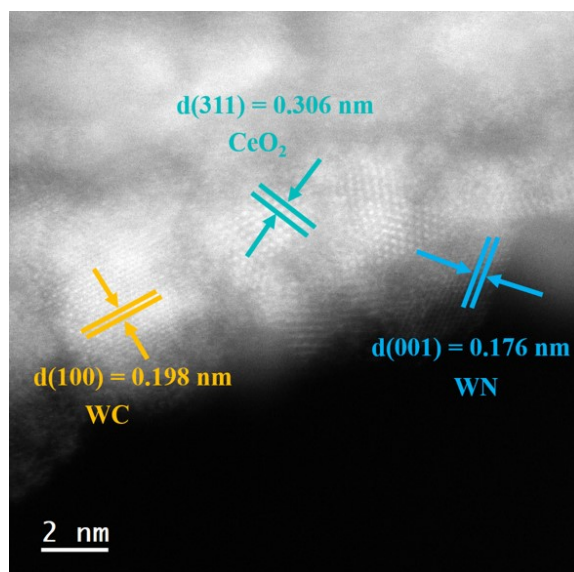


Figure S6. High-resolution TEM images of WN/WC-CeO_{2-x}@PNC.

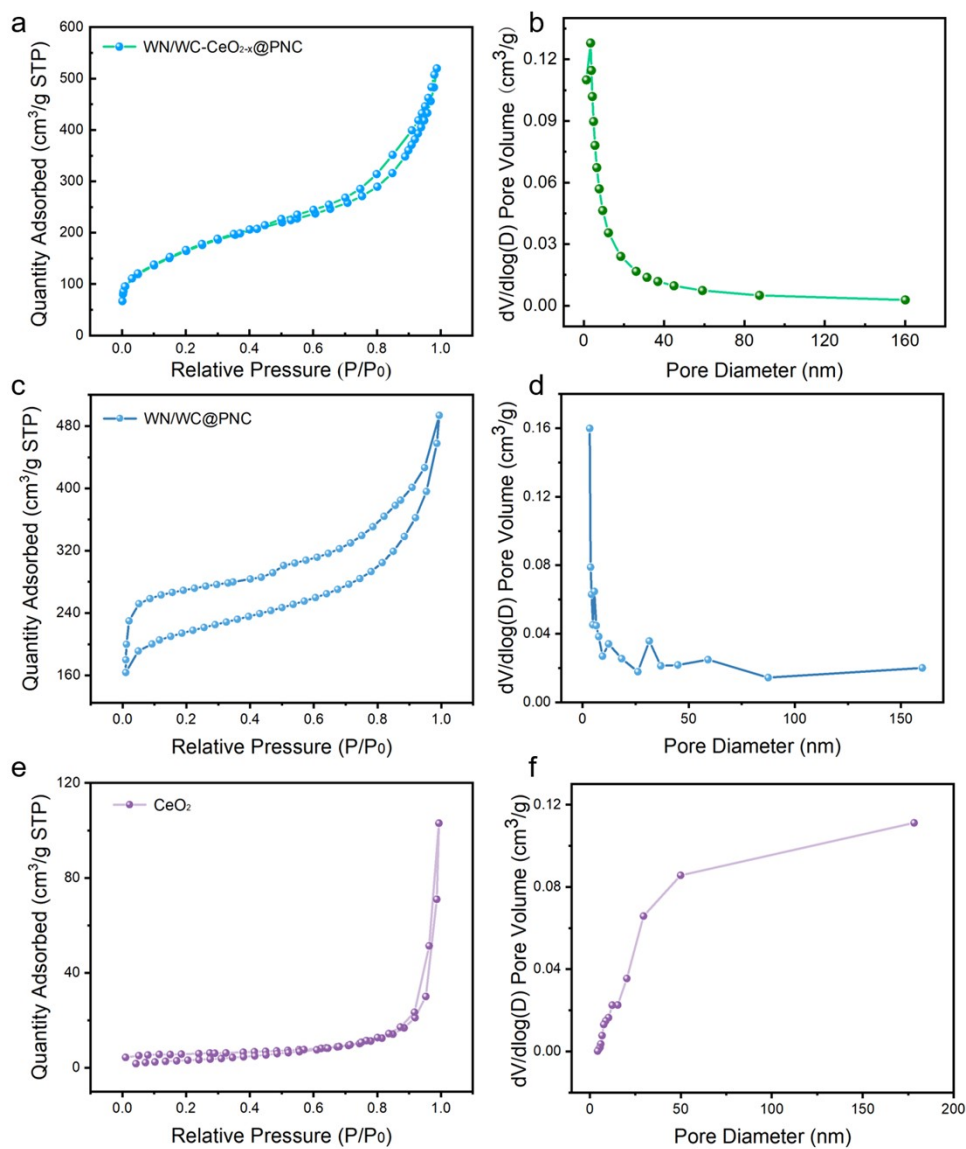


Figure S7. N_2 adsorption–desorption isotherms and (inset) using the BJH (Barrett-Joyner-Halenda) method calculated corresponding pore size distributions of the (a, b) $\text{WN/WC-CeO}_{2-x}\text{@PNC}$, (c, d) WN/WC@PNC , and (e, f) CeO_2 .

