

## Electronic Supplementary Material

### Ruthenium-doped Ni(OH)<sub>2</sub> to enhance the activity of methanol oxidation reaction and promote the efficiency of hydrogen production

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## Materials characterization

Transmission Electron Microscopy (TEM) and EDS elemental mapping were observed by JEM 2100F (Japan) at 200 kV. X-ray diffraction (XRD) was carried out on Rigaku Ultima IV diffractometer (Japan) with Cu K $\alpha$  radiation, scanning speed of 8° min<sup>-1</sup>, and the 2 $\theta$  range 10° - 80°. Scanning electron microscopy (SEM) was performed on Hitachi S-4800 (Japan) to observe the microstructure and morphology details. under an accelerating voltage of 15.0 kV. X-ray Photoelectron Spectroscopy (XPS) was measured by Escalab 250xi with Al K $\alpha$  radiation under the condition of 12.5 kV and 250 W (America), the energy of 284.8 eV is used as the basis for correction. High pressure liquid chromatography (HPLC) was recorded on Agilent1200 (America).

## Instruments and measurements

The electrochemical experiments were investigated on a CH Instruments (CHI 760 E, Shanghai, China) electrochemical workstation, where, the Ru/Ni(OH)<sub>2</sub>/NF was shear into 1 \* 1 cm and straight employed as the working electrode, the counter electrode: graphite rod, reference electrode: 3 M KCl-saturated Ag/AgCl electrode (CH Instruments, CHI 111), and the electrolyte was 1 M KOH (pH = 14) solution. Potentials were calculated used the reversible hydrogen electrode (RHE) scale ( $E$  vs. RHE =  $E_{Ag/AgCl} + 0.059 * pH + 0.197$  V).<sup>1</sup> For MOR and HER, electrochemical impedance spectroscopy (EIS) was used at 100000 Hz and 0.01 Hz at the voltage of 0.5 V vs. RHE (MOR) and -1.12 V vs. RHE (HER), respectively, and an amplitude of 5 mV. Estimated electrochemical double layer capacitance ( $C_{dl}$ ) was obtained by the cyclic voltammetry (CV) testing in the non-Faraday region between -0.05 V and -0.15 V vs. Ag/AgCl with the scan rates from 20 mV s<sup>-1</sup> to 100 mV s<sup>-1</sup>. For HER, the CV cycling

stability were swept between 0 ~ -0.8 V vs. RHE at a scan rate of 0.1 V·s<sup>-1</sup>. The linear sweep voltammetry (LSV) were recorded at a scan rate of 5 mV s<sup>-1</sup>. The *i*-*t* curves of HER and MOR were tested at potentials of -1.07 V and 0.34 V, respectively. All the electrochemical measurements were proceeded at room temperature of 25° C.

In 1 M KOH with 1 M MeOH at room temperature, the as-synthesized Ru/Ni(OH)<sub>2</sub>/NF (1×1 cm) was used cathode and anode to investigate the performance of MOR coupled with HER in a single-chamber membrane-less cell, and the electrolyte was 20 mL KOH solution. The polarization curves were collected by linear sweep voltammetry from 1 V to 2 V at a scan rate of 5 mV s<sup>-1</sup>. The *i*-*t* measurement at a voltage of 2.1 V, H<sub>2</sub> production was collected by the water displacement method with a 100 mL graduated cylinder.

All electrochemical tests were not *i*R corrected.

### **Calculation of product (H<sub>2</sub> or formate) yield and faradaic efficiency**

The Faraday efficiency (%) of the H<sub>2</sub> and formate can be determined by the following equation:<sup>2,3</sup>

$$FE = V_{(measured)} / V_{(calculated)}$$

Where *V (measured)* is the experimentally collected gas yield by water displacement method, and *V (calculated)* is the theoretical gas yield, which is calculated as follow:

$$V (Calculated) = V_m * [Q / (n * F)]$$

$$FE = (N \times Z \times F / Q) \times 100\%$$

where *N* is the mole of product (H<sub>2</sub> or formate) reduced, *V<sub>m</sub>* is the gas molar volume of 24.5 mol L<sup>-1</sup> at room temperature and pressure, *Q* is the passed charge, *F* is the Faraday constant (96 485 C mol<sup>-1</sup>), and *Z* is the number of electrons transferred for a mole of H<sub>2</sub> (*Z* = 2) and

