

Supporting Information

Quick Drying Process: Promising Strategy for Preparing an Egg-shell-type Cu/ γ -Al₂O₃ Catalyst for Direct N₂O Decomposition

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Table S1. Conditions of deN₂O tests.

	Balance	N ₂ O	NF ₃	Steam	Temp. (°C)	GHSV (h ⁻¹)
Case 1	N ₂	1%	-	-	400-650	1,800
Case 2	Air		-	-	400-650	1,800
Case 3	Air		-	7.5%	400-650	1,960
Case 4	N ₂	1-20%	-	-	450-600	1,800

Table S2. Cu shell thickness of the prepared catalysts.

Sample	Cu Shell thickness (mm)					
	1	2	3	4	5	Mean
OD-Cu(1)	0.99	1.05	1.00	0.97	0.99	1.00
VOD-Cu(1)	0.63	0.66	0.67	0.65	0.68	0.66
QD-Cu(1)	0.34	0.30	0.34	0.30	0.30	0.32
QD-Cu(5)	0.38	0.39	0.40	0.41	0.40	0.40
QD-Cu(10)	0.46	0.48	0.48	0.47	0.49	0.48
QD-Cu(15)	0.55	0.53	0.55	0.54	0.52	0.54

Table S3. Turnover frequency (TOF) value over OD-, VOD-, and QD-Cu(1)/ γ -Al₂O₃ catalysts.

Catalyst	Temp.(°C)	r ($\mu\text{mols}^{-1}\text{g}_{\text{cat}}^{-1}$)	Active site ($\mu\text{molg}_{\text{cat}}^{-1}$)	TOF (s^{-1})
OD-Cu(1)	450	0.011	135	7.8×10^{-5}
VOD-Cu(1)		0.014	139	9.9×10^{-5}
QD-Cu(1)		0.023	143	1.6×10^{-4}

Table S4. N₂O conversion over the QD-Cu(10)/ γ -Al₂O₃ catalyst at 1% N₂O concentration and different feed conditions with time on stream.

Section	1	2	3	4	5	6	7	8	9	10	11	12	13	14
Balance	N ₂	Air	Air	Air	N ₂	N ₂	N ₂	N ₂	Air	Air	Air	N ₂	N ₂	N ₂
Steam (%)	-	-	7.5	-	-	1.8 → 7.5	7.5	7.5	7.5	7.5	-	-	-	-
Temp. (°C)	500	500	500	500	500	550 → 580	580	580	580	600	570	500	R.T	500
Conv. (%)	~99	~83	~54	~83	~99	~73	~98	~98	~96	~98	~99	~99	0	~99
Time (h)	24	24 -48	48 -72	72 -96	96 -161	161 -166	166 -171	171 -183	183 -190	190 -207	207 -231	231 -291	291 -313	313 -360

Table S5. N₂O conversion over the QD-Cu(10)/ γ -Al₂O₃ catalyst at 20% N₂O concentration and different feed conditions with time on stream.

Section	1	2	3	4	5	6	7	8	9	10
Balance	N ₂	Air	Air	Air	Air	Air	Air	N ₂	N ₂	N ₂
Steam (%)	-	-	-	-	7.5	7.5	7.5	7.5	7.5	-
Temp. (°C)	550	550	550 →600	600	600	600 →630	630 →650	650	650 →640	640 →550
Conv. (%)	~99	~95	~99	~99	~96	~98	~99	~99	~99	~99
Time (h)	356	357 -358	358-372		373 -375	375 -376	377 -397	397 -399	400 -422	422 -500

Table S6. Long-term stability test of various catalysts in N₂O decomposition.

No.	Catalyst	Shape	Feed condition	GHSV (h ⁻¹)	T. (°C)	Initial conv. value (%)	Durability (%)	Ref.
a	Sm _{0.06} Ni	Powder	2000 ppmv N ₂ O + 5 vol.% H ₂ O in Ar balance	20,000	350	59	56 after 8 h	¹
b	Ce ₂₀ CO	Powder	1000 ppm N ₂ O in He balance	80,000	350	90	54 after 24 h	²
c	Co/MgO-15%	Powder	1% N ₂ O in He balance	30,000	500	100	100 after 100 h	³
d	Pb _{0.04} Co	Powder	2000 ppmv N ₂ O in Ar with or without 10 vol.% CO ₂ + 5vol.% O ₂	20,000	350	100	100 after 15 h	⁴
e	CuO	Powder	2600 ppm N ₂ O in He balance, p=0.3 MPa	19,000	480	100	5 after 15 h	⁵
	Cu _{0.67} Ce _{0.33} O _y	Powder	2600 ppm N ₂ O in He balance, p=0.3 MPa	19,000	480	100	91 after ~120 h	
f	Cu-ZSM-5	Powder	5000 ppm N ₂ O in He balance	-	475	80	80 after 50 h	⁶
g	γ-Al ₂ O ₃	Pellets	1 mol.% N ₂ O in N ₂ balance	1,818	700	100	100 after 350 h	⁷
h	Cu(10)/γ-Al ₂ O ₃	Pellets	1 mol.% N ₂ O, 0-7.5% H ₂ O in N ₂ or Air balance	1,800 -1,960	500- 600	99	99 after 360 h	This study
i			20 mol.% N ₂ O, 0-7.5% H ₂ O in N ₂ or Air balance	1,800 -1960	550- 650	99	99 after 500 h	

