

## Supporting Information

### **Heterointerface regulation of covalent organic framework-anchored graphene *via* a solvent-free strategy for high-performance supercapacitor and hybrid capacitive deionization electrodes**

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## Materials

Benzene-1,2,4,5-tetraamine tetrahydrochloride (BA, 97%) was purchased from Bide Pharmatech Ltd. Hexaketocyclohexane octahydrate (HC, 98%) was purchased from Meryer (Shanghai) Chemical Technology Co., Ltd. P-toluenesulfonic acid monohydrate (PTSA, 98%), polyvinylidene fluoride (PVDF,  $\geq 99.5\%$ ), 1-methyl-2-pyrrolidone (NMP,  $\geq 99.5\%$ ), and sodium chloride (NaCl,  $\geq 99.5\%$ ) purchased from Sinopharm Chemical Reagent Co., Ltd (Shanghai, China). AC (4~7  $\mu\text{m}$ ) was purchased from Kuraray (Shanghai) Co., Ltd. All the chemicals were used without further purification.

## Structural characterizations

The microstructure of the samples was observed by scanning electron microscopy (SEM, Hitachi S-4800) and field emission transmission electron microscopy (TEM, JEM 2010 JEOL). The crystal structure was examined by X-ray diffraction (XRD, Panalytical PRO PW3040/60) with Cu K $\alpha$  ( $\lambda=1.54056$  Å). The chemical structure and elemental composition were observed by Fourier Transform Infrared Spectrometer (FT-IR, Nicolet iS-50) and powder X-ray photoelectron spectroscopy (XPS, Thermo ESCALAB 250XI). Specific surface area and pore size distribution were calculated by the Brunauer-Emmett-Teller (BET, Autosorb iQ) method, and the density functional theory pore model of Barret-Joyner-Halenda was used to analyze the specific surface area and pore size distribution.

## Preparation of working electrode

80 wt.% active material, 10 wt.% Super P (conductive agent) and 10 wt.% polyvinylidene fluoride (binder) were mixed in 1-methyl-2-pyrrolidone to form a homogeneous slurry. Then, the slurry was uniformly cast on graphite substrates (4 cm<sup>2</sup> for the three-electrode system and 32 cm<sup>2</sup> for the CDI cell). Finally, the working electrode was dried at 80 °C under vacuum conditions overnight. For the electrochemical and desalination tests, the mass loading of active material on the working electrode was about 4 mg and 60 mg, respectively.

## Electrochemical characterizations

The electrochemical performance of the working electrode was measured by cyclic voltammetry (CV), galvanostatic charge-discharge (GCD), and electrochemical impedance spectroscopy (EIS) in an open environment using a CHI660E electrochemical analyzer (Shanghai, China) with 1 M NaCl solution as electrolyte. In the three-electrode system, Ag/AgCl and a platinum mesh were used as the reference and counter electrodes, respectively.

## Electrochemical calculation

For the three-electrode system, the specific capacitance ( $C_{S1}$ , F g<sup>-1</sup>) of the material was calculated from CV curves according to the following formula:<sup>1</sup>

$$C_{S1} = \frac{\int_{E_1}^{E_2} i(E)d(E)}{2mv(E_2 - E_1)} \quad (S1)$$

where  $E_1$  and  $E_2$  are the cutoff potentials in CV,  $i(E)$  is the instantaneous current,  $i(E)d(E)$  is the total voltammetric charge obtained by integration of the positive and negative sweeps in the CV,  $v$  is the scan rate, and  $m$  is the mass of the individual sample. The specific capacitance ( $C_{S2}$ , F g<sup>-1</sup>) was calculated from the GCD curves according to the following equation:<sup>2</sup>

$$C_{S2} = \frac{I * \Delta t}{m * \Delta V} \quad (S2)$$

where  $I$ ,  $\Delta t$ ,  $m$ , and  $\Delta V$ , refer to the current (A), discharge time (s), mass of active material (g), and potential window (V), respectively.

For the two-electrode system, the specific capacitance ( $C_{S3}$ , F g<sup>-1</sup>) was calculated by the following formula:<sup>3</sup>

$$C_{S3} = \frac{I * \Delta t}{m * \Delta V} \quad (S3)$$

where  $I$ ,  $\Delta V$ ,  $\Delta t$ , and  $m$  are the discharge current (A), the voltage window (V), the discharge time (s), and the total mass (g) of the active material of two electrodes, respectively. The energy density ( $E$ , Wh kg<sup>-1</sup>) and power density ( $P$ , W kg<sup>-1</sup>) were calculated by the following two equations:<sup>4</sup>

$$E = \frac{C_{S3} * \Delta V^2}{2 * 3.6} \quad (S4)$$

$$P = \frac{3600 * E}{\Delta t} \quad (S5)$$

where  $C_{S3}$ ,  $\Delta t$ , and  $\Delta V$  are specific capacitances (F g<sup>-1</sup>), discharge time (s), and voltage window (V).

