

**Supporting Information for**

# Efficient Electrosynthesis of Hydrogen Peroxide in Neutral Media using Boron and Nitrogen Doped Carbon Catalysts

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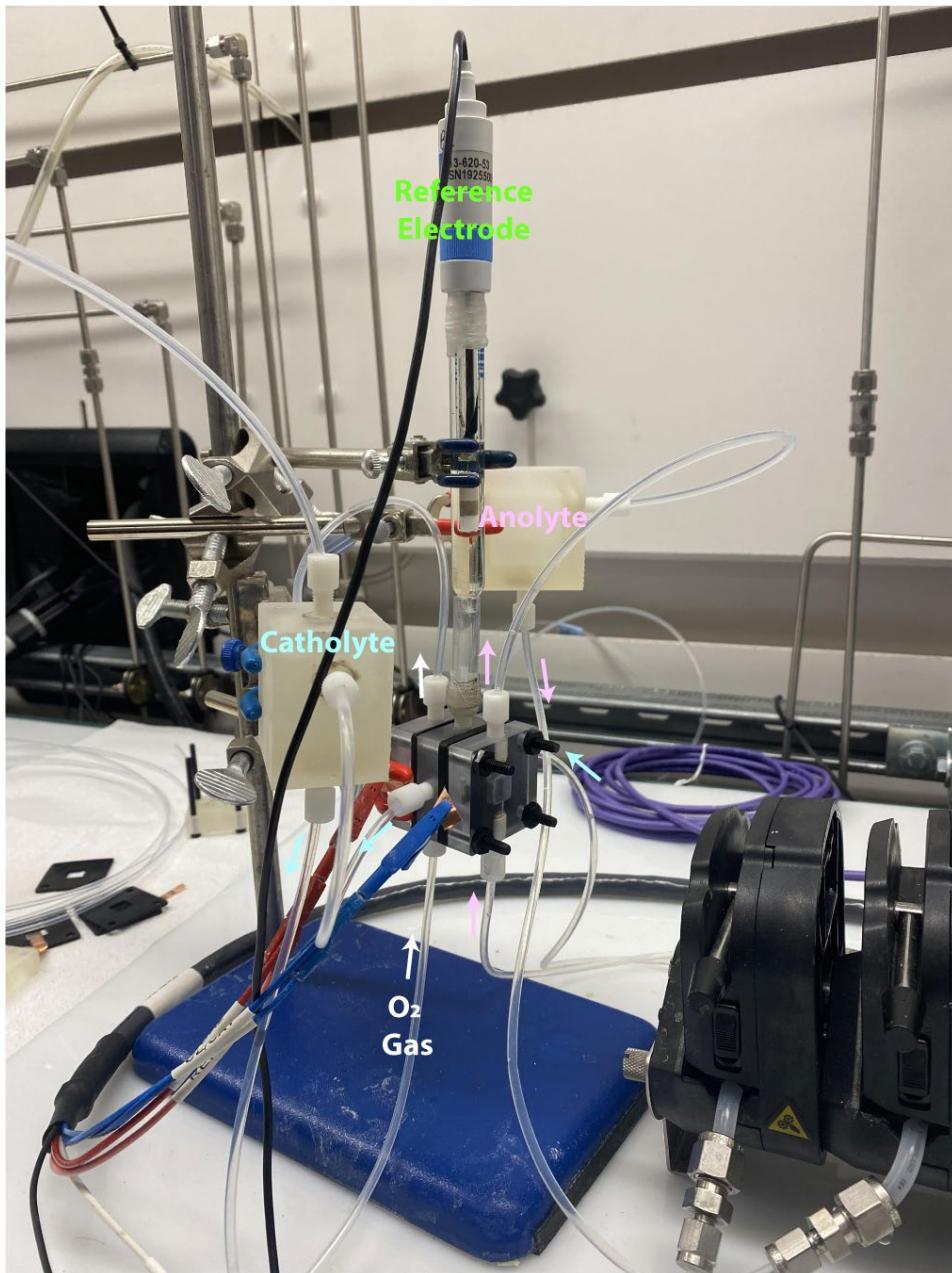
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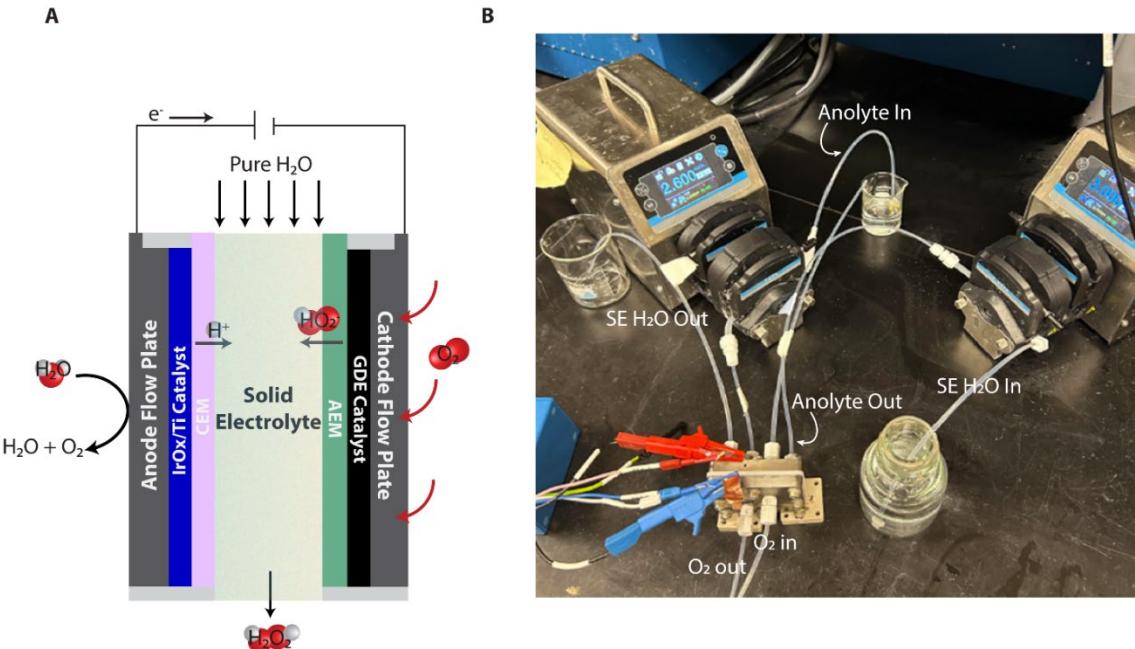
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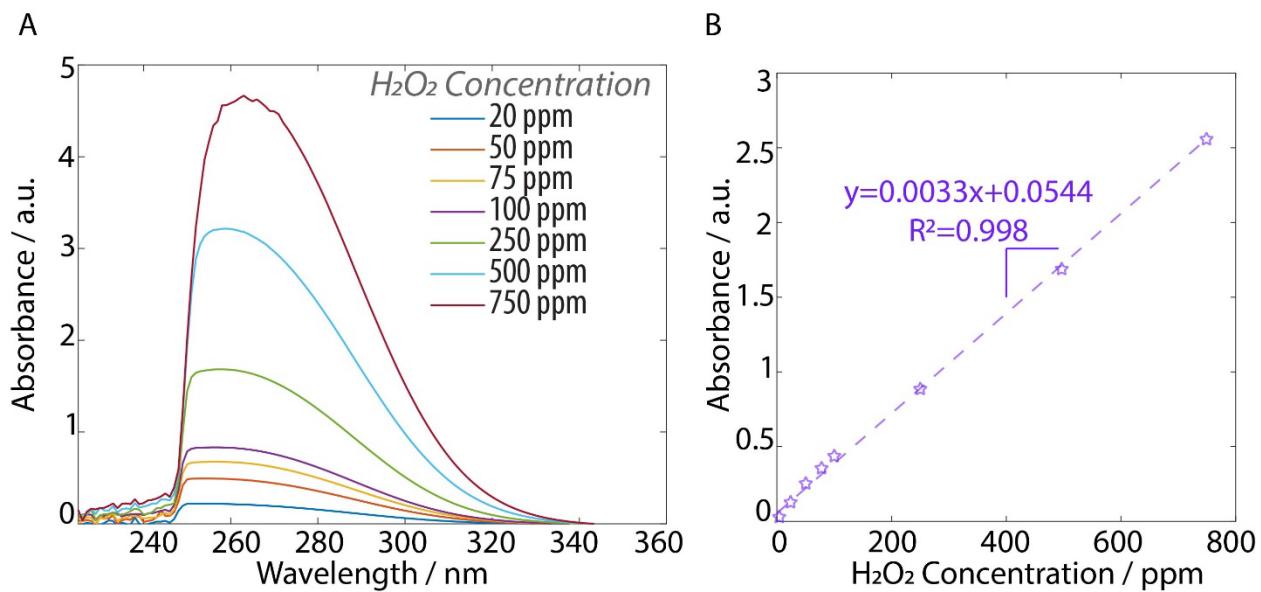
## Section S1. Methods and Reactor Designs



**Figure S1.** Demonstration of three-electrode gas diffusion electrode (GDE) electrochemical flow cell set-up.



**Figure S2.** A) Schematic and B) set-up demonstration of  $H_2O_2$  electrosynthesis in a two-electrode dual membrane electrode assembly (MEA) solid electrolyte flow cell. Note schematic not drawn to scale.

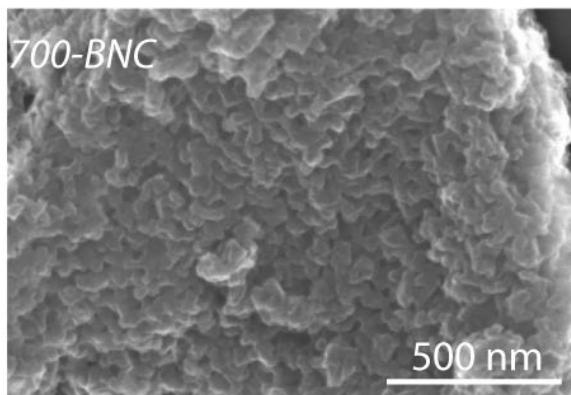


**Figure S3.** H<sub>2</sub>O<sub>2</sub> quantification. A) UV-vis spectra of Co/CO<sub>3</sub> assay with various concentrations of H<sub>2</sub>O<sub>2</sub> (ppm) and B) its corresponding calibration curve.

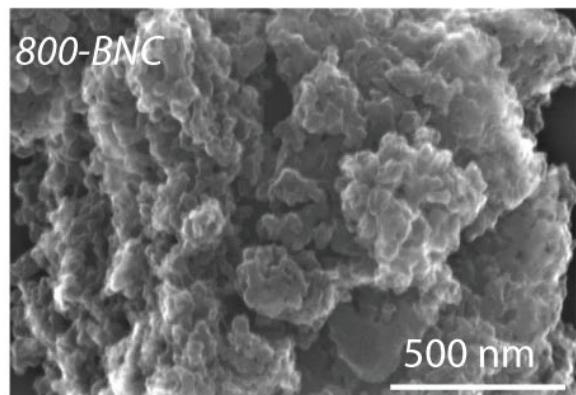
The produced H<sub>2</sub>O<sub>2</sub> was quantified using a cobalt-carbonate (Co/CO<sub>3</sub>) assay coupled with UV-vis spectrophotometry.<sup>1</sup> The Co/CO<sub>3</sub> assay contains a mixture of KHCO<sub>3</sub> and cobalt sulfate heptahydrate (CoSO<sub>4</sub>·7H<sub>2</sub>O) both of which dissociate in water and exhibit a light pink color solution. H<sub>2</sub>O<sub>2</sub> oxidizes Co<sup>2+</sup> in the presence of bicarbonate likely forming a ‘carbonatocobaltate’ complex (Co(CO<sub>3</sub>)<sub>3</sub><sup>3-</sup>) which strongly absorbs at 290 nm and weakly in the visible region (440 and 635 nm), exhibiting a dark green color. The 290 nm feature was used for quantification unless otherwise specified. The absorbance of the Co(CO<sub>3</sub>)<sub>3</sub><sup>3-</sup> complex is measured which is linearly proportional to the concentration of H<sub>2</sub>O<sub>2</sub> present. The Co/CO<sub>3</sub> assay was prepared by first mixing 1.35 mL of 2 M KHCO<sub>3</sub> and 35.8  $\mu$ L of 2 mM CoSO<sub>4</sub>·7H<sub>2</sub>O in a cuvette. Next, 35.8  $\mu$ L of our H<sub>2</sub>O<sub>2</sub> sample (known or unknown concentration) was added to the cuvette and mixed. Immediately afterward, 1.425 mL of 2 M KHCO<sub>3</sub> was added to the cuvette and mixed. The absorbance of these samples was measured in the wavelength range 200-800 nm with 1 nm resolution and scanning rate of 2 nm/s (Agilent Cary 6000i). The UV-vis spectra were background-subtracted using a baseline measurement of the same analyte solutions with 35.8  $\mu$ L of H<sub>2</sub>O added instead of H<sub>2</sub>O<sub>2</sub> containing samples. A typical calibration curve was plotted by linear fitting the absorbance values at wavelength of 290 nm for various known concentrations of H<sub>2</sub>O<sub>2</sub> from 20 ppm to 750 ppm.