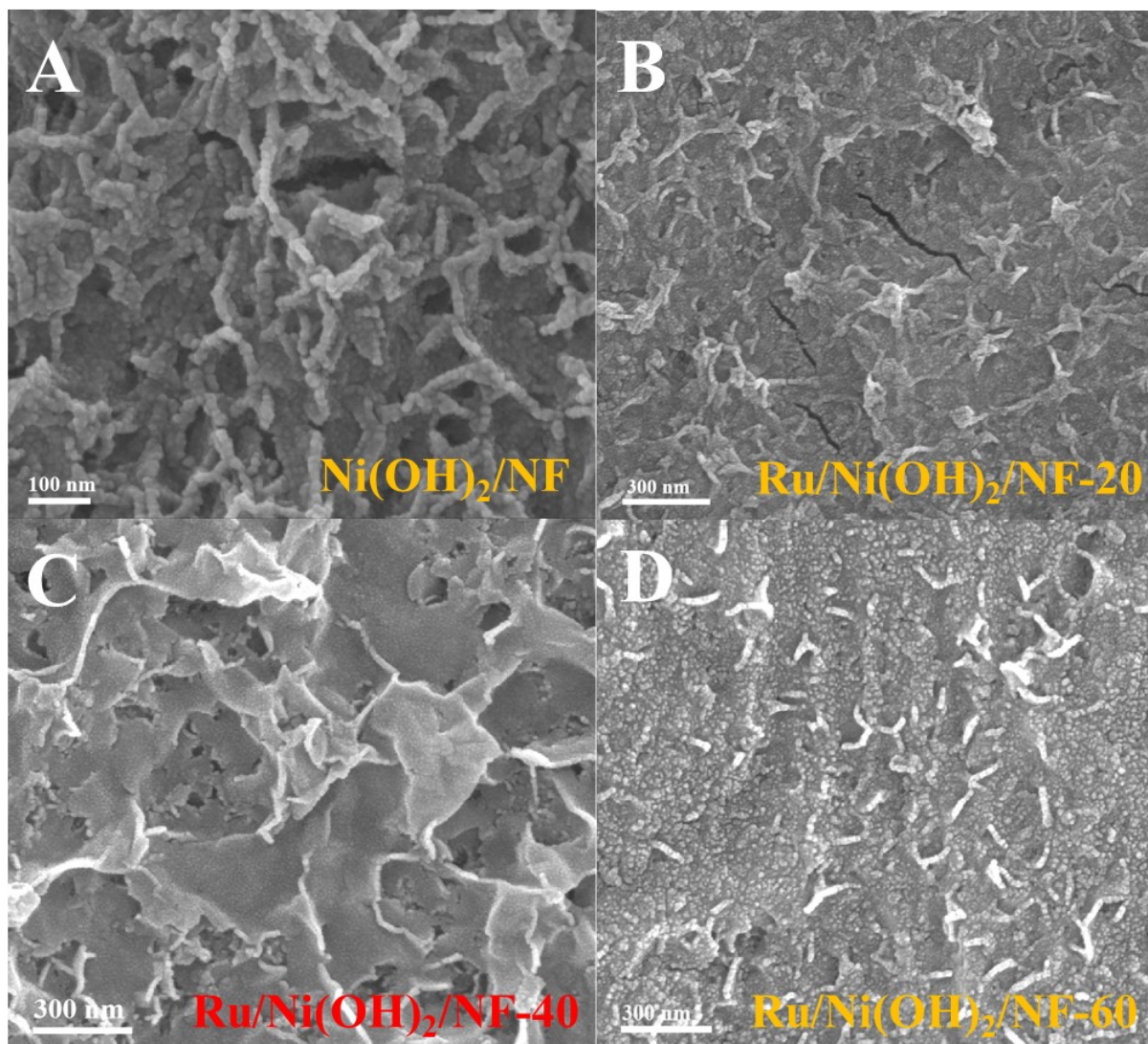
formate ( $Z = 4$ ) formation.

### **Energy Consumption Efficiency:<sup>3</sup>**

$W = U \times I \times t = U \times Q$ , where  $U$  is the applied voltage (V),  $I$  is the current (A),  $t$  is the time (s), and  $Q$  is the passed charge (C). When producing the same amount of hydrogen by HER and MOR and HER and OER (consumed the same  $Q$ ), the required electrical energy of former is  $W_1 = U_1 \times Q_1$ , while the latter is  $W_2 = U_2 \times Q_2$ . So  $W_1 / W_2 = U_1 / U_2$ . The energy consumption saving is equal to  $(U_2 - U_1) / U_2 \times 100\%$ .

### **Calculation of ECSA:**

$ECSA = C_{dl} / C_s \times 1$ , (the specific capacitance ( $C_s$ ) was taken as  $0.060 \text{ mF cm}^{-2}$ ),<sup>4</sup> the geometric area of the working electrode is  $1 \text{ cm}^2$ ), Current density differences ( $\Delta j / 2 = j_a - j_c$ ) at  $-0.01 \text{ V}$  (vs. Ag/AgCl) were plotted against scan rates, the linear slope was used to represent  $C_{dl}$ .



**Fig. S1.** The SEM image of the Ni(OH)<sub>2</sub>/NF (A), Ru/Ni(OH)<sub>2</sub>/NF-20 (B), Ru/Ni(OH)<sub>2</sub>/NF-40 (C), Ru/Ni(OH)<sub>2</sub>/NF-60 (D).

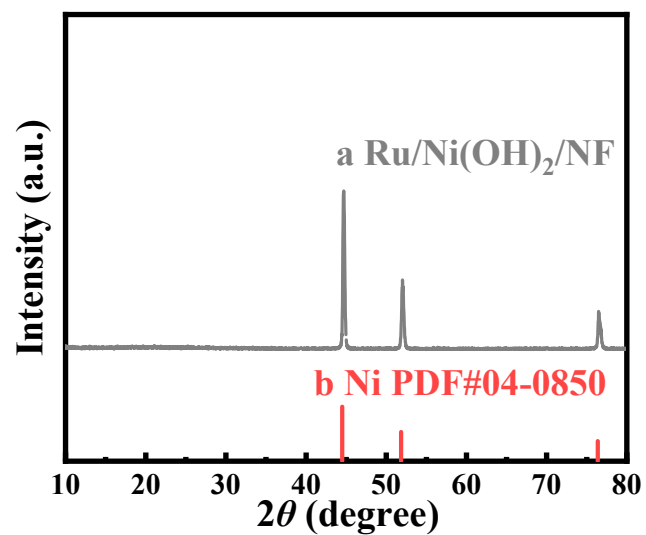


Fig. S2. (A) The XRD patterns of the Ru/Ni(OH)<sub>2</sub>/NF.

