

Supplementary information for

Enhancing Ammonia Recovery Efficiency through pH Polarization in Bipolar Membrane Electrodialysis

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Table S1 Initial and final pH of the reactors used in back-diffusion experiments

	Test 1		Test 2		Test 3	
	L	H	L	H	L	H
Initial	6.35	6.26	13.56	11.20	6.51	11.22
	±	±	±	±	±	±
	0.20	0.13	0.09	0.03	0.10	0.13
Final	6.75	6.16	13.72	11.38	6.48	11.31
	±	±	±	±	±	±
	0.10	0.11	0.09	0.13	0.12	0.27

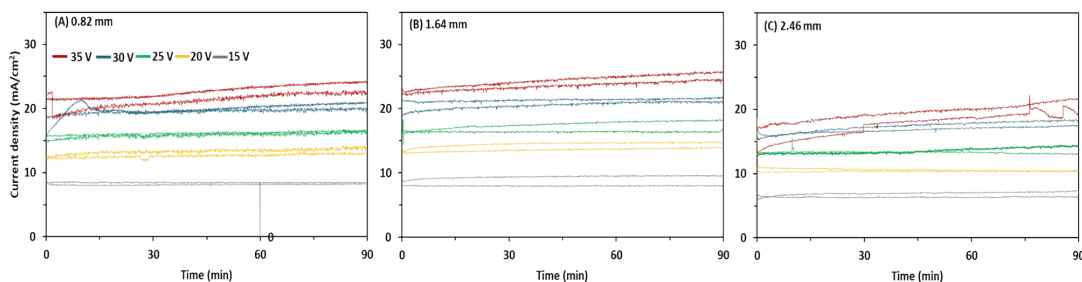


Figure S1 Change in current density over time at different voltage applications with (A) 0.82, (B) 1.64, and (C) 2.46 mm intermembrane distances

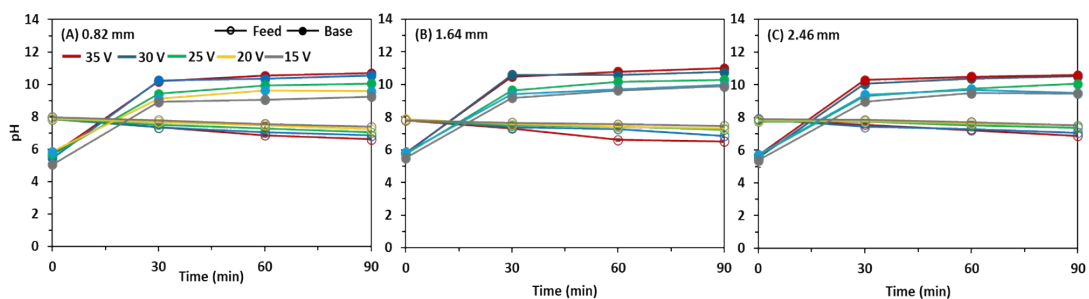


Figure S2 Change in conductivity of feed and base reservoirs over time at different voltage applications with (A) 0.82, (B) 1.64, and (C) 2.46 mm intermembrane distances

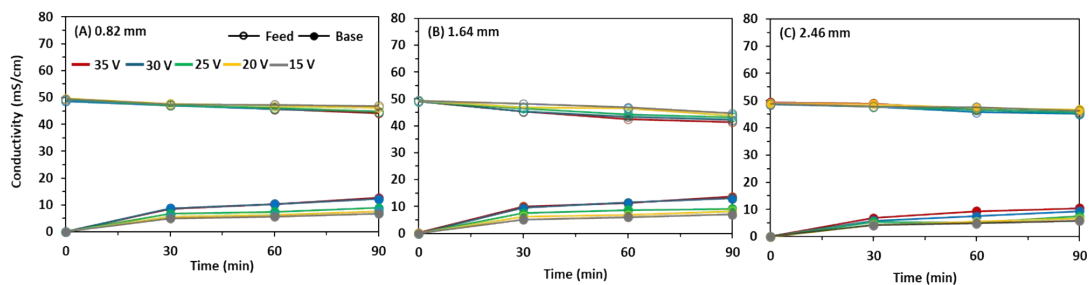


Figure S3 Change in pH of feed and base reservoirs over time at different voltage applications with (A) 0.82, (B) 1.64, and (C) 2.46 mm intermembrane distances

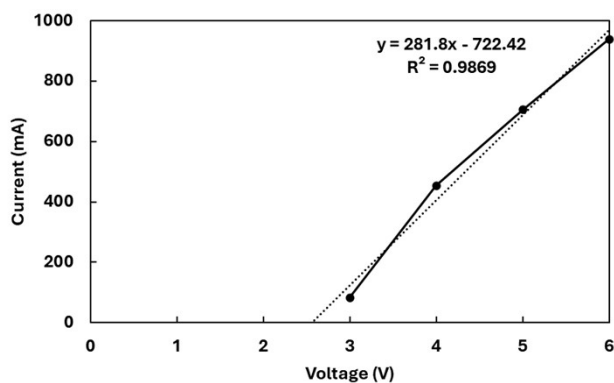


Figure S4 Change of current with voltage for estimation of voltage drop in the electrode rinse cells