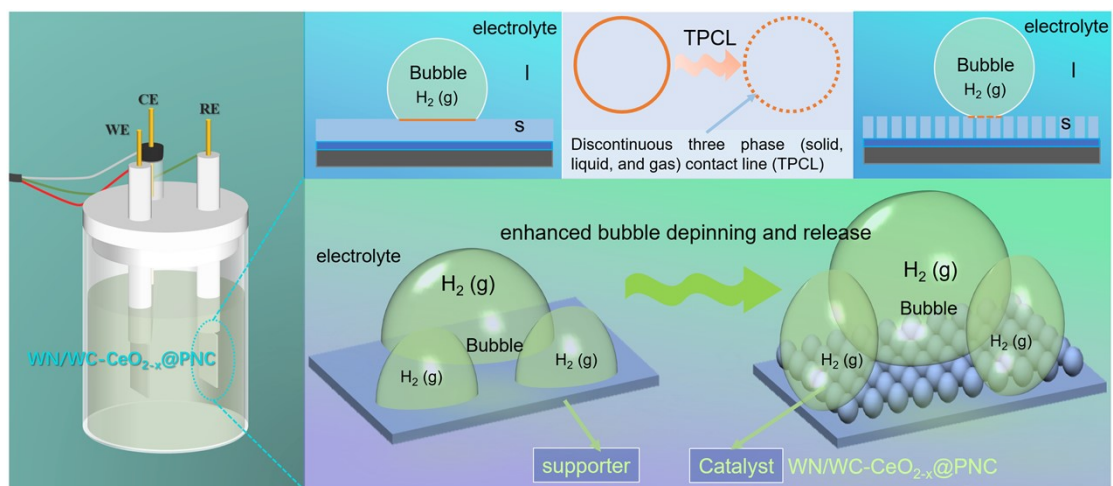


Figure S8. Schematic illustration of how the surface roughness affecting the bubble contact angle at the

$\text{WN/WC-CeO}_{2-x}\text{@PNC}$

clusters.

