

## SUPPLEMENTARY INFORMATION

### Improving the catalytic performance of Co/BaCeO<sub>3</sub> catalyst for ammonia synthesis by Y-modification of the perovskite-type support

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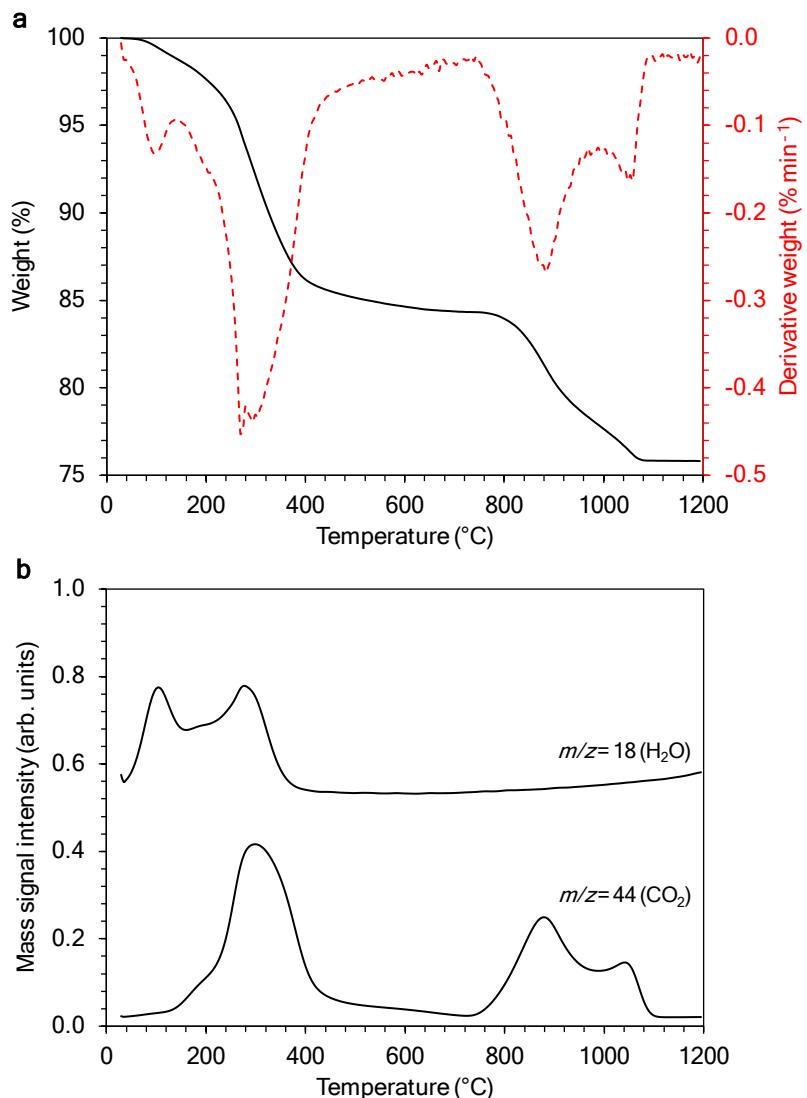
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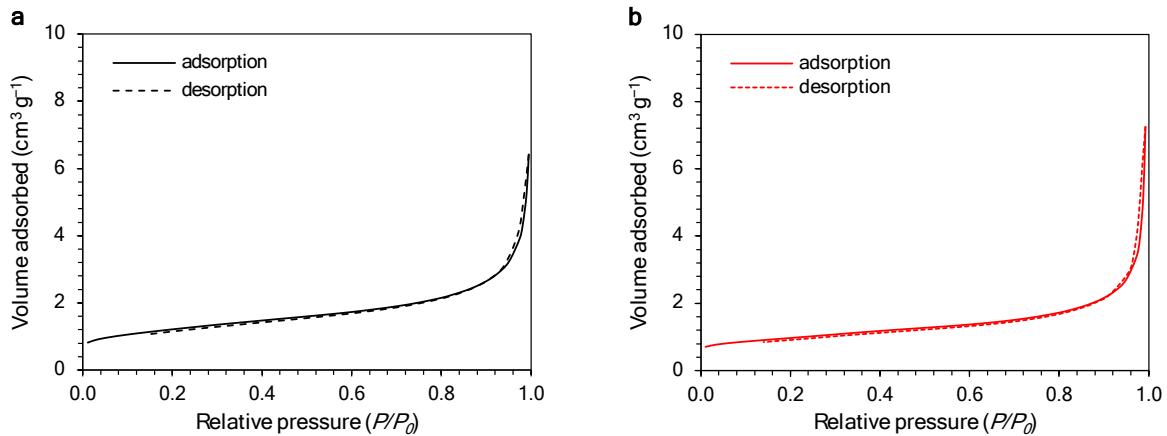
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**Table S1.** Average reaction rate ( $r_{\text{NH}_3}$ ) of ammonia synthesis reaction over catalysts with different active metals (10 wt% of Co, Ni, Mo, or Fe) supported on BaCe<sub>1-x</sub>Y<sub>x</sub>O<sub>3-δ</sub> (x=0.10).

