## **Supplementary Information**

# Deep reconstruction of crystalline-amorphous heterojunction electrocatalysts for efficient and stable water and methanol electrolysis

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### **1. Experimental section**

#### 1.1 Chemicals

Nickel foam (NF), cobalt nitrate ( $Co(NO_3)_2 \cdot 6H_2O$ ), iron nitrate ( $Fe(NO_3)_3 \cdot 9H_2O$ ), 2methylimidazole ( $C_4H_6N_2$ ), and thioacetamide ( $C_2H_5NS$ ), ruthenium(IV) oxide ( $RuO_2$ ), activation carbon, and N-Methyl Pyrrolidone ( $C_5H_9NO$ ) were purchased form Sigma-Aldrich. All reagents did not require further purification. NF was used as a substrate, which was ultrasonically cleaned with ethanol and deionized water for 5 min, respectively.

#### 1.2 Synthesis of ZIF-67

Firstly,  $Co(NO_3)_2 \cdot 6H_2O$  (0.5 mmol, 0.1455 g) was dissolved into 10 mL Milli Q distilled water (DI water) and then NF (4 × 1 cm<sup>2</sup>) immersed into solution 30 min. Then,  $C_4H_6N_2$  (4 mmol, 0.3284 g) was dissolved into 10 mL DI water and then quickly added into the above solution and kept for 2 h. Thus, ZIF-67 can be received after washing with distilled water and dried 12 h at 60 °C.

#### 1.3 Synthesis of Co-Ni<sub>3</sub>S<sub>2</sub> and Ni<sub>3</sub>S<sub>2</sub>

Synthesis of Co-Ni<sub>3</sub>S<sub>2</sub> by solvothermal method using ZIF-67 as Co source. First, 0.6 g  $C_2H_5NS$  was dissolved in 60 mL ethanol and kept stirring for 10 min. Then, a piece of ZIF-67 on the NF was immersed in the above solution, and solvothermal process was performed at 120 °C for 4 h. After that, Co-Ni<sub>3</sub>S<sub>2</sub> was prepared by washing with water and drying at 50 °C. To verify that NF also participated in the reaction as a nickel source, only pure NF was added to prepare pure Ni<sub>3</sub>S<sub>2</sub> through the above method.

#### 1.4 Synthesis of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>

FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> heterostructure was prepared by using Co-Ni<sub>3</sub>S<sub>2</sub> as the substrate to support FeBO. First, the NF loaded with Co-Ni<sub>3</sub>S<sub>2</sub> was placed in 47.5 ml of deionized water solution containing 0.5 mmol Fe(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O. Subsequently, 2.5 ml of NaBH<sub>4</sub> solution (0.5M) was gradually added to the above solution. After reacting at room temperature for 2 h, wash with plenty of water. The final product was dried at 50 °C overnight for further characterization and catalytic activity analysis. For comparison, NF-loaded FeBO nanostructures were also prepared in the same way. The electrocatalyst loading was calculated by weighing the NF electrode before and after catalyst synthesis. In this work, the electrocatalyst loading of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> was approximately 3.8 mg cm<sup>-2</sup>.

#### 1.5 Preparation of RuO<sub>2</sub> electrode

 $RuO_2$  was coated on the NF to prepare  $RuO_2$  catalyst by universal approach. A total 6 mg  $RuO_2$  was ultrasonically dispersed for at least 5 min in a mixture solution containing 0.16 mL of NMP and PVDP, and 1 mg Activation carbon.

#### **1.6 Characterizations**

Powder X-ray diffraction (XRD) was carried out on a X'Pert PRO Multi-Purpose X-Ray Diffractometer (PANalytical) using Cu K $\alpha$  radiation. Raman spectra were studied by NRS-5100 using 532 nm laser source. Fourier transform infrared (FT-IR) were collected on a Spectrum 400. The morphology and microstructure of the prepared materials were tested by field emission scanning electron microscope (FE-SEM Gemini 500 + EDS (Oxford)) and field emission transmission electron microscope (FE-TEM, JEM-2100F, JEOL LTD). High-performance X-ray photoelectron spectroscopy (HP-XPS, K-ALPHA+) was used to characterize the elemental

information of catalysts. The electro-oxidation of methanol to formate was confirmed using <sup>1</sup>H NMR (400 MHz) AVANCE III HD 400.

