

Electronic Supplementary Information for

Thermocatalytic synthesis of 2-butanol from biomass-derived levulinic acid using carbon-doped titania supported ruthenium

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- 1) XRD pattern of (*op*)Ru@C-TiO₂ catalysts with different amount of carbon doping ((a) 1.0 wt%, (b) 2.0 wt%, (c) 3.0 wt%) after reduction with H₂ at 400 °C for 2 h (**Fig. S1**).
- 2) Pore sizes distribution calculated by using Hovartz-Kawazoe (HK) method for (*op*)Ru@C-TiO₂ sample with (a) different amount of C-doping and (b) different reduction temperature with H₂ for 2 h (**Fig. S2**).
- 3) ATR-IR spectra of (a) @TiO₂, (b) @C-TiO₂ (2.0 wt%), and (c) (*op*)Ru@C-TiO₂ (2.0 wt%) catalysts after drying in room temperature (**Fig. S3**).
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- 5) TEM analysis of (*op*)Ru@C-TiO₂ (2.0 wt%) catalysts after reduction with H₂ at (a) 300 °C, (b) 400 °C and (c) 500 °C for 2 h, and (d) recovered (*op*)Ru@C-TiO₂ 400 °C/H₂ catalyst (**Fig. S5**).
- 6) SEM analysis of (*op*)Ru@C-TiO₂ with different amount of C-doping (a) 1.0 wt%; (b) 2.0 wt%) and (c) 3.0 wt%, and (d) typical EDS spectra of (*op*)Ru@C-TiO₂ (1.0 wt%) catalysts after reduction with H₂ at 400 °C for 2 h (**Fig. S6**).
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- 15) The catalytic conversion of LA to GVL over Ru-based catalysts (**Table S2**).
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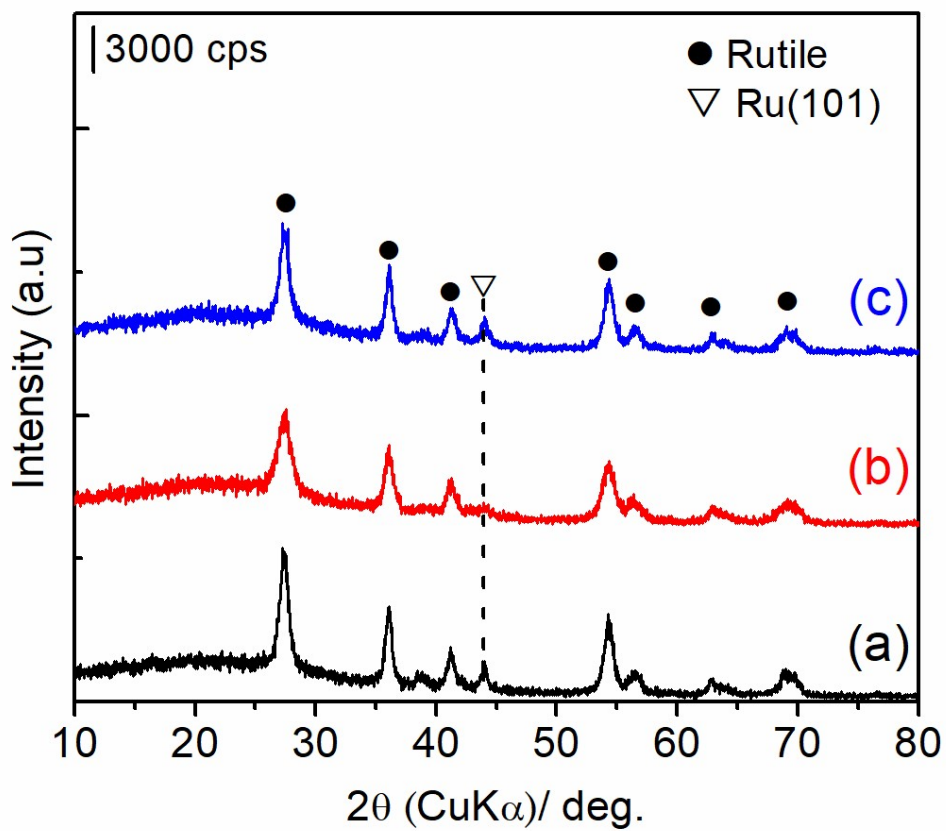


Fig. S1 XRD pattern of (*op*)Ru@C-TiO₂ catalysts with different amount of carbon doping ((a) 1.0 wt%, (b) 2.0 wt%, (c) 3.0 wt%) after reduction with H₂ at 400 °C for 2 h.

