## Supporting information

## RAFT/ROP binary polymerization towards well-defined graft

## copolymers

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**Fig. S1** GPC traces of PHEAA-*g*-PCL synthesized by RAFT/ROP binary polymerization after extending the reaction time.



**Fig. S2** GPC traces of PHEAA<sub>50</sub>-*g*-PCL<sub>20</sub> synthesized by (a) RAFT/ROP binary polymerization; (b) "grafting-through"; (c) "grafting-from".



**Fig. S3** GPC traces of PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub> synthesized by (a) RAFT/ROP binary polymerization; (b) "grafting-through"; (c) "grafting-from".

Entry	Synthesis method	Time (h)	Conversion (%) <sup>a</sup>		$M = b^{b}(Da)$		
	Synthesis method		HEAA	CL	Mn,GPC (Da)	FDI	
1	RAFT/ROP binary polymerization	24	89	82	93900	1.10	
2	grafting-through	48	90	94	90700	1.11	
3	grafting-from	48	85	93	97500	1.23	

 Table S1
 Summary of graft copolymers PHEAA<sub>100</sub>-g-PCL<sub>20</sub> prepared via three methods.

 $^{\it a}$  Calculated from the integration ratios of the characteristic peaks  $^1{\rm H}$  NMR.

<sup>b</sup> Determined by GPC eluted with DMF calibrated by PMMA standards.

<sup>c</sup> Integration of PDI does not include the peak at higher elution times.



**Fig. S4** GPC traces of purified PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub> synthesized by (a) RAFT/ROP binary polymerization; (b) "grafting-through"; (c) "grafting-from".



**Fig. S5** Performance characterization of PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub>. (a) TGA thermograms; (b) DSC curves; (c) X-ray diffractograms.



**Fig. S6** TEM images of PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub> synthesized by three methods. (a) RAFT/ROP binary polymerization; (b) "grafting-through; (c) "grafting-from".



**Fig. S7** Kinetic curves of PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub> synthesized by RAFT/ROP binary polymerization and corresponding kinetics of RAFT control and ROP control. (a) Conversion of HEAA (blue solid line) and  $\varepsilon$ -CL (red solid line) versus reaction time in binary polymerization; (b) Conversion of HEAA versus reaction time in binary polymerization (blue solid line); (c) Conversion of  $\varepsilon$ -CL versus reaction time in binary polymerization (blue dashed line); (c) Conversion of  $\varepsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line); (d) Ln([M]<sub>0</sub>/[M]) of HEAA (blue solid line) and  $\varepsilon$ -CL (red solid line) versus reaction time in binary polymerization; (e) Ln([M]<sub>0</sub>/[M]) of HEAA versus reaction time in binary polymerization; (e) Ln([M]<sub>0</sub>/[M]) of HEAA versus reaction time in binary polymerization (blue solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\varepsilon$ -CL versus reaction time in binary polymerization (blue solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\varepsilon$ -CL versus reaction time in binary polymerization (red solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\varepsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\varepsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\varepsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line).



**Fig. S8** Kinetic curves of PHEAA<sub>50</sub>-*g*-PCL<sub>40</sub> synthesized by RAFT/ROP binary polymerization and corresponding kinetics of RAFT control and ROP control. (a) Conversion of HEAA (blue solid line) and  $\epsilon$ -CL (red solid line) versus reaction time in binary polymerization; (b) Conversion of HEAA versus reaction time in binary polymerization (blue solid line); (c) Conversion of  $\epsilon$ -CL versus reaction time in binary polymerization (blue dashed line); (c) Conversion of  $\epsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line); (d) Ln([M]<sub>0</sub>/[M]) of HEAA (blue solid line) and  $\epsilon$ -CL (red solid line) versus reaction time in binary polymerization; (e) Ln([M]<sub>0</sub>/[M]) of HEAA versus reaction time in binary polymerization; (e) Ln([M]<sub>0</sub>/[M]) of HEAA versus reaction time in binary polymerization (blue solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\epsilon$ -CL versus reaction time in binary polymerization (blue solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\epsilon$ -CL versus reaction time in binary polymerization (red solid line) and in RAFT control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\epsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\epsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (blue dashed line); (f) Ln([M]<sub>0</sub>/[M]) of  $\epsilon$ -CL versus reaction time in binary polymerization (red solid line) and in ROP control (red dashed line).