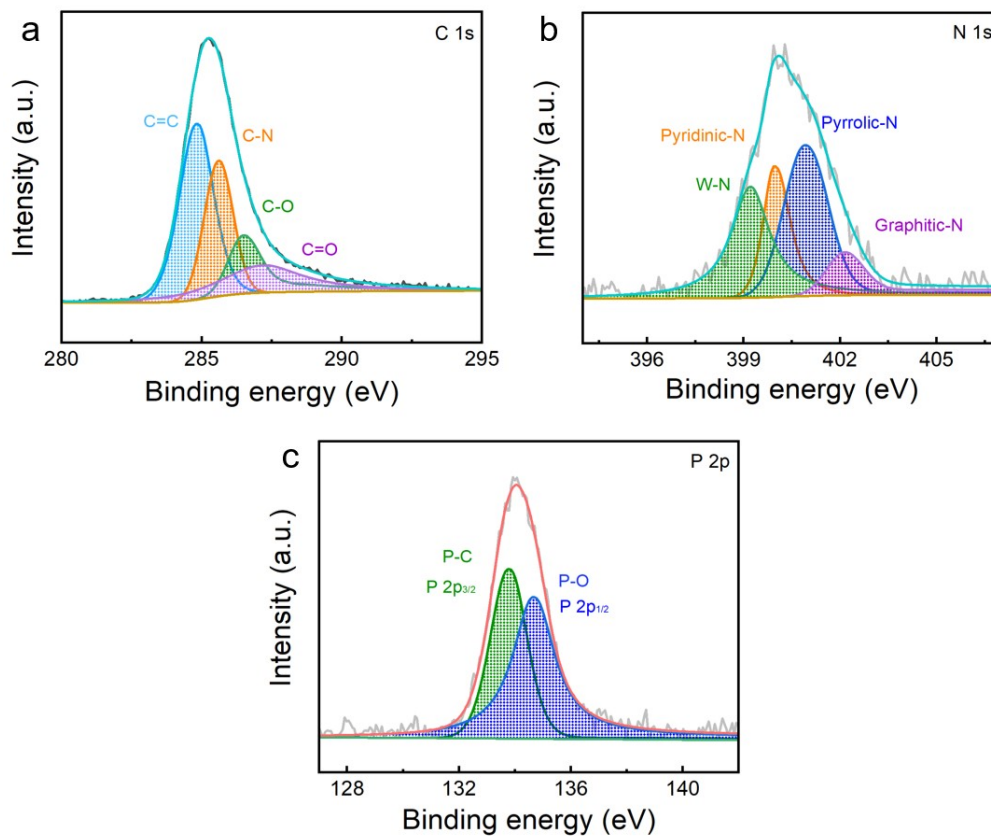


Figure S9. XPS survey spectra and high-resolution (a) C 1s, (b) N 1s, and (c) P 2p, XPS profiles of WN/WC-CeO_{2-x}@PNC.

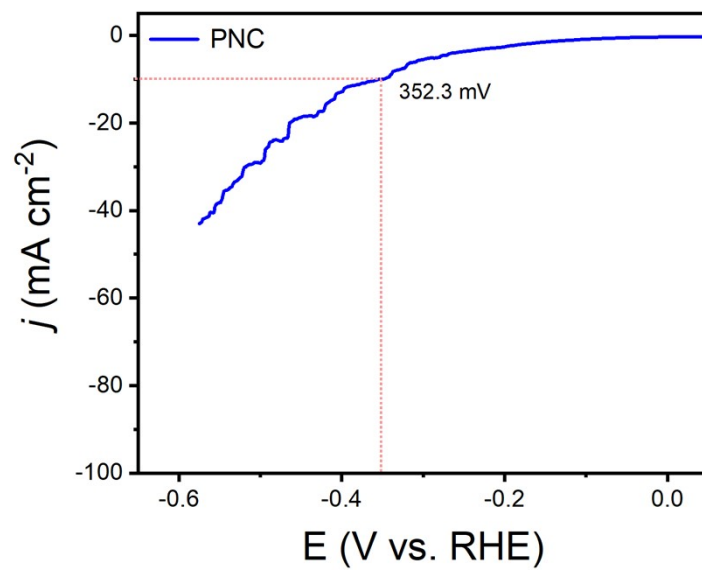


Figure S10. LSV curves of PNC samples in 1.0 M KOH for HER.