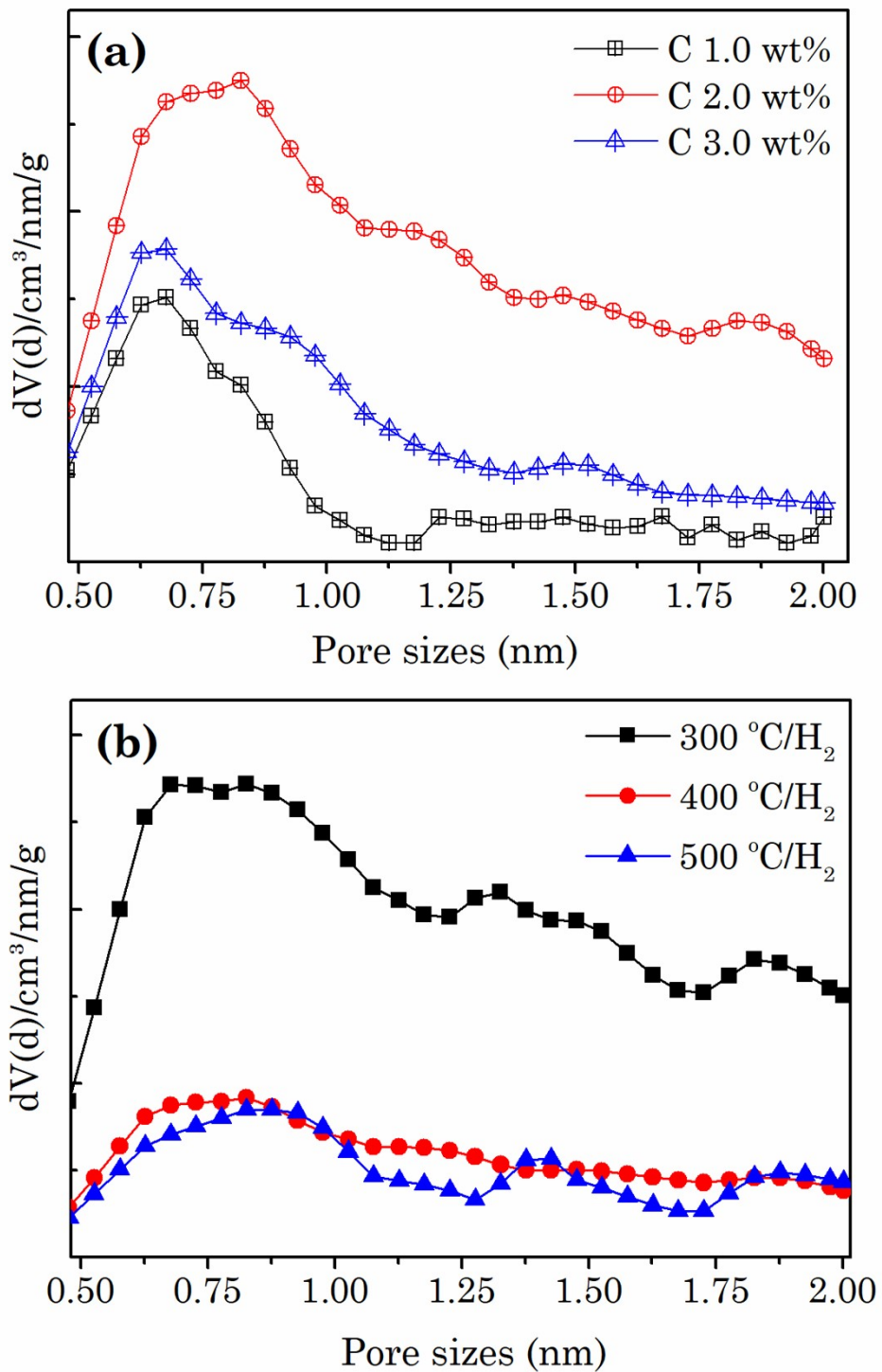


Fig. S2 Pore sizes distribution calculated by using Hovartz-Kawazoe (HK) method for $(op)Ru@C-TiO_2$ sample with (a) different amount of C-doping and (b) different reduction temperature with H_2 for 2 h.

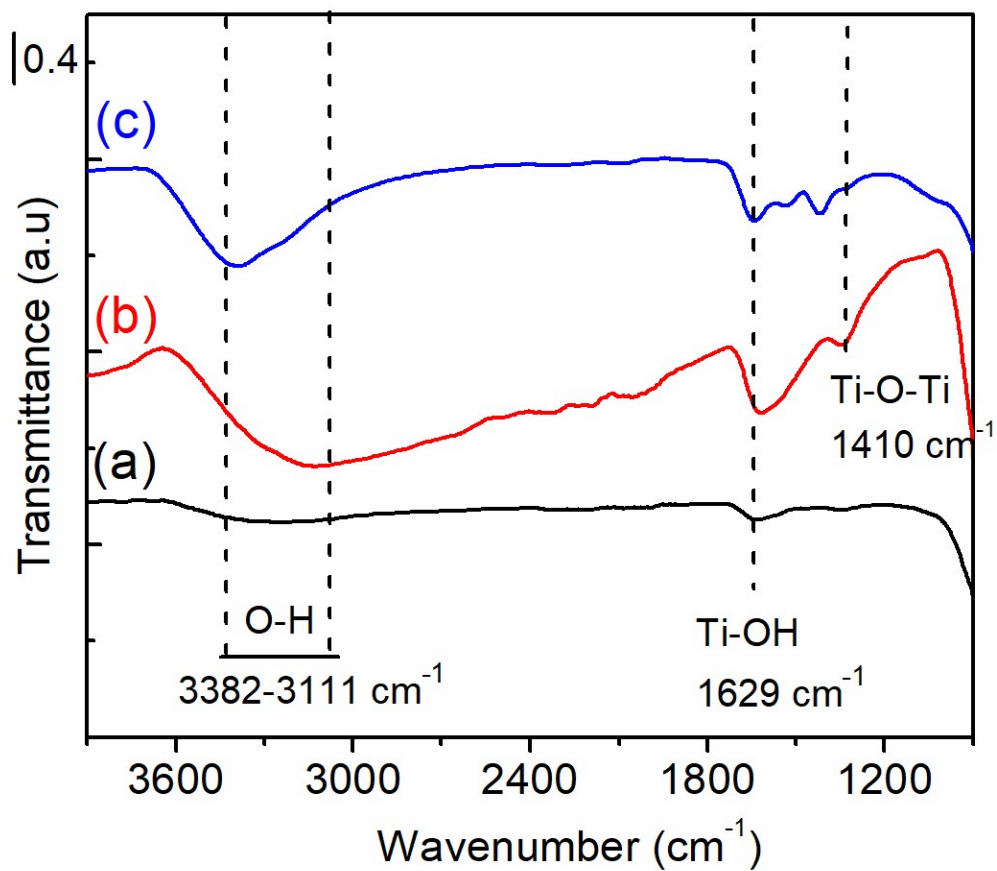


Fig. S3 ATR-IR spectra of (a) @TiO₂, (b) @C-TiO₂ (2.0 wt%), and (c) (*op*)Ru@C-TiO₂ (2.0 wt%) catalysts after drying at room temperature.

