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## Supporting Information

### Alkali-promoted indium oxide as highly active and selective catalyst for the photo-thermal CO<sub>2</sub> hydrogenation

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#### 1. Catalyst Characterization

Powder X-ray diffraction (PXRD) analysis was conducted employing a Bruker D8 diffractometer configured in the Bragg-Brentano geometry. Cu K $\alpha$  radiation ( $\lambda=1.5418$  Å) was utilized, with operational parameters set at 40 kV and 40 mA for voltage and current respectively. Data collection spanned the  $2\theta$  range from 10 to 80 °, with increments of 0.02 ° and a time of 7 seconds per step.

Thermogravimetric (TG) measurements were recorded in an air atmosphere employing a Mettler-Toledo thermal analyzer. The temperature was ramped at a rate of 5 °C per minute within the range of 25 °C to 800 °C, while maintaining a gas flow of 25 mL · min<sup>-1</sup>.

N<sub>2</sub> adsorption-desorption measurements were performed using a Micromeritics ASAP 2040 instrument at 77 K. Prior to the analysis, the catalysts underwent a degassing process under vacuum at 150 °C for 720 minutes.

The UV-Vis spectra were conducted by using a JASCO V-670 spectrophotometer. The diffuse reflectance spectra were obtained in a range of 300 – 1500 nm using halogen and deuterium lamps as light sources.

Raman spectroscopy was performed using a confocal Raman microscope WITec Apyron equipped with a 532 nm laser and power of 10 mW. The measurements were carried out using an objective lens with a magnification of 50x, and a grating of 1800 g/mm.

The CO<sub>2</sub> temperature-programmed desorption (CO<sub>2</sub>-TPD) analyses were analyzed using a Micromeritics AutoChem 2920 unit. Initially, 200 mg of catalyst was preheated with helium at 200 °C for 60 minutes, followed by cooling to 50 °C. Subsequently, the catalyst was exposed to a CO<sub>2</sub> flow for 60 minutes. To eliminate physically adsorbed CO<sub>2</sub>, the treated catalyst underwent helium flushing at the same temperature for 30 minutes. Following this, the catalyst was subjected to heating in a helium flow up to 800 °C, with a heating rate of 10 °C · min<sup>-1</sup>, to observe the CO<sub>2</sub>-TPD signal.

*In situ* diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) measurements were registered using the Kubelka-Munk mode on a Thermo Scientific Nicolet 6700 series Fourier transform infrared (FT-IR) spectrometer equipped with a Harrick Praying Mantis High-Temperature reaction chamber. The sample was placed into the catalyst bed and packed. Before the collection of spectra, the sample was preheated to 200 °C under a He flow of 20 mL · min<sup>-1</sup>, and the background spectra were collected with 248 scans at 4 cm<sup>-1</sup> resolution. After that, a mixture of H<sub>2</sub> and CO<sub>2</sub> (4:1) was introduced into the chamber at a flow of 20 mL · min<sup>-1</sup>. Once the reaction chamber was purged, it was pressurized to 10 bar. IR spectra were recorded with 64 scans at 4 cm<sup>-1</sup> resolution every 2 min in the temperature range from 20 °C to 350 °C (ramp rate 3 °C·min<sup>-1</sup>). To investigate the effect of illumination on both the reaction pathway and intermediates, light was introduced into the reaction chamber during the DRIFTS measurements using a white LED source (UHP-T-WCS-DI, Prizmatrix).

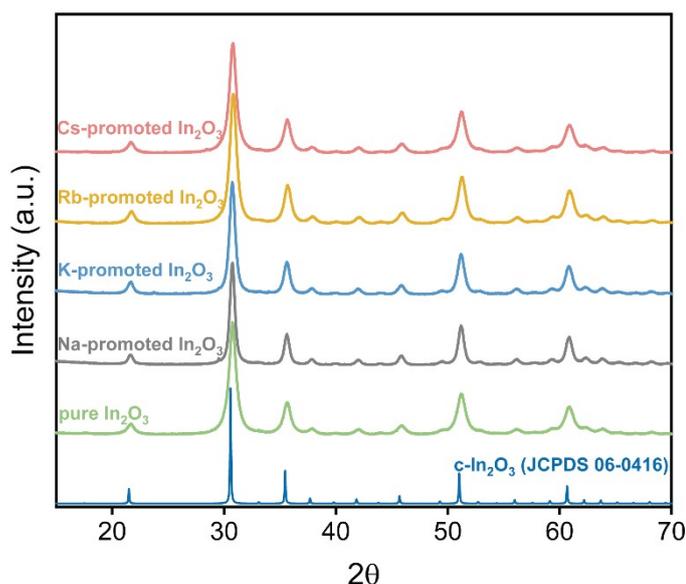
The CO<sub>2</sub> temperature-programmed desorption (CO<sub>2</sub>-TPD) analyses were performed using the same equipment as the above-mentioned *in-situ* DRIFTS experiments. Prior to collecting the background, the sample was preheated with a flow of helium at 200 °C for 30 minutes. The background spectra were collected with 248 scans at 4 cm<sup>-1</sup> resolution when sample cooled down to 50 °C. After that, the sample was exposed to a flow of CO<sub>2</sub> for 60 minutes and then flushed with helium for 30 minutes at 50 °C. Subsequently, the temperature was increased from 50 to 600 °C at a ramping rate of 5 °C·min<sup>-1</sup> under a flow of helium. During this stage, IR spectra were recorded with 64 scans at 4 cm<sup>-1</sup> resolution every 2 min. Meanwhile, the corresponding gas phase evolution was monitored via INFICON Transceptor CPM100 mass spectrometry (MS).