## Desalination tests

All desalination experiments were carried out in a batch-mode HCDI system with continuously

circulating the NaCl solution through the HCDI unit by using a peristaltic pump (volume: 70 mL, flow rate: 100 mL min<sup>-1</sup>, temperature: room temperature). The concentration of the pump effluent was recorded in real-time by an ion conductivity meter (DDSJ-308A, Precision & Scientific Instrument). The working electrode of HCDI consists of a BAHC/BAHCGO cathode and an AC anode separated by a spacer and anion/cation-exchange membrane. The desalination experiments of NaCl solutions with different initial concentrations (100, 200, 300, 500, 1000 mg L<sup>-1</sup>) were carried out at ±1.6 V, while different current densities (50, 100, 150, 200, 250 mA g<sup>-1</sup>) were employed for the tests in 500 mg L<sup>-1</sup> NaCl solution. Our previous work described the relationship between NaCl solution conductivity and concentration.<sup>5</sup>

### Desalination calculation

The desalination capacity (SAC, mg g<sup>-1</sup>), mean desalination rate (MSAR, mg g<sup>-1</sup> min<sup>-1</sup>), and charge efficiency (Λ) were defined as follows:<sup>6,7</sup>

$$\text{SAC} = \frac{(C_0 - C_e) * V}{m} \quad (\text{S6})$$

$$\text{MSAR} = \frac{\text{SAC}}{t} \quad (\text{S7})$$

$$\Lambda = \frac{(C_0 - C_e) * V * F}{1000 * M * Q} * 100\% \quad (\text{S8})$$

where  $C_0$  and  $C_e$  are the initial and final NaCl concentrations (mg L<sup>-1</sup>),  $V$  is the volume of NaCl solution (L),  $m$  is the mass of the active materials (g),  $t$  (s) is the charge time,  $F$  is the Faraday constant (96,485 C mol<sup>-1</sup>),  $M$  (58.44 g mol<sup>-1</sup>) is the relative molar mass of NaCl, and  $Q$  (charge, C) is the total charge.