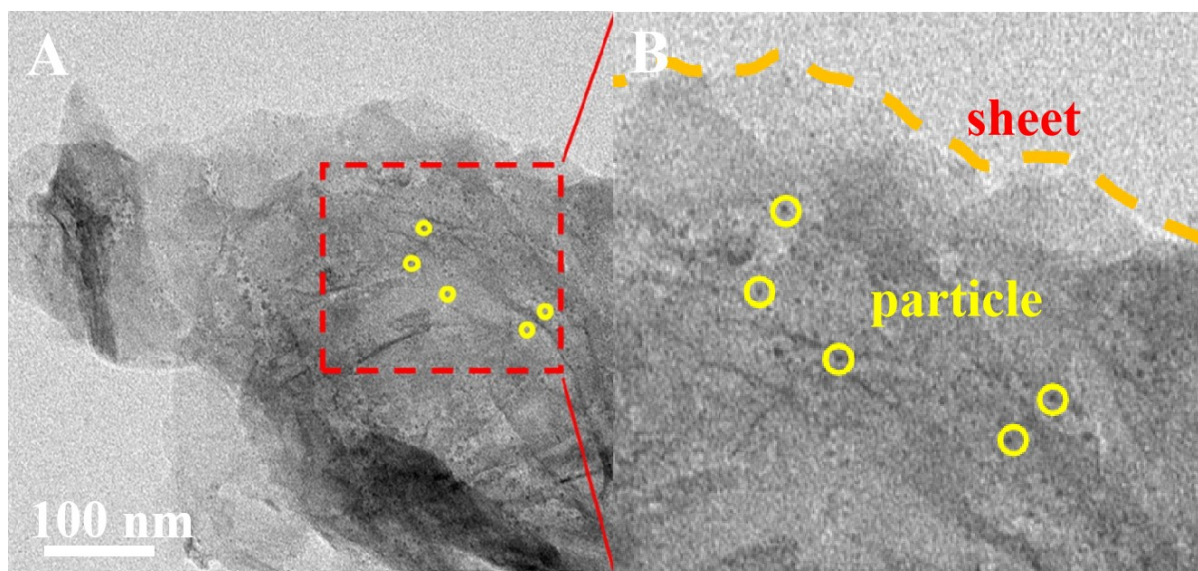
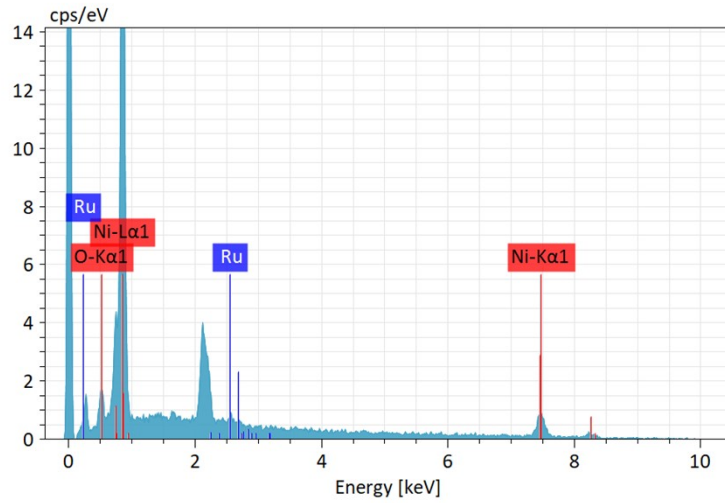
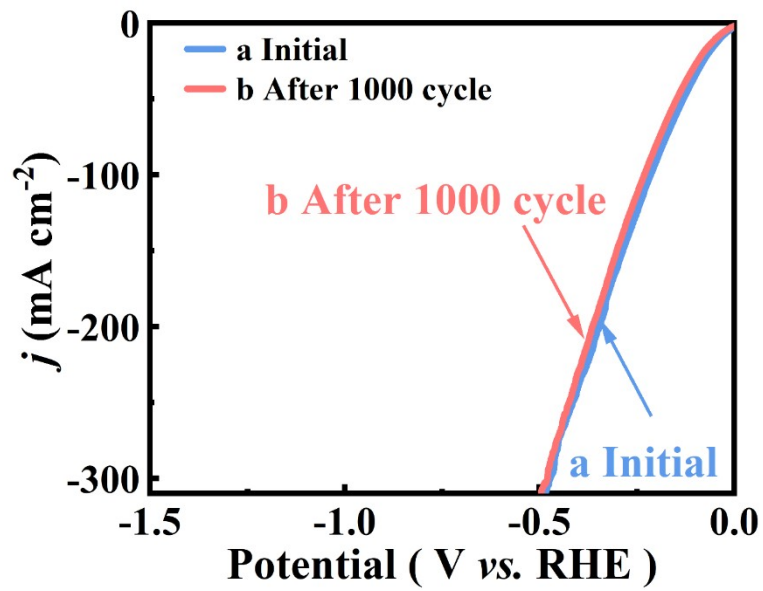


