# **Supporting Information**

# Dual active site-mediated Ir single-atom-doped RuO<sub>2</sub> catalysts for highly efficient and stable water splitting

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## **Experimental Details**

## **1.1 Computational Details**

The Density functional theory (DFT) calculations were conducted in the Vienna Abinitio Simulation Package (VASP). The electron exchange and correlation energy were treated with the Perdew-Burke-Ernzerhof (PBE) functional within the generalized gradient approximation (GGA)<sup>[1,2]</sup>. The ion cores-valence electrons interactions were described through the projected augmented wave (PAW) means, and the van der Waals interactions were eliminated with Grimme's method<sup>[3]</sup>. The simulations were implemented with a plane-wave basis set defined by a kinetic energy cutoff of 400 eV, and a  $1\times1\times1$  Monkhorst Pack k-point grid was used to integrate the Brillouin zone<sup>[4,5]</sup>. The geometry optimization and energy calculation were terminated when the electronic selfconsistent iteration and force reached  $10^{-5}$  eV and 0.02 eV Å<sup>-1</sup>. The theoretical models were built based on the (110) of RuO<sub>2</sub> (PDF#40-1290) and (110) of IrO<sub>2</sub> (PDF 04-006-7402).

The calculation model of Ir single atom doped  $RuO_2$  ( $Ir_{SA}/RuO_2$ ) was constructed by Replacement of Ru atoms in  $RuO_2$  crystals by Ir atoms (96 O, 47Ru, 1 Ir atoms). A vacuum space as large as 15 Å was used along the c direction to avoid periodic interactions. The k-point sampling was obtained from the Monkhorst-Pack scheme with a (3×2×1) mesh for optimization and a (3×2×1) mesh for calculations of electronic structure.

The alkaline HER reaction could be divided into two elementary reactions:

 $H_2O + e - + * = *H + OH^*$ 

 $H = * + 1/2 H_2$ 

Where \*H signifies the H moiety on the adsorption site. The energy of H+/e- is approximately equal to the energy of  $1/2 H_2$ .

The OER process is divide into the four fundamental reactions as following:

- (1)  $H_2O + * = OH^* + H^+ + e^-$
- (2) OH\* = O\* + H+ + e-
- (3) 0\* + H<sub>2</sub>O = OOH\* + H+ + e-
- (4) OOH\* = O<sub>2</sub> + H+ + e-

OOH\*, O\* and OH\* present the OOH, O and OH moieties on the adsorption site.

The change in Gibbs free energy ( $\Delta$ G) of each adsorbed intermediate was calculated according to the computational hydrogen electrode method developed by Nørskov et al<sup>[6]</sup>. At standard conditions (T = 298.15 K, pH = 0, and U = 0 V (vs. SHE), the free energy is defined as the following equation:

 $\Delta G = \Delta E + \Delta EZPE - T\Delta S$ 

Where  $\Delta E$  represents the energy change obtained from DFT calculation,  $\Delta EZPE$  is the difference between the adsorbed state and gas, which is calculated by summing vibrational frequency for all model based on the equation:  $EZPE = 1/2\sum hV_i$ . T is the temperature (298.15 K) in the above reaction system, and  $\Delta S$  represents the difference on the entropies between the adsorbed state and gas phase. The entropies of free molecules were obtained from NIST database (https://janaf.nist.gov/). And the free energy of the adsorbed state \*H can be taken as:  $\Delta G^*H = \Delta E^*H + 0.24.[7]$ 

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#### **1.2 Materials and Reagents**

Ruthenium chloride (RuCl<sub>3</sub>) and iridium chloride (IrCl<sub>3</sub>) were purchased from Aladdin Reagents Ltd. Ammonium fluoride, Urea and ethanol were obtained from Sinopharm Chemical Reagent Co., Ltd. Nafion solution (5%), Commercial Pt/C and Commercial RuO<sub>2</sub> catalyst were obtained from Sigma-Aldrich Chemical Reagent Co., Ltd. All regents were analytical reagents and used without further purification.