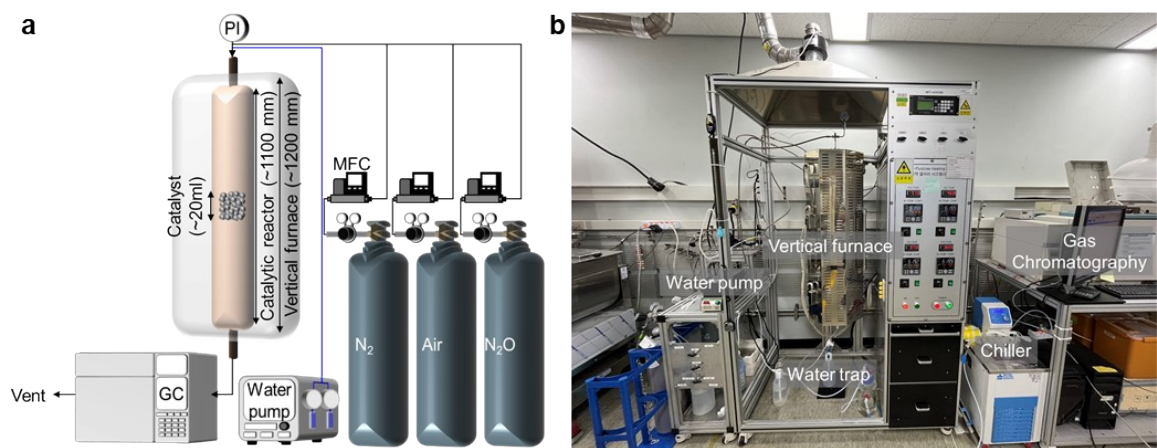


Fig. S1. (a) Schematic diagram and (b) optical image of the N_2O decomposition test system.

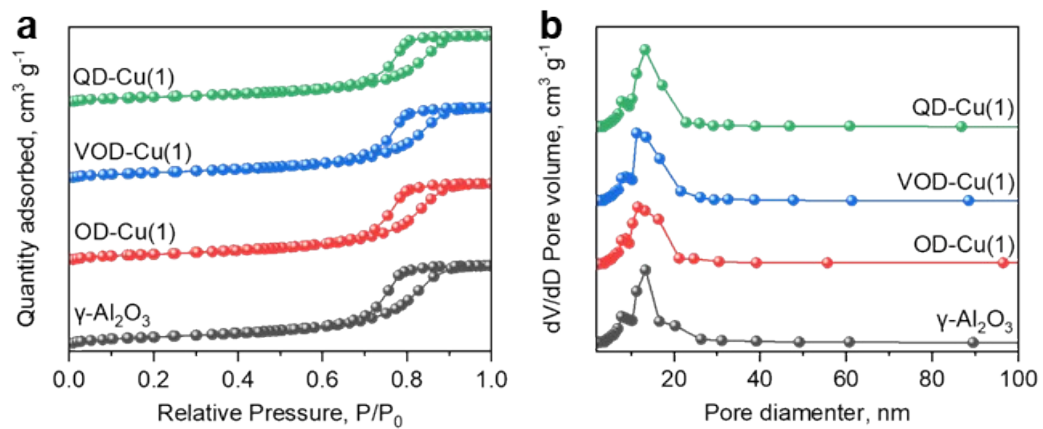


Fig. S2. (a) N₂ adsorption and desorption isotherms and (b) pore size distributions of the γ -Al₂O₃ and OD-, VOD-, and QD-Cu(1)/ γ -Al₂O₃ catalysts.