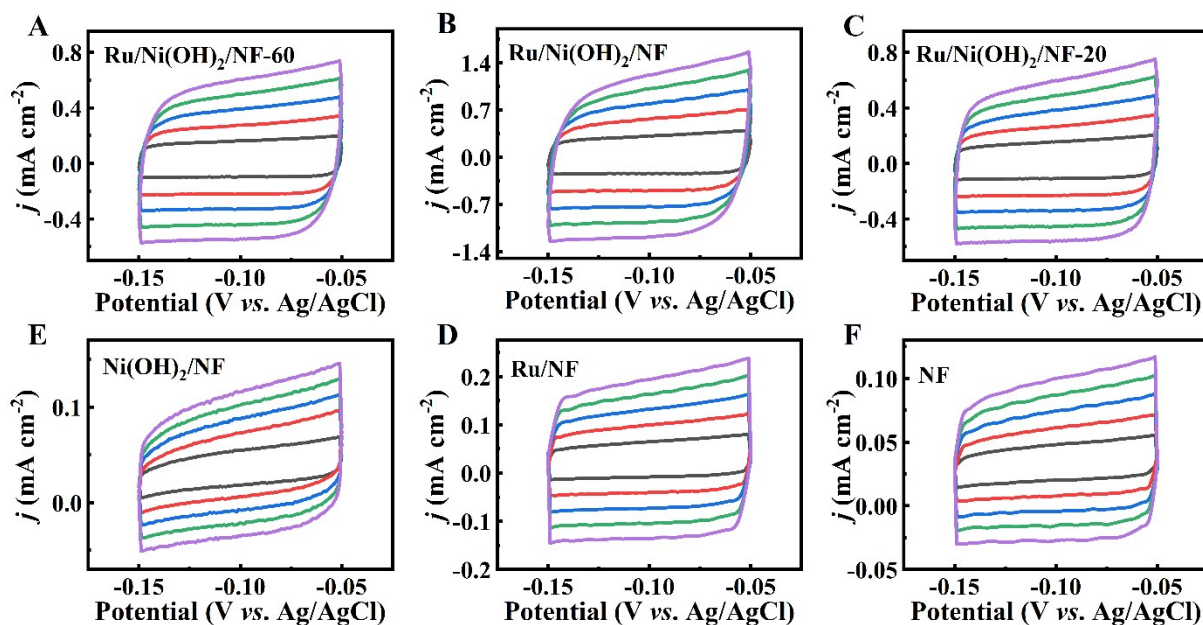
Fig. S3. The HRTEM image of the Ru/Ni(OH)<sub>2</sub>/NF.



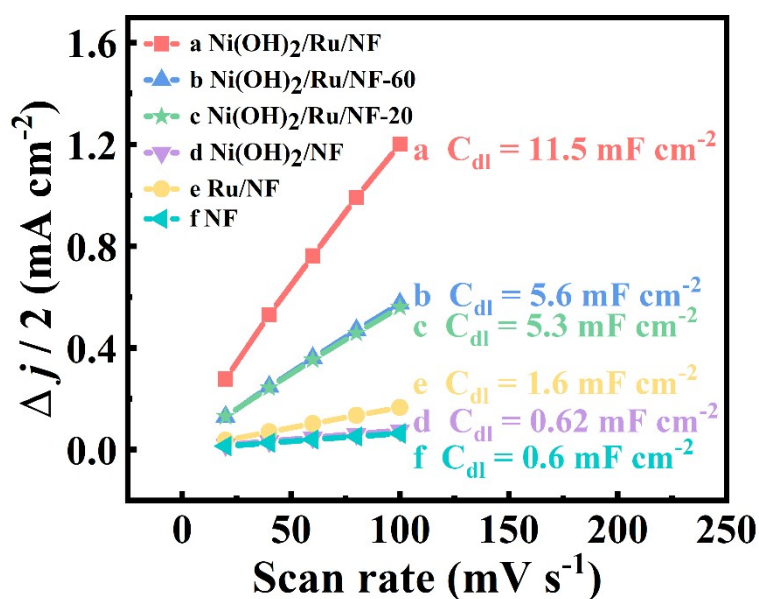
**Fig. S4.** The EDS image of the Ru/Ni(OH)<sub>2</sub>/NF



**Fig. S5.** The LSV curves of the Ru/Ni(OH)<sub>2</sub>/NF before (a) and after (b) 1000 CV cycles.



**Fig. S6.** (A-F) The CV tests of different catalysts, the scanning rates range (20 ~ 100 mV s<sup>-1</sup>) in 1 M KOH.



**Fig. S7.** The corresponding  $C_{dl}$  value comparison of the Ru/Ni(OH)<sub>2</sub>/NF (a), the Ru/Ni(OH)<sub>2</sub>/NF-60 (b), the Ru/Ni(OH)<sub>2</sub>/NF-20 (c), the Ni(OH)<sub>2</sub>/NF (d), the Ru/NF (e) and the NF (f) in 1 M KOH.