In the case of hydrogen temperature-programmed reduction (H<sub>2</sub>-TPR) analyses, the samples were initially pretreated at 200 °C for 30 minutes under He flow. After cooling down to room temperature, the H<sub>2</sub>-TPR measurement was performed by recording the amount of H<sub>2</sub> consumption via INFICON Transceptor CPM100 mass spectrometry (MS) while heating the catalyst from 20 °C to 600 °C at a rate of 5 °C · min<sup>-1</sup> under a gas flow of 6 vol% H<sub>2</sub>/Ar. The H<sub>2</sub>-TPR measurement was conducted both under dark and light conditions using a white LED source, as previously indicated.

X-ray photoelectron spectroscopy (XPS) measurements were performed using a Kratos Axis Ultra DLD instrument equipped with a monochromatic  $Al_{K\alpha}$  X-ray source ( $h\nu=1486.71$  eV) operating at 150 W under ultra-high vacuum ( $\approx 10^{-9}$  mbar). Photoelectron peak C1s (284.8 eV for adventitious carbon) was used for binding energy correction.

Dark-field imaging was conducted using scanning transmission electron microscopy (STEM) with a high-angle annular dark-field (HAADF) detector. The STEM-HAADF data were acquired using a convergence angle of 18.2 mrad and an inner angle of 50 mrad for HAADF. The image size was set to  $2048 \times 2048$  pixels, with a dwell time of 8  $\mu$ s. Furthermore, a combination of X-ray energy dispersive spectrometer (XEDS) and DF-STEM imaging was employed to obtain STEM-EDS spectral image datasets. The images were configured to a size of  $1024 \times 1024$  pixels, with a dwell time of 4  $\mu$ s and 100 frames. Subsequently, the generated maps of In, O and Cs underwent mild filtering using a Gaussian filter ( $\sigma = 0.5$ ) and were represented in weight percent (wt %). All STEM samples were prepared on dry copper grids coated with a lacey Carbon film (200 mesh).

## 2. Supplementary Figures



**Fig S1.** PXRD patterns of pure In<sub>2</sub>O<sub>3</sub> and alkali-promoted In<sub>2</sub>O<sub>3</sub>.

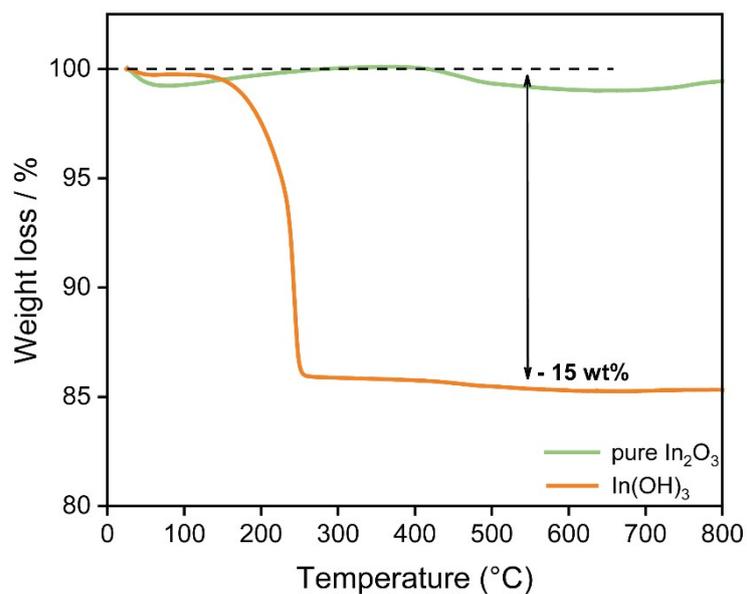


Fig S2. TGA of In(OH)<sub>3</sub> precursor and pure In<sub>2</sub>O<sub>3</sub>.

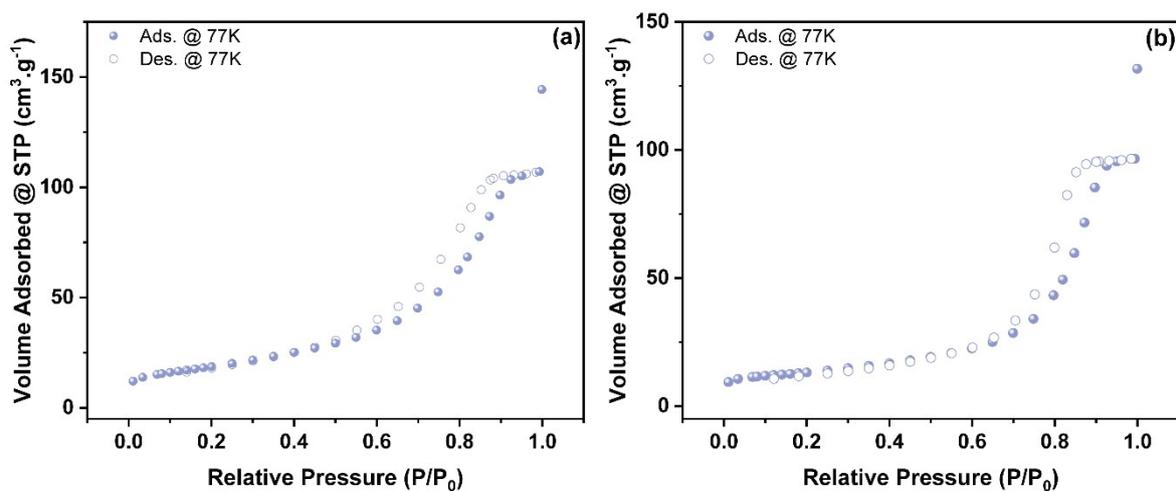
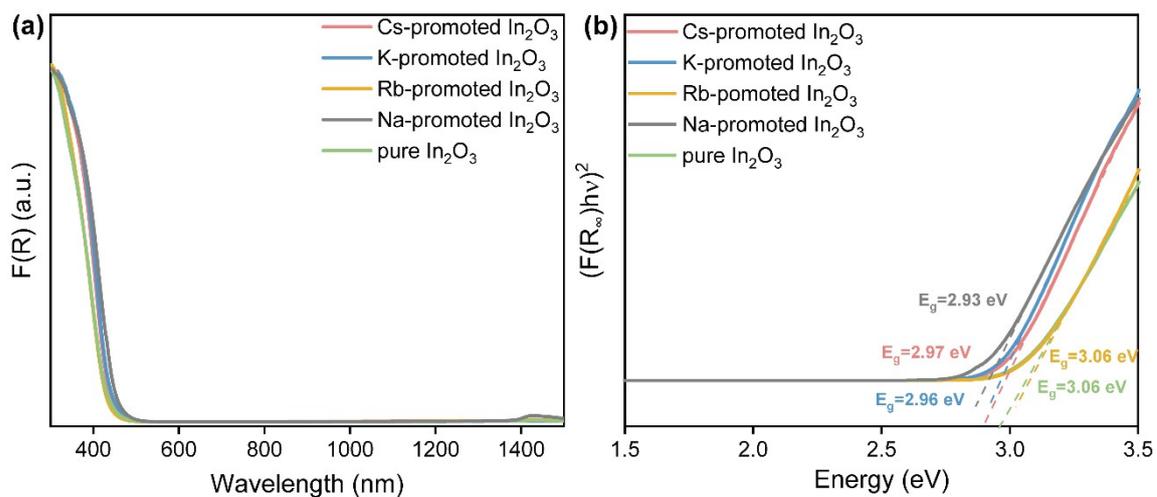


