

SUPPORTING INFORMATION  
for  
High-Performance Rh@MgO Catalysts for Complete  
Dehydrogenation of Hydrazine Borane: A Comparative Study

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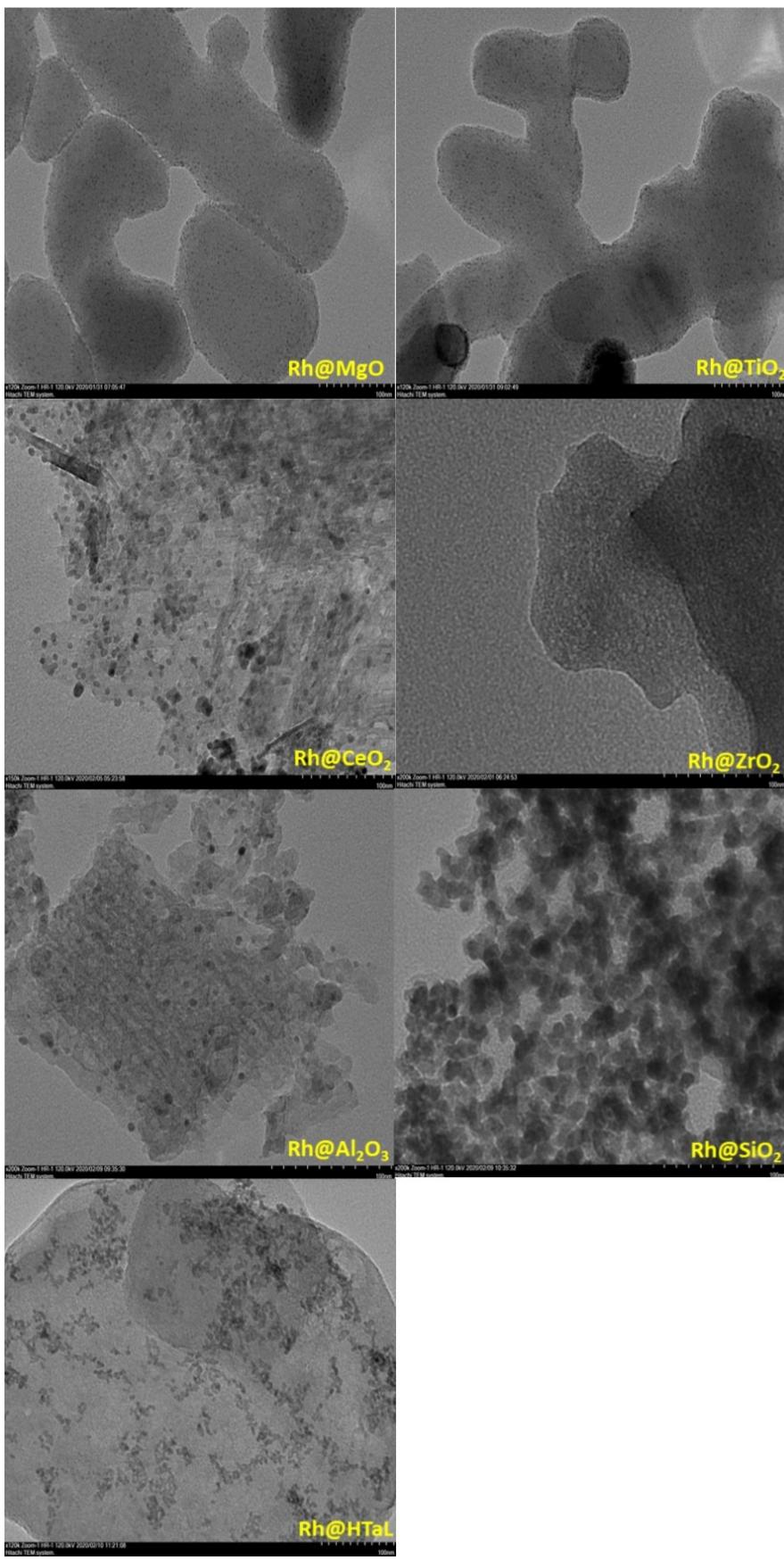


Figure S1. TEM images of monometallic Rh(0) nanoclusters immobilized on different support materials.