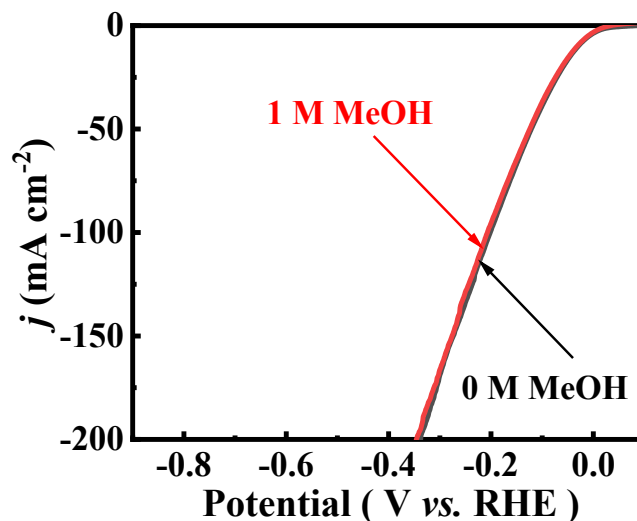


Fig. S8. The LSV curves of the Ru/Ni(OH)<sub>2</sub>/NF in 1 M KOH with 1 M methanol.

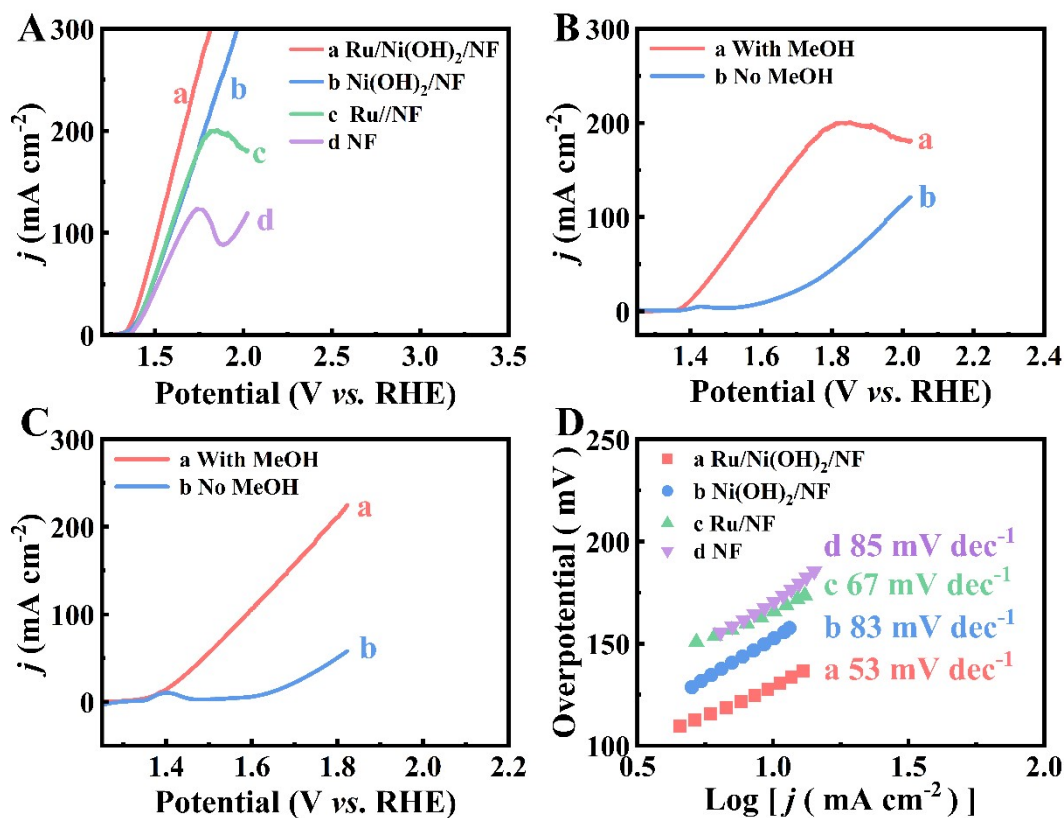
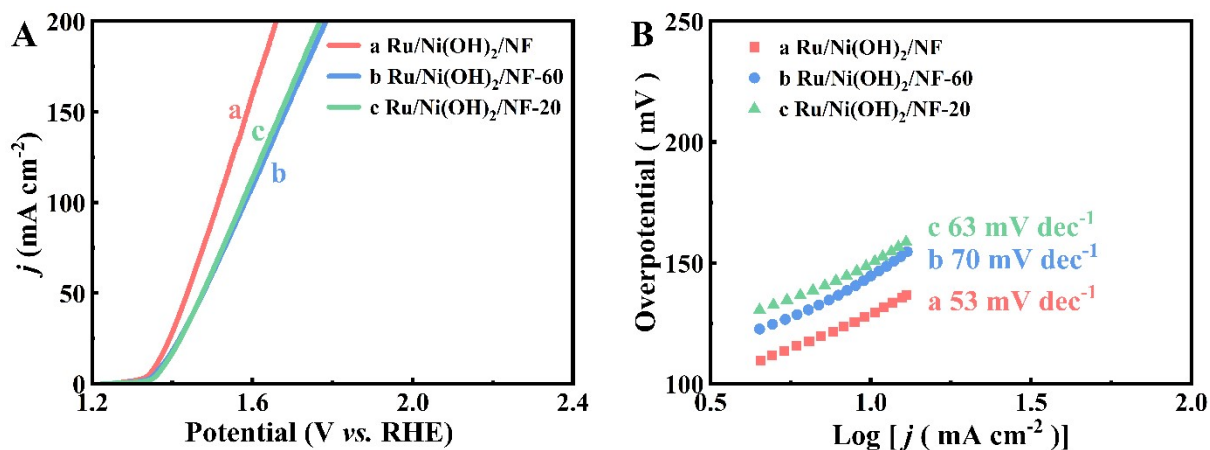
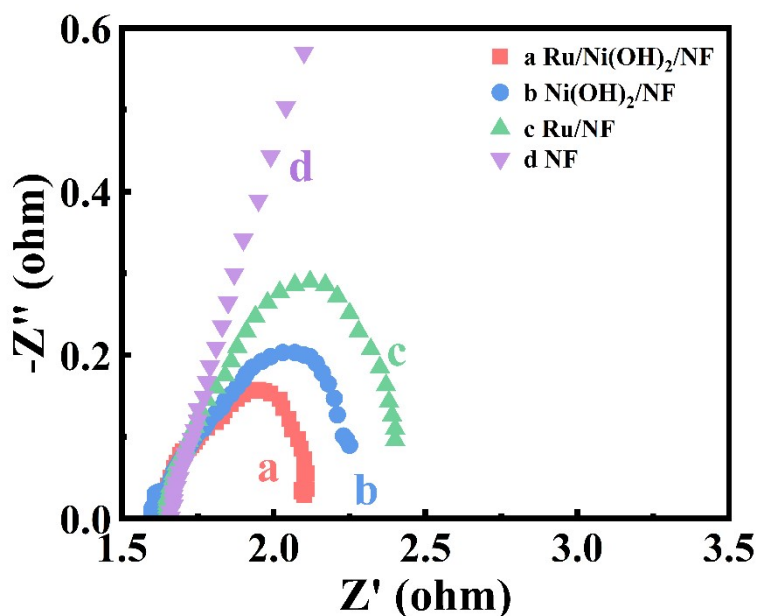