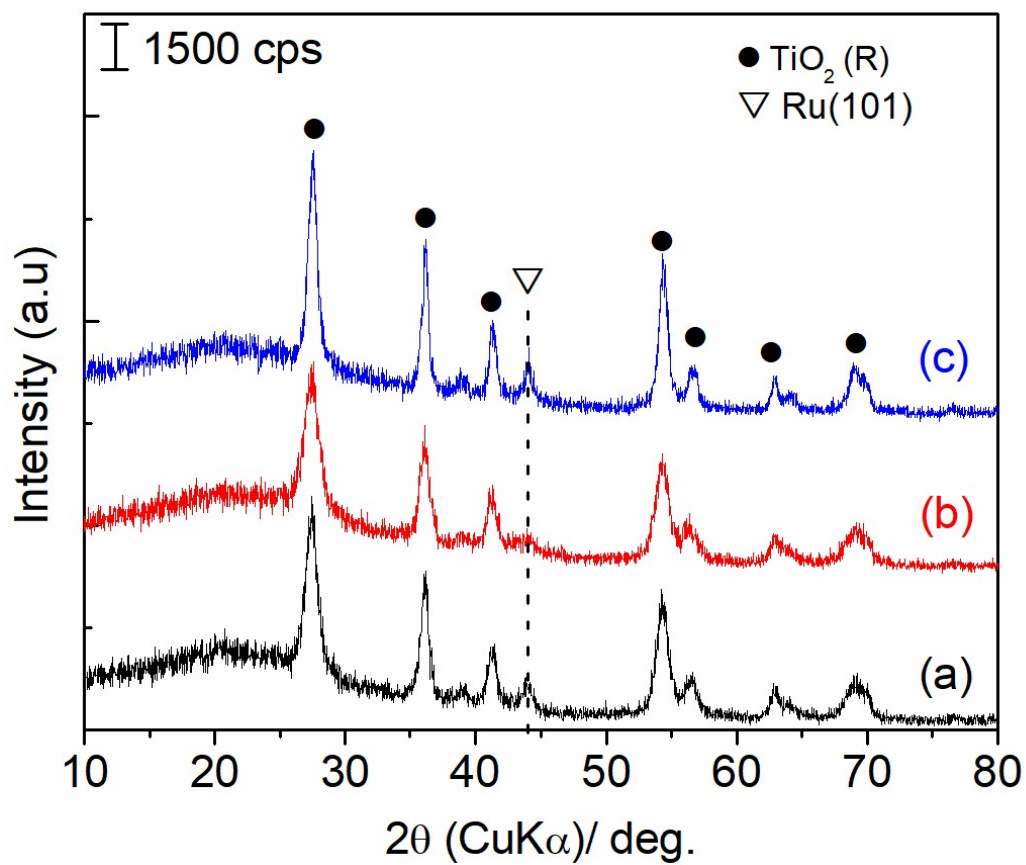


Fig. S4 XRD patterns of (op)Ru@C-TiO₂ (C = 2.0 wt%) after reduction with H₂ at different temperatures of (a) 300 °C, (b) 400 °C, and (c) 500 °C for 2 h.

