## **Supporting Information**

# Construction of Ni-Co alloy/zeolite nanosheet catalysts for hydrodeoxygenation of fatty acid to alkanes

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#### **Section 1. Materials and Methods**

Tetraethylorthosilicate (TEOS, Tianjin Fuchen Chemical Reagents Company), tetrabutylammonium hydroxide solution (TBAOH, 40 wt % Aladdin), ammonia solution (25%–28%, Sinopharm Chemical Reagent Company), aluminium isopropoxide (Al(C<sub>3</sub>H<sub>7</sub>O)<sub>3</sub>, Tianjin Fuchen Chemical Reagents Company), nickel acetate (Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Sinopharm Chemical Reagent Company), ammonium chloride (NH<sub>4</sub>Cl, Sinopharm Chemical Reagent Company), cobalt acetate (Co(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Sinopharm Chemical Reagent Company, sodium hydroxide (NaOH, Sinopharm Chemical Reagent Company), ammonium nitrate (NH<sub>4</sub>NO<sub>3</sub>, Sinopharm Chemical Reagent Company), stearic acid (98%, Aladdin), dodecane (98%, Aladdin), Commercial ZSM-5 zeolite (Nankai Catalyst Corporation, China). All reagents were used without further purification. Deionized (DI) water was used in all experiments.

*Synthesis of self-pillared ZSM-5 zeolites.* The self-pillared ZSM-5 was synthesized using tetrabutylammonium hydroxide as the structural directing agent, with the gel molar ratio of 1SiO<sub>2</sub>: 0.3 TBAOH: 0.01 Al(C<sub>3</sub>H<sub>7</sub>O)<sub>3</sub>: 0.0125 NaOH: 10 H<sub>2</sub>O. Firstly, 12.4 g of TBAOH solution was mixed with 3 g of deionized water, then 122 mg of aluminum isopropoxide was added and stirred for 30 minutes. After that, 12 mg of NaOH and 12.48 g of TEOS were added and stirred for 4 hours until TEOS was completely hydrolyzed. Finally, the obtained solution was transferred into a 100 mL stainless steel autoclave and crystallized in a pre-heated oven at 80 °C for 1 day and then at 160 °C for 2 days. The as-synthesized solid product was centrifuged, washed with deionized water and ethanol several times, and then dried at 80 °C in the oven

overnight, followed by calcination at 550 °C in air for 6 hours to remove the organic template agent. Finally, the calcined zeolite was converted to the proton form via the ion exchange method. 1 g of calcined zeolite was added into 50 mL 1 M NH<sub>4</sub>NO<sub>3</sub> aqueous solution with continuous stirring at 80 °C for 4 hours. The solid product was centrifuged and washed with deionized water. The process was repeated three times, and the resulted solid product was calcined in air at 550 °C for 6 hours.

*Synthesis of ZSM-5@Ni-Co silicate.* ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.62:0.38 was prepared through a simple hydrothermal process. Typically, 8.7 mg of Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, 4.5 mg of Co(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, 56.1 mg of NH<sub>4</sub>Cl, and 95.6 mg of NH<sub>3</sub>·H<sub>2</sub>O (28%) were added under stirring in 5.25 g of deionized water. Then 10 mg of the self-pillared ZSM-5 was added to the above solution and ultrasonicated for 30 min to form a uniform suspension, then the mixture was heated to 100 °C for 3 h. The resulting solid precipitate was collected, washed several times with deionized water and ethanol and dried at 80 °C in the oven for 4 hours. The ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.75:0.25 was synthesized using a similar experimental process as the ZSM-5@Ni-Co silicate with the Ni/Co silicate with the Ni/Co ratio of 0.62:0.38 except involving the use of 8.7 mg of Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, 2.25 mg of Co(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, 46.75 mg of NH<sub>4</sub>Cl, 79.63 mg of NH<sub>3</sub>·H<sub>2</sub>O, and 4.375 g of deionized water.

Synthesis of ZSM-5@Ni-Co/SiO2. ZSM-5@Ni-Co silicate was reduced under a H2 flow (flow

rate: 20 mL min<sup>-1</sup>) at 550 °C for 0.5 h with a heating rate of 5 °C min<sup>-1</sup>, and black power of ZSM-5@Ni-Co/SiO<sub>2</sub> was collected. The obtained catalysts were designated as ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub> and ZSM-5@Ni<sub>0.75</sub>Co<sub>0.25</sub>/SiO<sub>2</sub> separately.

Synthesis of commercial ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>. Commercial ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub> (C-ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>) was prepared using a similar experimental process as ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>, with the only difference being the substitution of self-pillared ZSM-5 zeolites with commercial ZSM-5 zeolites.