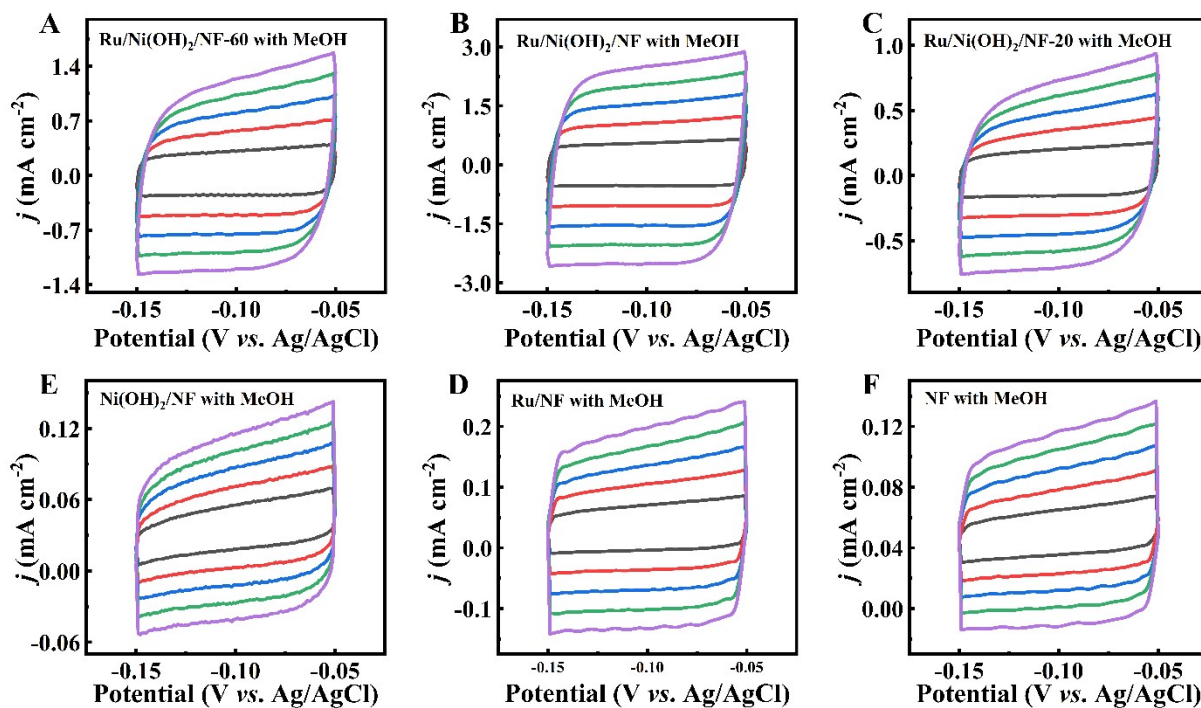
Fig. S9. (A) The LSV curves of the Ru/Ni(OH)<sub>2</sub>/NF (a), the Ni(OH)<sub>2</sub>/NF (b), the Ru/NF(c), the NF (d) in 1 M KOH with 1 M MeOH. (B) The LSV curves of the Ru/NF and (C) the Ni(OH)<sub>2</sub>/NF in 1 M KOH with (a) and without (b) 1 M methanol. (D) Tafel plots of the Ru/Ni(OH)<sub>2</sub>/NF (a) , the Ni(OH)<sub>2</sub>/NF (b), the Ru/NF(c), the NF (d) in 1 M KOH with 1 M MeOH.