## Section S2. Material Characterization

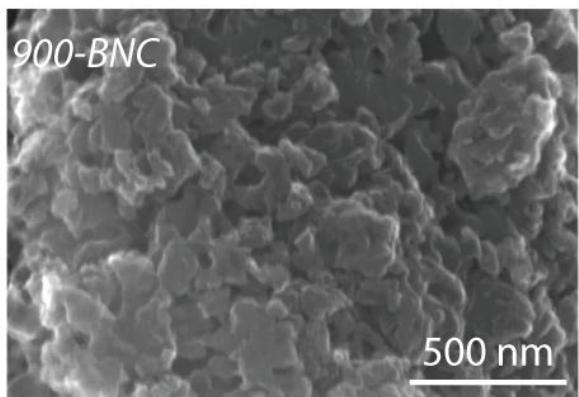
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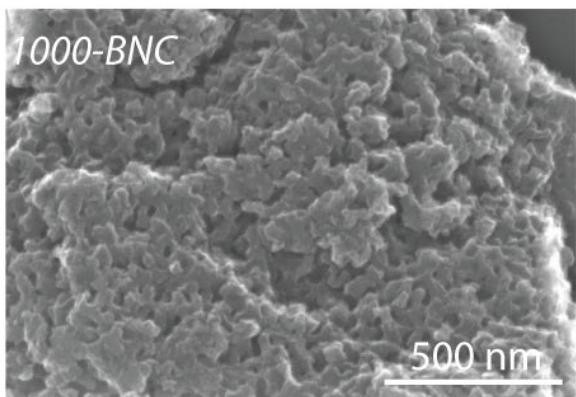
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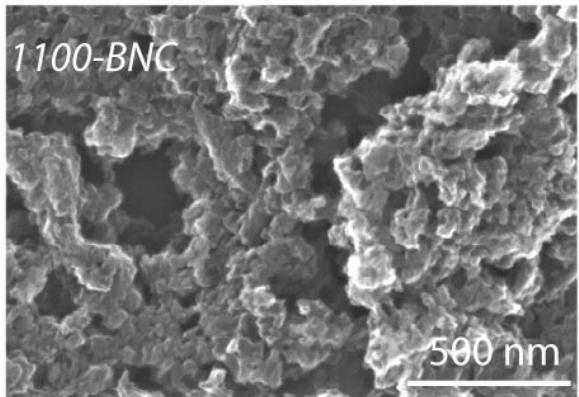
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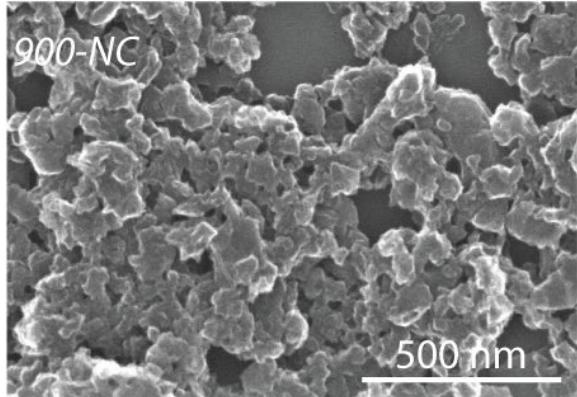
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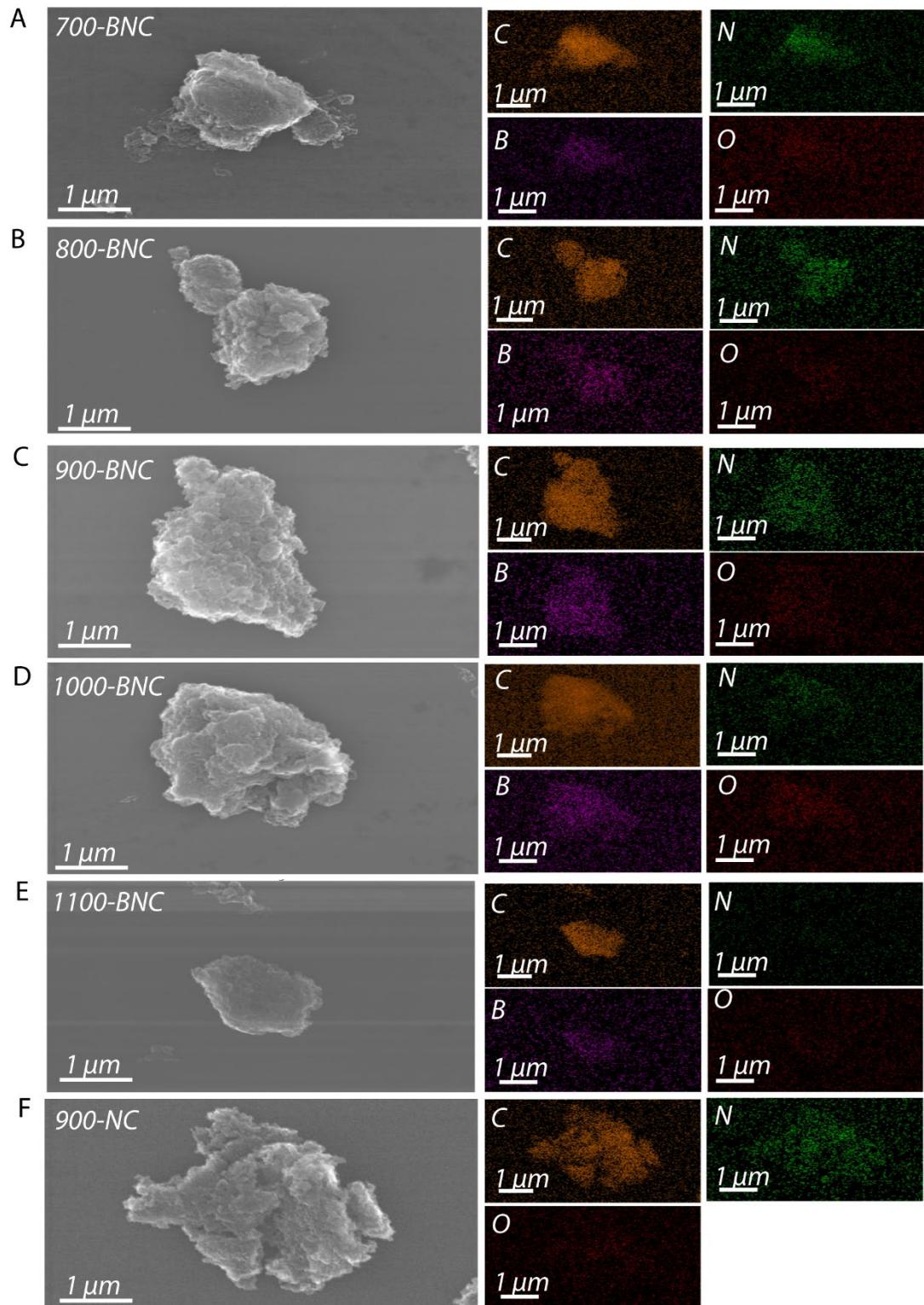
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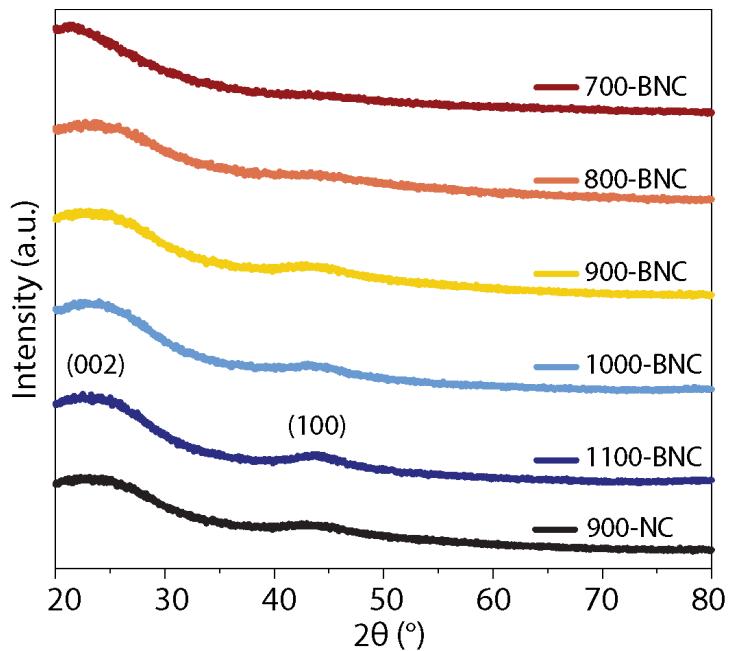
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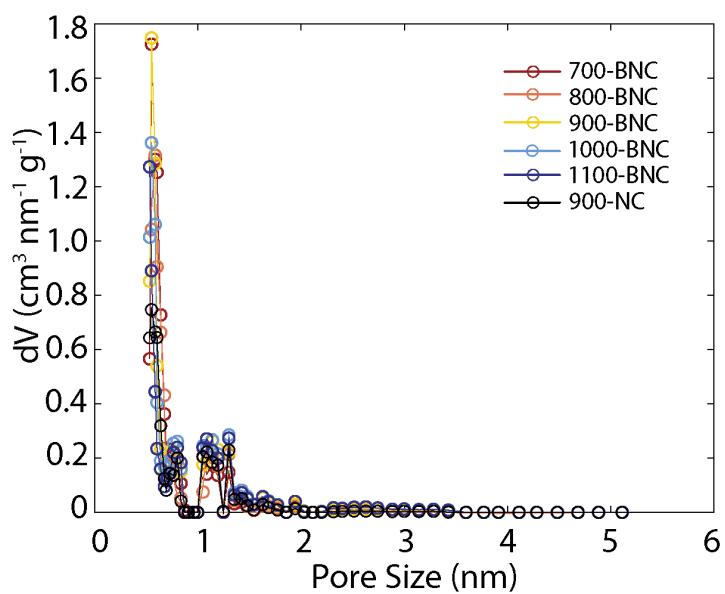
**Figure S4.** Scanning electron microscopy (SEM) reveals morphological evolution of the BNC catalysts pyrolyzed at A) 700°C, B) 800°C, C) 900°C, D) 1000°C, and E) 1100°C. F) Nitrogen doped carbon pyrolyzed at 900°C (900-NC).