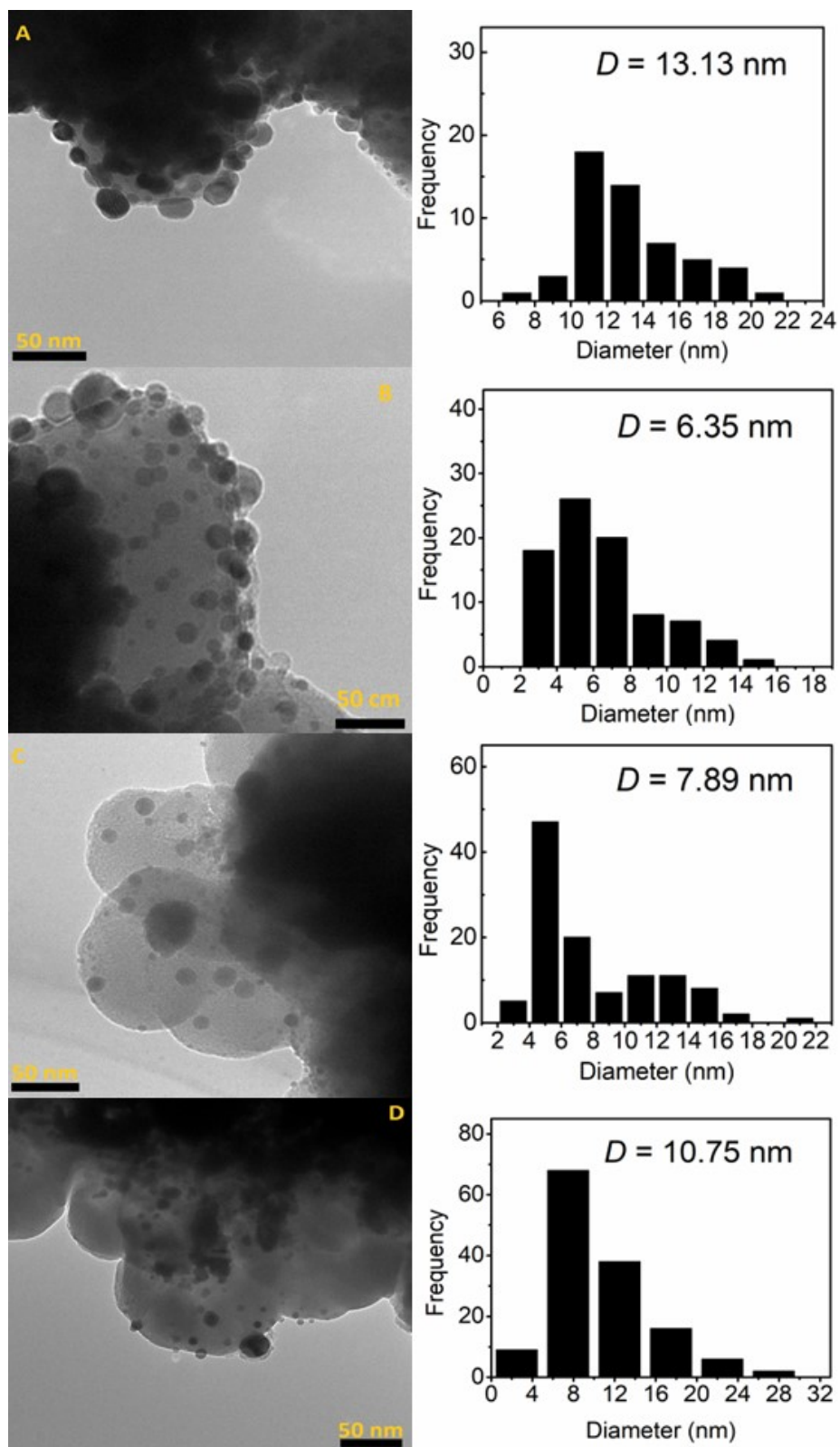


Fig. S5 TEM analysis of $(op)Ru@C-TiO_2$ (2.0 wt%) catalysts after reduction with H_2 at (a) 300 °C, (b) 400 °C and (c) 500 °C for 2 h, and (d) recovered $(op)Ru@C-TiO_2$ 400 °C/ H_2 catalyst.

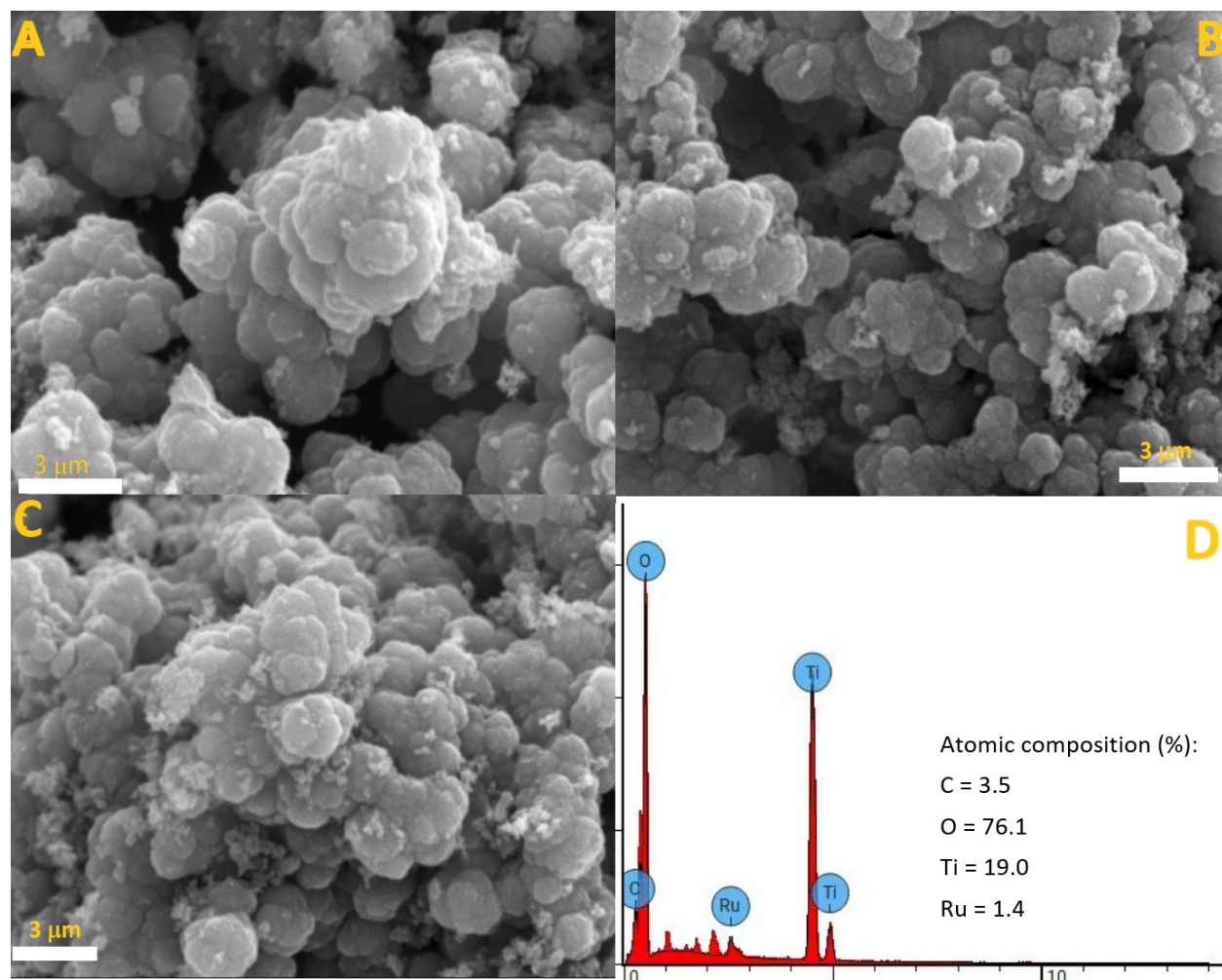


Fig. S6 SEM analysis of $(op)Ru@C-TiO_2$ with different amount of C-doping (a) 1.0 wt%; (b) 2.0 wt%) and (c) 3.0 wt%, and (d) typical EDS spectra of $(op)Ru@C-TiO_2$ (1.0 wt%) catalysts after reduction with H_2 at 400 °C for 2 h.

Table S1 Overall carbon content and bulk composition (%) of synthesised Ru@C-TiO₂ catalyst

Entry	Sample	Ru ^a (wt%)	Ti ^a (wt%)	C ^b (wt%)
1	(<i>op</i>)Ru@C-TiO ₂ (1.0 wt%)	4.91	53.12	0.29
2	(<i>op</i>)Ru@C-TiO ₂ (2.0 wt%)	4.92	50.23	1.05
3	(<i>op</i>)Ru@C-TiO ₂ (3.0 wt%)	4.89	51.72	1.72
4	(<i>cop</i>)Ru@C-TiO ₂	4.54	57.21	1.17

^aThe bulk composition (%) was determined by using inductively coupled plasma atomic emission spectroscopy (ICP-AES). ^bOverall carbon contents were obtained by performing an elemental analysis.