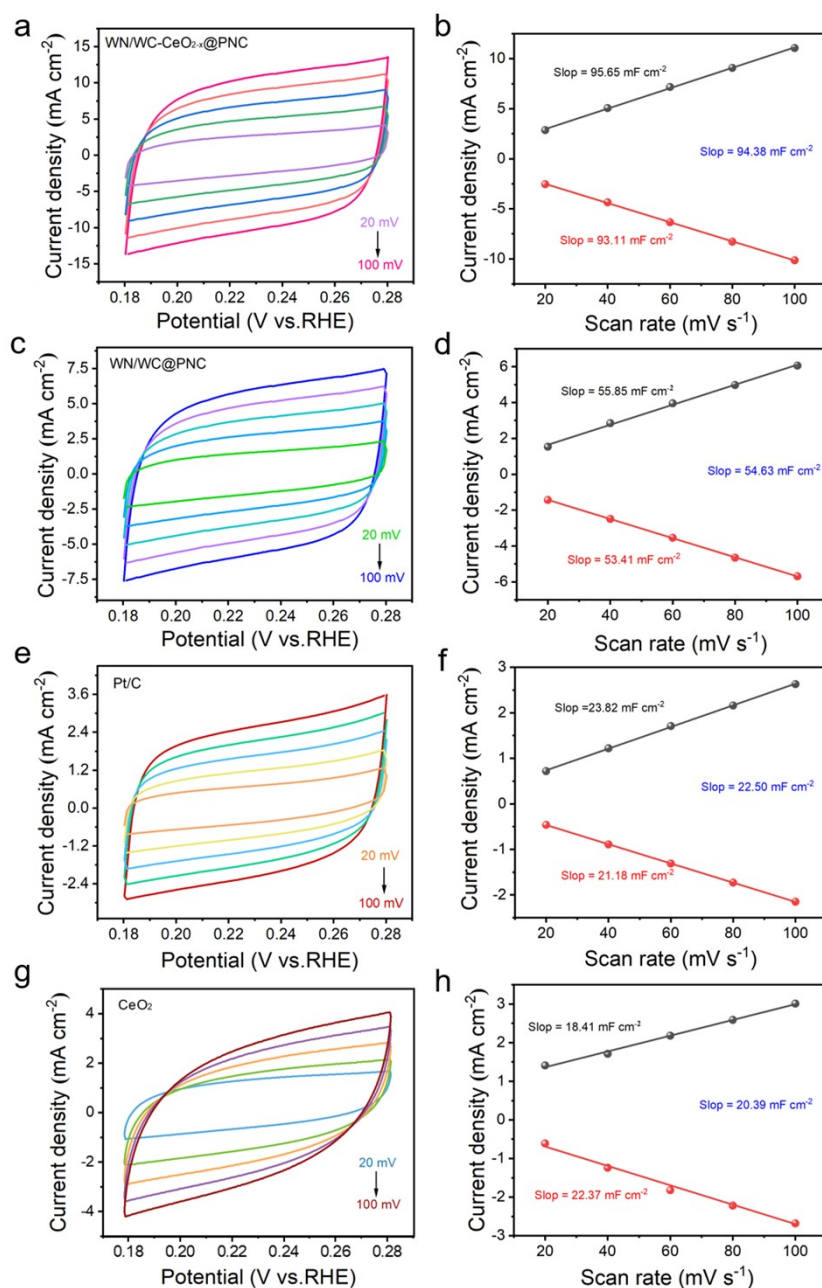


Figure S11. In the non-faradic capacitance current range of 20 to 100 mV s⁻¹, cyclic voltammograms of (a, b) WN/WC-CeO_{2-x}@PNC, (c, d) WN/WC@PNC, (e, f) Pt/C, and (g, h) CeO₂ were recorded.

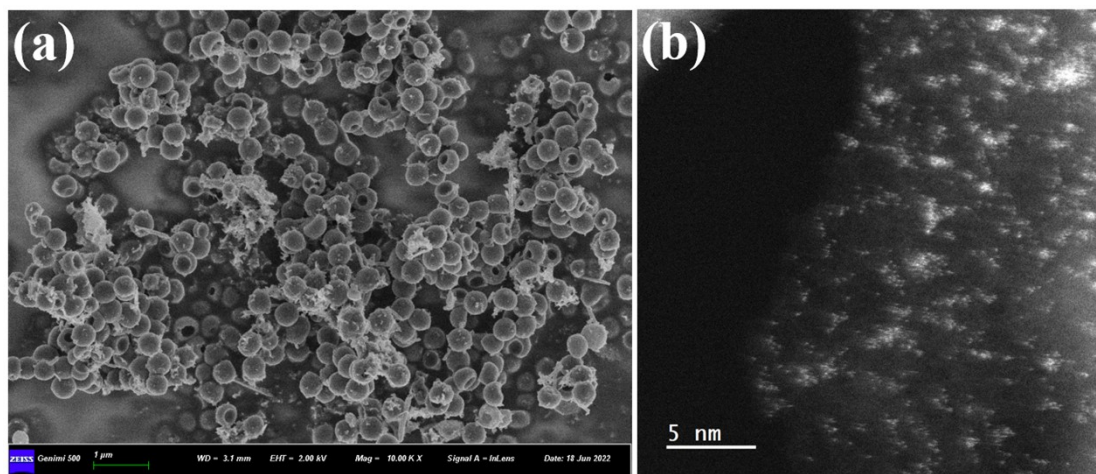


Figure S12. (a) SEM and (b) STEM images of WN/WC-CeO_{2-x}@PNC after the HER durability test at different magnifications.