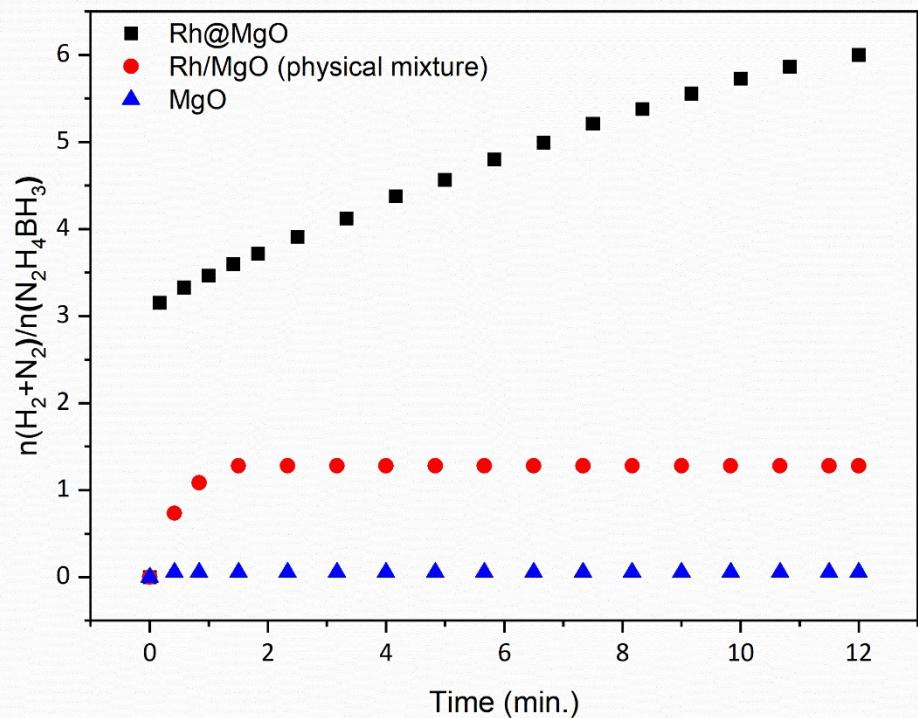


Figure S2. Mole ratio of generated gas ( $\text{H}_2 + \text{N}_2$ )/HB versus time graph for the Rh@MgO, Rh/MgO (physical mixture) and MgO-catalyzed dehydrogenation of aqueous HB.