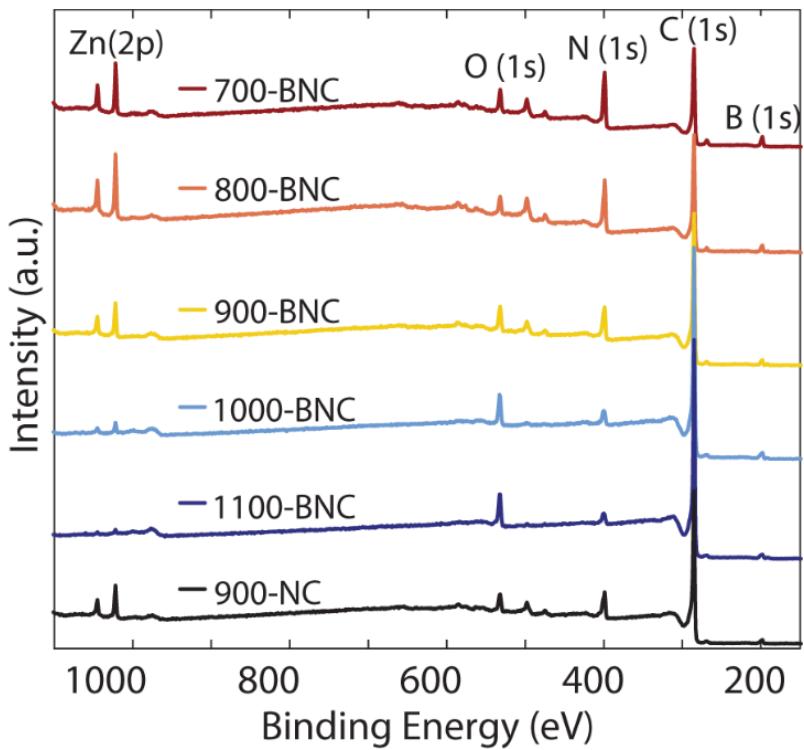
**Figure S5.** Energy dispersive spectroscopy (EDS) elemental mapping of the BNC catalysts pyrolyzed at A) 700°C, B) 800°C, C) 900°C, D) 1000°C, and E) 1100°C. F) Nitrogen doped carbon pyrolyzed at 900°C (900-NC).



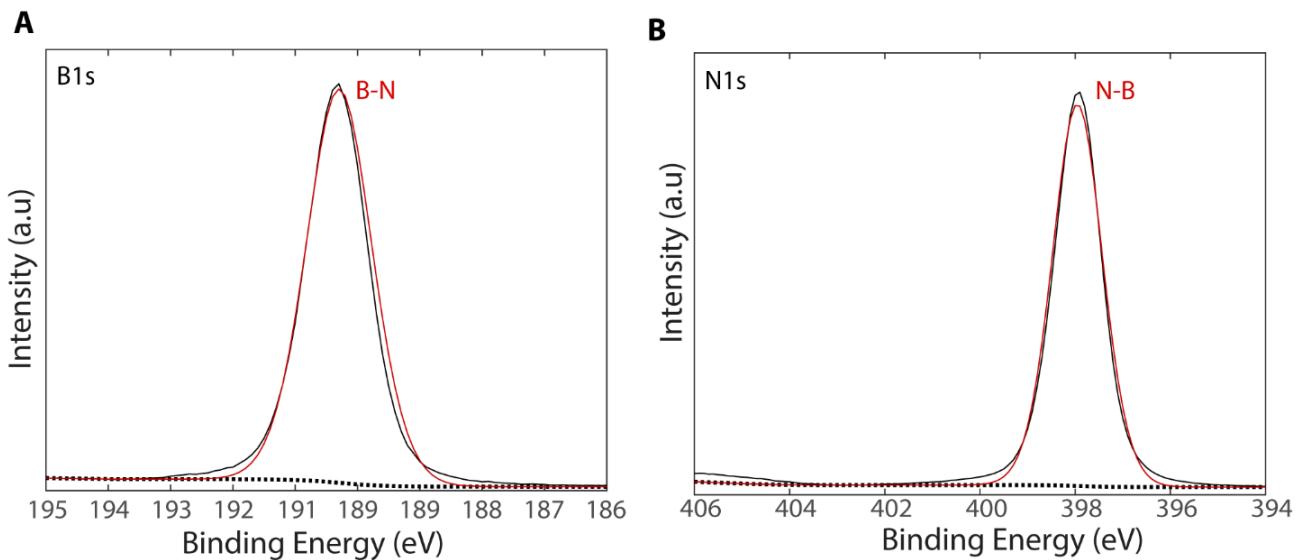
**Figure S6.** Powder X-ray diffraction (XRD) patterns of the as-prepared catalysts.



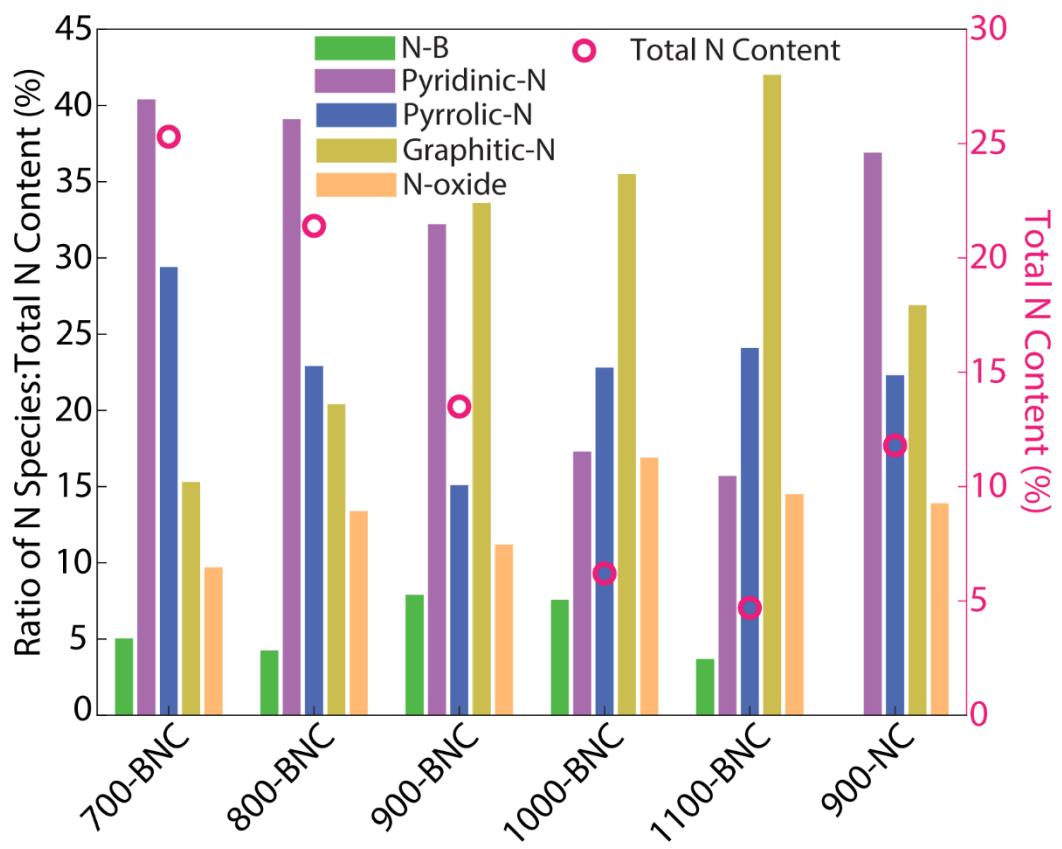
**Figure S7.** Pore size distributions of the as-prepared catalysts derived non-local density functional theory analysis of  $\text{N}_2$  adsorption-desorption isotherms.



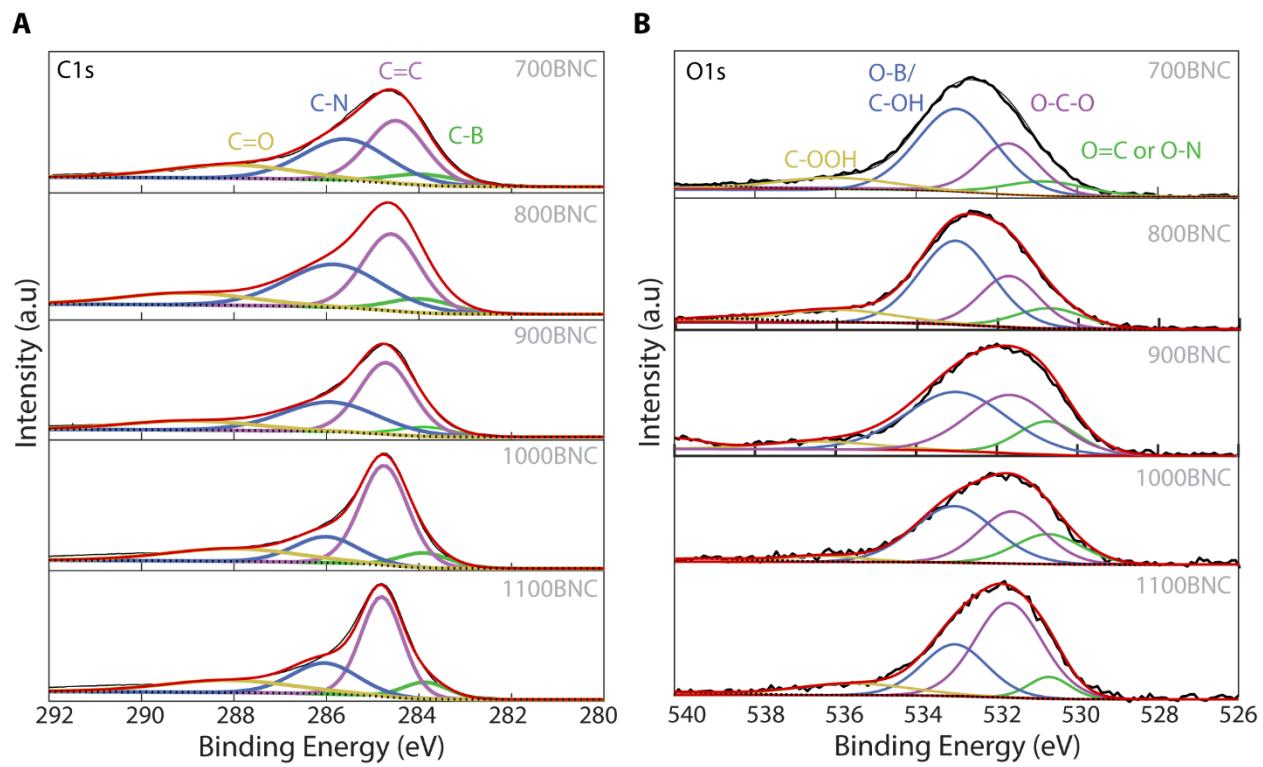
**Figure S8.** X-ray photoelectron spectroscopy (XPS) survey spectra of the BNC and NC catalysts.



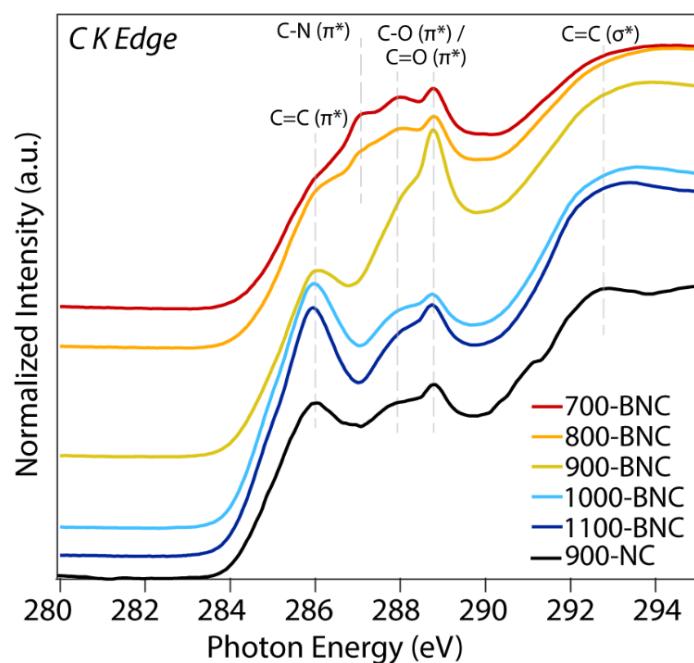
**Figure S9.** Fitting for A) B1s and B) N1s XPS spectra for boron nitride (*h*-BN) reference material derived from XPS measurements.



**Figure S10.** Ratio of nitrogen species to total nitrogen content in as-prepared BNC samples derived from XPS measurements. 900-NC included for comparison.