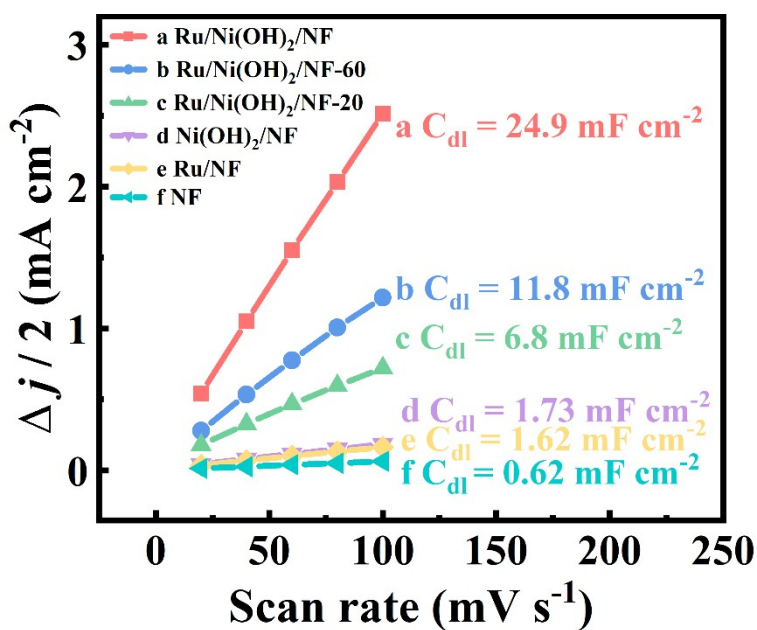
**Fig. S10.** (A) The LSV curves and (B) Tafel plots of the Ru/Ni(OH)<sub>2</sub>/N (a), the Ru/Ni(OH)<sub>2</sub>/NF-60 (b), the Ru/Ni(OH)<sub>2</sub>/NF-20 (c) in 1 M KOH with 1 M MeOH.



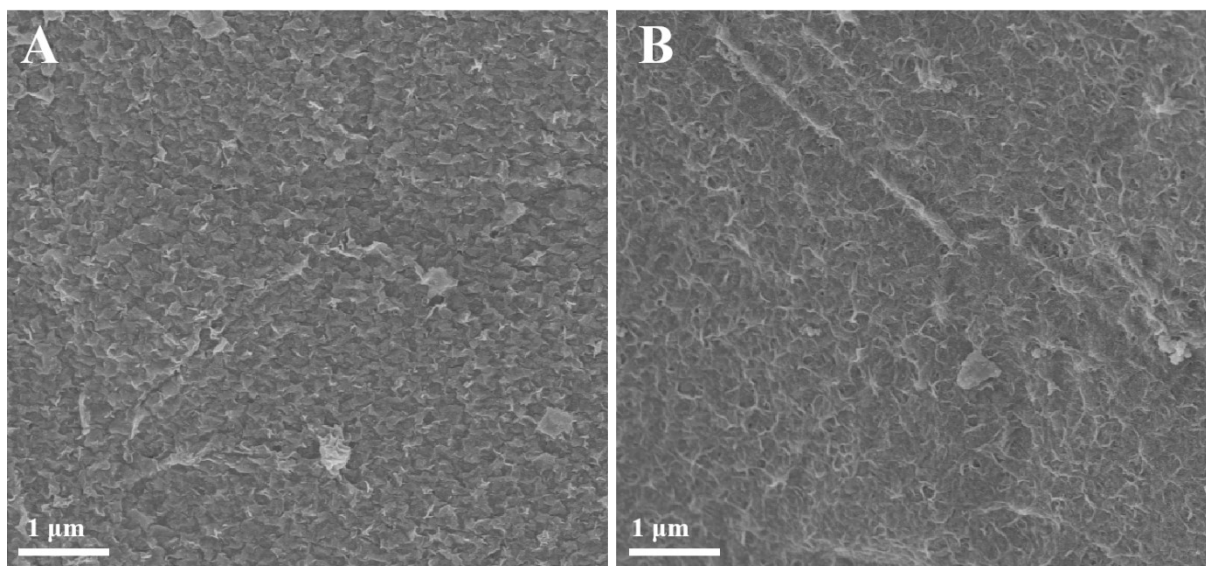
**Fig. S11.** The electrochemical impedance spectroscopy (EIS) analyses of the catalysts for methanol oxidation. Nyquist plots of the Ru/Ni(OH)<sub>2</sub>/NF (a), the Ni(OH)<sub>2</sub>/NF (b), the Ru/NF (c) and the NF (d) for methanol electro-oxidation process in 1 M KOH with 1 M methanol.