#### **1.7 Electrochemical measurement**

The electrochemical performance was tested at an Autolab potentiostat (CHI Instruments, USA) using a three-electrode system. Platinum electrode and Ag/AgCl electrode were used as counter electrode and reference electrode, respectively, and the as-prepared materials on NF were used as working electrode. For electrocatalytic reactions, 1 M KOH and 1 M KOH + 0.5 M methanol were employed as the electrolytes, respectively. All the electrochemical experiments were carried out in electrolyte at 25 °C. The area of the work electrode immersed in the electrolyte is  $1 \times 1$  cm<sup>2</sup>. Linear sweep voltammetry (LSV) was tested at scan rate of 1 mV s<sup>-1</sup>. Convert the potential measured in this work to a reversible hydrogen electrode (RHE) according to equation E (vs. RHE) = E (vs. Ag/AgCl) +  $0.197 + 0.059 \times pH$ . The overpotential ( $\eta$ ) was calculated according to the following equation:  $\eta = E$  (vs. RHE) – 1.23 V. Electrochemical impedance spectroscopic (EIS) was carried out using a high-performance potentiostat (Zive Potentiostat/Galvanostat/EIS, Wonatech, Republic of Korea) at a bias potential of 300 mV in the frequency range of 0.1 Hz-10000 Hz. Electrochemical active surface areas (ECSAs) were calculated based on the formula: ECSAs =  $C_{dl}/C_s$ . Among them, the double-layer capacitance ( $C_{dl}$ ) was obtained by cyclic voltammetry (CV), while for Ni-/Co-based catalysts, Cs is usually adopted at 0.04 mF cm<sup>-2</sup>. CV was tested in non-Faradaic region at scan rates of 20 to 100 mV s<sup>-1</sup>. The prepared electrocatalysts' long-term stability was tested using chronopotentiometry (CP) at a current density of 10 mA cm<sup>-2</sup> and a measurement time of 100 or 25 h. The overall water and methanol splitting uses FeBO/Co- $Ni_3S_2$  as anode and cathode.



Fig. S1. FT-SEM image of ZIF-67.



Fig. S2. XRD patterns of ZIF-67.



Fig. S3. Enlargement of partial XRD patterns of Co-Ni $_3S_2$  and Ni $_3S_2$ .



Fig. S4. XRD pattern of FeBO.



Fig. S5. Raman magnified image of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>, Co-Ni<sub>3</sub>S<sub>2</sub>, and Ni<sub>3</sub>S<sub>2</sub> samples.



Fig. S6. FE-SEM images of (a) Ni<sub>3</sub>S<sub>2</sub>, (b) Co-Ni<sub>3</sub>S<sub>2</sub>, and (c) FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>.



Fig. S7. HR-TEM image: the interfaces between crystalline  $\text{Co-Ni}_3\text{S}_2$  and amorphous FeBO are marked with the yellow lines.



Fig. S8. XPS survey spectra of FeBO/Co-Ni $_3S_2$ .



Fig. S9. LSV curves of ZIF-67,  $RuO_2$  and NF for OER.



Fig. S10. Corresponding overpotentials of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>, FeBO, Co-Ni<sub>3</sub>S<sub>2</sub>, and Ni<sub>3</sub>S<sub>2</sub> samples at different current densities.



Fig. S11. Tafel slopes of ZIF-67,  $RuO_2$ , and NF.

**Table S1.** Comparison of OER performance between FeBO/Co-Ni $_3S_2$  and previously reportedelectrocatalysts using 1 M KOH as the electrolyte and NF as the substrate.