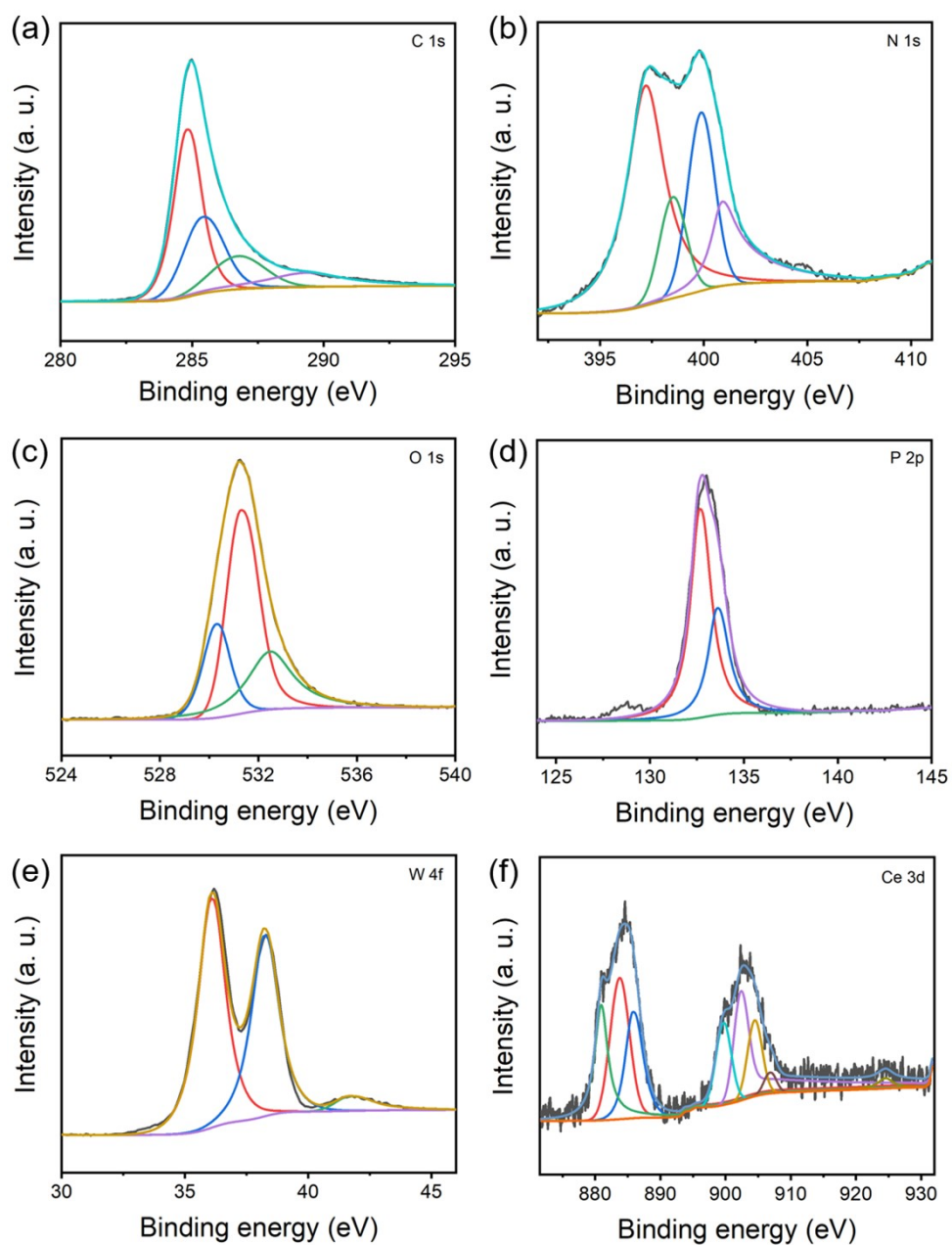


Figure S13. Post characterizations of WN/WC-CeO_{2-x}@PNC catalyst after HER stability test. (a)

C 1s, (b) N 1s, (c) O 1s, (d) P 2p, (e) W 4f and (f) Ce 3d core level XPS spectra.