**Fig. S9** Kinetic curves of RAFT polymerization at different reaction conditions. (a) Conversion of HEAA versus reaction time; (b) Ln([M]<sub>0</sub>/[M]) of HEAA versus reaction time

## Construction of RAFT/ROP binary polymerization kinetic model

In the RAFT/ROP binary polymerization, the hybrid function  $\Phi_i$  (i = 1, 2; 1 denotes HEAA, 2 denotes  $\epsilon$ -CL) was incorporated into the kinetic equation to represent the relationship between RAFT and ROP. The kinetic model could be described using the following equation:

$$\frac{dM_1}{dt} = -k_{11} \cdot M_1^{\alpha_1} \cdot \Phi_1 \qquad \Phi_1 = e^{-\varphi_{21} \cdot p_2^m}$$
(1)

$$\frac{\mathrm{d}M_2}{\mathrm{d}t} = -k_{22} \cdot M_2^{\alpha_2} \cdot \Phi_2 \qquad \Phi_2 = e^{-\varphi_{12} \cdot p_1^{\mathrm{n}}}$$
(2)

where (1) represents the rate of consumption of the HEAA, while (2) represents the rate of consumption of the  $\varepsilon$ -CL.  $M_1$  refers to the concentration of HEAA, and  $M_2$  refers to the concentration of  $\varepsilon$ -CL. The  $p_1$  represents the conversion of HEAA, and the  $p_2$  represents the conversion of  $\varepsilon$ -CL.  $k_{11}$  represents the RAFT homopolymerization rate constant, while  $k_{22}$  represents the ROP homopolymerization rate constant. Since both RAFT and ROP exhibited first-order kinetic behavior, we assigned  $\alpha_1 = \alpha_2 = 1$ . Therefore, the kinetic model could be further described by the following equation:

$$\frac{dM_{1}}{dt} = -k_{11} \cdot M_{1} \cdot \Phi_{1} \qquad \Phi_{1} = e^{-\varphi_{21} \cdot p_{2}^{m}}$$
(3)  
$$\frac{dM_{2}}{dt} = -k_{22} \cdot M_{2} \cdot \Phi_{2} \qquad \Phi_{2} = e^{-\varphi_{12} \cdot p_{1}^{n}}$$
(4)

In order to optimize the kinetic model, the values of m and n in the hybrid function  $\Phi$  were discussed. Specifically, this discussion focuses on the cases where m and n were equal to 0, 1, and 2. Three graft copolymers with varied DPs of backbone and side chains were fitted as shown in the Fig. S10-S12.



**Fig. S10** Simulation of RAFT/ROP binary polymerization for different m, n values in PHEAA<sub>50</sub>-*g*-PCL<sub>20</sub> (dots for experimental results, lines for simulation results; red for ROP, blue for RAFT polymerization).



**Fig. S11** Simulation of RAFT/ROP binary polymerization for different m, n values in PHEAA<sub>100</sub>-*g*-PCL<sub>20</sub> (dots for experimental results, lines for simulation results; red for ROP, blue for RAFT polymerization).



**Fig. S12** Simulation of RAFT/ROP binary polymerization for different m, n values in PHEAA<sub>50</sub>-*g*-PCL<sub>40</sub> (dots for experimental results, lines for simulation results; red for ROP, blue for RAFT polymerization).

The figures illustrate that when both m and n were equal to 0, the fitted curves aligned closely with the experimental data for kinetic process, as different values were assigned to m and n, the fitted curves started to deviate to varying extents. Hence, the hybrid function was ultimately chosen to be m = n = 0, leading to the determination of the RAFT/ROP binary polymerization kinetic model described in equations (5) and (6):

$$\frac{dM_{RAFT}}{dt} = -k_{RAFT} \cdot M_{RAFT} \cdot e^{-\varphi_{ROP/RAFT}}$$
(5)

$$\frac{dM_{\rm ROP}}{dt} = -k_{\rm ROP} \cdot M_{\rm ROP} \cdot e^{-\varphi_{\rm RAFT/ROP}}$$
(6)