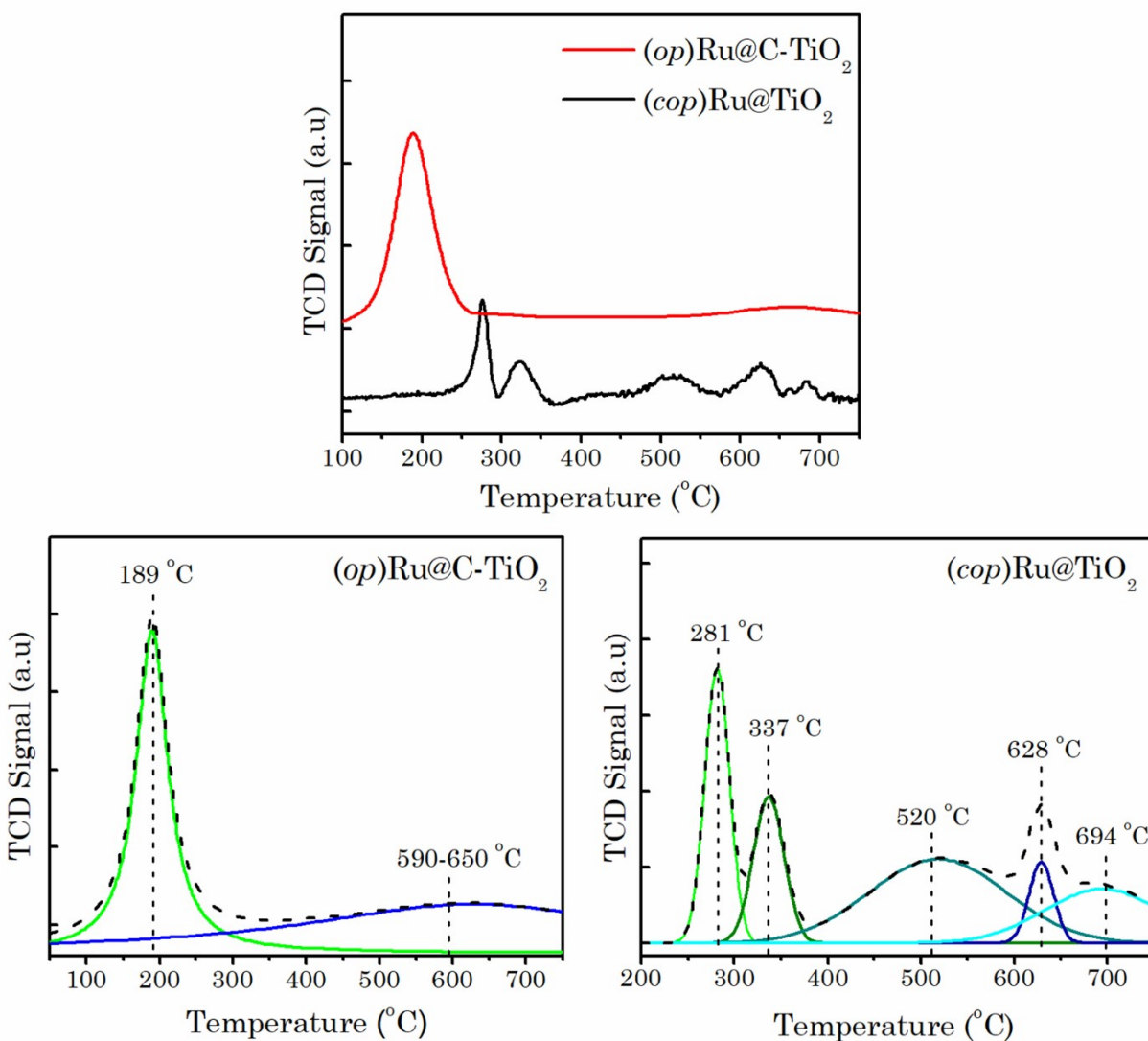


Fig. S7 The H₂-TPR profiles of Ru@TiO₂ and (*op*)Ru@C-TiO₂ (2.0 wt%) catalysts and their deconvoluted spectra.