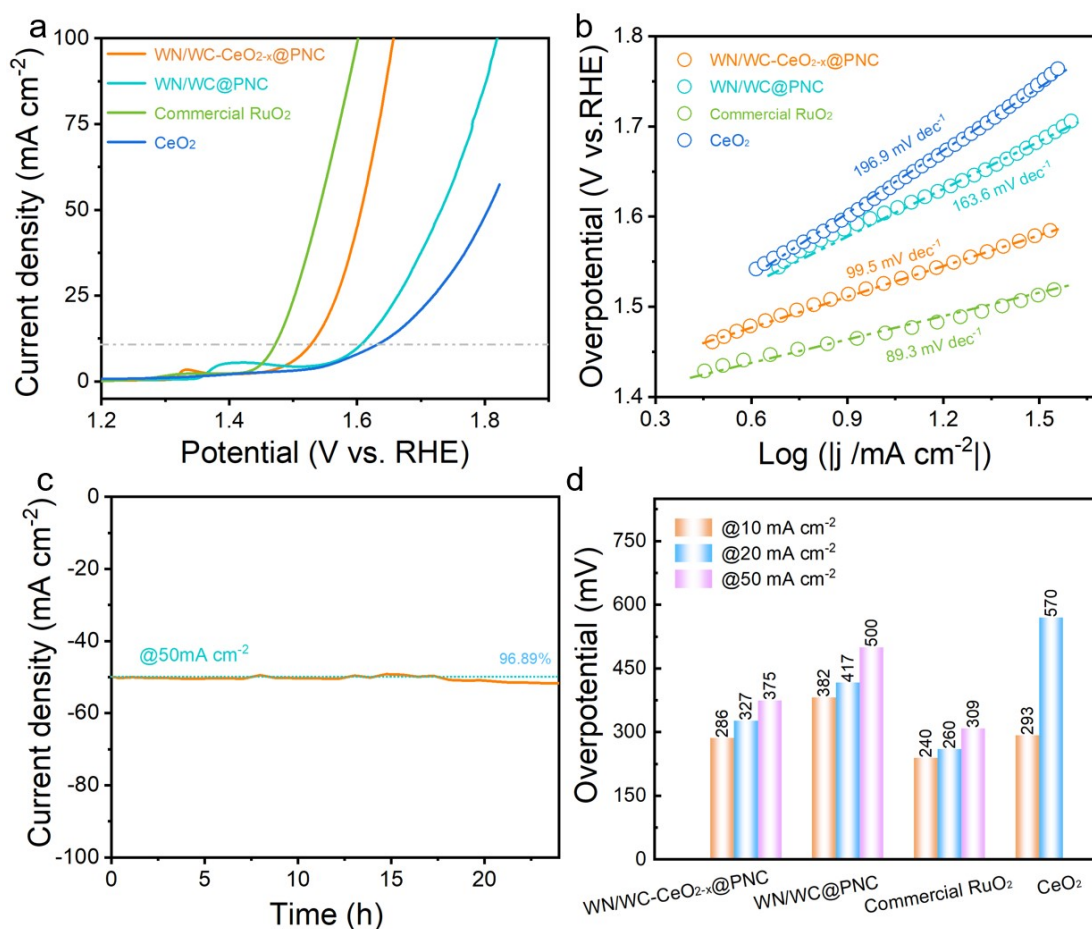


Figure S14. OER catalytic activity evaluation. (a) Polarization curves of all the catalysts for OER. (b) Tafel plots derived from (a) for various catalysts. (c) Chronoamperometric curve of WN/WC-CeO_{2-x}@PNC electrode. (d) Potential requirements at 10, 20 and 50 mA cm^{-2} for all the catalysts.

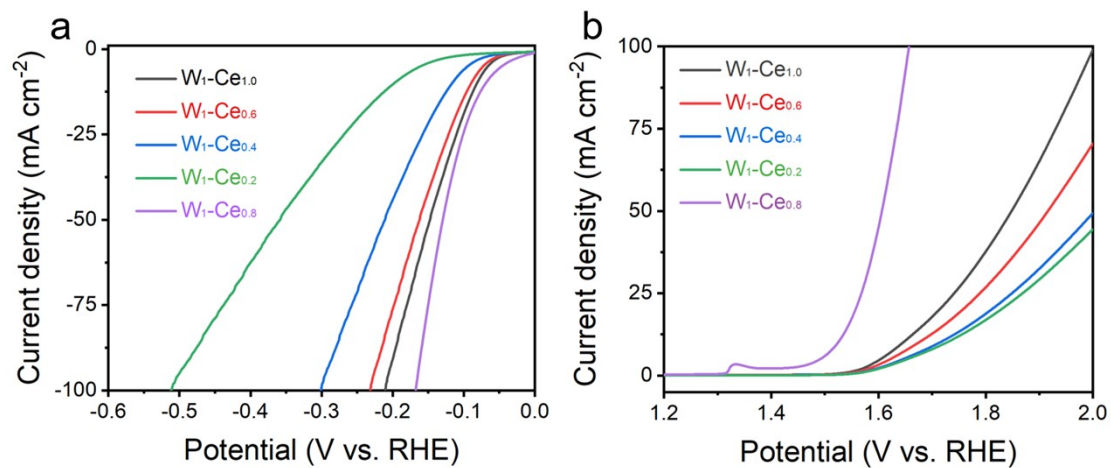


Figure S15. Electrodes with varying W:Ce molar ratios were used for the polarization curves of (a) HER and (b) OER.

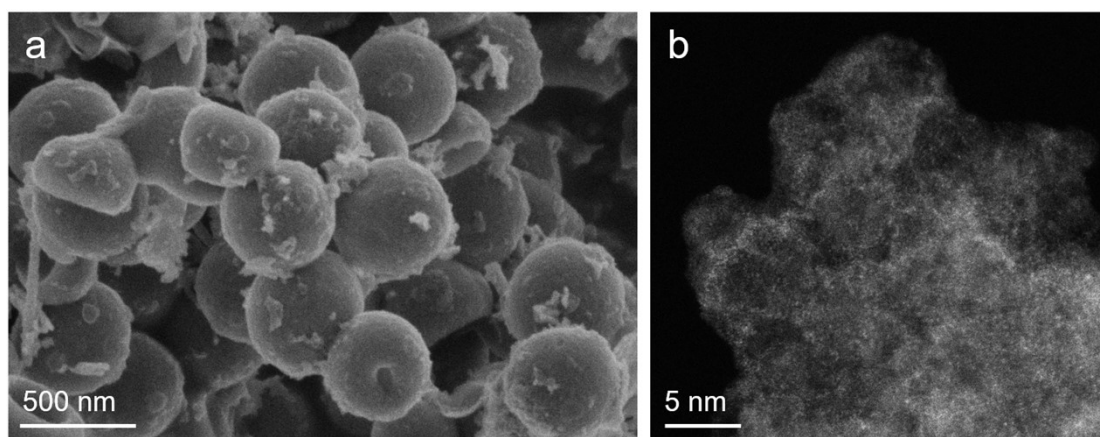


Figure S16. (a) SEM image and (b) STEM image of Ce₁-W_{0.2} catalyst.