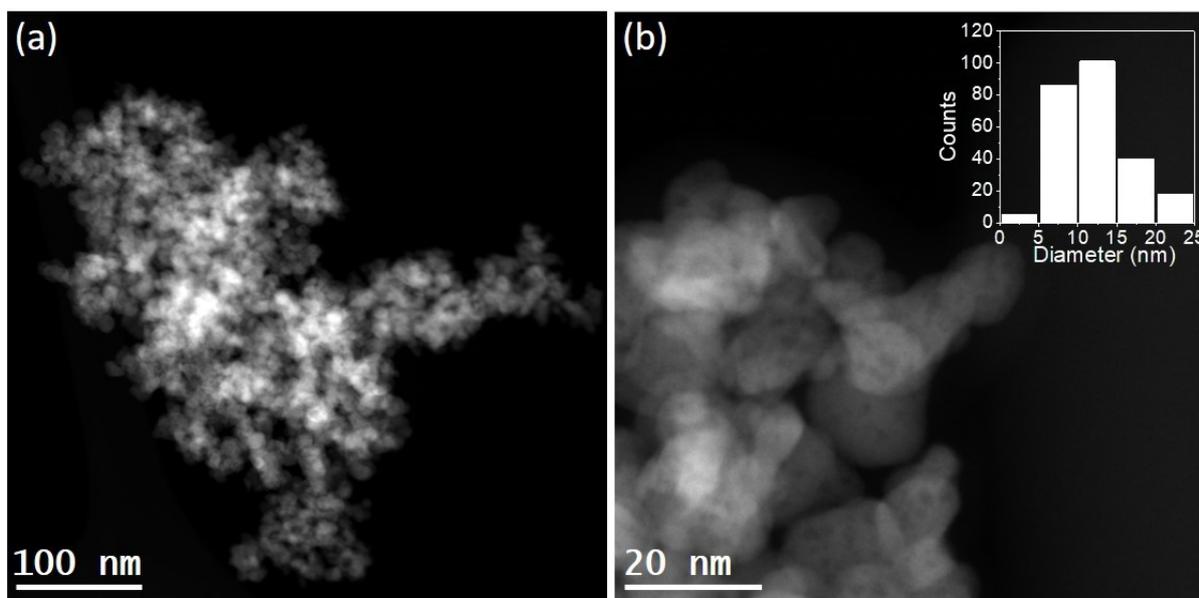
Fig S3. N<sub>2</sub> adsorption isotherms of a) pure In<sub>2</sub>O<sub>3</sub> and b) Cs-promoted In<sub>2</sub>O<sub>3</sub> at 77 K.

Table S1. Specific surface areas of pure and Cs-promoted In<sub>2</sub>O<sub>3</sub>.

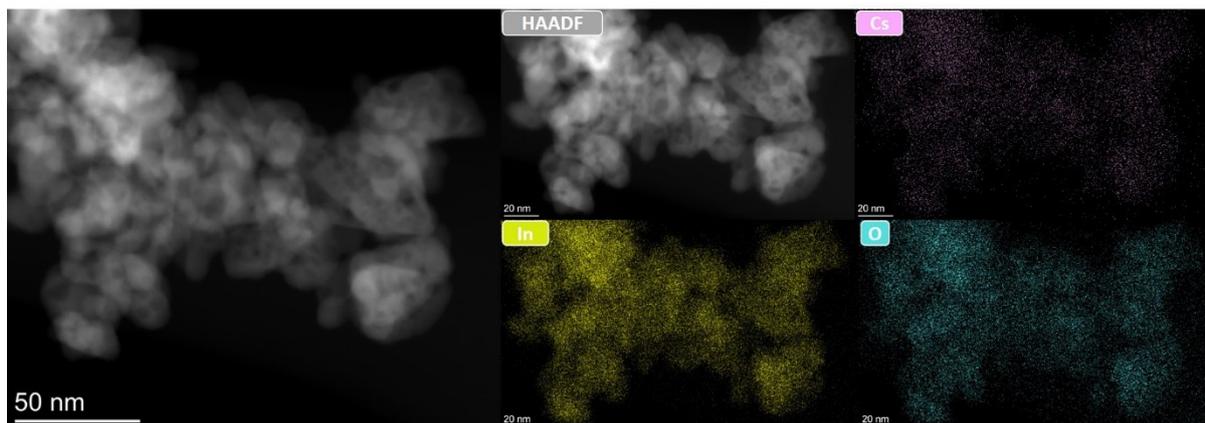
Sample	Specific surface area
Pure In <sub>2</sub> O <sub>3</sub>	67 m <sup>2</sup> g <sup>-1</sup>
Cs-promoted In <sub>2</sub> O <sub>3</sub>	44 m <sup>2</sup> g <sup>-1</sup>