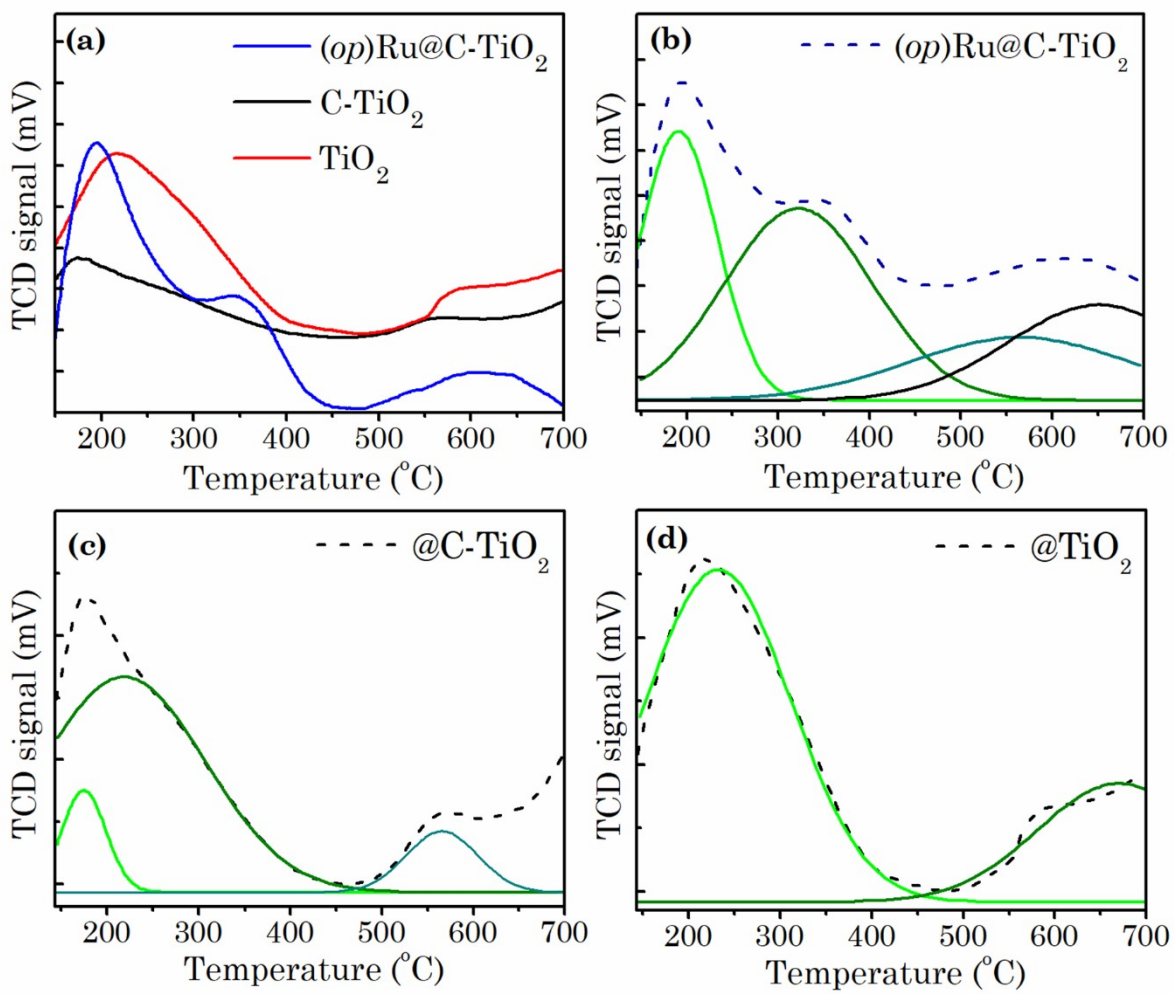


Fig. S8 NH₃-TPD spectra of @TiO₂, @C-TiO₂ supports and (*op*)Ru@C-TiO₂ (2.0 wt%) catalysts and their deconvoluted spectra.

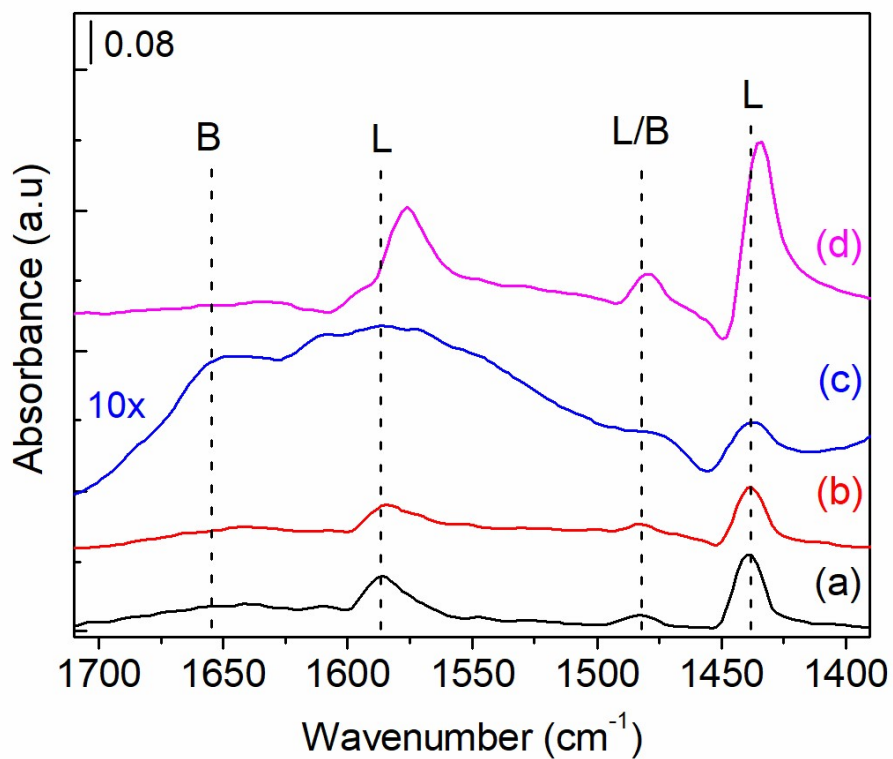


Fig. S9 ATR-IR spectra of adsorbed pyridine on the surface of (a) (*cop*)Ru@TiO₂ (*op*)Ru@C-TiO₂ (1.0 wt%), (c) (*op*)Ru@C-TiO₂ (2.0 wt%), and (d) (*op*)Ru@C-TiO₂ (3.0 wt%) catalysts.