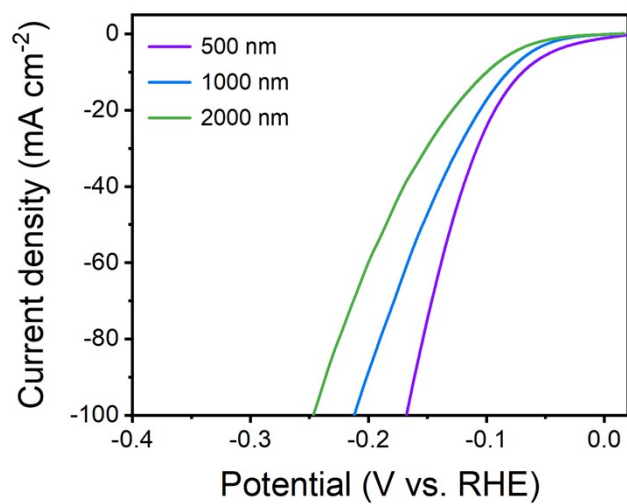


Figure S17. Polarization curves of different sized catalyst electrodes for HER.

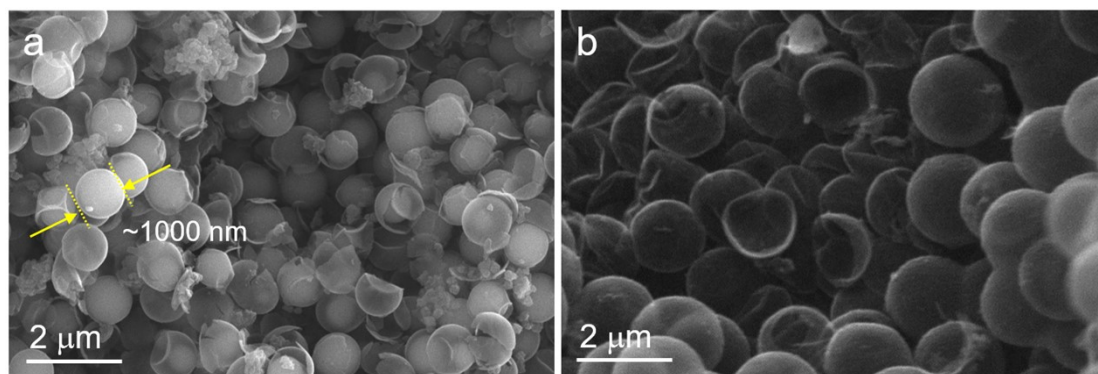


Figure S18. SEM images of Ce₁-W_{0.8} catalysts at different sizes.

3. Supporting Tables

Table S1. Lattice parameters of the samples.

Samples	Lattice types	Lengths(Å)			Angles(°)		
		a	b	c	α	β	γ
WN/WC	P	8.412	8.427	32.000	90	90	119.976
WN/WC-CeO ₂	P	8.072	8.080	35.000	90	90	119.988
WN/WC-CeO _{2-x} -O _v	P	8.072	8.080	35.000	90	90	119.988

Table S2. The specific surface area, pore diameter, and pore volume of the sample.

Catalyst	Surface area (m²/g)	Pore volume (cm³/g)	Average pore (nm)
WN/WC-CeO_{2-x}@PNC	188.63	0.128	3.123
WN/WC@PNC	120.31	0.113	3.201
CeO₂	36.27	0.085	13.62

Table S3. Metal content of WN/WC-CeO_{2-x}@PNC by ICP-OES.

WN/WC-CeO _{2-x} @PNC	W (wt%)	Ce (wt%)
	8.22 %	1.09 %
post-HER of WN/WC-CeO _{2-x} @PNC	W (mg/L)	Ce (mg/L)
	1.306	0.002

Table S4. HER performances of WN/WC-CeO_{2-x}@PNC and other reported electrocatalysts in the literature.