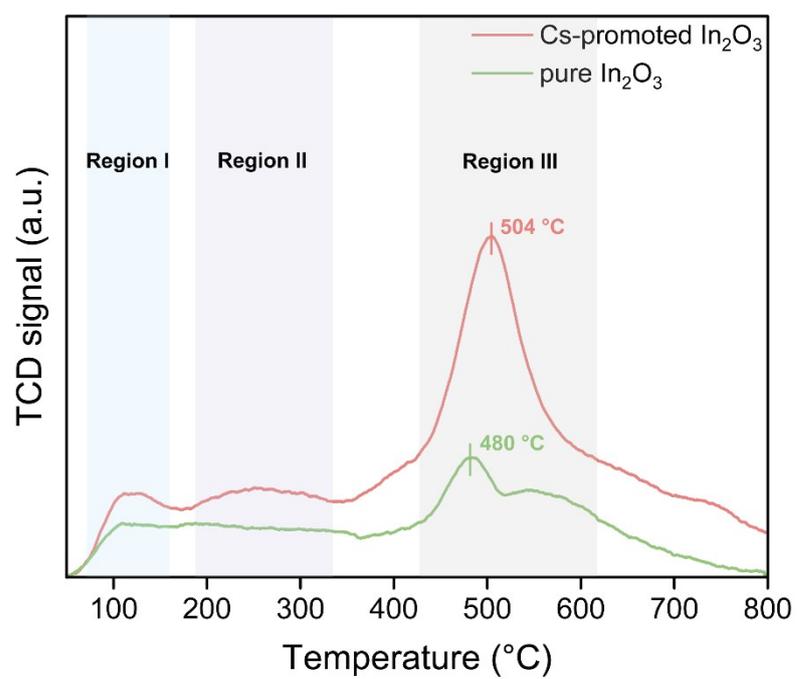
**Fig S4.** a) UV-vis-NIR absorption spectra and b) calculated band gap values of alkali-promoted and pure  $\text{In}_2\text{O}_3$ .



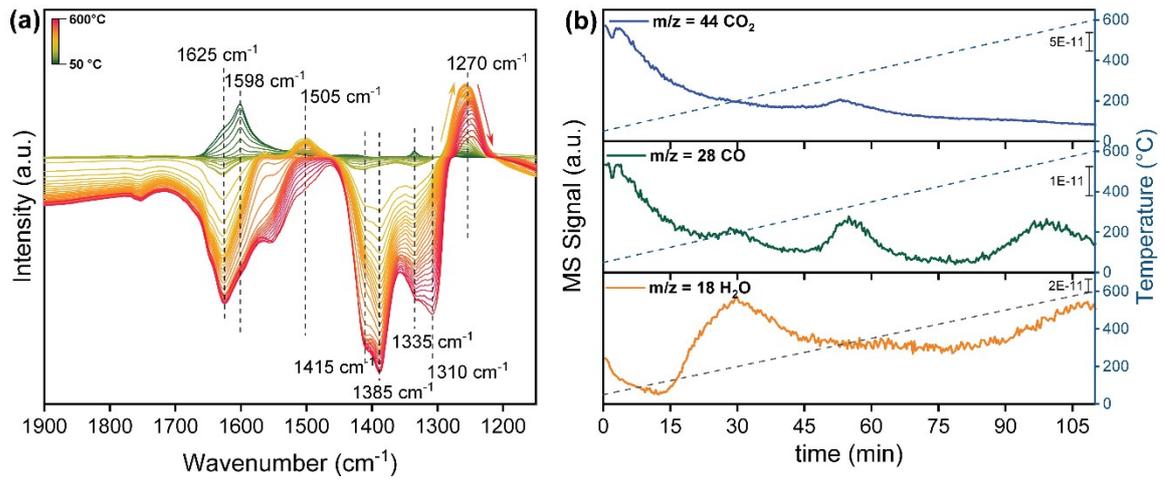
**Fig S5.** STEM images of pure  $\text{In}_2\text{O}_3$  at a) low and b) high magnification. Inset in b) corresponds to the particle size distribution.



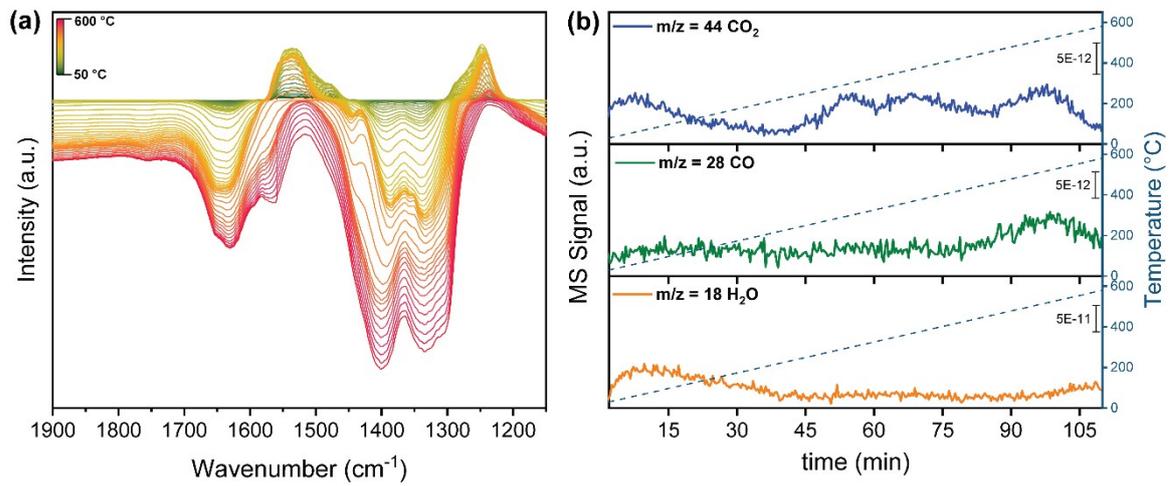
**Fig S6.** STEM images of Cs-promoted  $\text{In}_2\text{O}_3$  with elemental mapping by EDX.