*Synthesis of ZSM-5@Ni*<sub>3</sub>*Si*<sub>2</sub>*O*<sub>5</sub>*(OH)*<sub>4</sub>. Typically, 8.7 mg of Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, 37.4 mg of NH<sub>4</sub>Cl, and 63.7 mg of NH<sub>3</sub>·H<sub>2</sub>O (28%) were added under stirring in 3.5 g of deionized water. Then 10 mg of the self-pillared ZSM-5 was added to the above solution and ultrasonicated for 30 min to form a uniform suspension, then the mixture was heated to 100 °C for 3 h. The resulting solid precipitate was collected, washed several times with deionized water and ethanol and dried at 80 °C in the oven for 4 hours.

*Synthesis of ZSM-5@Ni/SiO*<sub>2</sub>. ZSM-5@Ni<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub> was reduced under a H<sub>2</sub> flow (flow rate: 20 mL min<sup>-1</sup>) at 550 °C for 0.5 h with a heating rate of 5 °C min<sup>-1</sup>, and black power of ZSM-5@Ni/SiO<sub>2</sub> was collected.

Synthesis of ZSM-5@Co<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub>. ZSM-5@Co<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub> was prepared under a similar

experimental process as ZSM-5@Ni<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub>, with the only difference being the substitution of the Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O with Co(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O.

*Synthesis of ZSM-5@Co/SiO*<sub>2</sub>. ZSM-5@Co<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub> was reduced under a H<sub>2</sub> flow (flow rate: 20 mL min<sup>-1</sup>) at 550 °C for 0.5 h with a heating rate of 5 °C min<sup>-1</sup>, and black power of ZSM-5@Co/SiO<sub>2</sub> was collected.

#### **Section 2. Characterizations**

The powder X-ray diffraction measurements were performed on a Rigaku D-Max 2550 diffractometer by using Cu Kα radiation. Scanning electron microscopy images were measured with JEOL JSM-7800F. The transmission electron microscopy images and the elemental mappings were measured with a Tecnai F20 electron microscope. High resolution transmission electron microscopy (HRTEM) and energy dispersive spectrometer (EDS) mapping were performed on a JEOL JEM-2100F microscope. The H<sub>2</sub>-TPR measurements were measured on a Micromeritics AutoChem II 2920 instrument. Chemical compositions of samples were analyzed by Inductively Coupled Plasma-Optical Emission Spectrometry (ICP-OES) using iCAP 7000 Series. Nitrogen adsorption/desorption measurements were carried out on a Micromeritics ASAP 3-flex analyzer at 77 K after the samples were degassed at 350 °C under vacuum. XPS spectra of the catalysts were performed using a Thermo ESCALAB 250 spectrometer (Thermo Scientific, NY, USA). Fourier transform infrared (FTIR) spectra were recorded on a BRUKER vertex 80v; samples before testing were pelleted with KBr powder.

#### Section 3. Catalytic tests

The deoxygenation reaction of stearic acid (SA) was carried out in a batch autoclave (CHEMN Instrument, 100 mL). In a typical run, 0.1 g of catalysts, 1 g of SA and 40 mL of dodecane were introduced into the batch autoclave. The autoclave was sealed and firstly purged with N<sub>2</sub> (30 bar) three times to remove the residual air, followed by filling it with the reaction gas H<sub>2</sub> (40 bar) at room temperature. The reaction was performed at 260 °C at a stirring speed of 1000 rpm. The liquid products were obtained by *in-situ* sampling every 20 min and analyzed by gas chromatography (GC, Agilent 7890B) equipped with HP-innowax column (30 m × 320  $\mu$ m × 25  $\mu$ m) and FID detector. The methyl heptadecanoate was used as a quantitative internal standard in GC measurement. The mass balance was above 98%.

The yield, conversion, and normalized rate were calculated based on the following equations:

The conversion (%) = mass of the converted SA (g)/mass of the starting SA (g) ×100% (By GC analysis) (Equation S1) The selectivity (%) = mass of one product (g)/mass of all the products (g) ×100% (By GC analysis) (Equation S2)

The yield (%) = conversion×selectivity×100% (Equation S3)

The reaction rate  $(g_{SA} g_{cat}^{-1} h^{-1}) = mass of converted SA (g)/mass of catalyst (g)/reaction time (h)$ (Equation S4)

## Section 4. Additional figures and tables



Fig. S1 (a, b) SEM and (c, d) TEM images of ZSM-5 zeolites with self-pillared nanosheet morphology.



**Fig. S2** (a, b) SEM and (c, d) TEM images of ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.62:0.38.



Fig. S3 TEM image of ZSM-5@Ni $_{0.62}$ Co $_{0.38}$ /SiO<sub>2</sub> catalysts.



Fig. S4 H<sub>2</sub>-TPR profile of ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.62:0.38.



Fig. S5 NH<sub>3</sub>-TPD profiles of ZSM-5 and ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>.



Fig. S6 (a, d, g) SEM and (b, c, e, f, h, i) TEM images of (a–c) ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.75:0.25, (d–f) ZSM-5@Ni<sub>3</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub>, and (g–i) ZSM- $5@Co_3Si_2O_5(OH)_4$ .



Fig. S7 XRD patterns of (a) ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.75:0.25, (b)  $ZSM-5@Ni_3Si_2O_5(OH)_4$ , and (c)  $ZSM-5@Co_3Si_2O_5(OH)_4$ .