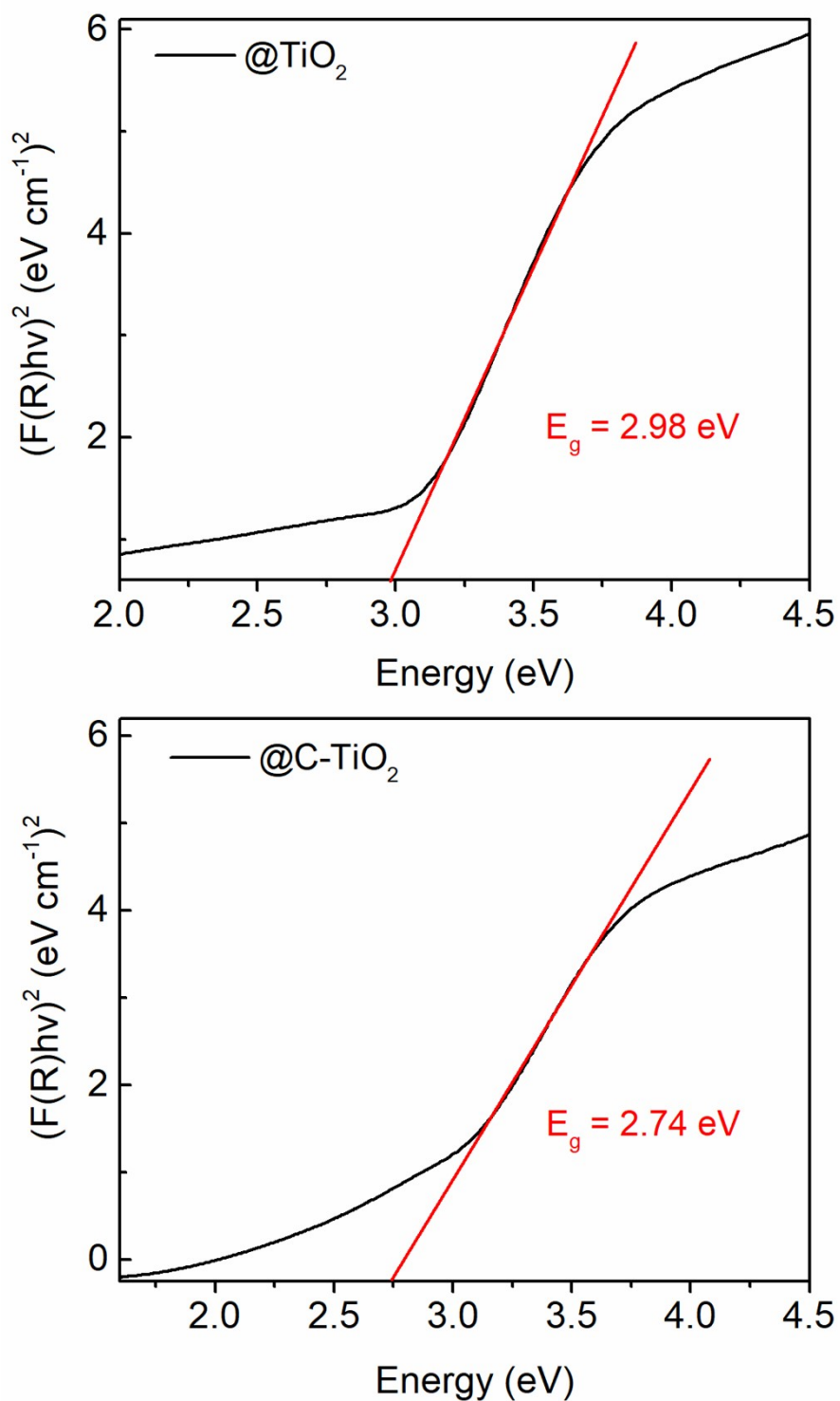


Fig S10. The Kubelka-Munk profiles of (a) @TiO₂ and (b) @C-TiO₂ powders derived from UV-Vis DRS spectra.

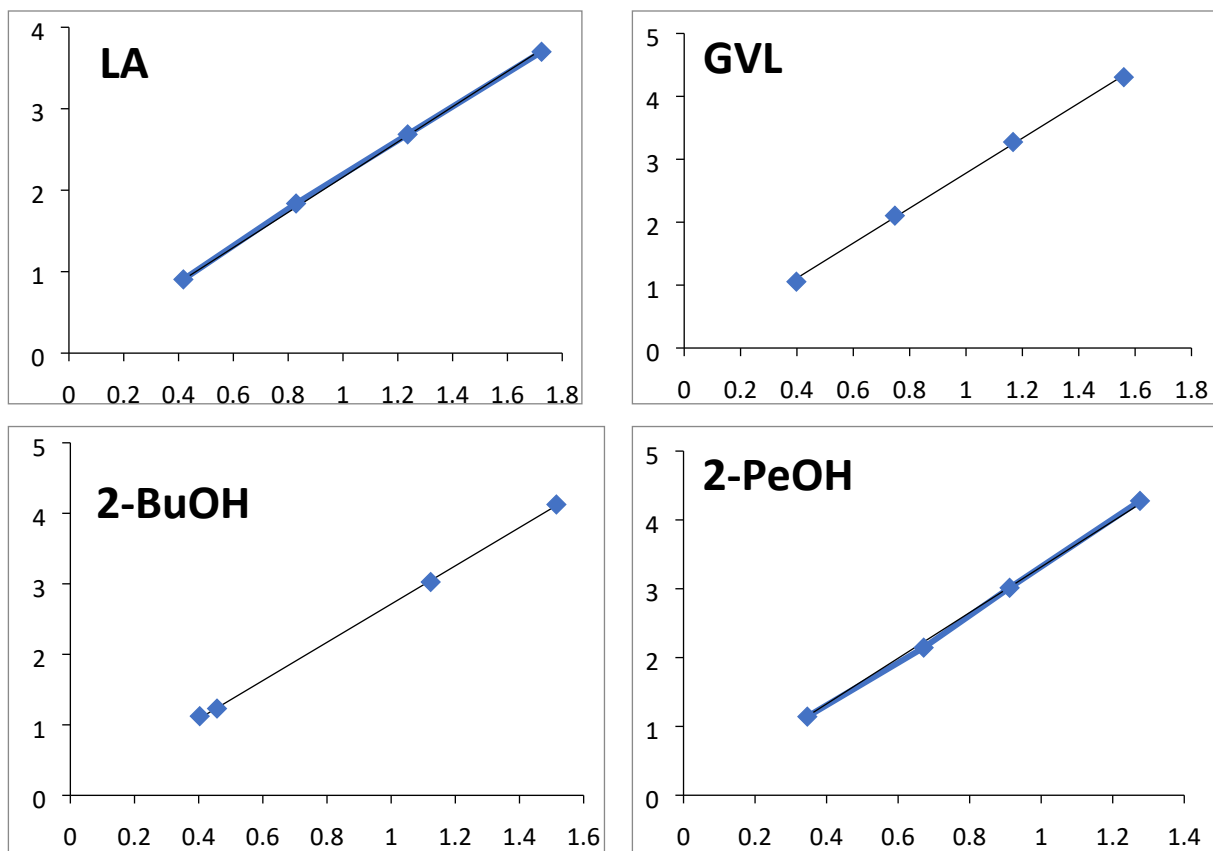


Fig. S12 Calibration curves of reactant (LA) and products (GVL, 2-BuOH, and 2-PeOH) to obtain their response factors.