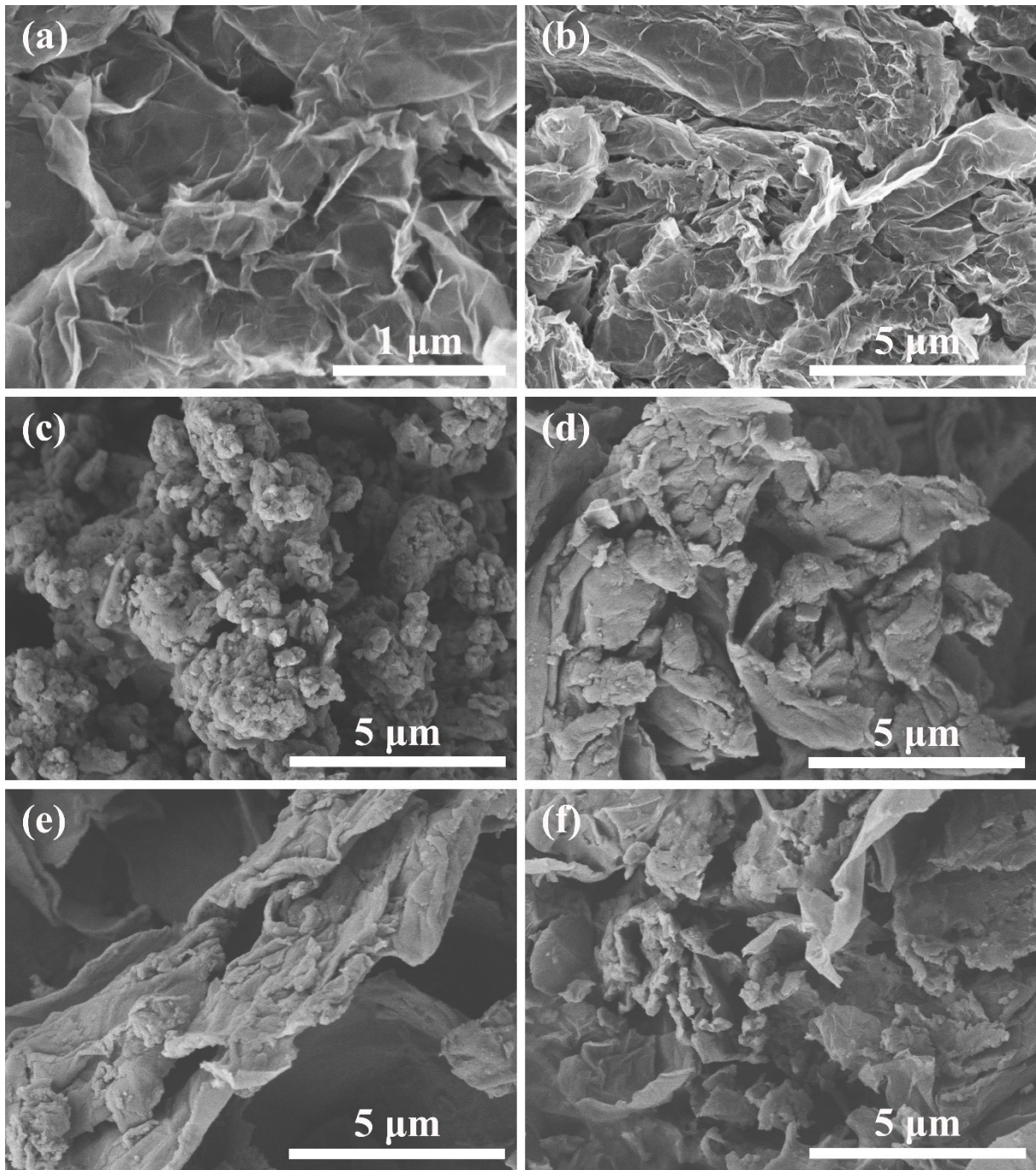
### Complex capacitance calculation

The complex capacitance ( $C(\omega)$ , F) was defined as follows:<sup>6,7</sup>

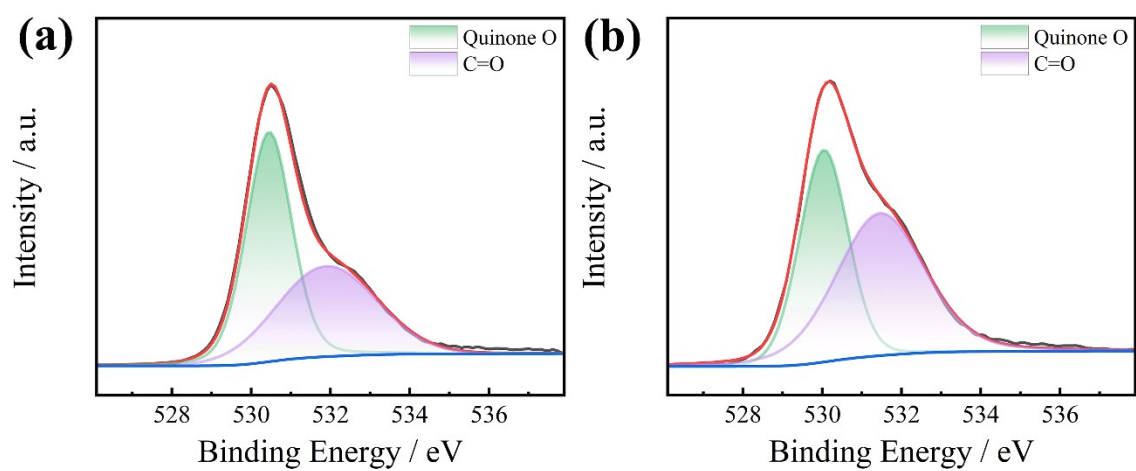
$$\text{SAC} = \frac{(C_0 - C_e) * V}{m} \quad (\text{S6})$$

$$\text{MSAR} = \frac{\text{SAC}}{t} \quad (\text{S7})$$

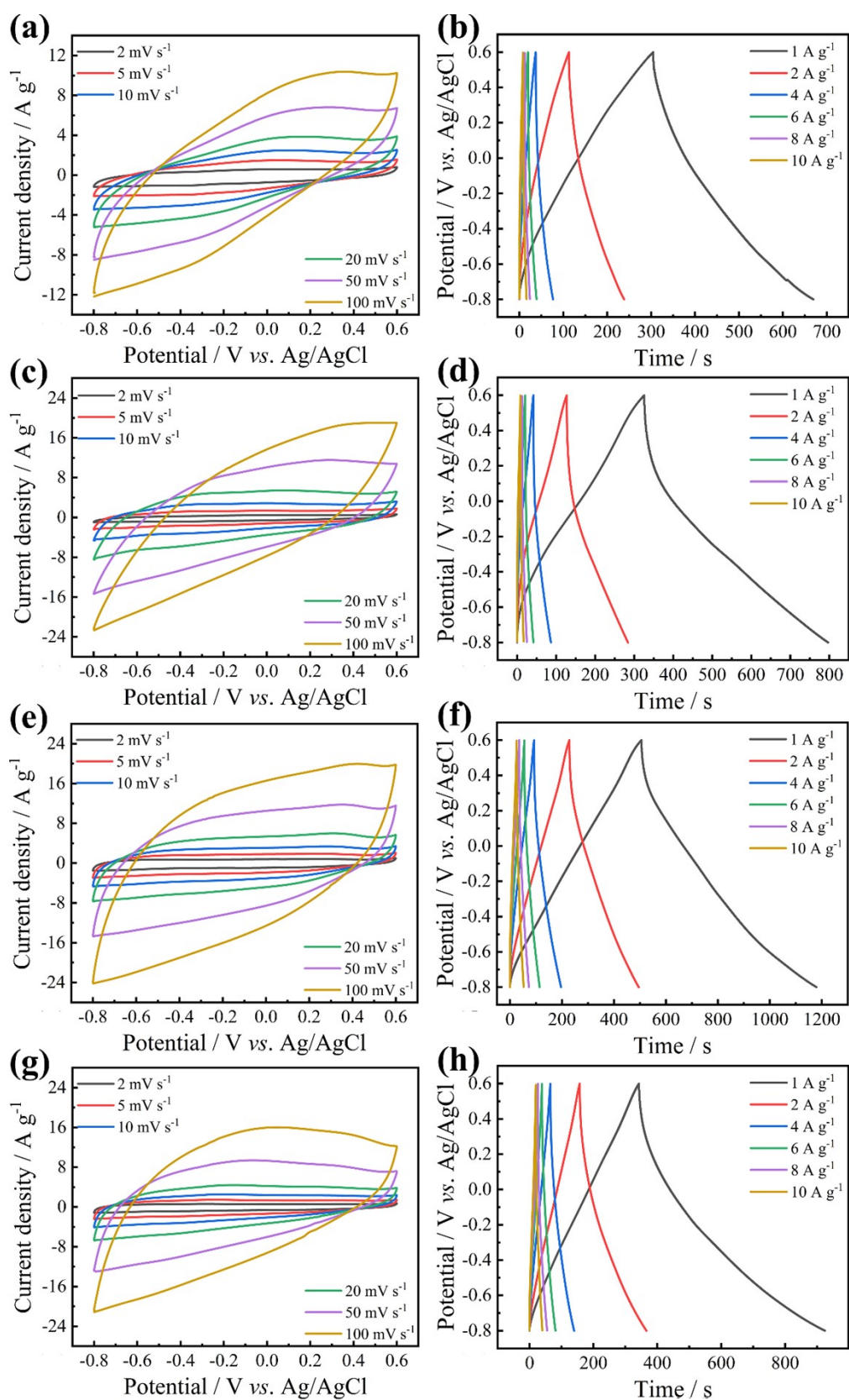
where  $C_0$  and  $C_e$  are the initial and final NaCl concentrations ( $\text{mg L}^{-1}$ ),  $V$  is the volume of NaCl solution (L),  $m$  is the mass of the active materials (g),  $t$  (s) is the charge time,  $F$  is the Faraday constant ( $96,485 \text{ C mol}^{-1}$ ),  $M$  ( $58.44 \text{ g mol}^{-1}$ ) is the relative molar mass of NaCl, and  $Q$  (charge, C) is the total charge.