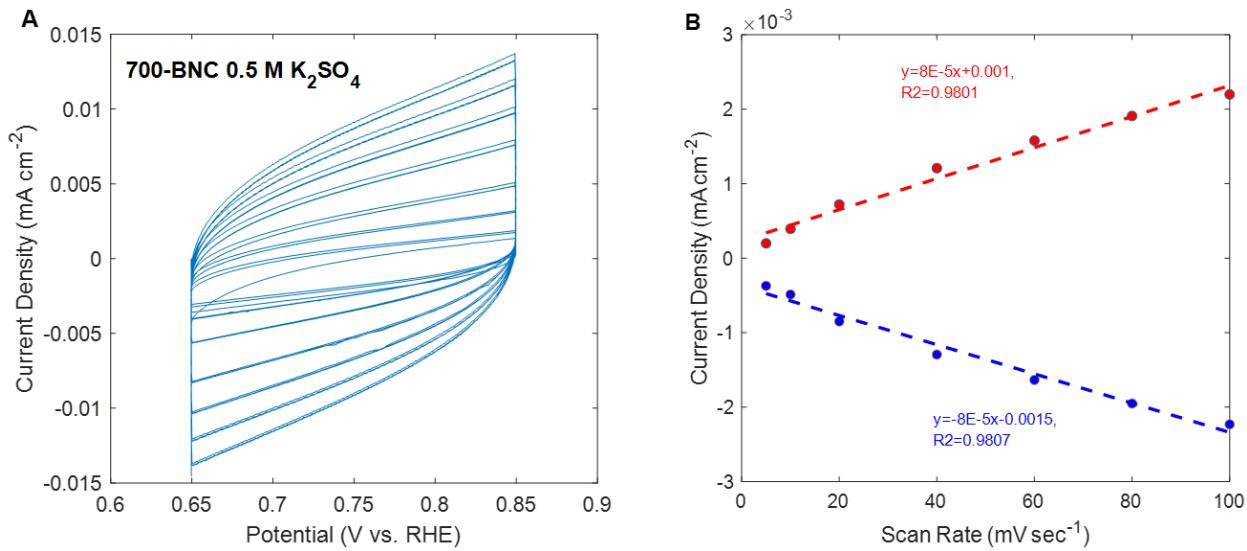


**Figure S11.** Deconvoluted A) C 1s and B) O 1s XPS spectra of BNC catalysts.

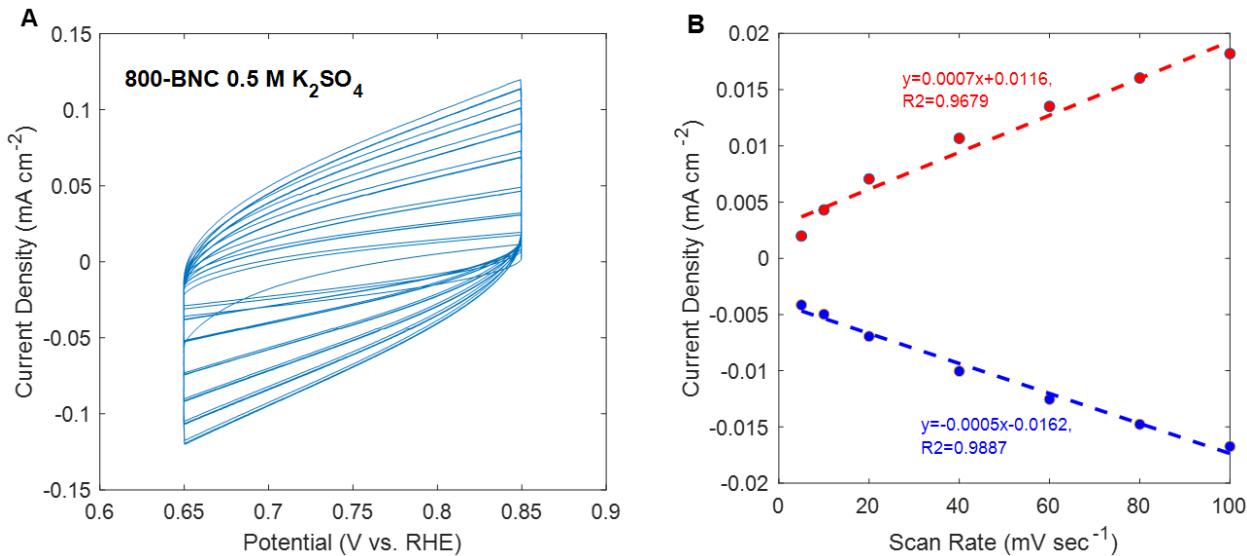


**Figure S12.** Carbon K-edge X-ray absorption spectroscopy (XAS) spectra for the different as-prepared catalysts.

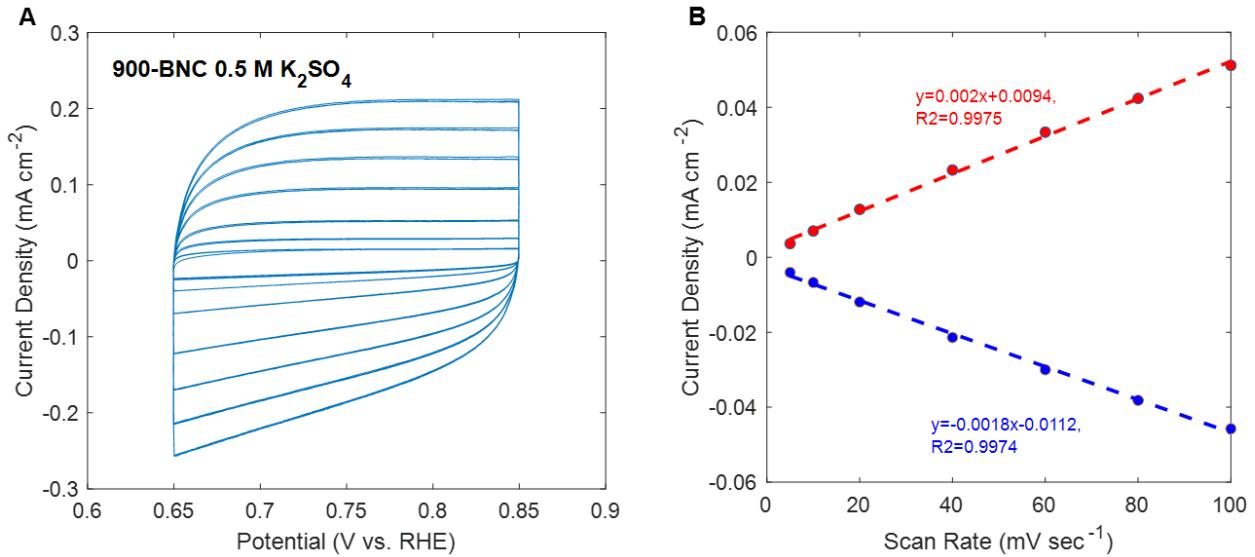
## Section S2. Rotating Ring-Disk Electrode Measurements



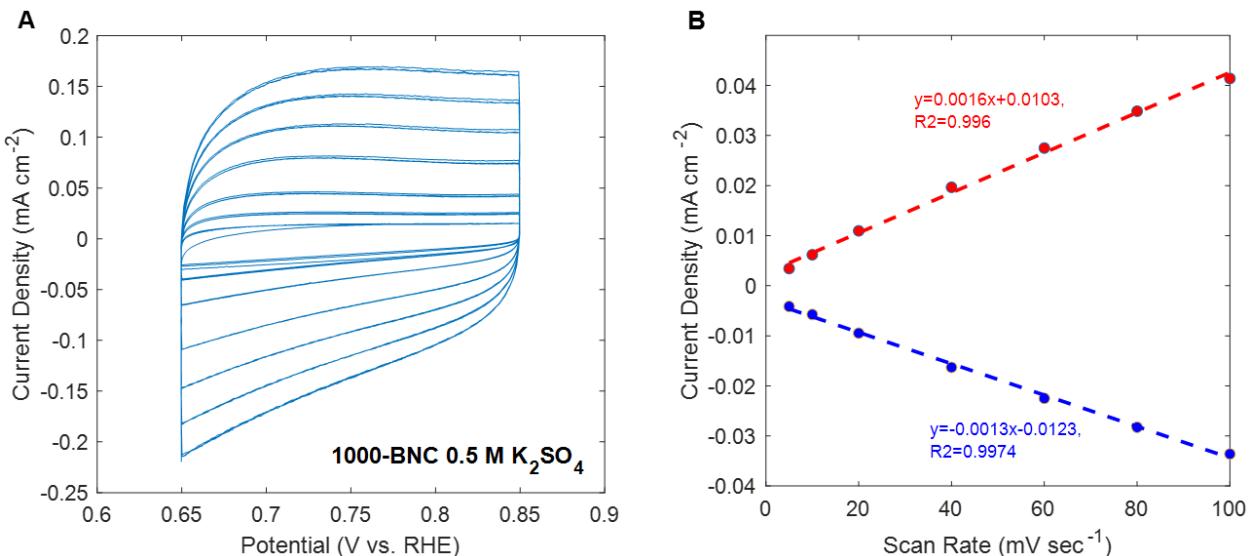
**Figure S13.** A) Cyclic voltammogram (CV) curves of 700-BNC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100  $\text{mV s}^{-1}$  in 0.5 M  $\text{K}_2\text{SO}_4$  aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.



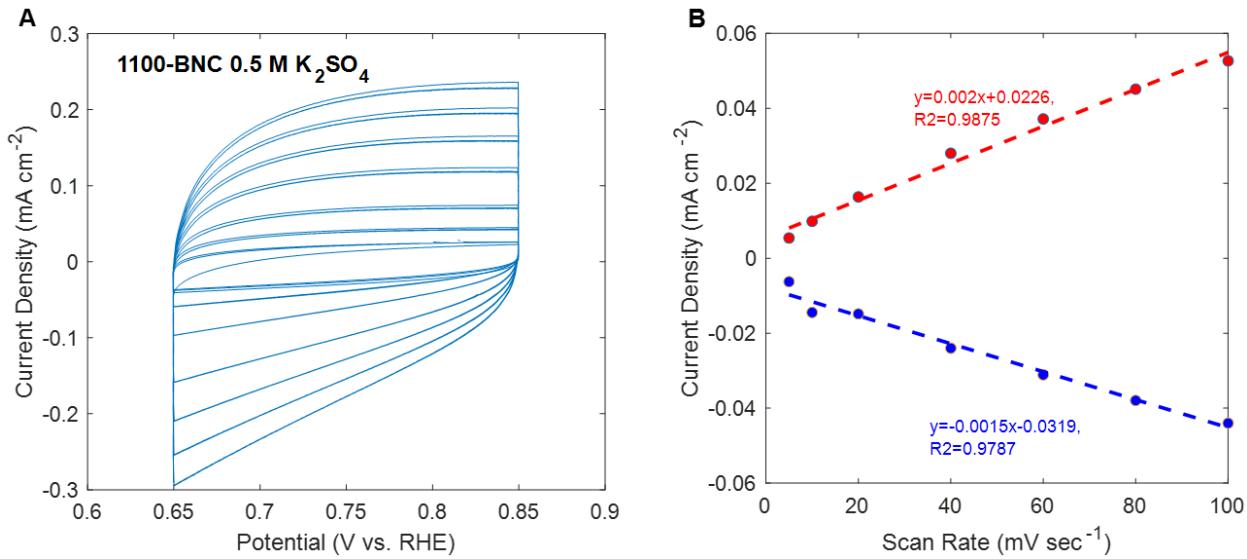
**Figure S14.** A) Cyclic voltammogram (CV) curves of 800-BNC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100  $\text{mV s}^{-1}$  in 0.5 M  $\text{K}_2\text{SO}_4$  aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.