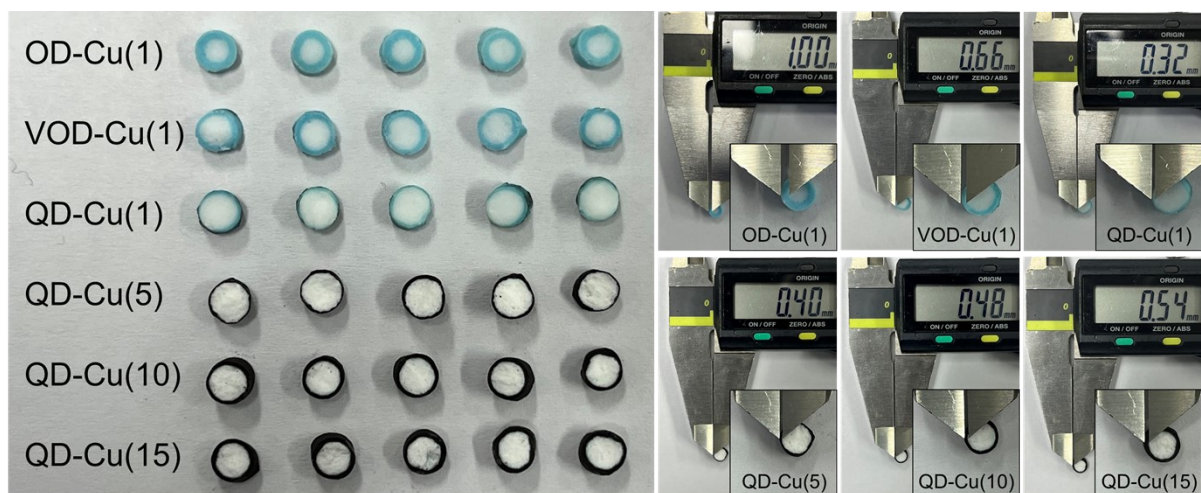


Fig. S3. Cross-sectional image of the prepared catalysts.

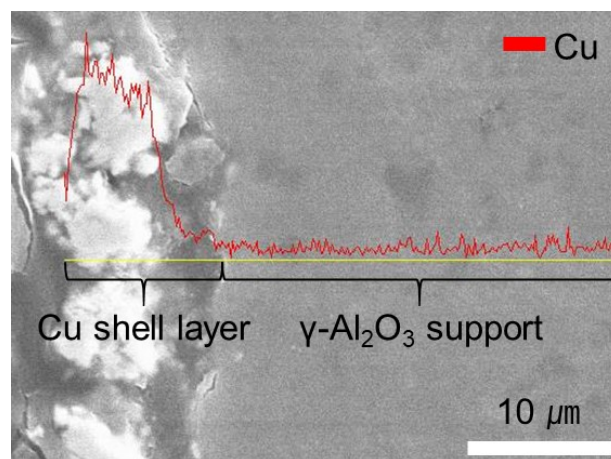


Fig. S4. EDS line scanning analysis of the QD-Cu(10)/ γ -Al₂O₃ catalyst.

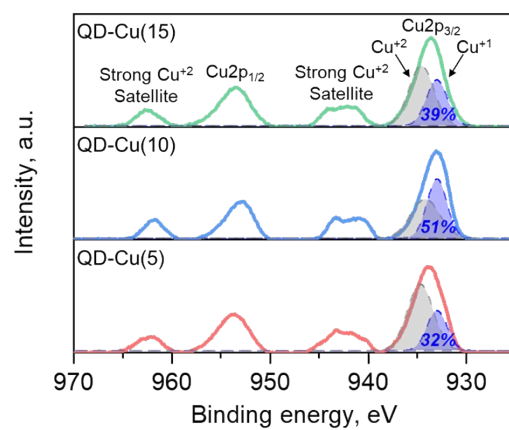


Fig. S5. XPS spectra of Cu 2p of the QD-Cu(x)/ γ - Al_2O_3 catalysts (x: 5, 10, 15 wt.%).

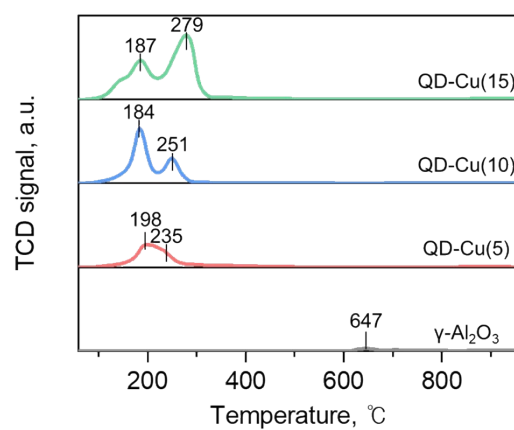


Fig. S6. H₂-TPR curves for the γ -Al₂O₃ and of the QD-Cu(x)/ γ -Al₂O₃ catalysts (x: 5, 10, 15 wt.%).