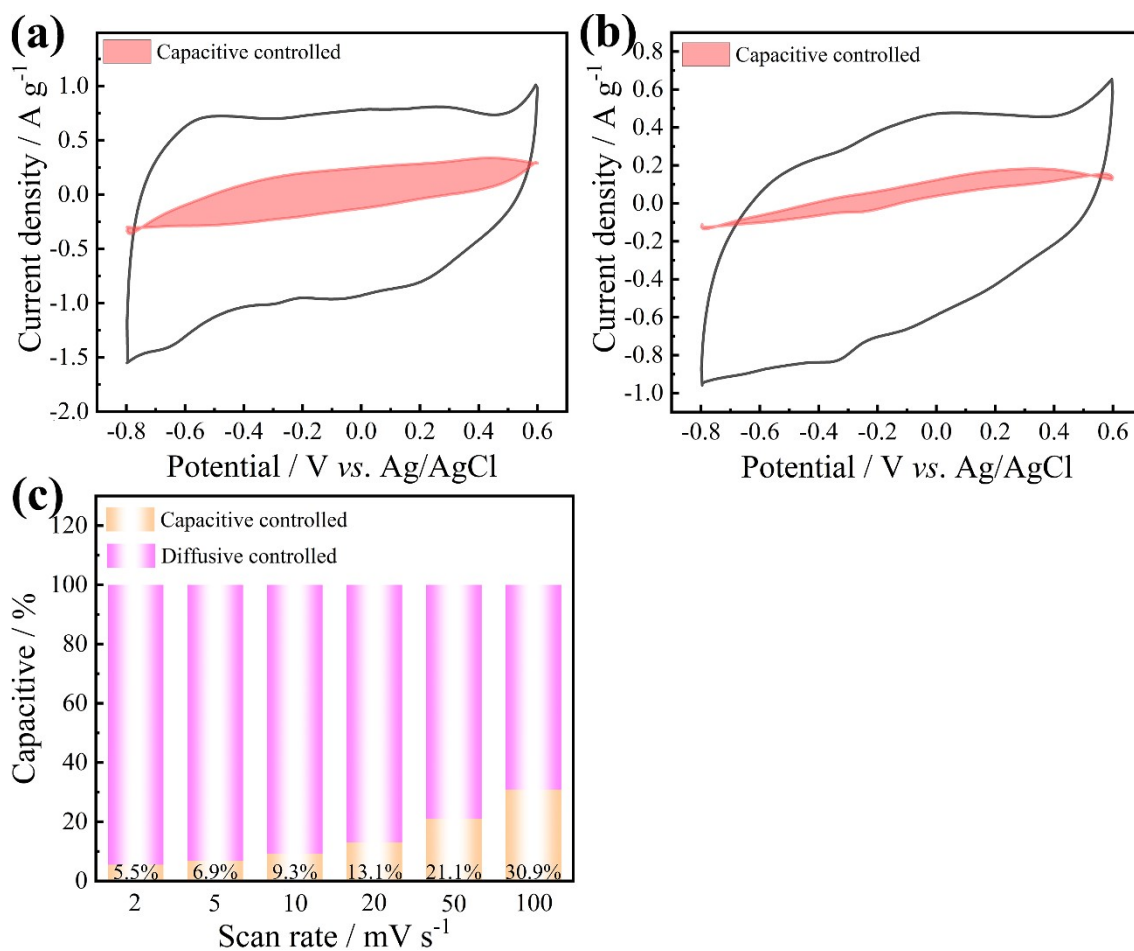
**Fig. S1.** SEM images of (a,b) rGO, (c) BAHC, (d) BAHCGO-50, (e) BAHCGO-75, and (f) BAHCGO-100.



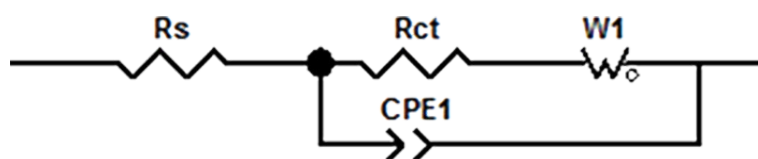
**Fig. S2.** High-resolution XPS O 1s spectra of (a) BAHC and (b) BAHCGO-75.



**Fig. S3.** Electrochemical performances of (a, b) BAHC, (c, d) BAHCGO-50, (e, f) BAHCGO-75, and (g, h) BAHCGO-100 under the three-electrode system.