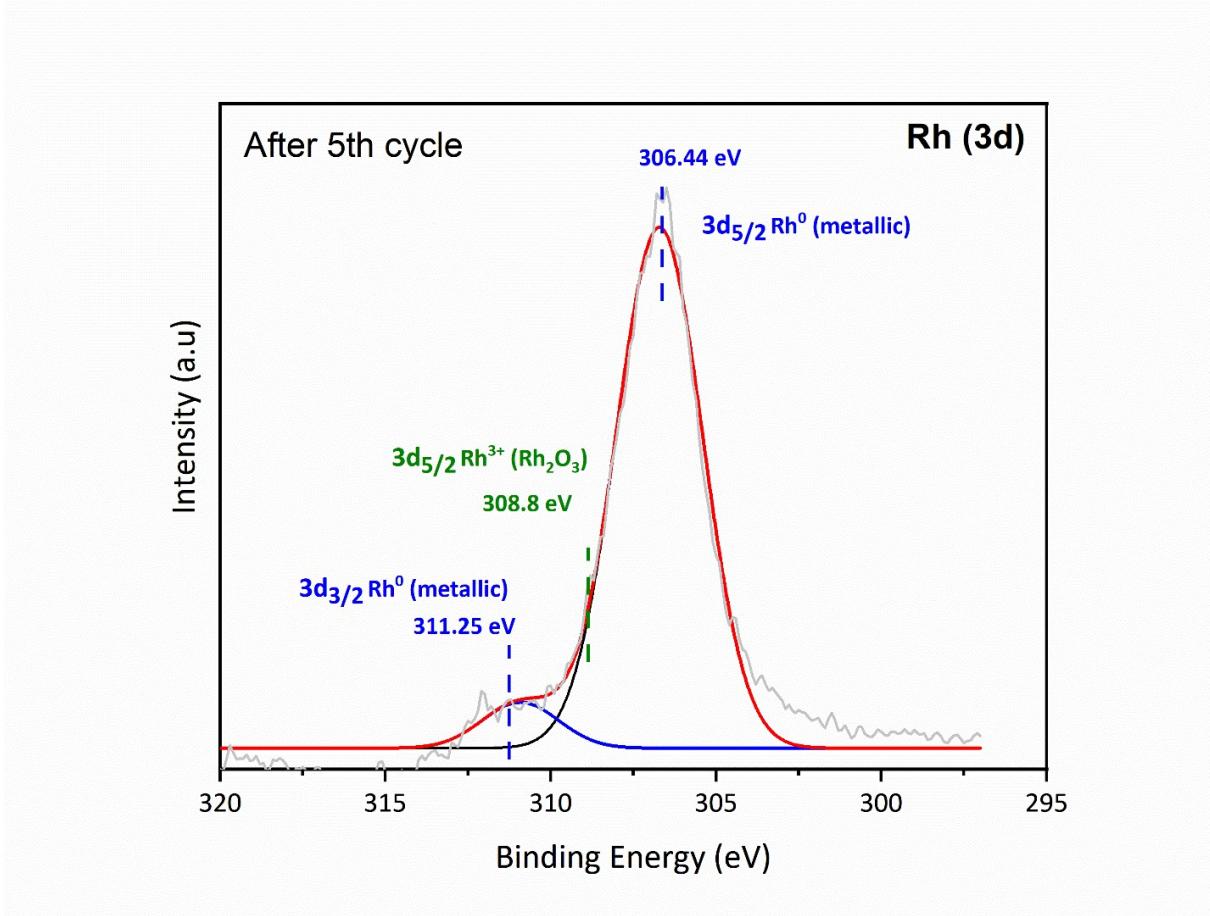


Figure S3. Rh (3d) XPS spectra of Rh@MgO after the 5th reuse cycle, showing the preservation of the metallic Rh structure with minimal shifts, indicating catalyst stability over multiple cycles.

Table S1. Heterogeneous catalysts tested for the complete degradation reaction of hydrazine borane ( $\text{N}_2\text{H}_4\text{BH}_3$ ) in water and capable of conversion.

No	Catalyst	Temperature (K)	TOF (h <sup>-1</sup> )	Ref.
1	Ni@RhNi/Al <sub>2</sub> O <sub>3</sub>	323	72 h <sup>-1</sup>	1
2	Rh <sub>0.8</sub> Ni <sub>0.2</sub> @CeO <sub>x</sub> /rGO	323	667 h <sup>-1</sup>	2
3	Ni <sub>0.9</sub> Pt <sub>0.1</sub> /Graphene	323	242 h <sup>-1</sup>	3
4	Ni <sub>0.9</sub> Pt <sub>0.1</sub> /CeO <sub>2</sub>	323	234 h <sup>-1</sup>	4
5	Ni <sub>0.9</sub> Pt <sub>0.1</sub> /MIL-101	323	1515 h <sup>-1</sup>	5
6	NiIr/Cr <sub>2</sub> O <sub>3</sub>	323	248 h <sup>-1</sup>	6
7	Ni-MoO <sub>x</sub> /BN	323	600 h <sup>-1</sup>	7
8	Ni <sub>0.5</sub> Fe <sub>0.5</sub> -CeO <sub>x</sub> /MIL-101	323	352 h <sup>-1</sup>	8
9	Cu <sub>0.4</sub> Ni <sub>0.6</sub> Mo	323	108 h <sup>-1</sup>	9
10	Ni <sub>0.75</sub> Ir <sub>0.25</sub> /La <sub>2</sub> O <sub>2</sub> CO <sub>3</sub>	323	1250 h <sup>-1</sup>	10
11	Rh <sub>0.5</sub> (Mox) <sub>0.5</sub>	323	2000 h <sup>-1</sup>	11
12	Ni <sub>0.22</sub> @Ir <sub>0.78</sub> /OMS-2	323	2590 h <sup>-1</sup>	12
13	Rh@MgO	323	2005 h <sup>-1</sup>	This Work

### Determination of Average Turnover Frequency (TOF) Values

The activity values in this report are not corrected for the number of exposed surface atoms; that is, the values given are lower limits.

For Rh@MgO catalyst; mol (Rh) = 1.496 µmol, mol (HB) = 1 mmol , Rh@MgO catalyst provides 6 moles equiv. gas generation at t = 12 min.

TOF(average) = moles of product / moles of catalyst × time (where 100 % conversion was achieved)

$$\text{TOF(average)} = (6 \times 10^{-3} \text{ mol}) / (1,496 \times 10^{-5} \text{ mol}) \times (12/60 \text{ h})$$

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