Supplementary information

Efficient adsorptive removal of potassium from potassium perrhenate solution by cationic ion exchange resin

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Text S1. Adsorption isotherm models

Adsorption isotherm is used to describe the relationship between adsorption capacity and concentration of solution after adsorption equilibrium at a certain temperature. Adsorption isotherm is usually fitted by adsorption isotherm models. At present, there are four commonly used models include Langmuir model, Freundlich model, Temkin model and Dubinin–Radushkevich model ¹⁻³, as follows:

Langmuir model:

$$q_e = \frac{q_{\max}K_L C_e}{1 + K_L C_e} \tag{S-1}$$

$$R_{L} = \frac{1}{1 + K_{L}C_{0}}$$
(S-2)

Freundlich model:

$$q_e = K_F C_e^{1/n} \tag{S-3}$$

Temkin model:

$$q_e = B_T \ln K_T + B_T \ln C_e \tag{S-4}$$

$$B_T = RT / b \tag{S-5}$$

Dubinin-Radushkevich model:

$$\ln q_e = \ln q_m - K_{DR}\varepsilon^2 \tag{S-6}$$

$$\varepsilon = RT \ln(1 + \frac{1}{C_e}) \tag{S-7}$$

$$E = \frac{1}{\sqrt{2K_{DR}}}$$
(S-8)

Where C_e , C_0 are the equilibrum and initial concentration of the adsorbate in the solution (mg·L⁻¹), respectively, q_e is the adsorption capacity of adsorbent to adsorbate after adsorption equilibrium, (mg·g⁻¹), q_{max} is maximum adsorption capacity of single molecular layer of adsorbent related to adsorption sites (mg·g⁻¹), n is Freundlich constant indicating the adsorption intensity, b represent the Temkin constant, q_m refers to theoretical isotherm saturation capacity (mg·g⁻¹), K_L , K_F , K_T and K_{DR} are the equilibrium constants of Langmuir, Freundlich, Temkin, and Dubinin-Radushkevich models, respectively, ε refers to the Polanyi potential constant (J/mol), and E refers to energy per molecule of adsorbate (kJ/mol)

Text S2. Adsorption kinetic models

Adsorption kinetics mainly describes the change of adsorption rate and the influence of external factors on the adsorption process. The models of Pseudo-first-order, Pseudo-second-order and Weber-Morris^{4, 5} are commonly used adsorption kinetic models, as follows:

Pseudo-first-order equation:
$$q_t = q_e(1 - e^{-K_1 t})$$
 (S-9)

Pseudo-second-order equation:
$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e}$$
 (S-10)

Weber-Morris equation:
$$q_t = K_p t^{1/2} + C$$
 (S-11)

where K_1 is the adsorption rate constant of the Pseudo-first-order model, min⁻¹; K_2 is the adsorption rate constant of the Pseudo-second-order model, g·mg⁻¹·min⁻¹; K_p is the intra-particle diffusion rate constant, mg·g⁻¹·min^{-0.5}; *C* is a constant, which is related to the thickness of boundary layer.



Fig. S1 The potassium adsorption efficiency of C160 and C160H $(KReO_4 \text{ solution concentration of } 2 \text{ g} \cdot \text{L}^{-1}, \text{ solid-to- liquid ratio of } 1:20, \text{ rotating speed of } 180 \text{ rpm},$ temperature of 25°C, contact time of 6h)



Fig. S2 Adsorption of potassium by resin according to various isotherm models: (a)-Langmuir; (b)-Freundlich; (c)-Temkin; (d)-Dubinin-Radushkevich



Fig. S3 SEM-EDS scanning results of C160H resin loaded with potassium: (a) SEM images, (b-f) EDS maps for elemental distribution, and (g) elemental composition spectrum



Fig. S4 SEM-EDS scanning results of C160H resin before adsorption: (a)SEM images, (b-f) EDS maps for elemental distribution, and (g) elemental composition spectrum



 $\label{eq:Ebinding} \begin{array}{ll} \Delta E_{binding} & 321.24\,kcal\cdot mol^{-1} & 5.43\,kcal\cdot mol^{-1} \end{array}$ Fig. S5 Binding energy between $H^+/\,K^+$ and ligand

Preperty	Description
Structure	Macroporous
Matrix	Polystyrene / divinylbenzene
Functional group	Sulfonic Acid
Ionic form	Na^+
Bead size	0.3-1.2 mm
Specific gravity	1.3 g/mL (in Na ⁺ form)
Moisture retention	35%-40% (in Na ⁺ form)
Total capacity	2.3 meq/mL (in Na ⁺ form)

Table S1 Physical and chemical properties of Purolite C160 ion exchange resin

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