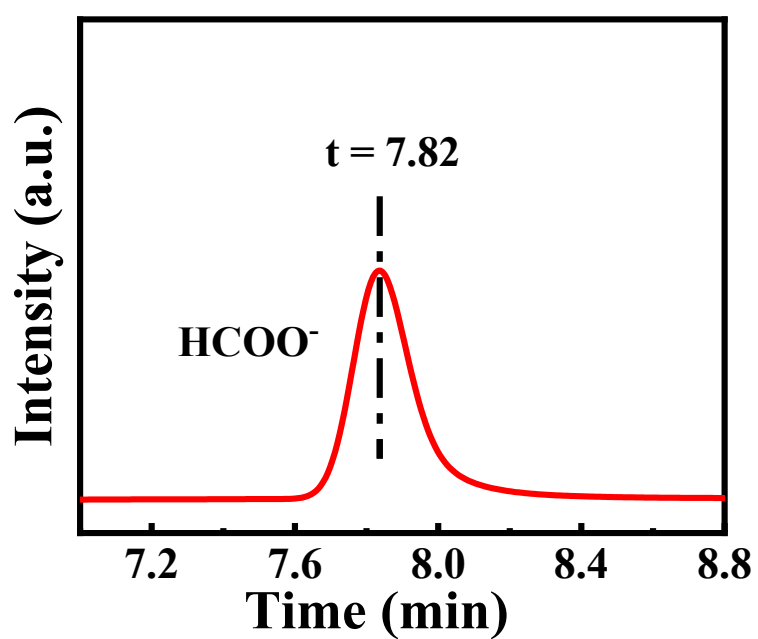
**Fig. S12.** (A-F) The CV tests of different catalysts, the scanning rates range ( $20 \text{ mV s}^{-1} \sim 100 \text{ mV s}^{-1}$ ) in 1 M KOH with 1 M methanol.



**Fig. S13.** The corresponding  $C_{dl}$  value comparison of the Ru/Ni(OH)<sub>2</sub>/NF (a), the Ru/Ni(OH)<sub>2</sub>/NF-60 (b), the Ru/Ni(OH)<sub>2</sub>/NF-20 (c), the Ni(OH)<sub>2</sub>/NF (d), the Ru/NF (e), and the NF (f) in 1 M KOH with 1 M MeOH.



**Fig. S14** The SEM images of the Ru/Ni(OH)<sub>2</sub>/NF after 1000 cycles of CV cycle stability of HER (A) and MOR test (B).



**Fig. S15.** Formate standard materials were tested on the HPLC.

**Table S1.** Comparison of the HER performances of various catalysts in 1 M KOH.

Catalysts	iR compensation	Electrode	Overpotentia (mV) @ 10 mA/cm <sup>2</sup>	Ref.
<b>Ru/Ni(OH)<sub>2</sub>/NF</b>	<b>0%</b>	<b>NF</b>	<b>42</b>	<b>This work</b>
MoP-Ru <sub>2</sub> P/NPC	95%	GCE	47	5
Ru/Ni(OH) <sub>2</sub> /TM-0.2	95%	Ti mesh	135	6
(Ru-Co)O <sub>x</sub> /CC	95%	CC	44.1	7
CoSA-NC@Ru	95%	CC	14	8
Ru/Ni(OH) <sub>2</sub> /NF	95%	NF	25	9
Ru/Ni(OH) <sub>2</sub>	80%	CP	31	10
R-NiRu/NF	95%	NF	16	11
Ru-NC-700	85%	GCE	47	12

**Table S2.** Representative electrochemical reforming of the MOR.

catalysts	Electrolyte	Main anode product	Cell voltage at 10 mA cm <sup>-2</sup> (V)	Ref.
<b>Ru/Ni(OH)<sub>2</sub>/NF</b>	<b>1 M KOH + 1 M methanol</b>	<b>formate</b>	<b>1.36</b>	<b>this work</b>
NiMoO/NF	1 M KOH + 0.5 M Urea	N <sub>2</sub> , CO <sub>2</sub>	1.37	13
CoCu-UMOF Ns	1 M KOH + 3 M methanol	formate	1.365	14
Co <sub>3</sub> O <sub>4</sub> NSs/CP	1 M KOH + 1 M Ethanol	Ethyl acetate	1.445	15
Co <sub>3</sub> O <sub>4</sub> NWS/CC	1 M KOH + 40 mg L <sup>-1</sup> triclosan	Phenol	1.54	16
Ni-MOF	1 M KOH + 0.33 M Urea	N <sub>2</sub> , CO <sub>2</sub>	1.36	17
NF-Pt/C	1 M KOH + 0.5 M Urea	N <sub>2</sub> , CO <sub>2</sub>	1.48	18
Co@NPC-800	1 M KOH + 0.1 M glucose	formate	1.46	19

**Table S3.** Comparison of the chemical-assisted hydrogen evolution reaction performance.

Bifunctional catalysts	Electrolyte	Main anode product	Cell voltage at 10 mA cm <sup>-2</sup> (V)	Ref.
<b>Ru/Ni(OH)<sub>2</sub>/NF</b>	<b>1 M KOH + 1 M methanol</b>	<b>formate</b>	<b>1.45</b>	<b>this work</b>
Pd/Ni(OH) <sub>2</sub> @C/NF	1 M KOH + 1 M ethanol	-	1.49	20
Co-Rh <sub>2</sub>	1 M KOH + 1 M methanol	formate	1.55	21
Ni(OH) <sub>2</sub> /NF	1 M KOH + 0.5 M methanol	formate	1.52	22
MnO <sub>2</sub> /MnCo <sub>2</sub> O <sub>4</sub> /Ni	1 M KOH + 0.5 M Urea	N <sub>2</sub> , CO <sub>2</sub>	1.58	23
Ni <sub>0.33</sub> Co <sub>0.67</sub> (OH) <sub>2</sub> /NF	1 M KOH + 0.5 M methanol	formate	1.50	24
Os-Ni <sub>x</sub> P/N-C/NF	1 M KOH + 1 M methanol.	formate	1.43	25
NiAl-LDH-NS <sub>s</sub>	1 M KOH + 1 M ethanol	formate	1.72	26
Co-S-P/CC	1 M KOH + 1 M ethanol	acetic acid	1.63	27

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