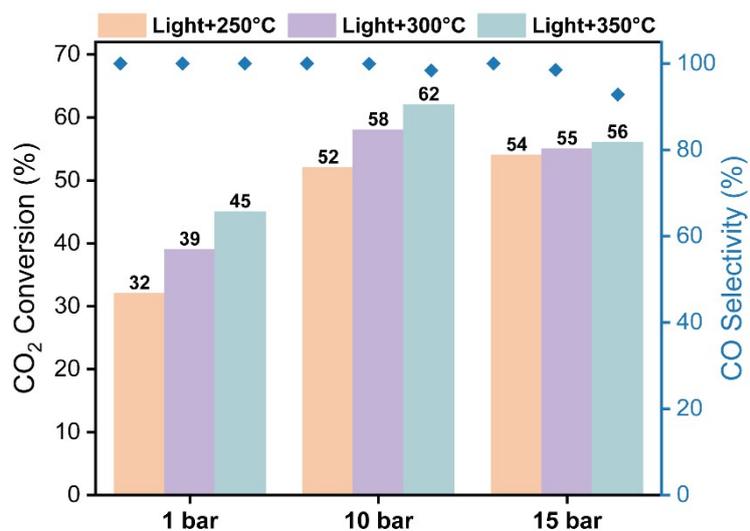
**Fig S7.**  $\text{CO}_2$ -TPD profiles of pure and Cs-promoted  $\text{In}_2\text{O}_3$ .



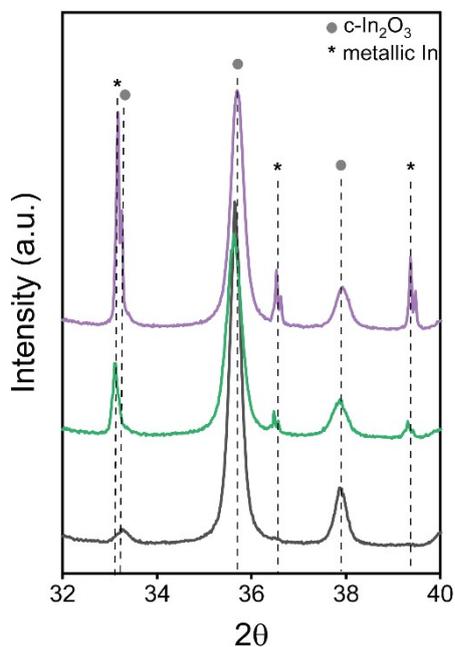
**Fig S8.** a) In-situ DRIFTS spectra of Cs-promoted  $\text{In}_2\text{O}_3$  catalyst and b) corresponding MS signal.



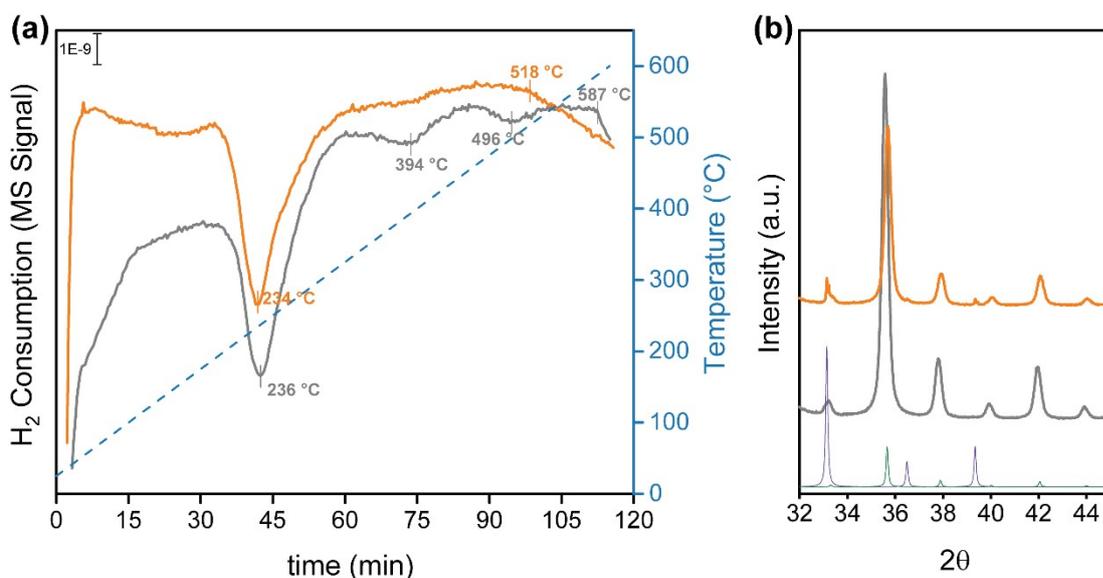
**Fig S9.** a) In-situ DRIFTS spectra of pure  $\text{In}_2\text{O}_3$  catalyst and b) corresponding MS signal.