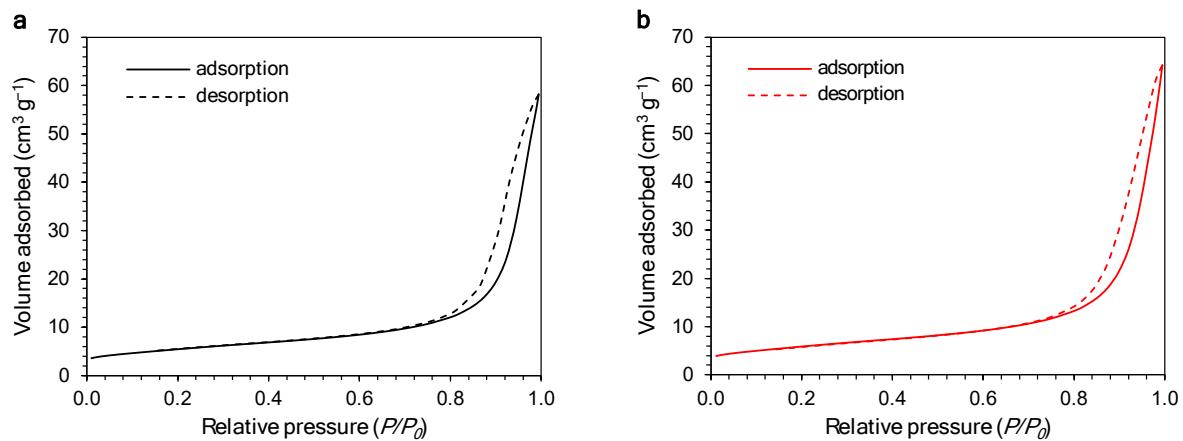
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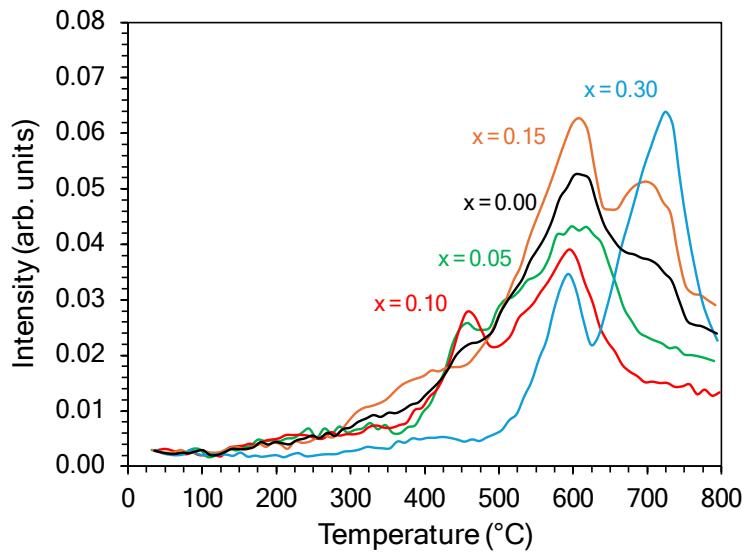
**Figure S1.** TGA-MS profile of thermal decomposition of the  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0$ ) support precursor obtained by co-precipitation (according to the procedure described in section 2.1). (a) mass loss curve (TG) and derivative of mass loss curve (DTG) during sample heating, (b) mass signals of water vapour ( $m/z=18$ ) and carbon dioxide ( $m/z=44$ ) evolved during sample heating (measurement conditions: 50 mg sample, flow 100 mL min<sup>-1</sup> of air, heating 10 °C min<sup>-1</sup> in the temperature range of 30–1200 °C).