#### **1.3 Materials Syntheses**

Firstly, 0.2 g of urea and 0.1 g of ammonium fluoride were added to 40 ml of water and 20 ml of ethanol solution until completely dissolved, followed by the addition of 2 mmol RuCl<sub>3</sub> and 0.06 mmol IrCl<sub>3</sub> and stirring until completely dissolved, then the above solutions were transferred to a 100 ml Teflon-lined autoclave and maintained

at 160  $^\circ \mathrm{C}$  for 10 h, and the sample obtained were centrifuged and dried to obtain the

precursor. The obtained precursor was then subjected to heat treatment in at different conditions (650  $^{\circ}$ C, 4 h; 750  $^{\circ}$ C, 4 h; 850  $^{\circ}$ C, 4h; 950  $^{\circ}$ C, 4 h) to obtain the final catalysts, which were named Ir<sub>SA</sub>/RuO<sub>2</sub>-650, Ir<sub>SA</sub>/RuO<sub>2</sub>-750, Ir<sub>SA</sub>/RuO<sub>2</sub>-850, and Ir<sub>SA</sub>/RuO<sub>2</sub>-950, respectively.

Synthesis of RuO<sub>2</sub>: The precursor is obtained in the same way as described above except that IrCl<sub>3</sub> was not added, the synthesized samples were centrifuged as well as

dried in vacuum. Subsequently, the precursor was heat-treated under 850  $^{\circ}$ C, 4 h to obtain the final catalysts.

# 1.4 Characterization

The characterization of the synthesized products was carried out using various techniques. X-ray diffraction (XRD) was performed using a Bruker D8 diffractometer with Cu Kα radiation to investigate the crystalline structure of the products in the range of 10-80° at room temperature. Transmission electron microscopy (TEM) was used to observe the morphology and microstructure of the products. The morphology and structure were characterized by double spherical aberration-corrected scanning transmission electron microscope (AC-STEM, Titan Cubed Themis G2 300) X-ray photoelectron spectroscopy (XPS) was used to detect the surface chemical composition and state of the products. The binding energies were calibrated relative to the C1 s peak at 284.6 eV. Inductively coupled plasma optical emission spectrometer (ICP-OES) was used to detect the amount of dissolved metal in the postreaction electrolyte. These analytical techniques were chosen to provide comprehensive information about the synthesized products, including their crystal structure, morphology, microstructure, chemical composition, and metal dissolution behavior.

# **1.5 Electrochemical measurements**

To evaluate the electrocatalytic performance of the catalysts, a typical three-electrode cell was used, which was connected to an electrochemical workstation (CHI660E). The working electrode, reference electrode, and counter electrode were chosen as glassy carbon (GC) electrode, Hg/HgO (SCE) and graphite rod, respectively. The electrolyte is 1 mole per liter potassium hydroxide (1M/L KOH). To prepare the catalyst ink, 5 mg of the as-prepared sample and 1 mg of conductive XC-72 powder were dispersed into a mixture containing 870  $\mu$ L isopropyl alcohol, 100  $\mu$ L water, and 30  $\mu$ L 5% Nafion solution. The mixture was then ultrasonically dispersed for 30 minutes. Afterward, 6  $\mu$ L of the ink was coated on the GC electrode with a diameter of 3 mm and dried under an infrared lamp to obtain the catalyst layer with a loading of 0.425 mg cm<sup>-2</sup>. For comparison, 5 mg of commercial catalyst powder (20 wt% Pt/C/RuO<sub>2</sub>) was evenly dispersed into the same mixture. The ink is applied to the GC electrode for overall water splitting.