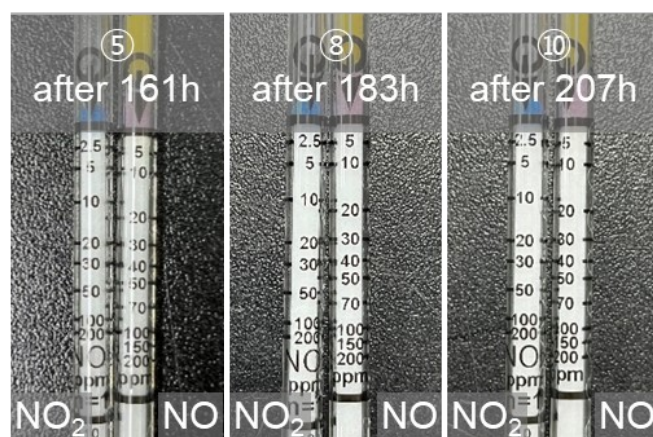


Fig. S7. NO_x (NO and NO₂) concentration at the outlet of the catalytic reactor measured by a gas detector during the deN₂O test using the QD-Cu(10)/ γ -Al₂O₃ catalyst.

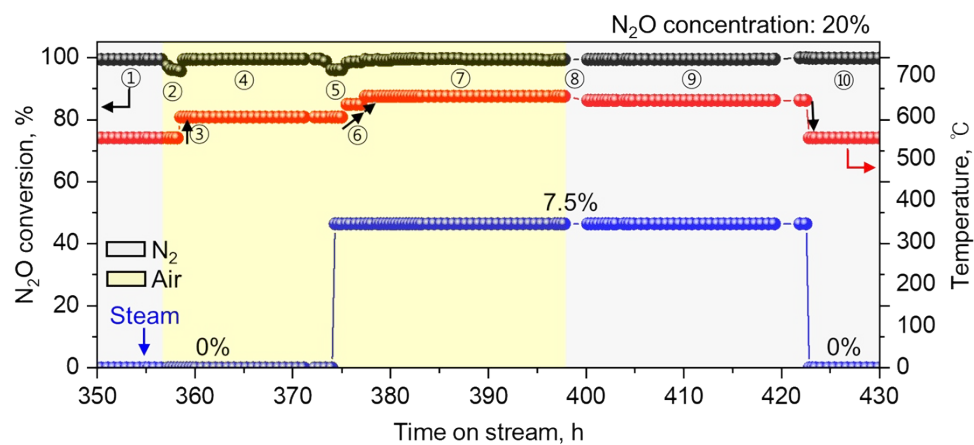
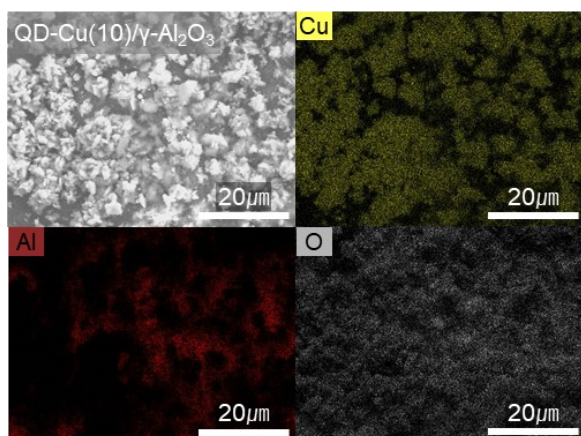


Fig. S8. N₂O conversion over the QD-Cu(10)/ γ -Al₂O₃ catalyst at 20% N₂O concentration under different feed conditions with time on stream.



Element	Weight%
O K	32.88
Al K	16.46
Cu K	50.65
Totals	100.00

Fig. S9. SEM/EDS mapping analysis after 500hr stability test of the QD-Cu(10)/ γ -Al₂O₃ catalyst surface.

References

1. J. Qi, X. Qi, Y. Pan, J. Cui, Y. Xiong, W. Shan and H. Yu, Appl. Surf. Sci., 2023, **611**, 155657.
2. Y. You, H. Chang, L. Ma, L. Guo, X. Qin, J. Li and J. Li, Chem. Eng. J., 2018, **347**, 184-192.
3. Q. Shen, L. Li, J. Li, H. Tian and Z. Hao, J. Hazard. Mater., 2009, **163**, 1332-1337.
4. H. Yu, M. Tursun, X. Wang and X. Wu, Applied Catalysis B: Environmental, 2016, **185**, 110-118.
5. H. Zhou, Z. Huang, C. Sun, F. Qin, D. Xiong, W. Shen and H. Xu, Applied Catalysis B: Environmental, 2012, **125**, 492-498.
6. W. Zou, P. Xie, W. Hua, Y. Wang, D. Kong, Y. Yue, Z. Ma, W. Yang and Z. Gao, J. Mol. Catal. A: Chem., 2014, **394**, 83-88.
7. E.-H. Lee, T.-W. Kim, S. Byun, D.-W. Seo, H.-J. Hwang, J. Baek, E.-S. Jeong, H. Kim and S.-K. Ryi, Clean Technology, 2023, **29**, 126-134.