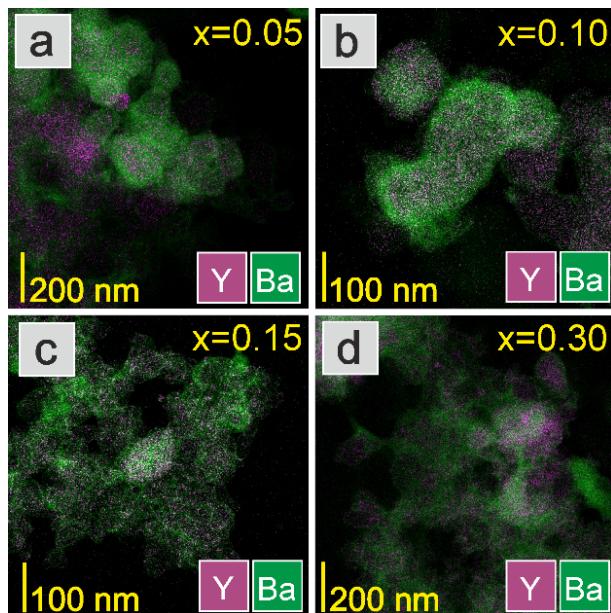
**Figure S2.** Exemplary N<sub>2</sub> adsorption-desorption isotherms of (a)  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0$ ) and (b)  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0.10$ ) supports.



**Figure S3.** Exemplary N<sub>2</sub> adsorption-desorption isotherms of (a) Co/BaCe<sub>1-x</sub>Y<sub>x</sub>O<sub>3-δ</sub> ( $x=0$ ) and (b) Co/BaCe<sub>1-x</sub>Y<sub>x</sub>O<sub>3-δ</sub> ( $x=0.10$ ) catalyst precursors.



**Figure S4.**  $\text{H}_2\text{-TPR}$  profiles of the  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0\text{--}0.30$ ) supports.



**Figure S5.** EDX maps of distribution of Ba and Y on the  $\text{Co/BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0.05\text{--}0.30$ ) catalysts surface (catalyst after reduction in  $\text{H}_2$  at  $600\text{ }^{\circ}\text{C}$ ).

**Table S1.** Average reaction rate ( $r_{\text{NH}_3}$ ) of ammonia synthesis reaction over catalysts with different active metals (10 wt% of Co, Ni, Mo, or Fe) supported on  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0.10$ ). Activation conditions: 470 °C (72 h) → 520 °C (24 h) → 550 °C (48 h) → 600 °C (24 h), flow of  $\text{H}_2/\text{N}_2$  mixture (75/25 mol%, 30  $\text{dm}^3 \text{ h}^{-1}$ ), atmospheric pressure. Measurement conditions: 470°C, 6.3 MPa, flow of  $\text{H}_2/\text{N}_2$  mixture (75/25 mol%, 70  $\text{dm}^3 \text{ h}^{-1}$ ).

Catalyst	Active phase	$r_{\text{NH}_3} (\text{g}_{\text{NH}_3} \text{ g}_{\text{cat}}^{-1} \text{ h}^{-1})$
Mo/ $\text{BaCe}_{0.90}\text{Y}_{0.10}\text{O}_{3-\delta}$	Mo	0.01
Ni/ $\text{BaCe}_{0.90}\text{Y}_{0.10}\text{O}_{3-\delta}$	Ni	0.14
Fe/ $\text{BaCe}_{0.90}\text{Y}_{0.10}\text{O}_{3-\delta}$	Fe	0.32
Co/ $\text{BaCe}_{0.90}\text{Y}_{0.10}\text{O}_{3-\delta}$	Co	2.66

**Table S2.** Structural parameters of the  $\text{BaCe}_{1-x}\text{Y}_x\text{O}_{3-\delta}$  ( $x=0-0.30$ ) supports based on the Rietveld analysis.

Support	x	Phase	a /Å	b /Å	c /Å	b /°	V /Å <sup>3</sup>
$\text{BaCeO}_3$	0.00	<i>Pmcn</i>	8.7745(2) <sup>a</sup>	6.2323(2)	6.2131(2)	-	339.77(2)
$\text{BaCe}_{0.95}\text{Y}_{0.05}\text{O}_{3-\delta}$	0.05	<i>Pmcn</i>	8.7745(2)	6.2326(2)	6.2148(1)	-	339.88(1)
$\text{BaCe}_{0.90}\text{Y}_{0.10}\text{O}_{3-\delta}$	0.10	<i>Pmcn</i>	8.7760(2)	6.2366(1)	6.2174(1)	-	340.25(1)
$\text{BaCe}_{0.85}\text{Y}_{0.15}\text{O}_{3-\delta}$	0.15	<i>Pmcn</i>	8.7567(5)	6.222(1)	6.218(1)	-	338.74(9)
$\text{BaCe}_{0.70}\text{Y}_{0.30}\text{O}_{3-\delta}$	0.30	<i>I2/m</i>	6.2478(4)	8.7676(6)	6.2215(4)	90.946(4)	340.76(4)

<sup>a</sup> Uncertainty of the last digit (within parentheses).