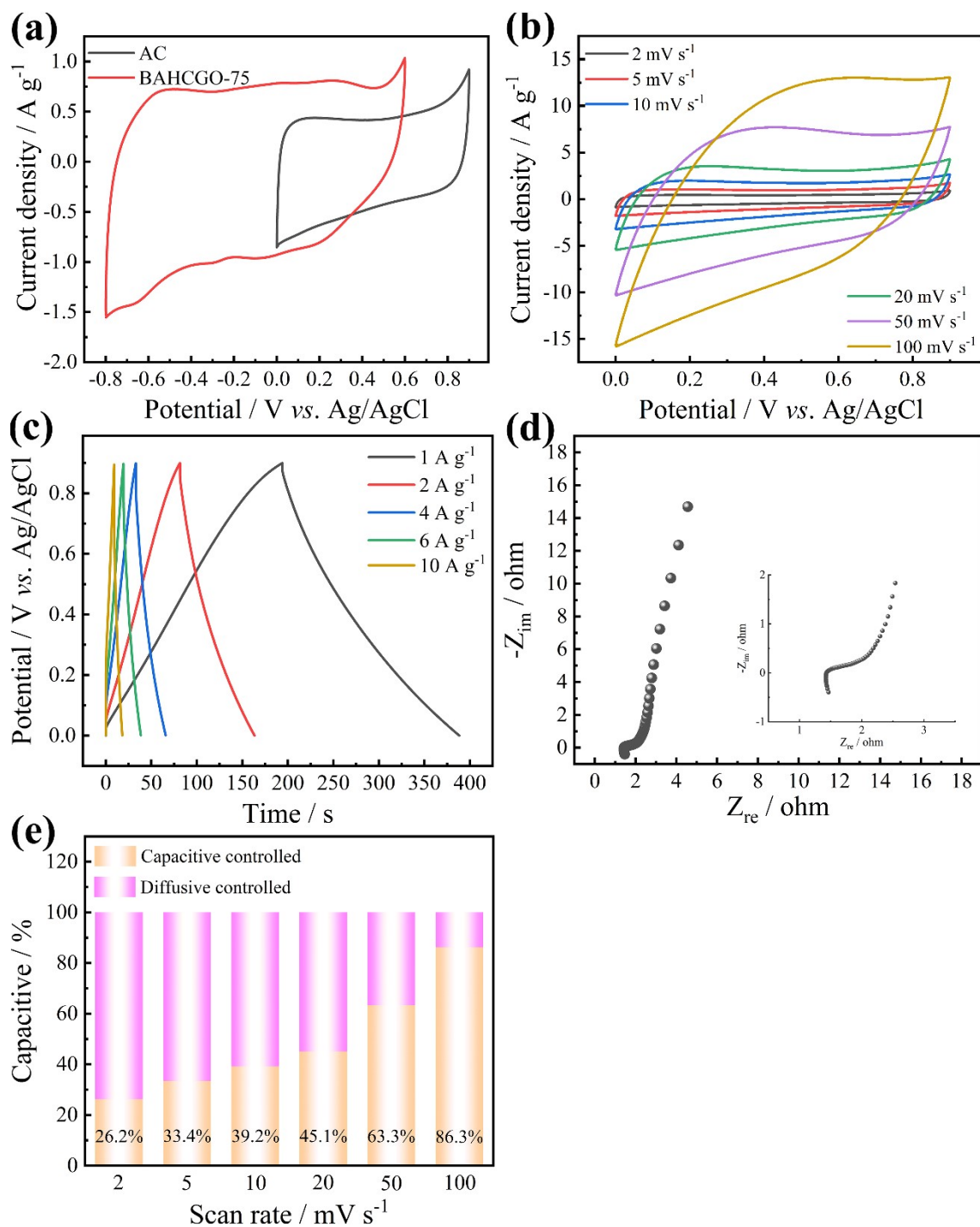


**Fig. S4.** CV curves with the capacitive contribution of (a) BAHCGO-75 and (b) BAHC at 2 mV s<sup>-1</sup>. Percentages of capacitive and diffusion contributions of (c) BAHC.