Catalyst	Electrolyte	$\eta_{10}(\text{mV})$ ($j=10\text{mA cm}^{-2}$) 2)	Tafel slope (mV dec^{-1})	Reference
WN/WC-CeO _{2-x} @PNC	1 M KOH	68.6	39.1	This work
Co ₂ P/WC@NC	1 M KOH	180	90	10
W ₂ N/WC	1 M KOH	148.5	47.4	11
Cu@WC	1 M KOH	119	88.7	12
WN-Ni@N,P-CNT	1 M KOH	70	151.7	13
Mo ₂ C-WC/NCA	1 M KOH	126	59	14
Co/WC@NC	1 M KOH	142	91	15
RuO ₂ -WC NPs	1 M KOH	58	66	16
CeO ₂ /Co(OH) ₂ HCs	1 M KOH	309	144	17
WSe ₂	1 M KOH	150	78	18
Co/CeO ₂ /Co ₂ P/CoP@NC	1 M KOH	195	66	19
WP ₂ /NF	1 M KOH	130	94	20
Ni-rGO/CeO ₂	1 M KOH	113	121	21
VN/WN@NC	1 M KOH	122	67	22
W ₂ N layer	1 M KOH	232	102	23
N-doped W ₂ C/WC	1 M KOH	127	62.7	24
W ₂ C	1 M KOH	274	112	25

Co/WC@NC	1 M KOH	142	91	26
W-W ₂ C/CNT	1 M KOH	147	51	27
W ₂ C-NC-WN	1 M KOH	145	96	28
W ₂ C/WP@NC	1 M KOH	116	59	29
W ₂ C/C NFs	1 M KOH	81	89	30

Table S5. Overall water splitting performances of WN/WC-CeO_{2-x}@PNC and other reported electrocatalysts in the literature.

Catalyst	Electrolyte	Cell voltage(V) ($j=10\text{mA cm}^{-2}$)	Reference
WN/WC-CeO _{2-x} @PNC	1 M KOH	1.55	This work
RuO ₂ -WC NPs	1 M KOH	1.66	31
WN-Ni(OH) ₂	1 M KOH	1.7	32
WP ₂ NW/NF	1 M KOH	1.65	33
W ₂ C/WP@NC	1 M KOH	1.72	34
WC/Co ₃ W ₃ N/Co@NC	1 M KOH	1.61	35
V-CoP@ a-CeO ₂	1 M KOH	1.56	36
g-C ₃ N ₄ /CeO ₂ /Fe ₃ O ₄	1 M KOH	1.94	37
Co/CeO ₂ /Co ₂ P/CoP@NC	1 M KOH	1.76	38
CeO ₂ /Ni-TMO	1 M KOH	1.58	39
Co ₃ S ₄ /CeO ₂ -CF	1 M KOH	1.64	40
Pt/C-RuO ₂	1 M KOH	1.7	40
CoWO ₄ /CoP ₂ /CNTF	1 M KOH	1.605	41
NiCoMnFe-P	1 M KOH	1.71	42
NiFe-LDHs@ γ -MnOOH	1 M KOH	1.69	43
CeO ₂ /Co@NCH	1 M KOH	1.74	44
Co ₃ O ₄ -CeO ₂ @FNF	1 M KOH	1.59	45

Table S6. Comparison of *STH* efficiency of reported water splitting systems in the literature.

A systematic comparison of the *STH* efficiencies reported in the literature confirms the present work achieves the highest reported *STH* efficiency (18.92%) under 1 sun illumination.

Year	Catalyst		STH (%)	Reference
	Cathode/anode			
2015	Pt/RuO ₂		8.0	46
2015	GaInP ₂		8.6	47
2015	Ni-Mo		10.5	48
2016	ZnO:Co		12.7	49
2017	Na _{0.08} Ni _{0.9} Fe _{0.1} O ₂		11.22	50
2018	NiFe NPs		9.7	51
2018	Ni-Co-S/Ni-Co-P		10.8	52
2019	NiMoFeP		12.3	53
2019	NiFe		17.52	54
2019	NiCo ₂ S ₄		18.01	55
2019	CC/TiC/Pt and NiFe LDH		18.7	56
2020	NiFe/carbon nanotube		12.3	57
2021	H-FeNiP		5.57	58
2021	Au- Fe ₃ O ₄ /N-TiO ₂		11.9	59
2021	(Co,Fe)PO ₄		12.8	60

2021	WO ₃	13	61
2021	NiMP/NF	14	62
2021	Co-NC@CC	15.26	63
2022	p-Ni ₅ P ₄ @NF	14.5	64
2022	Co ₂ P/Mo ₂ C@NC	18.1	65
2023	Er-NiCoP/NF	19.6	66
2023	NiFe(OH) _x -Ni ₃ S ₂ /NF	20.05	67
2023	NiFeO-CeO ₂ /NF	20.1	68
2023	WN/WC-CeO _{2-x} @PNC	18.92	This work

4. Supporting References

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