To test the performance of the catalysts for hydrogen evolution reaction (HER), linear

sweep voltammetry (LSV) was conducted with a scan rate of 5 mV s<sup>-1</sup> in different potential ranges. All polarization curves were 90% iR-corrected. Electrochemical impedance spectroscopy (EIS) was performed at the corresponding potentials of 10 mA cm<sup>-2</sup> obtained from the LSV curves, with a frequency range of 0.1 to 100,000 Hz. The double-layer capacitance (C<sub>dl</sub>) was determined by recording cyclic voltammetry curves in the non-reactive region with a scan rate of 20 to 120 mV s<sup>-1</sup>. The C<sub>dl</sub> was calculated using the formula  $C_{dl} = \Delta J/2v$ , where  $\Delta J$  represents the current density difference and v represents the scan rate. The electrochemical specific surface area (ECSA) was calculated using the formula ECSA =  $C_{dl}/C_s$ , where Cs is the specific capacitance for an ideal flat surface with a real surface area of 1 cm<sup>2</sup>. In this study, a general value of 60  $\mu$ F cm<sup>-2</sup> was adopted for C<sub>s</sub>. Stability can be assessed using CV accelerating tests and chronoamperometry tests.







Figure S2. EDS spectrum of  $Ir_{SA}/RuO_2$ -850.



Figure S3. TEM imagines of pure RuO<sub>2</sub>.



Figure S4. AC HAADF-STEM image of  $Ir_{SA}/RuO_2$ -850.



Figure S5. XPS spectrum of Ir single atom doped RuO<sub>2</sub>.



Figure S6. Tafel slopes of RuO<sub>2</sub>.



**Figure S7.** (a) Ir<sub>SA</sub>/RuO<sub>2</sub>-850 and (b) RuO<sub>2</sub> at different scan rates outside the OER region; (c) C<sub>dl</sub> and (d) ECSA of Ir<sub>SA</sub>/RuO<sub>2</sub>-850 and C-RuO<sub>2</sub>.



Figure S8. Mass activity of  $Ir_{SA}/RuO_2$ -850 and C-RuO<sub>2</sub> at overpotential of 400 mV.



Figure S9. The dissolved amount of Ru for  $Ir_{SA}/RuO_2$ -850 during the OER stability test.



Figure S10. LSV curves of initial and after stability performance testing of  $Ir_{SA}/RuO_2$ -850 catalyst.



Figure S11. (a) LSV curves of OER of catalyst and (b) overpotentials at current density at 10 mA cm<sup>-2</sup>, 50 mA cm<sup>-2</sup> of catalysts in acidic medium; (c) Tafel slop and (d) fitted EIS curves of catalysts; (e) Chronoamperometry test curves of  $Ir_{SA}/RuO_2$ -850 and C-RuO<sub>2</sub>.



Figure S12. Digital photographs of collected H<sub>2</sub> and O<sub>2</sub> at different time.



**Figure S13**. Optimal crystal structures of (a) RuO<sub>2</sub> and (b) Ir<sub>SA</sub>/RuO<sub>2</sub>, (c) charge density difference of two-dimensional slice on Ir<sub>SA</sub>/RuO<sub>2</sub> model.



Figure S14. Adsorption configurations of reaction intermediates at various sites for HER. (a-d) H<sub>2</sub>O, OH-H, H and 2H adsorption configurations on Ru site of Ir<sub>SA</sub>/RuO<sub>2</sub>. (e-h) H<sub>2</sub>O, OH-H, H and 2H adsorption configurations on Ir site of Ir<sub>SA</sub>/RuO<sub>2</sub>. (i-l) H<sub>2</sub>O, OH-H, H and 2H adsorption configurations on Ru site of RuO<sub>2</sub>.



Figure S15. Adsorption configurations of reaction intermediates at various sites for HER. (a-d) OH, O, OOH and 2-O adsorption configurations on Ru site of Ir<sub>SA</sub>/RuO<sub>2</sub>. (e-h) OH, O, OOH and 2-O adsorption configurations on Ir site of Ir<sub>SA</sub>/RuO<sub>2</sub>. (i-l) OH, O, OOH and 2-O adsorption configurations on Ru site of RuO<sub>2</sub>.