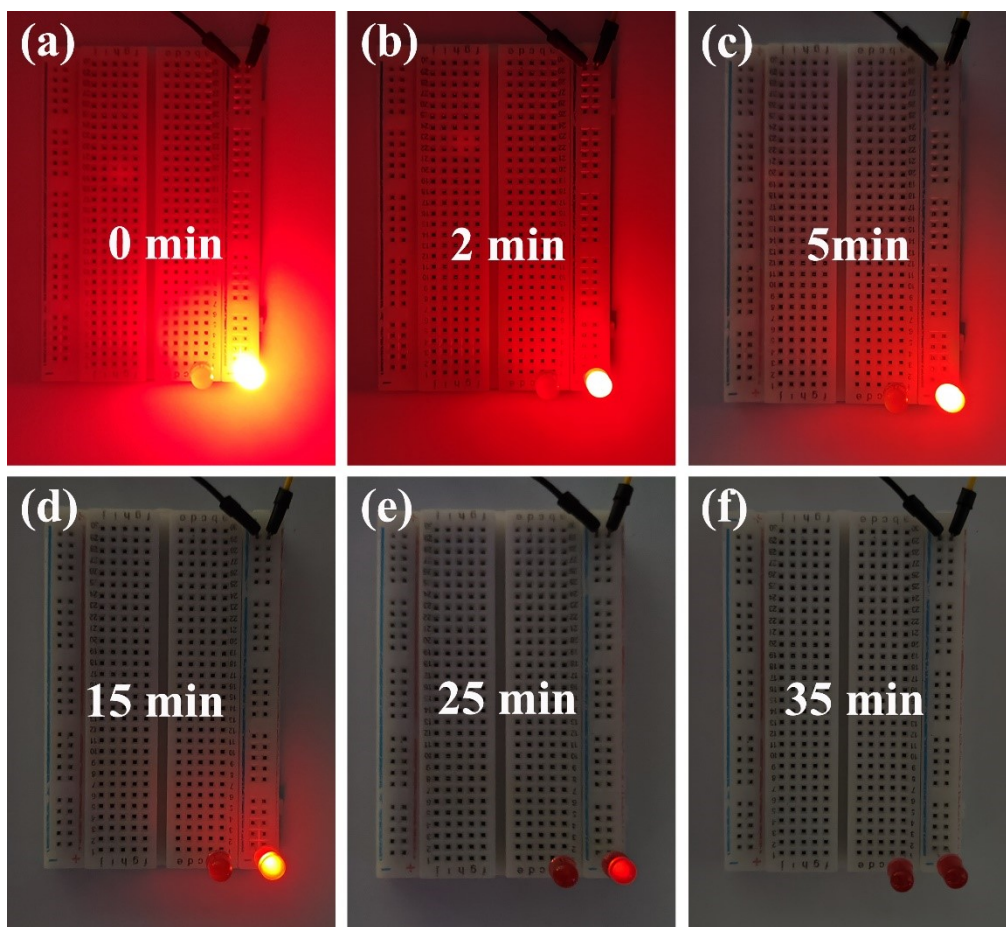


**Fig. S5.** The fitting equivalent circuit diagram of the EIS test.

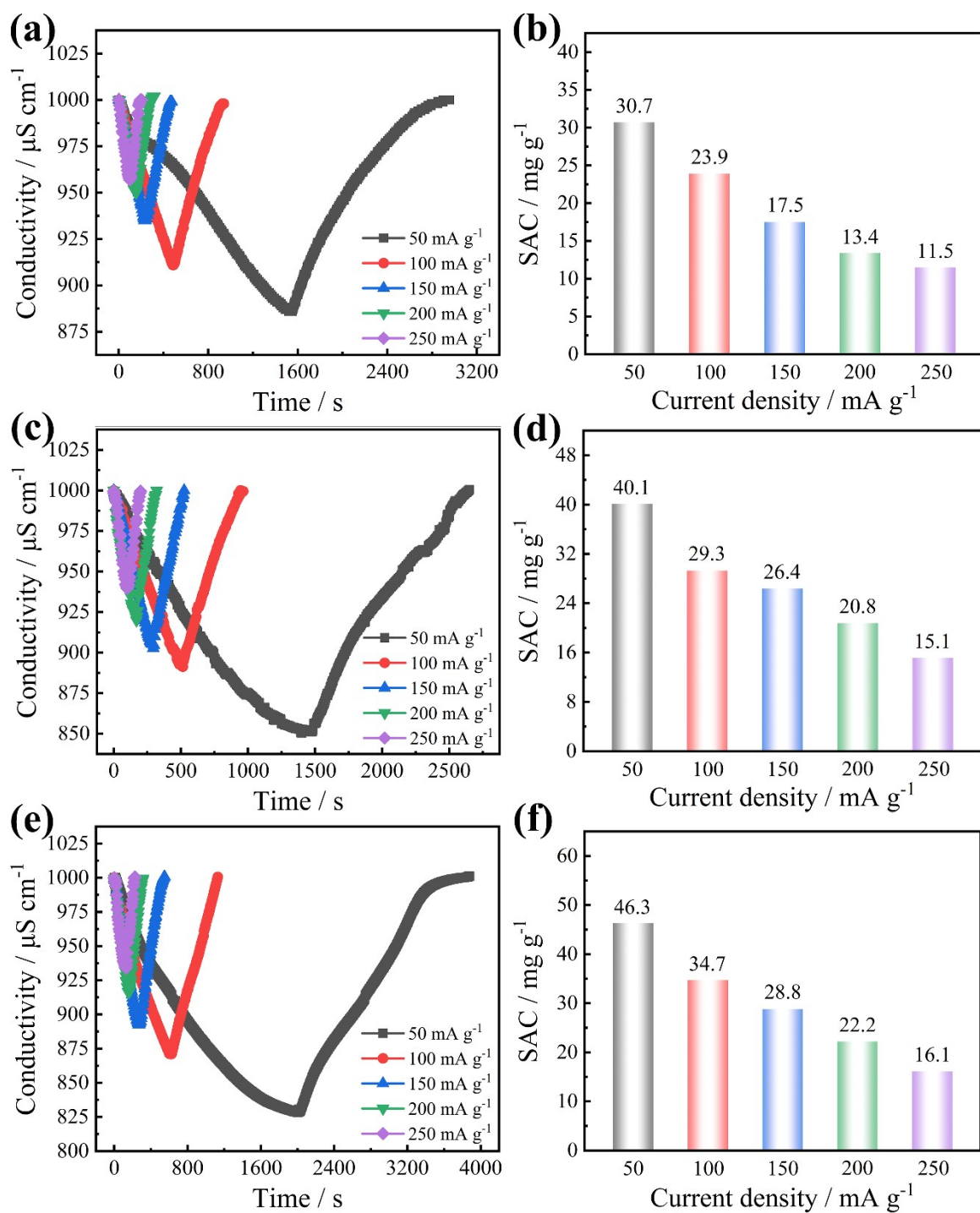




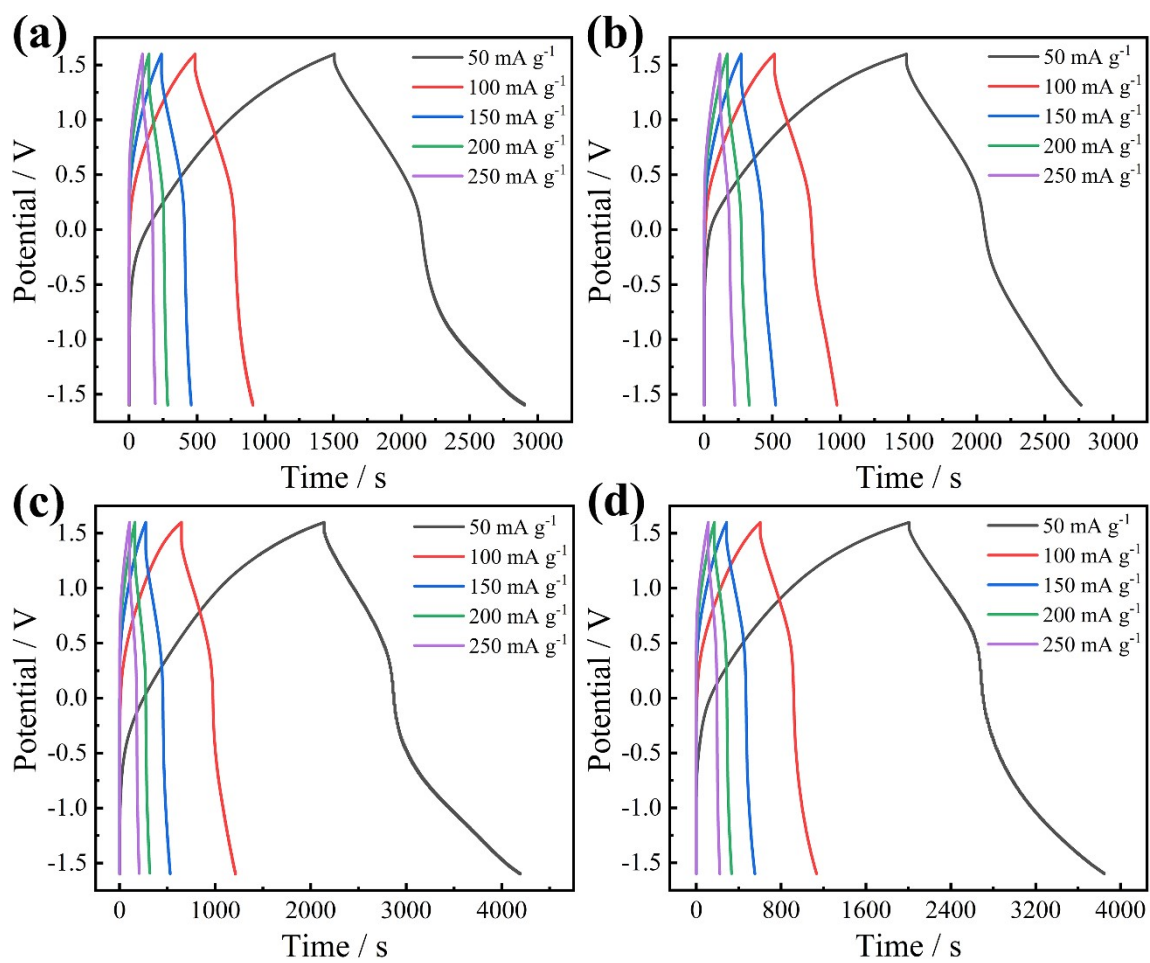
**Fig. S6.** (a) CV curves of AC and BAHCGO-75 at a scan rate of 2 mV s<sup>-1</sup>. (b) CV curves at 2-100 mV s<sup>-1</sup>, (c) GCD curve at 