Fig. S8 XRD patterns of (a) ZSM-5@Ni $_{0.75}$ Co $_{0.25}$ /SiO<sub>2</sub>, (b) ZSM-5@Ni/SiO<sub>2</sub>, and (c) ZSM-5@Co/SiO<sub>2</sub>.



Fig. S9 (a, b) SEM and (c, d) TEM images of commercial ZSM-5 zeolites.



**Fig. S10** (a, b) SEM and (c, d) TEM images of C-ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.62:0.38.



Fig. S11 (a) SEM image, (b, c) TEM images of C-ZSM-5@ $Ni_{0.62}Co_{0.38}/SiO_2$ , and (d) the corresponding size distribution of Ni-Co alloy nanoparticles.



**Fig. S12** XRD patterns of (a) C-ZSM-5@Ni-Co silicate with the Ni/Co ratio of 0.62:0.38 and (b) C-ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>.



Fig. S13  $N_2$  adsorption-desorption isotherms of C-ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub>.



Fig. S14 Time-dependent product yields with ZSM-5@Ni $_{0.75}$ Co $_{0.25}$ /SiO<sub>2</sub> catalysts.



Fig. S15 Time-dependent product yields with ZSM-5@Ni/SiO<sub>2</sub> catalysts.



Fig. S16 Time-dependent product yields with ZSM-5@Co/SiO<sub>2</sub> catalysts.



Fig. S17 Time-dependent product yields with C-ZSM-5@Ni<sub>0.62</sub>Co<sub>0.38</sub>/SiO<sub>2</sub> catalysts.



Fig. S18 The ratio of  $n-C_{18}/n-C_{17}$  in the product over different ZSM-5@Ni-Co alloy/SiO<sub>2</sub> catalysts.

	$S_{BET}^{a}$	S <sub>micro</sub> <sup>b</sup>	$\mathbf{S}_{\mathrm{ext}}^{b}$	V <sub>micro</sub> <sup>b</sup>	$V_{total}^{c}$	V <sub>meso</sub> <sup>d</sup>
Sample	(m <sup>2</sup> /g)	(m <sup>2</sup> /g)	(m <sup>2</sup> /g)	(cm <sup>3</sup> /g)	(cm <sup>3</sup> /g)	(cm <sup>3</sup> /g)
ZSM-5	464	359	105	0.14	0.72	0.58
ZSM-5@Ni-Co silicate	477	175	302	0.07	0.67	0.60
$ZSM-5@Ni_{0.62}Co_{0.38}/SiO_2$	448	162	286	0.07	0.66	0.59
C-ZSM-5@Ni <sub>0.62</sub> Co <sub>0.38</sub> /SiO <sub>2</sub>	323	214	109	0.10	0.42	0.32

 Table S1. The textural properties of the various samples.

<sup>*a*</sup> Specific surface area calculated from the nitrogen adsorption isotherm using the BET method. <sup>b</sup> S<sub>micro</sub> (micropore area), S<sub>ext</sub> (external surface area), and V<sub>micro</sub> (micropore volume) calculated using the t-plot method. <sup>c</sup> Total pore volume at P/P<sub>0</sub> = 0.99. <sup>d</sup> V<sub>meso</sub> = V<sub>total</sub> - V<sub>micro</sub>.

Catalyst	Metal loading (wt%)	Reaction composition <sup>a</sup>	Reaction conditions	Time (min)	Con. (%)	Rate $(g g_{cat}^{-1} h^{-1})$	HDO/DCO <sub>x</sub> <sup>b</sup>	Ref.
ZSM-5@Ni <sub>0.62</sub> Co <sub>0.38</sub> /SiO <sub>2</sub>	22.6	10/1	T=260 °C P=4.0 MPa H <sub>2</sub>	50	100	12	8.63	This work
Ni/Co-S	4	3/5	T=290 °C P=4.0 MPa H <sub>2</sub>	180	99.0	0.20	12.3	1
Co <sub>x</sub> Ni <sub>1-x</sub> P/SiO <sub>2</sub>	10	50/3	T=320 °C P=2.0 MPa H <sub>2</sub>	240	96.9	4.0	0.06	2
NiCo/SiO <sub>2</sub>	20	5/3	T=280 °C P=1.0 MPa H <sub>2</sub>	180	83.0	0.46	mainly DCO	3
NiCo/C-Na	20	5/3	T=280 °C P=1.0 MPa H <sub>2</sub>	180	100	0.55	mainly DCO	4

**Table S2.** Comparisons of catalytic activities for hydrodeoxygenation of fatty acids over literature reported catalysts with this work.

<sup>a</sup> The reaction composition refers to the mass ratio of the substrate to the catalyst in the reaction slurry.

<sup>*b*</sup> HDO/DCO<sub>x</sub> was calculated based on (selectivity of hydrodeoxygenation (HDO) products)/(selectivity of decarboxylation (DCO) or decarbonylation (DCO<sub>2</sub>) products).

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