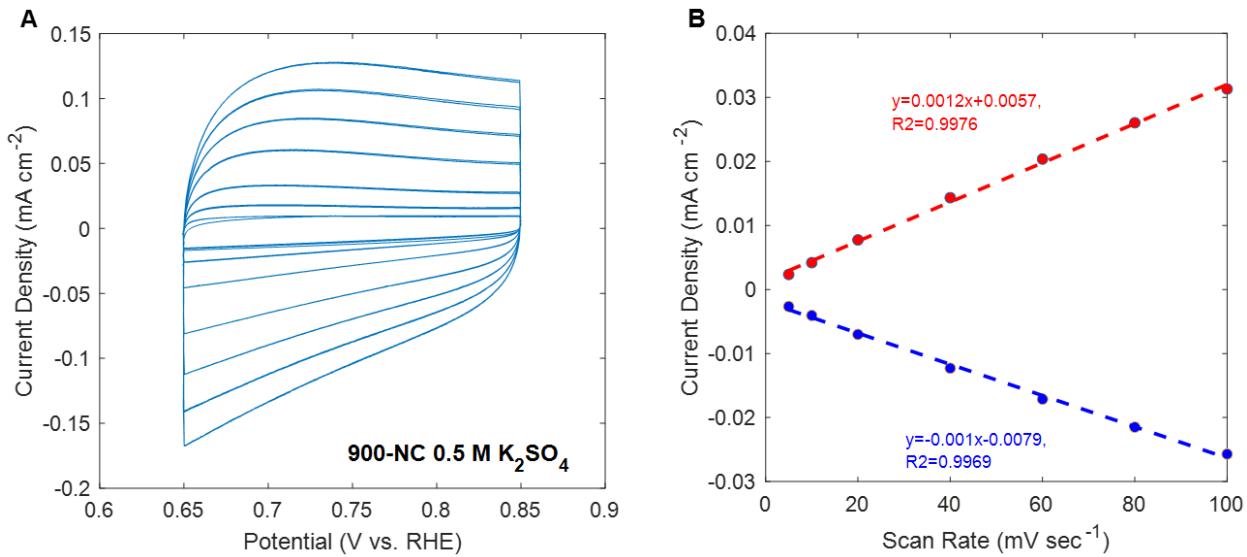
**Figure S15.** A) Cyclic voltammogram (CV) curves of 900-BNC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100  $\text{mV s}^{-1}$  in 0.5 M  $\text{K}_2\text{SO}_4$  aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.



**Figure S16.** A) Cyclic voltammogram (CV) curves of 1000-BNC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100  $\text{mV s}^{-1}$  in 0.5 M  $\text{K}_2\text{SO}_4$  aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.



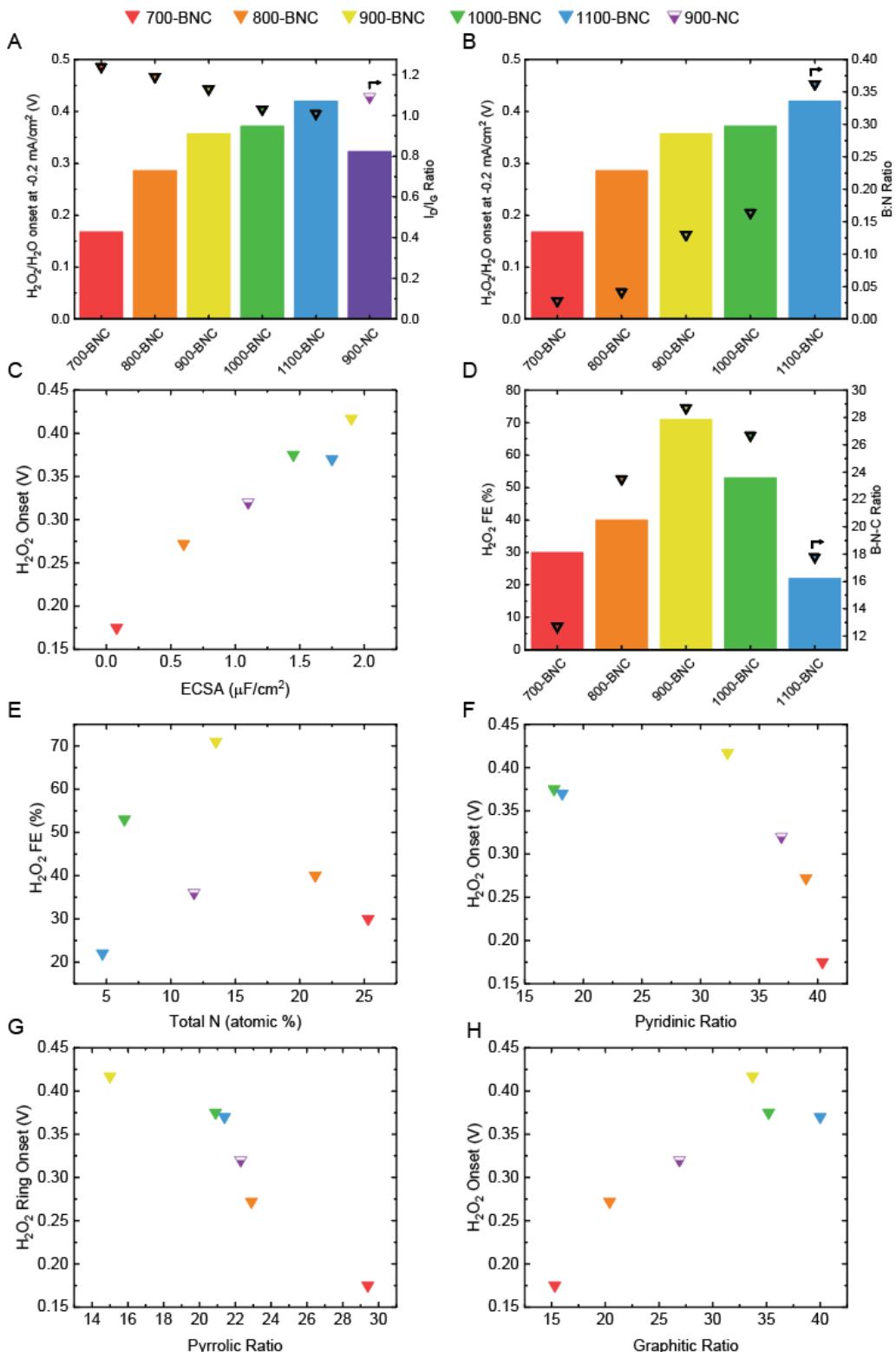
**Figure S17.** A) Cyclic voltammogram (CV) curves of 1100-BNC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100 mV s<sup>-1</sup> in 0.5 M K<sub>2</sub>SO<sub>4</sub> aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.



**Figure S18.** A) Cyclic voltammogram (CV) curves of 900-NC in the double layer region at scan rates 5, 10, 20, 40, 60, 80, and 100 mV s<sup>-1</sup> in 0.5 M K<sub>2</sub>SO<sub>4</sub> aqueous electrolyte; B) Current density (taken at 0.75 V vs. RHE) as a function of scan rate derived from CV curves.

Electrochemically active surface area (ECSA) was estimated by measuring the electrochemical double-layer capacitance ( $C_{dl}$ , Fig. S13-S18) via performing multiple CV curves over a 0.20 V potential range near the open circuit voltage (OCV) where no Faradaic reaction occurs with various scan rates between 5 to 100 mV s<sup>-1</sup>. The double layer capacitance is calculated as

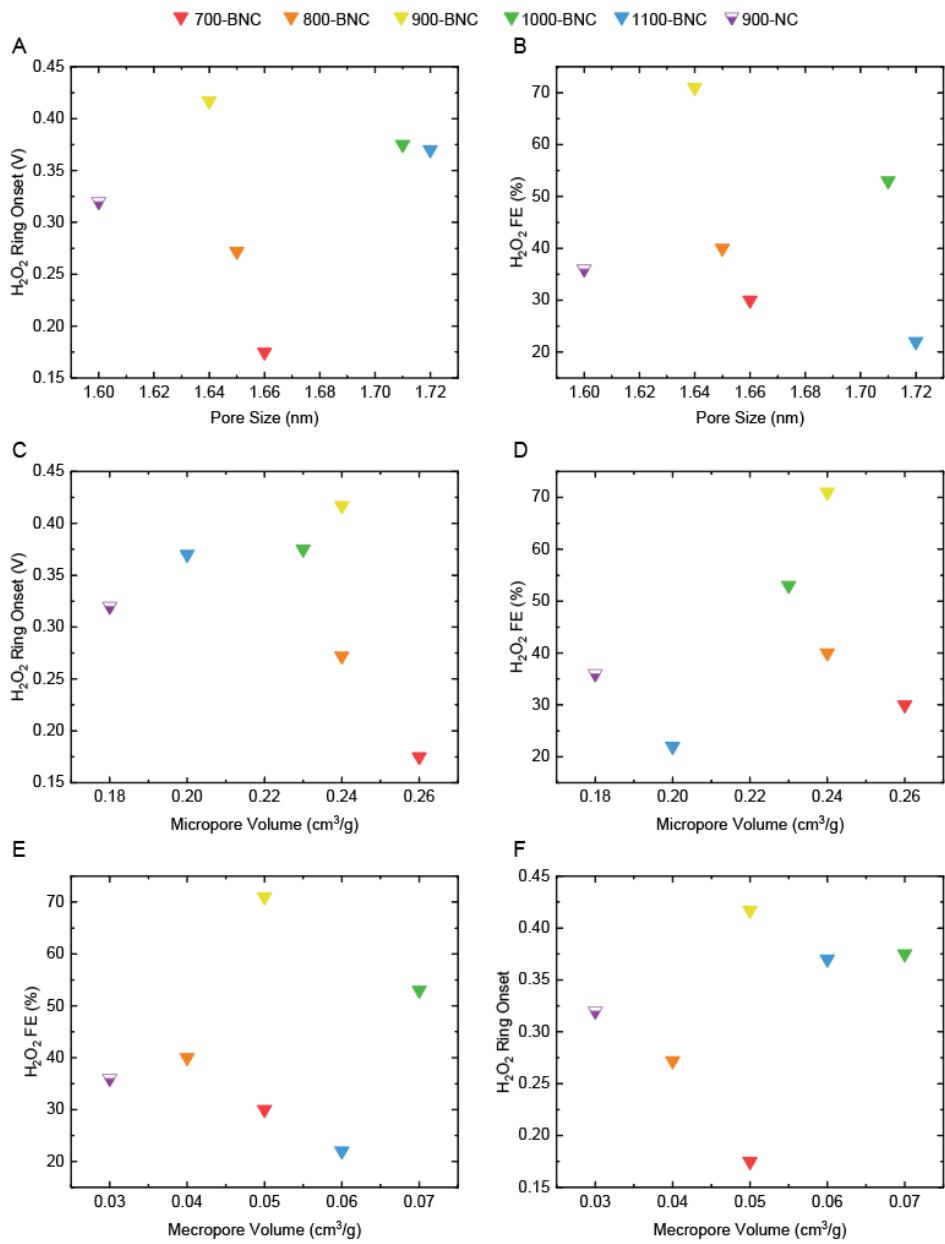
follows:  $C_{dl} = J / \frac{dV}{dt}$  where  $J$  is the current density at the center of the potential range,  $C_{dl}$  is the capacitance, and  $dV/dt$  represents the CV scan rate.