1-10 A g<sup>-1</sup>, (d) Nyquist plots (Inset shows the magnified plot in the high-frequency region), and (e) percentages of capacitive and diffusion contributions of AC.



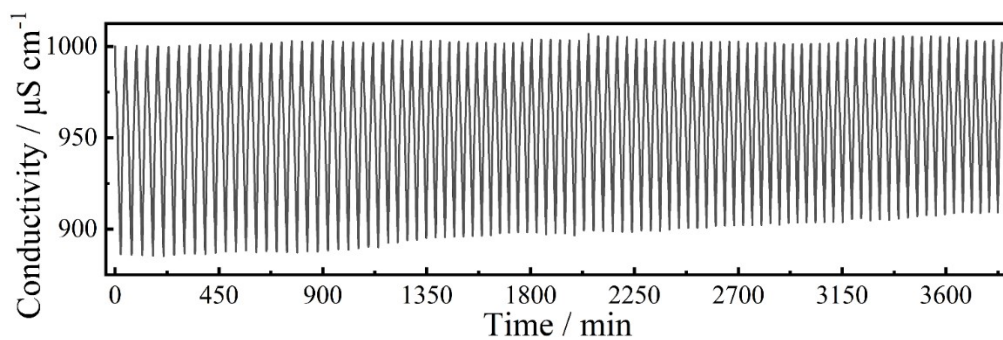
**Fig. S7.** Photographs presenting two BAHCGO-75//AC ASCs connected in series to successfully light up the red LDE lamp.