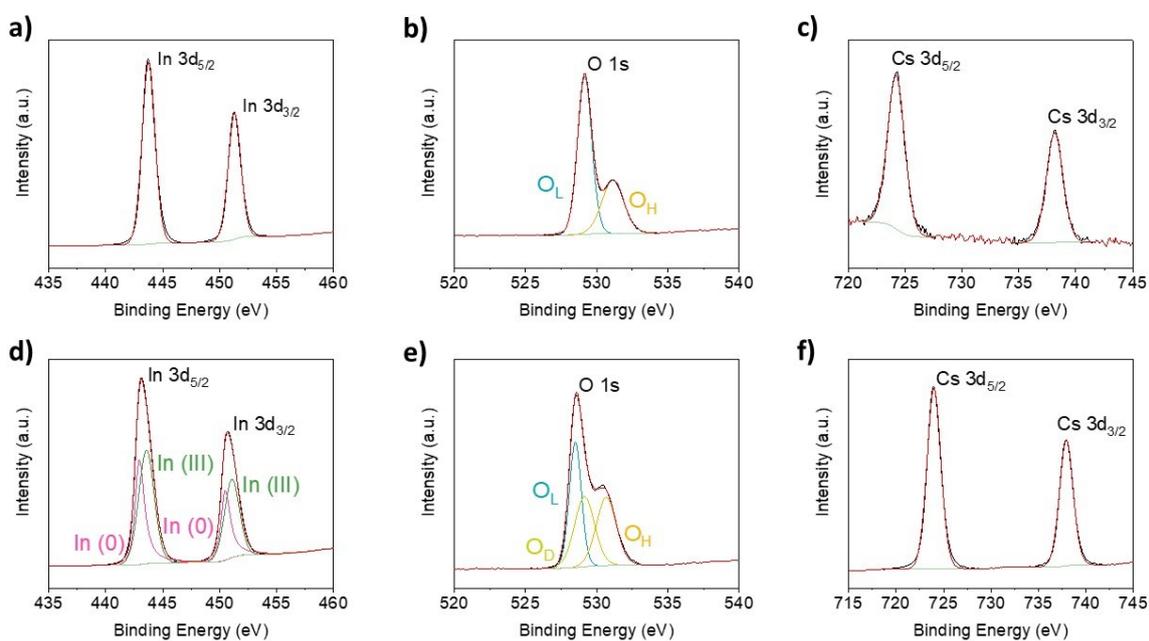
**Fig S10.** Study of the effect of pressure on the photo-thermal RWGS reaction over Cs-promoted  $\text{In}_2\text{O}_3$  with external heating at 250, 300 and 350 °C. Reaction conditions:  $3.3 \text{ W}\cdot\text{cm}^{-2}$  light intensity,  $\text{GHSV} = 15000 \text{ mL}\cdot\text{h}^{-1}\cdot\text{g}^{-1}$ .



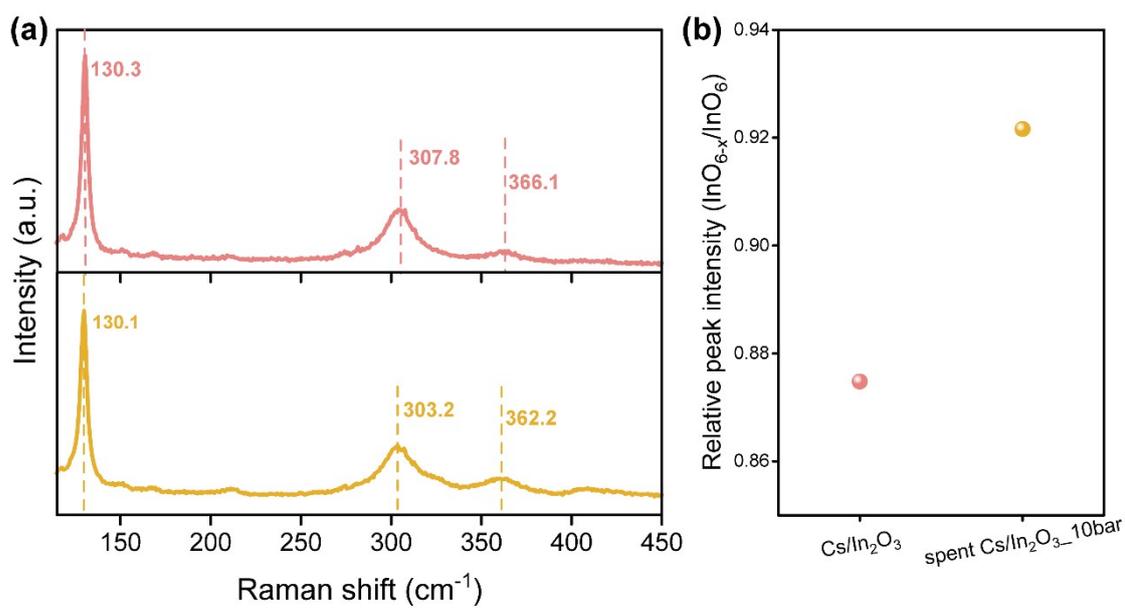
**Fig S11.** PXRD patterns of spent Cs-promoted  $\text{In}_2\text{O}_3$  samples after photo-thermal RWGS reaction at 1 (black line), 10 (green line) and 15 bar (purple line) and 350 °C.