**Figure S19.** A)  $\text{H}_2\text{O}_2/\text{H}_2\text{O}$  onset potential at -0.2 mA/cm<sup>2</sup> disk vs.  $I_{\text{D}}/I_{\text{G}}$  ratio measured by Raman. B)  $\text{H}_2\text{O}_2/\text{H}_2\text{O}$  onset potential at -0.2 mA/cm<sup>2</sup> disk vs. B:N ratio measured by XPS. C)  $\text{H}_2\text{O}_2$  ring overpotential vs. ECSA measured by double-layer capacitance of catalysts. D)  $\text{H}_2\text{O}_2$

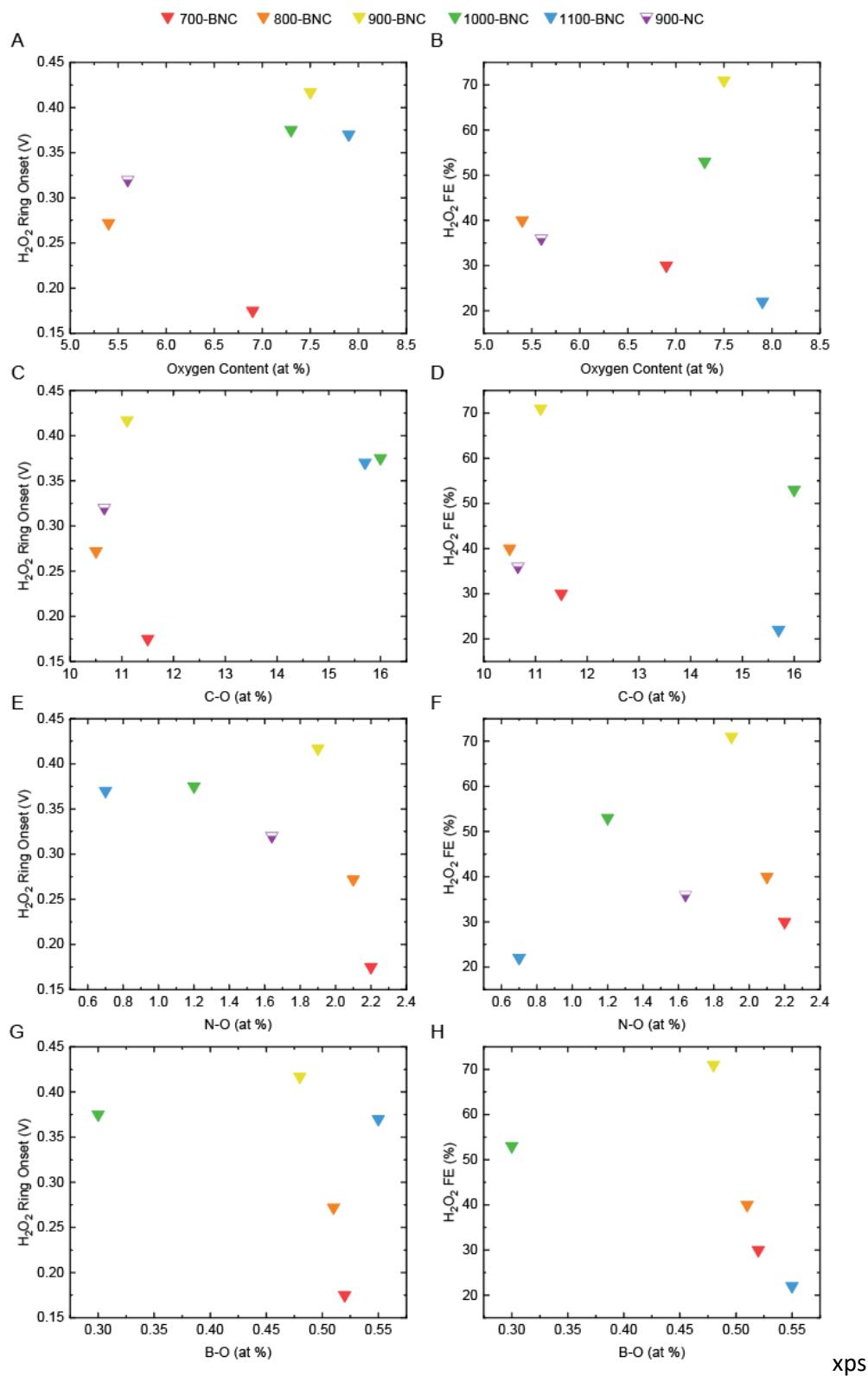
ring overpotential vs. pyrrolic ratio measured by XPS. E) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. graphitic ratio measured by XPS. F) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. pyridinic ratio measured by XPS. G) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. B-N-C ratio measured by XPS. H) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. total N content measured by XPS. Ratios represent the relative content of specified species compared to the total content. Values are displayed in Table S1, S4, and S5.

Figure S19 displays the key performance metrics as a function of the catalyst material properties. Figure S19A-B demonstrates the improvement in H<sub>2</sub>O<sub>2</sub>/H<sub>2</sub>O onset potential (overall ORR onset) trends with a higher degree of graphitization ( $I_D/I_G$  ratio) and an increase in the B:N ratio. Figure S19C displays a linear relationship between H<sub>2</sub>O<sub>2</sub> (ring) onset potential and ECSA. Figure S19D further shows how a higher content of local B-N-C dopant configurations leads to a more favorable selectivity toward H<sub>2</sub>O<sub>2</sub>. Figure S19E-H explores the relationship between N content and configurations with respect to H<sub>2</sub>O<sub>2</sub> performance. Figure S19E shows how moderate N doping is more favorable for 2e<sup>-</sup> ORR to H<sub>2</sub>O<sub>2</sub>. Figure S19F-G shows how pyrrolic and pyridinic moieties impede H<sub>2</sub>O<sub>2</sub> formation, while Figure S19H demonstrates how graphitic-N improves H<sub>2</sub>O<sub>2</sub> performance.



**Figure S20.** A)  $\text{H}_2\text{O}_2$  ring overpotential vs. pore size measured by  $\text{N}_2$  adsorption. B) Maximum  $\text{H}_2\text{O}_2$  FE vs. pore size. C)  $\text{H}_2\text{O}_2$  ring overpotential vs. micropore volume measured by  $\text{N}_2$  adsorption. D) Maximum  $\text{H}_2\text{O}_2$  FE vs. micropore volume. E)  $\text{H}_2\text{O}_2$  ring overpotential vs. mesopore volume measured by  $\text{N}_2$  adsorption. F) Maximum  $\text{H}_2\text{O}_2$  FE vs. mesopore volume. Values are displayed in Table S2.

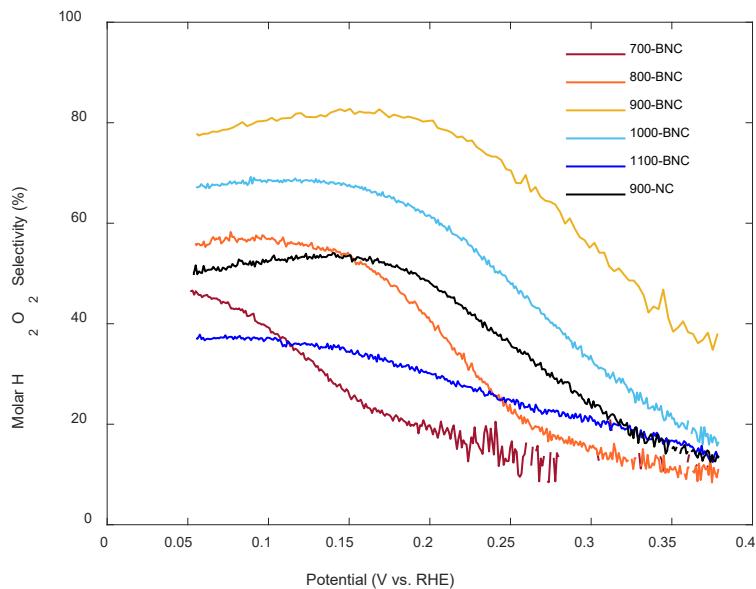
Figure S20 displays the effects of pore size, micropore volume, and mesopore volume on the performance of  $\text{H}_2\text{O}_2$  electrosynthesis (activity onset and FE). No significant contribution to changes in performance is observed with varying pore structures.



**Figure S21.** A) H<sub>2</sub>O<sub>2</sub> ring overpotential vs. O content measured by XPS. B) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. O content. C) H<sub>2</sub>O<sub>2</sub> ring overpotential vs. C-O bond ratio measured by XPS. D) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. C-O bond ratio. E) H<sub>2</sub>O<sub>2</sub> ring overpotential vs. N-O bond ratio measured by XPS. F)

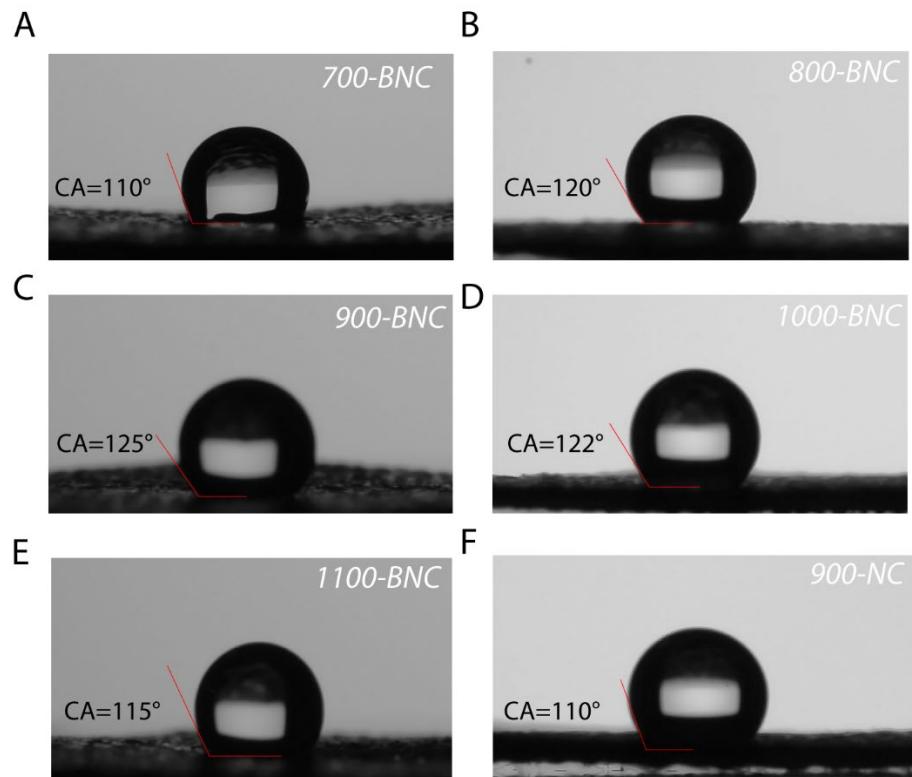
Maximum H<sub>2</sub>O<sub>2</sub> FE vs. N-O bond ratio. G) H<sub>2</sub>O<sub>2</sub> ring overpotential vs. B-O bond ratio measured by XPS. H) Maximum H<sub>2</sub>O<sub>2</sub> FE vs. B-O bond ratio. Values are displayed in Table S3-6.

Figure S21 shows the effect of O in BNC and NC catalysts on H<sub>2</sub>O<sub>2</sub> electrosynthesis performance. The total O content and amount of C-O bonds do not affect the performance. The H<sub>2</sub>O<sub>2</sub> FE shows a maximum at 1.9 at % N-O bonds (out of all N bonds) and 0.48 at % B-O bonds (out of all B bonds).

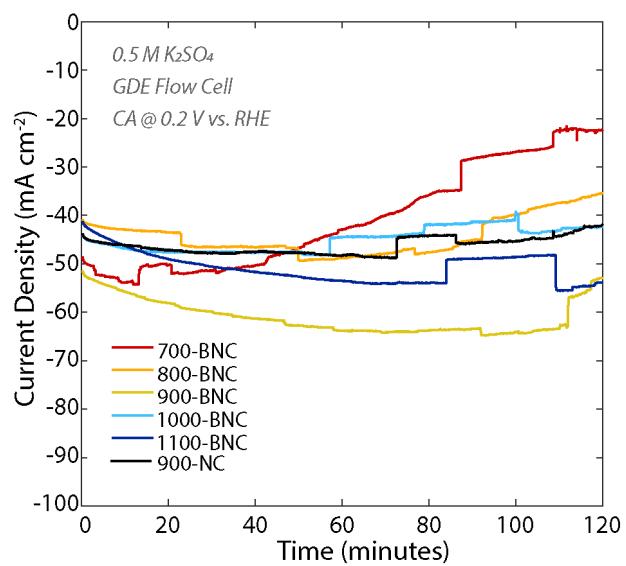


**Figure S22.** Calculated molar H<sub>2</sub>O<sub>2</sub> selectivity as a function of applied potential for the different BNC catalysts in 0.5 M K<sub>2</sub>SO<sub>4</sub>. 900-NC is included for comparison.