		η@j	Tafel slope	Deferrere	
Catalysts	Electrolytes	(mV @ mA cm <sup>-2</sup> )	(mV dec⁻¹)	Reference	
Ir <sub>sA</sub> /RuO <sub>2</sub> -850	1 M KOH	234@10	67.5	This work	
Ru/RuO <sub>2</sub> -PRS	1М КОН	288@10	68.67	1	
Ru/RuO <sub>2</sub> NF	1М КОН	237.4@10	78.98	2	
D-RuO <sub>2</sub> /TiO <sub>2</sub> /TM	1М КОН	295@10	46.6	3	
$RuO_2/CeO_2$	1М КОН	350@10	74	4	
NP-RuO <sub>2</sub> -450	1М КОН	250@10	52.6	5	
CoO <sub>x</sub> -RuO <sub>2</sub> /NF	1М КОН	260@50	69.6	6	
Ru/ZnRuO <sub>2</sub>	1М КОН	221@10	57.6	7	
$Mn_{0.1}Ru_{0.9}O_2$	1М КОН	231@10	62.06	8	
Mn <sub>0.05</sub> Ru <sub>0.95</sub> O <sub>2</sub> NFs	1М КОН	236@10	56.4	9	
Mn-RuO <sub>2</sub>	1М КОН	220@10	59.7	10	
Ru@V-RuO <sub>2</sub> /C	1М КОН	201@10	44.8	11	
Ru/RuO <sub>2</sub> -2.5 h	1М КОН	253@10	80.15	12	
RuO <sub>2</sub> -Ru/MoO <sub>2</sub> /CC	1М КОН	231@10	58.3	13	
Ru-RuO <sub>2</sub> /C 250NA	1М КОН	273.42@10	/	14	
Ru/RuO <sub>2</sub> -MoO <sub>2</sub> -500	1М КОН	260@10	65	15	
Fe <sub>3</sub> O <sub>4</sub> /RuO <sub>2</sub> -C	1М КОН	268@20	55	16	
CoO <sub>x</sub> /RuO <sub>2</sub> @500	1М КОН	230@10	50	17	
IW-Co <sub>3</sub> O <sub>4</sub> -RuO <sub>2</sub> -HS	1М КОН	250@10	55.4	18	
RuO <sub>2</sub> -Co <sub>3</sub> O <sub>4</sub>	1M KOH	260@10	73	19	

**Table S1.** Comparison of OER activity of  $Ir_{SA}/RuO_2$ -850 with other reported Ru-basedOER electrocatalysts in alkaline media.

Catalysts	Electrolytes	η@j	Tafel slope	Reference
		(mV @ mA cm <sup>-2</sup> )	(mV dec⁻¹)	
Ir <sub>sa</sub> /RuO <sub>2</sub> -850	0.5 M H <sub>2</sub> SO <sub>4</sub>	195@10	47.7	This work
Pt-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	228@10	51	20
Co-doped $RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	200@10	58.2	21
$Zn$ -doped $RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	206@10	49	22
Mg-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	228@10	48.6	23
Re-doped $RuO_2$	0.1 M HClO <sub>4</sub>	190@10	45.5	24
Cu-doped $RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	188@10	43.96	25
$Cr-doped RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	178@10	58	26
Ce-doped $RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	191@10	59.1	27
Nd-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	211@10	50	28
Bi-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	200@10	59.6	29
Nb-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	207@10	50	30
La-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	208@10	57.4	31
S-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	219@10	46.1	32
S-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	231@10	39.7	33
B-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	200@10	55	34
Si-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	220@10	53	35
Se-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	190@10	43.7	36
Sr/Ir-doped RuO <sub>2</sub>	0.5 M H <sub>2</sub> SO <sub>4</sub>	190@10	39	37
$Mn/Fe-doped RuO_2$	0.5 M H <sub>2</sub> SO <sub>4</sub>	270@10	41	38
$Pt/Co-doped RuO_2$	0.1 M HClO <sub>4</sub>	213@10	48.5	39
Ni/Co-doped RuO <sub>2</sub>	0.1 M HClO <sub>4</sub>	280@10	32	40

**Table S2.** Comparison of OER activity of  $Ir_{SA}/RuO_2$ -850 with other reported  $RuO_2$ -based OER electrocatalysts in acidic media.

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