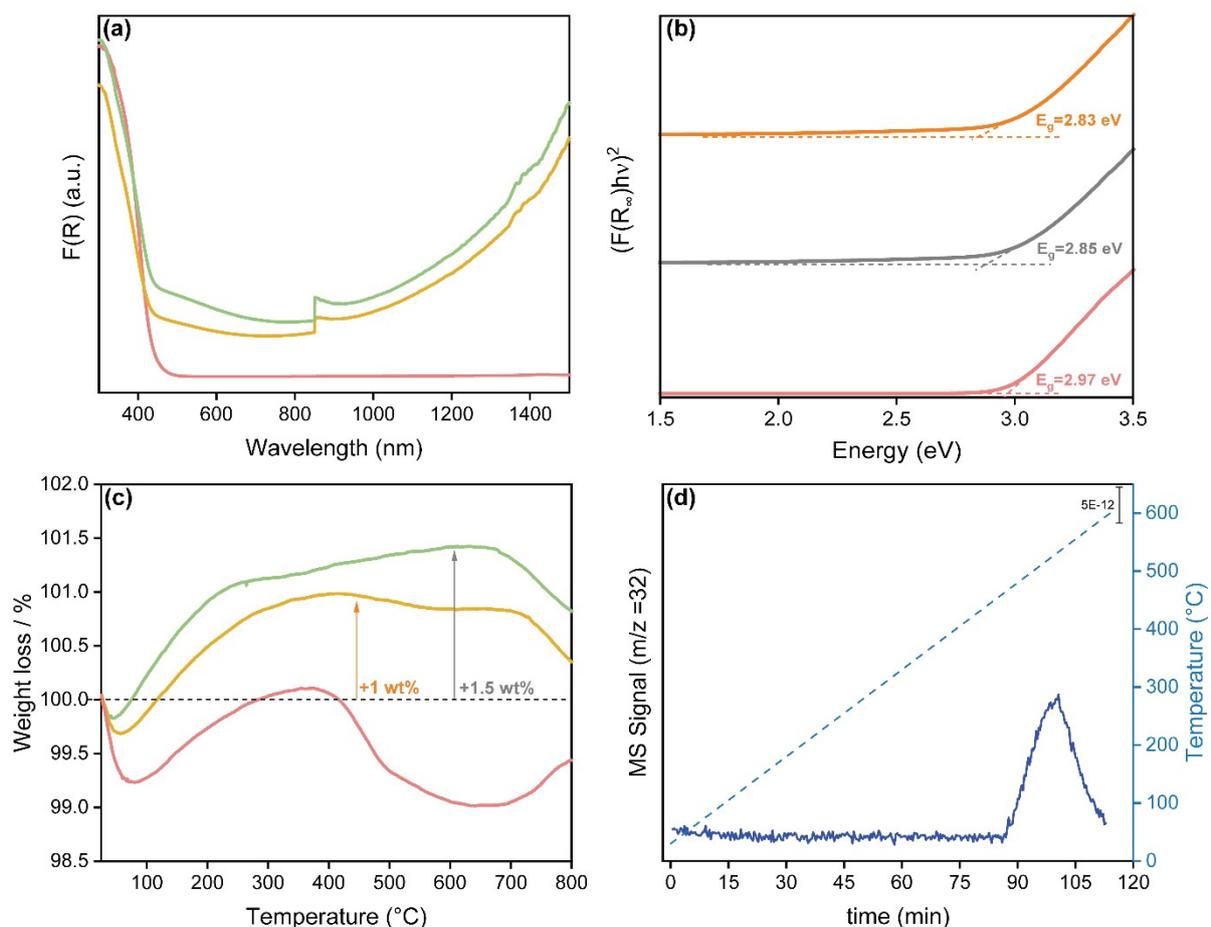
**Fig S12.** a)  $\text{H}_2$ -TPR of Cs-promoted  $\text{In}_2\text{O}_3$  under dark (grey line) and light irradiation (orange line) conditions. b) PXRD patterns of spent Cs-promoted  $\text{In}_2\text{O}_3$  samples after  $\text{H}_2$ -TPR under dark (grey line) and light irradiation (orange line) conditions. Simulated XRD patterns for c- $\text{In}_2\text{O}_3$  (green line) and metallic indium (purple line) are included for reference.



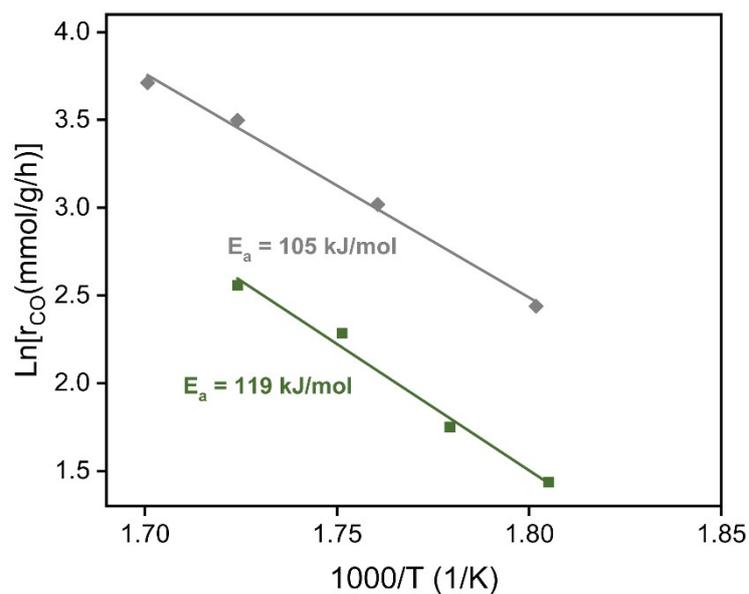
**Fig S13.** XPS measurements of fresh (top) and spent (bottom) Cs-promoted  $\text{In}_2\text{O}_3$  sample.



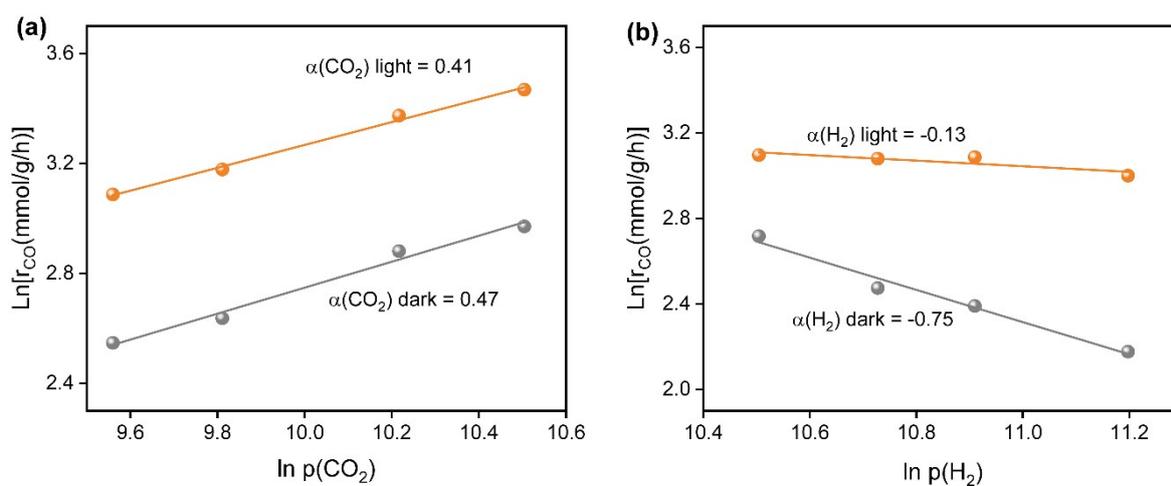
**Fig S14.** a) Raman spectra of fresh (red line) and spent (yellow line) Cs-promoted  $\text{In}_2\text{O}_3$  catalysts. b) Relative peak intensity ratio between  $\text{InO}_{6-x}$  and  $\text{InO}_6$ .