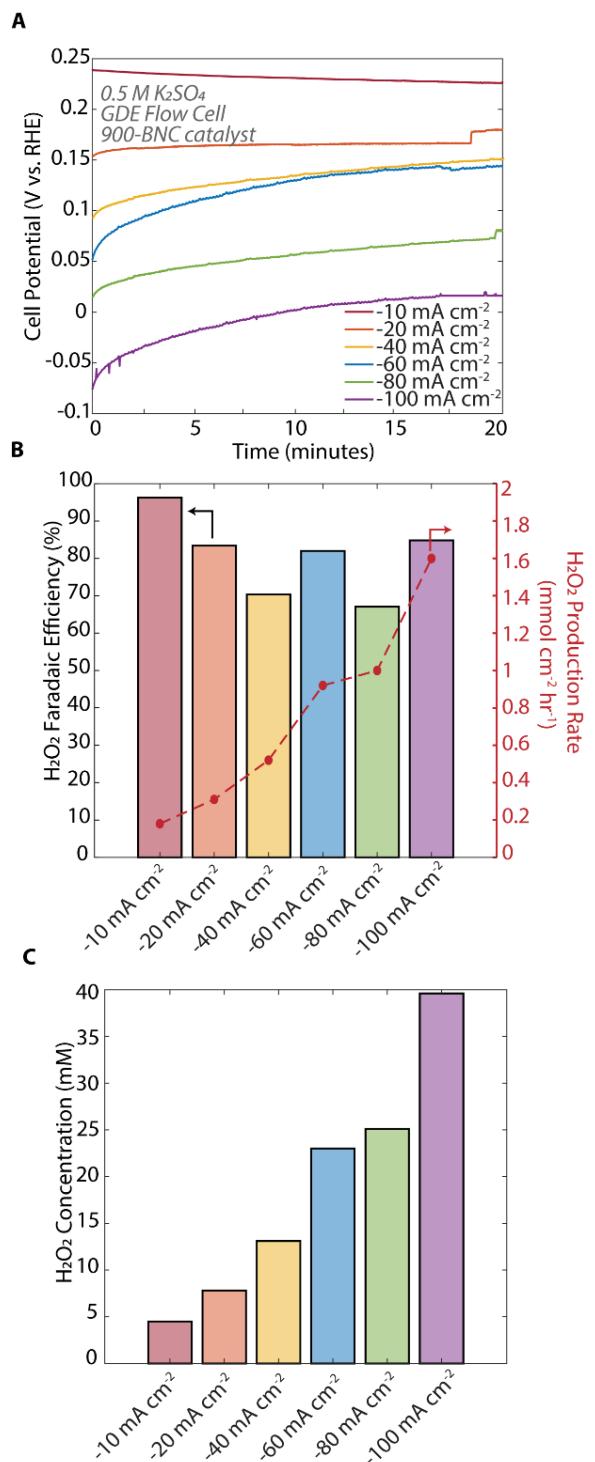
### Section S3. Electrochemical Flow Cell Measurements



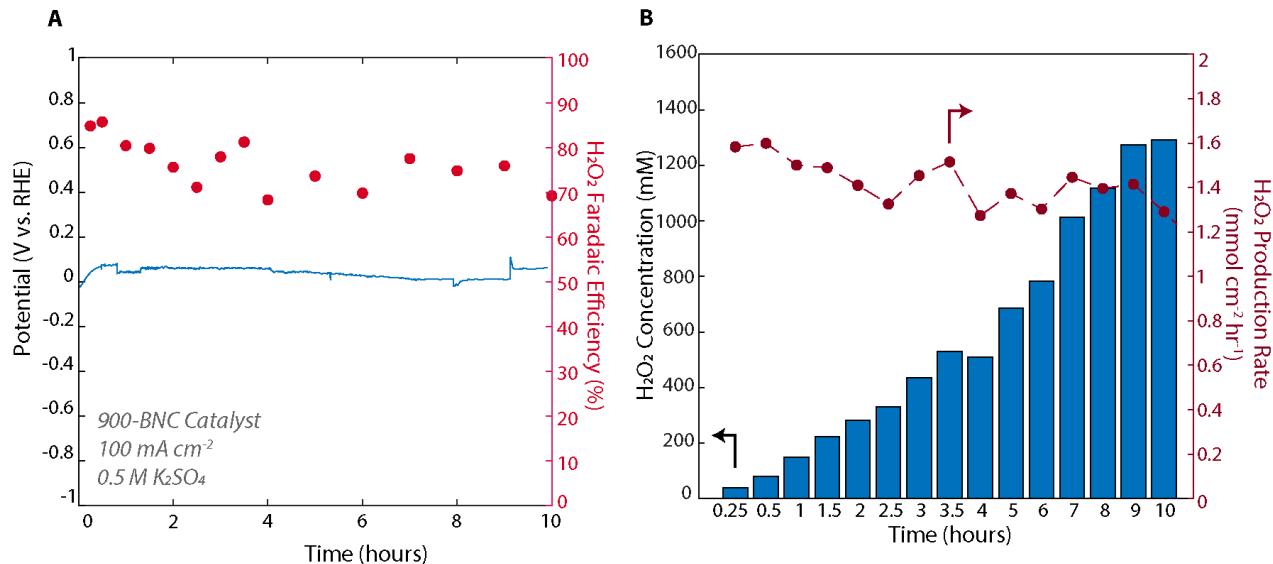
**Figure S23.** Contact angle measurements for the as-prepared catalysts spray coated on a carbon cloth electrode. A) 700-BNC, B) 800-BNC, C) 900-BNC, D) 1000-BNC, E) 1100-BNC, and F) 900-NC.



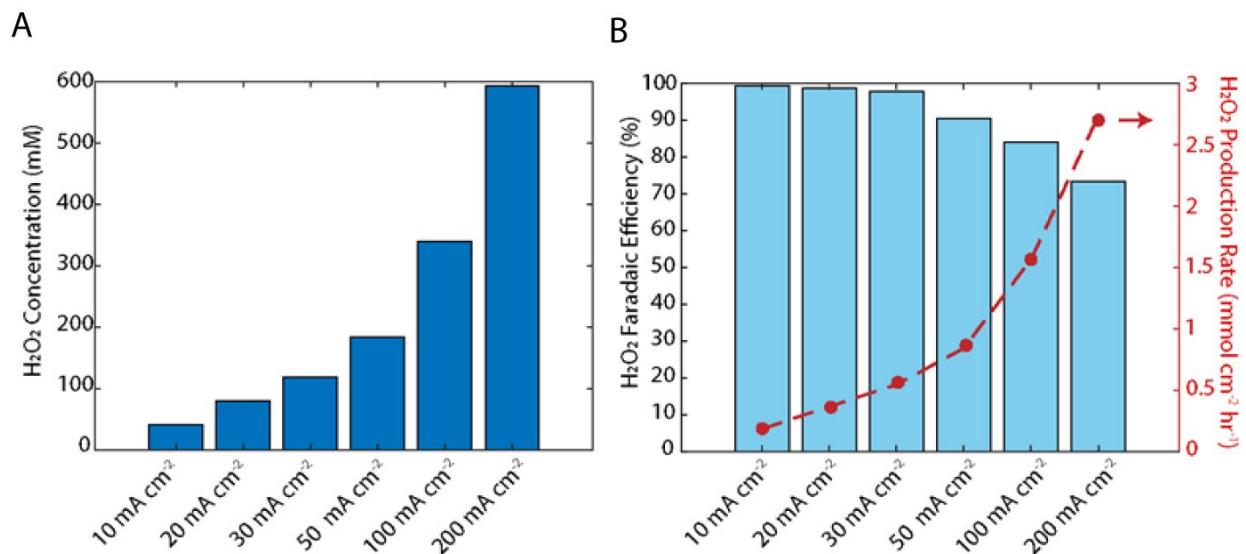
**Figure S24.** Chronoamperometry (CA) held at 0.20 V vs. RHE for 2 hours for different BNC catalysts in 0.5 M K<sub>2</sub>SO<sub>4</sub> in three-electrode gas diffusion electrode (GDE) flow cell. 900-NC included for comparison.



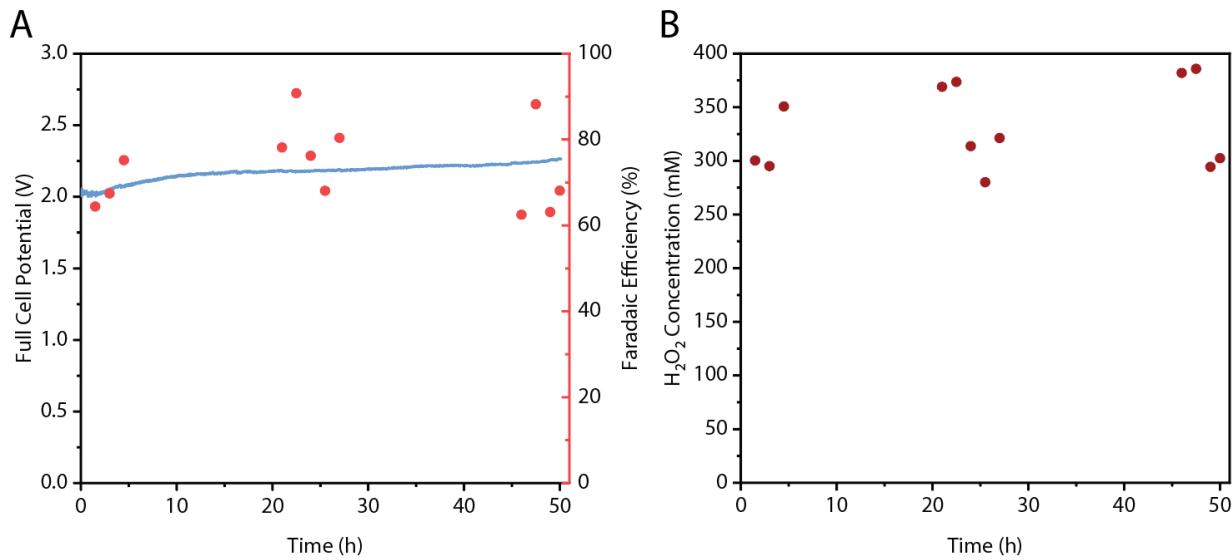
**Figure S25.** Chronopotentiometry (CP) measurements held for 15 minutes at different applied current densities (-10, -20, -40, -60, -80, and -100  $mA\ cm^{-2}$ ) for 900-BNC catalyst in three-electrode GDE flow cell. A) Cell potential vs. time. B)  $H_2O_2$  Faradaic efficiency (right axis) and  $H_2O_2$  production rate (left axis). C) Final  $H_2O_2$  concentration measured after 15 minutes under various applied current densities.



**Figure S26.** Stability test of 900-BNC in a three-electrode GDE flow cell at 100 mA cm<sup>-2</sup> in 0.5 M K<sub>2</sub>SO<sub>4</sub> electrolyte. A) Corresponding potential response (left axis) and H<sub>2</sub>O<sub>2</sub> Faradaic efficiency (right axis). C) H<sub>2</sub>O<sub>2</sub> concentration measured over 10 hours (left axis) and calculated H<sub>2</sub>O<sub>2</sub> production rate (right axis). H<sub>2</sub>O<sub>2</sub> was collected in the recycled catholyte stream.



**Figure S27.** H<sub>2</sub>O<sub>2</sub> production performance for 900-BNC in a two-electrode MEA solid electrolyte flow cell as a function of applied current density. A) Measured H<sub>2</sub>O<sub>2</sub> concentration and corresponding B) Faradaic efficiency (right axis) and production rate (left axis) measured after 30 minutes. H<sub>2</sub>O<sub>2</sub> was collected as a single pass rinse through solid electrolyte chamber.