Catalyst	Overpotential (mV) @ j (mAcm <sup>-2</sup> )	Tafel slope (mV.dec <sup>-1</sup> )	Stability (h) @ j (mAcm <sup>-2</sup> )	Ref
FeBO/Co-Ni <sub>3</sub> S <sub>2</sub>	205 (η <sub>10</sub> ) 253 (η <sub>100</sub> )	42	<b>100</b> (η <sub>10</sub> )	This work
Fe-Ni <sub>3</sub> S <sub>2</sub> /NF	214 (ŋ <sub>10</sub> )	54	20 (ŋ <sub>10</sub> )	1
$MoS_2/Ni_3S_2$ heterostructures	218 (ŋ <sub>10</sub> )	76	10 (η <sub>10</sub> )	2
MoS <sub>2</sub> –Ni <sub>3</sub> S <sub>2</sub> HNRs/NF	249 (ŋ <sub>10</sub> )	57	48 (ŋ <sub>40</sub> )	3
Ni <sub>2</sub> P-Ni <sub>3</sub> S <sub>2</sub> HNAs/NF	210 (ŋ <sub>10</sub> )	62	24 (ŋ <sub>10</sub> )	4
Au/Ni <sub>3</sub> S <sub>2</sub> /NF	230 (ŋ <sub>10</sub> )	51	60 (η <sub>10</sub> )	5
NiMoS	260 (ŋ <sub>10</sub> )	59	15 (η <sub>120</sub> )	6
f-NiFe-LDH-B	209 (ŋ <sub>10</sub> )	43.5	60 (ŋ <sub>10</sub> )	7
NiFeB@OCC	255 (ŋ <sub>20</sub> )	65	24 (ŋ <sub>100</sub> )	8
Fe-doped Ni <sub>3</sub> S <sub>2</sub> /rGO@NF	247 (ŋ <sub>20</sub> )	63	20 (ŋ <sub>20</sub> )	9

Table S2. Values of  $R_{\rm s}$  and  $R_{\rm ct}$  in the samples for OER.

Sample	$R_{s}(\Omega)$	$R_{ct}(\Omega)$
FeBO/Co-Ni <sub>3</sub> S <sub>2</sub>	0.305	0.108
FeBO	0.283	163
Co-Ni <sub>3</sub> S <sub>2</sub>	0.302	1.14
Ni <sub>3</sub> S <sub>2</sub>	0.477	20.3



Fig. S12. The CV curves of (a) FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>, (b) FeBO, (c) Co-Ni<sub>3</sub>S<sub>2</sub>, and (d) Ni<sub>3</sub>S<sub>2</sub>. All the curves were tested at different scan rates: 20, 40, 60, 80 and 100 mV s<sup>-1</sup>.



Fig. S13. The  $C_{dl}$  and ECSA values of the samples.



Fig. S14. The LSV curves normalized by mass.



Fig. S15. The LSV curves before and after long-term stability.



Fig. S16. The elemental mapping images of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> after the OER stability test.



Fig. S17. Fig. XPS spectrum of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> before and after stability test, (a) Ni 2p; (b) Fe 2p; (c) S 2p; and (d) B 1s.



Fig. S18. Comparison of Raman spectra of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> before, after OER, and after stability.



Fig. 19. Raman spectra of Co-Ni $_3S_2$ , and Ni $_3S_2$  catalysts after OER test.

Sample	$\mathbf{R}_{\mathrm{s}}\left(\Omega ight)$	$R_{ct}(\Omega)$
FeBO/Co-Ni <sub>3</sub> S <sub>2</sub>	0.334	0.047
FeBO	0.334	1.28
Co-Ni <sub>3</sub> S <sub>2</sub>	0.385	0.874
$Ni_3S_2$	0.509	0.245

Table S3. Values of  $R_{\rm s}$  and  $R_{\rm ct}$  in the samples for MOR.



Fig. S20. CV curves of (a) FeBO/Co-Ni<sub>3</sub>S<sub>2</sub>, (b) FeBO, (c) Co-Ni<sub>3</sub>S<sub>2</sub>, and (d) Ni<sub>3</sub>S<sub>2</sub> at different scan rates for MOR testing. (e)  $C_{dl}$  values.



Fig. S21. The FE-SEM image of FeBO/Co-Ni $_3$ S $_2$  after the MOR stability test.



Fig. S22. The XRD image of FeBO/Co-Ni $_3S_2$  after the MOR stability test.



Fig. S23. (a) The LSV curves for the HER of various catalysts; (b) HER polarization plots of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> in 1 M KOH electrolyte with and without 0.5 M methanol; (c) Tafel slopes for HER; (d) multi-current process of FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> and (e) corresponding overpotentials; (f) Long-term stability testing of HER.

Table S4. Comparison of the water and methanol electrolysis performance of FeBO/Co-

 $Ni_3S_2$  with previous.