**Fig S15.** a) UV-vis-NIR absorption spectra of fresh Cs-promoted  $\text{In}_2\text{O}_3$  (red line), Cs-promoted  $\text{In}_2\text{O}_3$  after illumination w/o external heating (yellow line) and Cs-promoted  $\text{In}_2\text{O}_3$  after illumination at  $250^\circ\text{C}$  (green line). b) calculated band gap values of fresh Cs-promoted  $\text{In}_2\text{O}_3$  (red line), spent Cs-promoted  $\text{In}_2\text{O}_3$  after photothermal reaction at  $250^\circ\text{C}$  and 1 bar (grey line) and spent Cs-promoted  $\text{In}_2\text{O}_3$  after photothermal reaction at  $250^\circ\text{C}$  and 10 bar (orange line). c) TGA curves of fresh Cs-promoted  $\text{In}_2\text{O}_3$  (red line), Cs-promoted  $\text{In}_2\text{O}_3$  after illumination w/o external heating (yellow line) and Cs-promoted  $\text{In}_2\text{O}_3$  after illumination at  $250^\circ\text{C}$  (green line). d) MS results for gas phase analysis of Cs-promoted  $\text{In}_2\text{O}_3$  under light illumination.



**Fig S16.** Calculated activation energies of Cs-promoted  $\text{In}_2\text{O}_3$  under light (grey line) and dark (olive line).



**Fig S17.** Dependence of CO production rate on the partial pressures of a)  $\text{CO}_2$  and b)  $\text{H}_2$  under light irradiation (orange spheres) and dark conditions (grey spheres), over Cs-promoted  $\text{In}_2\text{O}_3$ . Reaction conditions:  $3.3 \text{ W}\cdot\text{cm}^{-2}$  light intensity,  $\text{GHSV} = 15000 \text{ mL}\cdot\text{h}^{-1}\cdot\text{g}^{-1}$ , 1 bar.

### 3. Supplementary Tables

**Table S2.** Surface temperature and the difference of CO<sub>2</sub> conversion of direct and indirect illumination over Cs-promoted In<sub>2</sub>O<sub>3</sub> catalyst

Reaction condition	Surface temperature <sup>[a]</sup> (°C)	Surface temperature <sup>[b]</sup> (°C)	Difference of CO <sub>2</sub> conversion Δ(%)
Light	233	230	84.8
Light+250°C	315	311	60.8
Light+300°C	358	353	34.4

[a]: direct illumination; [b]: indirect illumination cover Ti<sub>2</sub>O<sub>3</sub>

**Table S3.** Surface temperature of direct and indirect light illumination under different light intensities over Cs-promoted In<sub>2</sub>O<sub>3</sub> catalyst.

Light intensity (W·cm <sup>-2</sup> )	Surface temperature <sup>[a]</sup> (°C)	Surface temperature <sup>[b]</sup> (°C)
3.3	315	312
3	307	303
2.52	295	291
2.15	284	280
1.75	275	273
1.37	266	264

[a]: direct illumination; [b]: indirect illumination cover Ti<sub>2</sub>O<sub>3</sub>

**Table S4.** Performance comparison of different photocatalysts for CO<sub>2</sub> hydrogenation

Catalyst	H <sub>2</sub> : CO <sub>2</sub>	Reactor type	Light source	P	T (°C)	CO production (mmol·g <sup>-1</sup> ·h <sup>-1</sup> )	CO Selectivity	Ref.
Cs/In <sub>2</sub> O <sub>3</sub>	4 : 1	flow	300W Xe lamp	1 bar	230 <sup>[a]</sup>	<b>28</b>	100%	this work
		flow	300W Xe lamp + 250 °C	1 bar	303 <sup>[a]</sup>	<b>38</b>	100%	
		flow	300W Xe lamp + 250 °C	10 bar	298 <sup>[a]</sup>	<b>67</b>	100%	
		flow	300W Xe lamp + 300 °C	10 bar	345 <sup>[a]</sup>	<b>74</b>	100%	
Fe/Al <sub>2</sub> O <sub>3</sub>	4 : 1	batch	300W Xe lamp	-	310	20	95.96%	1
2%Ni-LaInO <sub>3</sub>	4 : 1	flow	3 W/cm <sup>2</sup>	-	-	26	100%	2
In <sub>2</sub> O <sub>3-x</sub>	1 : 1	batch	300W Xe lamp	-	340	103.21	100%	3
Bi <sub>x</sub> In <sub>2-x</sub> O <sub>3</sub>	1 : 1	batch	300W Xe lamp	30 psi	-	8	-	4
In <sub>2</sub> O <sub>3-x</sub> (OH) <sub>y</sub> /Nb <sub>2</sub> O <sub>5</sub>	1 : 1	batch	300W Xe lamp	27 psi	-	1.4	100%	5

In <sub>2</sub> O <sub>3-x</sub> /In <sub>2</sub> O <sub>3</sub>	1 : 1	batch	300W Xe lamp	30 psi	-	23.88	100%	6
	1 : 1	flow		1 bar	300	0.16 mmol·m <sup>-2</sup> ·h <sup>-1</sup>	100%	
In <sub>2</sub> O <sub>3-x</sub> (OH) <sub>y</sub> /SiNW	1 : 1	batch	300W Xe lamp	2 atm	150	0.022	100%	7

[a]Surface temperature

## Reference

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