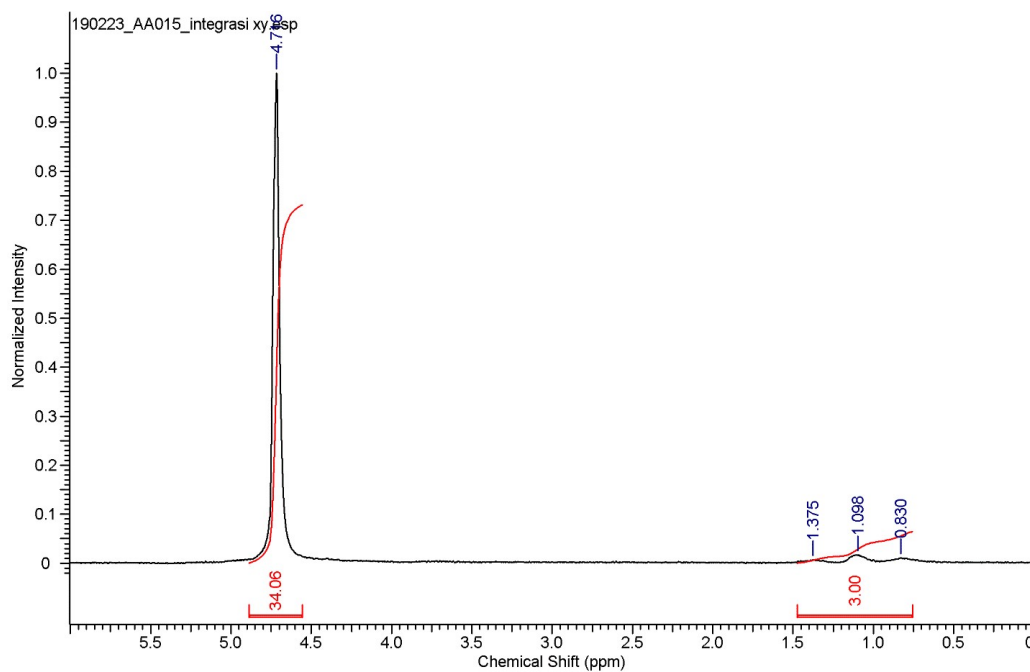


Fig. S13 ¹H-NMR spectra of reaction mixture obtained from LA reaction to 2-BuOH in D₂O solvent using (*op*)Ru@C-TiO₂ (2.0 wt%) catalyst at 200 °C, H₂ 30 bar after 3 h.

Table S2 Results of LA catalytic conversion over various supported Ru-based catalysts

Entry	Catalyst	Conv. ^a (%)	Yield ^a (%)				
			2-BuOH	2-PeOH	1,4-PeD	GVL	Others ^b
1	(<i>op</i>)Ni@C-TiO ₂	100	2	0	6	85	8
2	(<i>op</i>)Cu@C-TiO ₂	41	0	0	4	31	6
3	(<i>op</i>)Co@C-TiO ₂	34	4	0	26	4	0
4	Ru/ZrO ₂	97	11	0	10	74	2
5	Ru/γ-Al ₂ O ₃	100	25	0	5	36	27
6	Ru/Al ₂ O ₃ -500	100	32	0	1	58	15
7	Ru-Sn/γ-Al ₂ O ₃	100	0	0	0	98	2
8	Ru-Sn/C	100	1	0	31	63	5
9	Ru-Ni/C	100	1	0	0	88	11
10	Ru-MoOx/C	100	2	0	0	83	15
11	Ru-MoOx/TiO ₂	86	2	0	0	78	6
12	Ru-MoOx/SiO ₂	100	1	0	0	95	4
13	@C-TiO ₂	30	0	0	0	0	30
14	@TiO ₂	23	0	0	0	0	23

Reaction conditions: catalyst (50 mg), LA (2 mmol), H₂O (3 mL), 200 °C, 30 bar H₂, 3 h. ^aConversion of LA and Yield of products were determined by GC using an internal standard technique. ^bOthers (include 2-methyltetrahydrofuran (2-MeTHF) and 1-Pentanol (1-PeOH)) were determined by GC using total area to the LA conversion. 2-BuOH = 2-Butanol. 2-PeOH = 2-Pentanol. 1,4-PeD = 1,4-Pentenediol. GVL = γ-Valerolactone.

Table S3. Effect of catalyst dosage on the conversion of LA to 2-BuOH.

Entry	Catalyst dosage (g)	LA/Ru (molar ratio) ^a	Conv. ^b (%)	Yield ^b (%)				
				2-BuOH	2-PeOH	1,4-PeD	GVL	Others ^c
1	0.0522	75	100	87	11	0	2	0
2	0.0251	159	100	37	11	0	40	12
3	0.0126	324	100	2	0	0	93	5

Reaction conditions: catalyst = (*op*)Ru@C-TiO₂ (2.0 wt%) 400 °C/H₂, LA (2 mmol), solvent (3 mL), 200 °C, 30 bar H₂, 3 h. ^aThe molar ratio of reactant to catalyst was estimated based on the rough amount of Ru precursor in the (*op*)Ru@C-TiO₂. ^bConversion of LA and yield of products were determined by GC using an internal standard technique. ^cOthers (include 2-methyltetrahydrofuran (2-MeTHF) and 1-Pentanol (1-PeOH)) were determined by GC using total area to the LA conversion. 2-BuOH = 2-Butanol. 2-PeOH = 2-Pentanol. 1,4-PeD = 1,4-Pentenediol. GVL = γ-Valerolactone.