	Volt	age	Stab	ility (h)	Dof
Catalyst	(V) @ j (	mAcm <sup>-2</sup> )	@10 j	(mAcm <sup>-2</sup> )	Kei.
	OWS	OMS	OWS	OMS	
FeBO/Co-Ni <sub>3</sub> S <sub>2</sub>	1.58 (η <sub>10</sub> )	1.44 (η <sub>10</sub> )	100	25	This work
	1.86 (η <sub>100</sub> )	1.67 (η <sub>100</sub> )			
Pt-Ni <sub>3</sub> S <sub>2</sub>	1.886 (η <sub>100</sub> )	1.71 (η <sub>10</sub> )	-	36	10
Ni <sub>3</sub> S <sub>2</sub> /MoS <sub>2</sub>	1.62 (ŋ <sub>10</sub> )	-	100	-	11
Ni <sub>3</sub> S <sub>2</sub> @G	1.66 (η <sub>10</sub> )	-	30	-	12
3DG-Au-Ni <sub>3</sub> S <sub>2</sub>	1.63 (ŋ <sub>10</sub> )	-	19	-	13
Ni <sub>3</sub> S <sub>2</sub> @Ni	1.61 (η <sub>10</sub> )	-	30	-	14
Ni-Co-S HPNA	1.62 (ŋ <sub>10</sub> )	-	24	-	15
FeNi@FeNiB-700	1.65 (η <sub>10</sub> )	-	12	-	16
Fe <sub>1</sub> Mn <sub>1</sub> @BN-PCFs	1.622 (η <sub>10</sub> )	-	30	-	17
Co-S-INF	1.82 (η <sub>100</sub> )	1.70 (η <sub>100</sub> )	27	27	18
Co-Rh <sub>2</sub>	-	1.545 (η <sub>10</sub> )	-	4	19
NiTe <sub>2</sub> /Ni	1.77 (η <sub>10</sub> )	1.54 (η <sub>10</sub> )	12	12	20
Co(OH) <sub>2</sub> @HOS/CP	1.631 (ŋ <sub>10</sub> )	1.497 (η <sub>10</sub> )	-	20	21

The H<sub>2</sub> yield is calculated using the formula, H<sub>2</sub> yield rate =  $(V(experimental)/V(theoretical)) \times 100\%$ . The theoretical amount of H<sub>2</sub> released (V(theoretical)), is calculated using Faraday's law:

$$V_{Theo} = IRTt/PzF$$

 $V_{Theo}$  = Theoretical volume of evolved gas

I is working current density ( $I = 100 \text{ mA cm}^{-2}$ )

T is working temperature (T = 298 K), and 't' is time interval (t = 1200, 2400, and 3600 s)

R is the gas constant (R = 8.314459), and 'P' is the working pressure (P = 101.3 Kpa)

F is the Faraday's constant (F = 96485 C)

z is the number of electrons for generating 1 mol  $H_2$  (z = 2)

The actual amount of  $H_2$  produced during the electrolysis process was collected using a homemade H-type water electrolysis device in the laboratory and a water displacement method. Electrolysis conditions: The electrolysis was carried out in a two-electrode electrolytic cell with FeBO/Co-Ni<sub>3</sub>S<sub>2</sub> electrodes and a controlled current density (100 mA cm<sup>-2</sup>) for 1 h, where 1 M KOH and 1 M KOH + 0.5 M MeOH were used as electrolytes. The H<sub>2</sub> production results are visually represented in Fig. S24 and S25.

H<sub>2</sub> yield rate was calculated using the following equation:

 $H_2$  yield rate = Vg(experimental)/Vg(theoretical) x 100%.

The H<sub>2</sub> yield rate of the two-electrode system is shown in Table S5.



Fig. S24. The HER/OER dual-electrode system expands the drainage device during  $H_2$  collection at different intervals.



Fig. S25. The HER/MOR dual-electrode system expands the drainage device during  $H_2$  collection at different intervals.

System	H <sub>2</sub> yield rate	
Time	HER/OER	HER/MOR
20 min	99%	95%
40 min	92%	92%
60 min	88%	89%
Average	93%	92%

Table S5. The  $H_2$  yield rate of the two-electrode systems.

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