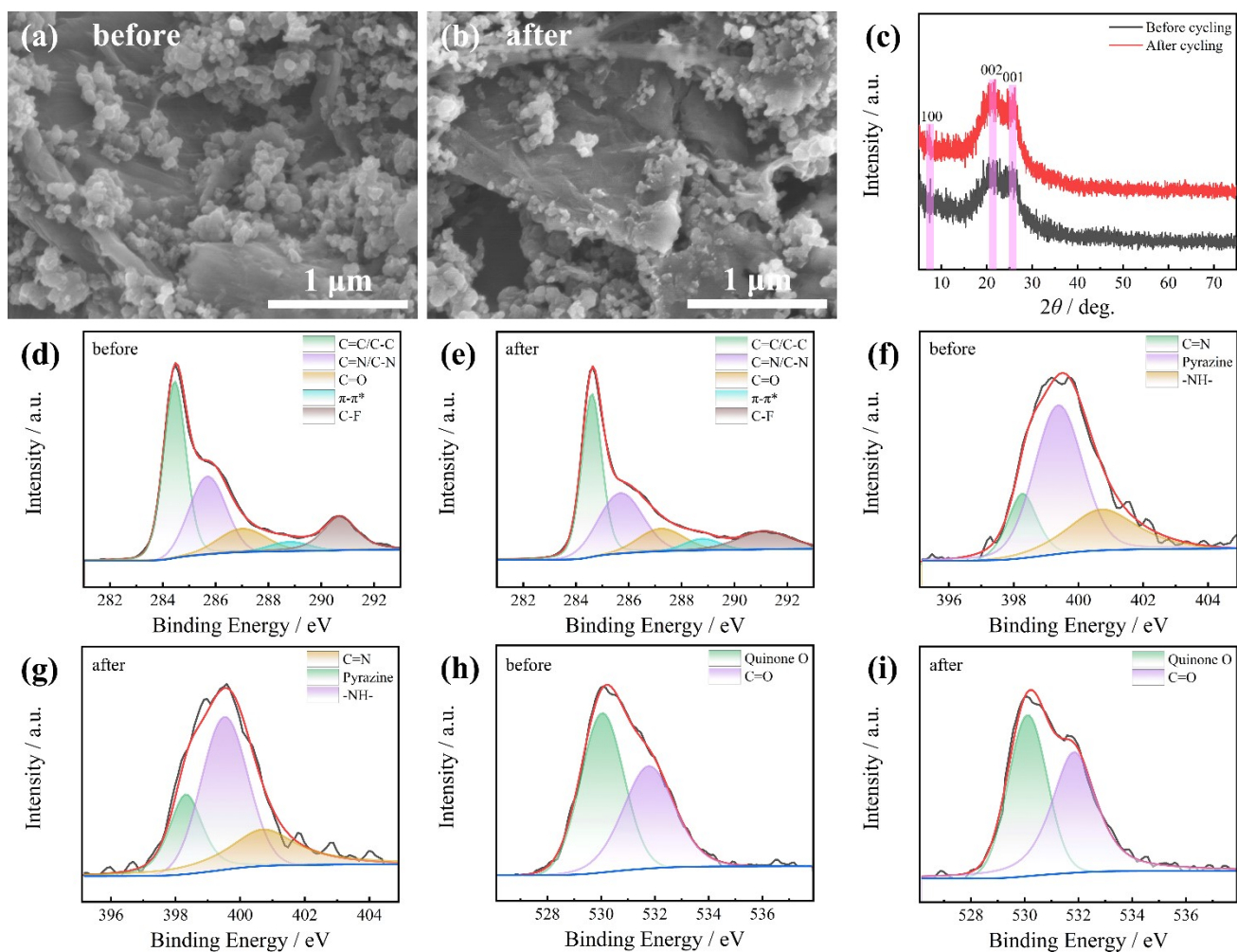
**Fig. S8.** Conductivity curves and SACs at different current densities of (a, b) BAHC, (c, d) BAHCGO-50, and (e, f) BAHCGO-100.



**Fig. S9.** Voltage response curves of (a) BAHC, (b) BAHCGO-50, (c) BAHCGO-75, and (d) BAHCGO-100 HCDI at various current densities.



**Fig. S10.** Cycling performance of BAHC.



**Fig. S11.** (a, b) SEM images, (c) XRD patterns, and high-resolution (d, e) C1s, (f, g) N 1s, and (h, i) O 1s XPS spectra of BAHCGO-75 electrode before and after desalination/regeneration performance test.

**Table S1.** Comparison of desalination performances of TFPDQGO-75 with carbon-based CDI reported in the literature.

<b>Material</b>	<b>SAC / mg g<sup>-1</sup></b>	<b>MSAR / mg g<sup>-1</sup> min<sup>-1</sup></b>	<b>Ref.</b>
BAHC-COF	30.7	1.68	This work
BAHCGO-75	50.5	5.40	This work
3D graphene-supported N-doped hierarchically porous carbon	25.5	0.64	[8]
Carbon foam	30.2	3.75	[9]
Heteroatom-doped hierarchical porous carbon	16.19	2.02	[10]
Defect-rich interconnected hierarchical porous carbon	31.25	3.95	[11]
KC-pre-intercalated carbon nanosheets	40.72	2.04	[12]
3D-printed thick carbon electrodes	10.67	0.28	[13]
N-doped polyporphyrin derived porous carbons	35.7	4.67	[14]
AC	8.1	0.49	[14]
N-doped hierarchically porous carbon	19.61	2.38	[15]
Zeolitic-imidazolate framework (ZIF)-derived carbon	14.19	3.99	[6]
Mg-MOF-74 derived carbon	16.82	2.28	[17]

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