**Figure S28.** H<sub>2</sub>O<sub>2</sub> production stability test for 900-BNC in a two-electrode MEA solid electrolyte flow cell as a function of applied current density. A) Full cell potential and corresponding Faradaic efficiency (right axis) and B) H<sub>2</sub>O<sub>2</sub> concentration over chronopotentiometry hold at 50 mA cm<sup>-2</sup>. H<sub>2</sub>O<sub>2</sub> was collected as a single pass rinse through solid electrolyte chamber

#### Section S4. Supplementary Tables

**Table S1.** Raman  $I_D/I_G$  intensity band ratios.

Sample	D Band Intensity ( $1350\text{ cm}^{-1}$ )	G Band Intensity ( $1580\text{ cm}^{-1}$ )	$I_D/I_G$ Ratio
700-BNC	10400	8400	1.24
800-BNC	11300	9500	1.19
900-BNC	5200	4610	1.13
1000-BNC	5730	5546	1.03
1100-BNC	1420	1400	1.01
900-NC	1655	1521	1.09

**Table S2.**  $\text{N}_2$  adsorption-desorption isotherms.

Sample	Specific Surface Area ( $\text{m}^2/\text{g}$ ) <sup>a</sup>	Total Pore Volume ( $\text{cm}^3/\text{g}$ ) <sup>a</sup>	Micropore Volume ( $\text{cm}^3/\text{g}$ ) <sup>b</sup>	Mesopore Volume ( $\text{cm}^3/\text{g}$ ) <sup>c</sup>	Average Pore Width (nm) <sup>d</sup>
700-BNC	760	0.31	0.26	0.05	1.66
800-BNC	680	0.28	0.24	0.04	1.65
900-BNC	715	0.29	0.24	0.05	1.64
1000-BNC	700	0.30	0.23	0.07	1.71
1100-BNC	620	0.26	0.20	0.06	1.72
900-NC	530	0.21	0.18	0.03	1.60

*a* – specific surface area and total pore volume is calculated with BET theory

*b* – micropore volume is calculated with *t*-plot value

*c* – mesopore volume is the difference of single pore volume and *t*-plot micropore volume

*d* – pore size is calculated with a non-local density functional theory model assuming slit carbon pores

**Table S3.** Elemental analysis of the catalyst materials obtained by different temperature treatments derived from XPS measurements.

Sample	C at%	N at%	O at%	Zn at%	B at%	B:N ratio
700-BNC	64.6	25.2	6.9	2.6	0.71	0.028
800-BNC	68.6	21.7	5.4	3.2	0.98	0.045
900-BNC	75.4	13.8	7.5	1.6	1.78	0.130
1000-BNC	85.0	6.3	7.3	0.4	1.01	0.161
1100-BNC	85.6	4.7	7.9	0.2	1.63	0.350
900-NC	80.9	11.7	5.6	1.8	-	-

**Table S4.** Elemental analysis of the different boron species in the catalyst materials derived from XPS measurements. The ratio represents the percentage of a specific B functional group in the total B content. The atom percent (at%) reflects the amount of a certain B functional group in the entire material.

Sample	Total B at%	B-N-C ratio/at% (190 eV)	B-N ratio/at% (191 eV)	B-O ratio/at% (192 eV)	Total B-N + B-N-C ratio
700-BNC	0.71	12.7 / <b>0.09</b>	14.1 / <b>0.10</b>	73.2 / <b>0.52</b>	26.8
800-BNC	0.98	23.5 / <b>0.23</b>	24.5 / <b>0.24</b>	52.0 / <b>0.51</b>	48.0
900-BNC	1.78	28.7 / <b>0.51</b>	44.4 / <b>0.79</b>	27.0 / <b>0.48</b>	73.0
1000-BNC	1.01	26.7 / <b>0.27</b>	43.6 / <b>0.44</b>	29.7 / <b>0.30</b>	70.3
1100-BNC	1.63	17.8 / <b>0.29</b>	48.5 / <b>0.79</b>	33.7 / <b>0.55</b>	66.3

**Table S5.** Elemental analysis of the different nitrogen species in the catalyst materials derived from XPS measurements. The ratio represents the percentage of a specific N functional group in the total N content. The atom percent (at%) reflects the amount of a certain N functional group in the entire material.

Sample	Total N at%	N-B ratio/at% (397.7 eV)	Pyridinic ratio/at% (398.5 eV)	Pyrrolic ratio/at% (399.5 eV)	Graphitic ratio/at% (400.7 eV)	N-oxide ratio/at% (403.5 eV)	Total N-C ratio
700-BNC	25.2	4.0 / <b>1.0</b>	46.1 / <b>11.7</b>	28.2 / 7.1	13.2 / 3.4	8.5 / <b>2.2</b>	87.5
800-BNC	21.7	4.8 / <b>1.1</b>	45.5 / <b>9.9</b>	27.0 / <b>5.9</b>	12.9 / <b>2.8</b>	9.8 / <b>2.1</b>	85.3
900-BNC	13.8	7.5 / <b>1.0</b>	39.2 / <b>5.4</b>	18.3 / <b>2.5</b>	21.2 / <b>2.9</b>	13.8 / <b>1.9</b>	78.7
1000-BNC	6.3	6.1 / <b>0.38</b>	17.7 / <b>1.1</b>	21.2 / <b>1.3</b>	35.8 / <b>2.24</b>	19.2 / <b>1.2</b>	74.8
1100-BNC	4.7	5.6 / <b>0.26</b>	18.1 / <b>0.84</b>	19.8 / <b>0.92</b>	41.4 / <b>1.9</b>	15.1 / <b>0.7</b>	79.3
900-NC	11.7	-	36.9 / <b>4.34</b>	22.3 / <b>2.63</b>	26.9 / <b>3.17</b>	13.9 / <b>1.64</b>	86.1

**Table S6.** Elemental analysis of the different carbon species in the catalyst materials derived from XPS measurements. The ratio represents the percentage of a specific C functional group in the total C content. The atom percent (at%) reflects the amount of a certain C functional group in the entire material.

Sample	Total C at%	C-B ratio/at% (283.9 eV)	C=C ratio/at% (284.5 eV)	C-N ratio/at% (286 eV)	C-O ratio/at% (288.3 eV)	Total C-B + C-N ratio
700-BNC	64.6	7.8 / <b>5.0</b>	37.7 / <b>24.3</b>	36.8 / <b>23.7</b>	17.8 / <b>11.5</b>	44.5
800-BNC	68.6	7.8 / <b>5.4</b>	39.7 / <b>27.5</b>	37.4 / <b>25.9</b>	15.1 / <b>10.5</b>	45.1
900-BNC	75.4	6.1 / <b>4.6</b>	46.0 / <b>34.9</b>	33.3 / <b>25.3</b>	14.6 / <b>11.1</b>	39.4
1000-BNC	85.0	8.7 / <b>7.4</b>	53.6 / <b>45.5</b>	18.9 / <b>16.0</b>	18.9 / <b>16.0</b>	27.6
1100-BNC	85.6	9.1 / <b>7.8</b>	48.9 / <b>41.7</b>	23.6 / <b>20.1</b>	18.4 / <b>15.7</b>	32.7

Lower concentration of C-B suggests higher concentration of B-N-C moieties are present.

**Table S7.** Calculated partial H<sub>2</sub>O<sub>2</sub> kinetic current density values at 0.20 V vs. RHE.

Catalyst	H <sub>2</sub> O <sub>2</sub> Kinetic Current Density (J <sub>kin, H<sub>2</sub>O<sub>2</sub></sub> )
700-BNC	0.012
800-BNC	0.16
900-BNC	0.82
1000-BNC	0.58
1100-BNC	0.29
900-NC	0.22

**Table S8.** Catholyte composition of boron measured via ICP-MS after electrochemical testing for 2 hours at 0.20 V vs. RHE.

Sample	Boron (ppm)
700-BNC	0.016
800-BNC	0.011
900-BNC	0.015
1000-BNC	0.012
1100-BNC	0.009
0.5 M K <sub>2</sub> SO <sub>4</sub>	0.007

Based on an initial catalyst loading of 0.5 mg/cm<sup>2</sup> for the 900-BNC electrode that contains 9 µg of total B, ICP-MS results indicate that only 0.08 µg B dissolved in the catholyte after 2 hours of ORR testing, corresponding to < 1 % dissolution. This suggests that the boron content of the 900-BNC catalyst remains highly stable under the explored reaction conditions.

**Table S9.** Comparison of H<sub>2</sub>O<sub>2</sub> performance of different carbon-based catalysts using RRDE.

<i>Material</i>	<i>pH</i>	<i>Onset Potential (V<sub>RHE</sub>)</i>	<i>H<sub>2</sub>O<sub>2</sub> Selectivity (%)</i>	<i>Reference</i>
Boron nitride islands	0.1 M KOH	0.8	78	<sup>8</sup>
Mesoporous nitrogen carbon (MNC-600)	0.1 M KHCO <sub>3</sub>	0.7	85	<sup>9</sup>
Hierarchically porous carbon	7	0.16	70.8	<sup>10</sup>
Activated carbon/carbon fiber	7	0.31	26.5	<sup>11</sup>
NCMK3IL50_800T	7	0.2	75.7	<sup>12</sup>
N-doped carbon (0.05 mg cm <sup>-2</sup> )	0.5 M H <sub>2</sub> SO <sub>4</sub> 0.1 M K <sub>2</sub> SO <sub>4</sub>	0.49 0.52	>90 90	<sup>13</sup>
Co–N–C	7.4	0.3–0.4	>60	<sup>14</sup>
O-CB (0.2 mg cm <sup>-2</sup> )	0.1 M Na <sub>2</sub> SO <sub>4</sub>	0.47	55	<sup>15</sup>
Boron doped carbon	0.1 M Na <sub>2</sub> SO <sub>4</sub>	0.35	80	<sup>16</sup>
Mesoporous nitrogen-doped carbon	1	0.1	>90	<sup>17</sup>
Mesoporous nitrogen doped carbon	0.5 M H <sub>2</sub> SO <sub>4</sub>	0.2	>90	<sup>18</sup>
Oxidized CNTs	0.1 M KOH 0.1 M PBS 0.1 M HClO <sub>4</sub>	0.70 0.40 0.15	~90 ~85 ~50	<sup>19</sup>
Co–N–C	1	0.3	>40	<sup>14</sup>
Single site Co-N-C (0.1 mg cm <sup>-2</sup> )	0.1 M K <sub>2</sub> SO <sub>4</sub> 0.5 M H <sub>2</sub> SO <sub>4</sub>	0.71 0.83	55 80	<sup>20</sup>
F-doped carbon (0.86 mg cm <sup>-2</sup> )	0.05 M H <sub>2</sub> SO <sub>4</sub>	0.425	97.5	<sup>21</sup>
900-BNC (0.1 mg cm <sup>-2</sup> )	0.5 M K <sub>2</sub> SO <sub>4</sub>	0.35	~80	<b>This work</b>

**Table S10.** Comparison of H<sub>2</sub>O<sub>2</sub> performance of different catalysts using different flow cells.

Material	Cell	pH	H <sub>2</sub> O <sub>2</sub> Faradaic Efficiency (%)	H <sub>2</sub> O <sub>2</sub> Production Rate (mmol cm <sup>-2</sup> sec <sup>-1</sup> )	Reference
CoPc-CNT(O) CoPc-CNT CNT(O) (0.2 mg cm <sup>-2</sup> )	Flow Cell	1 M Na <sub>2</sub> SO <sub>4</sub>	92 90 90	1.43E-3 1.4E-3 9.3E-3	<sup>22</sup>
B-C (0.5 mg cm <sup>-2</sup> )	Flow Cell	1 M KOH	80	2.6E-4	<sup>16</sup>
N-doped carbon (0.2 mg cm <sup>-2</sup> )	Flow Cell	0.5 M Na <sub>2</sub> SO <sub>4</sub> 0.1 M KOH 0.5 H <sub>2</sub> SO <sub>4</sub>	70 59.5 34.3	1.37E-4 1.17E-4 6.7E-5	<sup>23</sup>
OCNS <sub>900</sub> (1 mg cm <sup>-2</sup> )	Flow Cell	0.1 M KOH	89.6	2.14E-6	<sup>24</sup>
900-BNC (0.5 mg cm <sup>-2</sup> )	Flow Cell	0.5 M K <sub>2</sub> SO <sub>4</sub>	78	2.4E-4	<b>This work</b>

## Section S5. References

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