

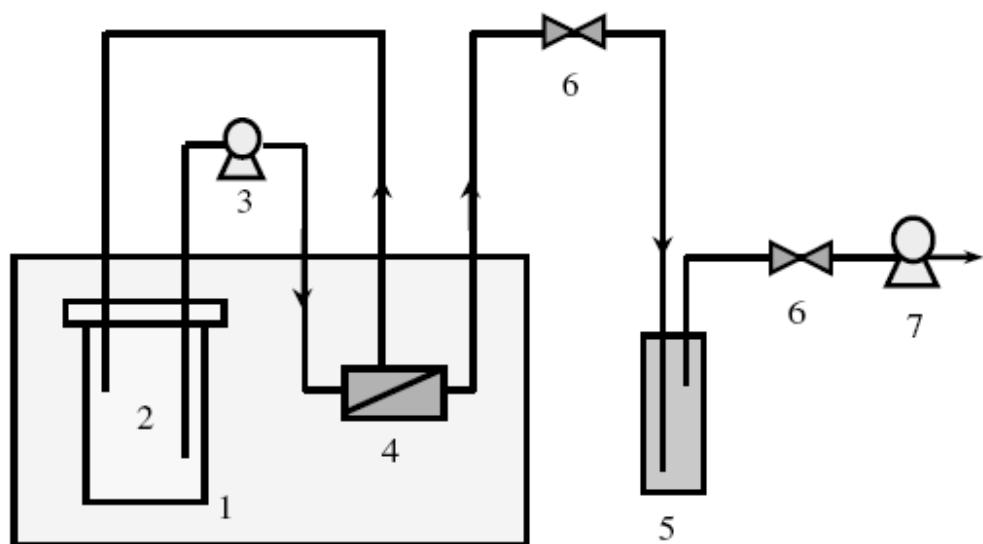
**Supporting information**

**Mussel-Inspired Polydopamine Modification of Supports for  
Facile Synthesis of Zeolite LTA Molecular Sieve Membranes**

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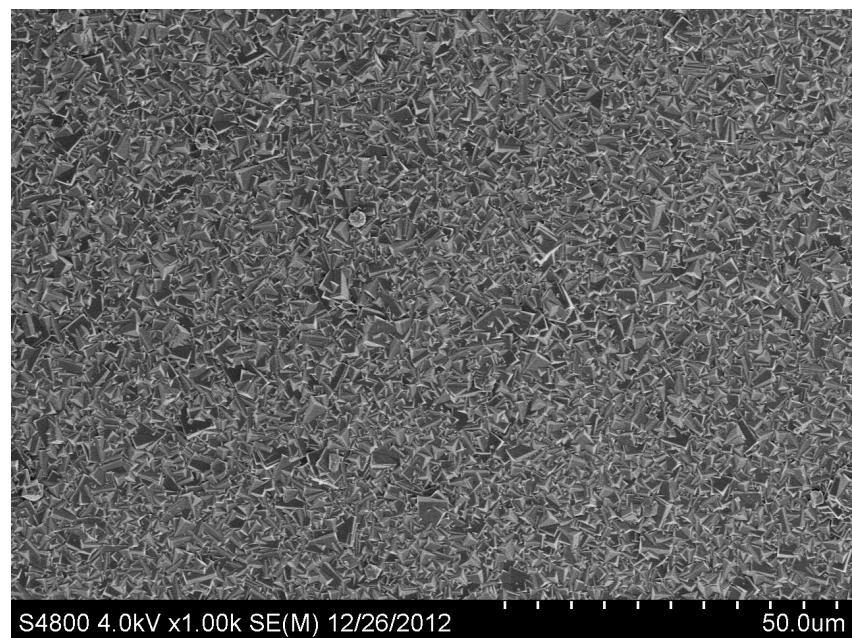
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**Figure S1**



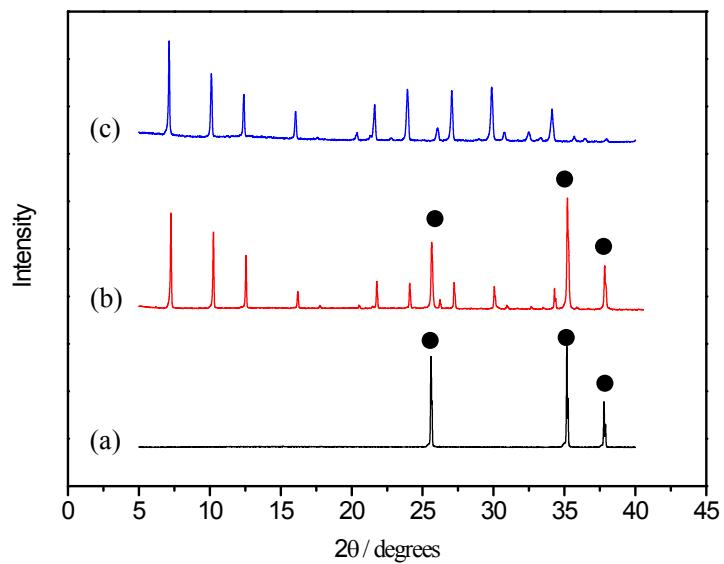
**Figure S1.** Schematic diagram of experimental apparatus for pervaporation. (1) Water bath, (2) liquid tank, (3) circle pump, (4) permeation cell, (5) cold traps, (6) ball value, (7) vacuum pump.

**Figure S2**



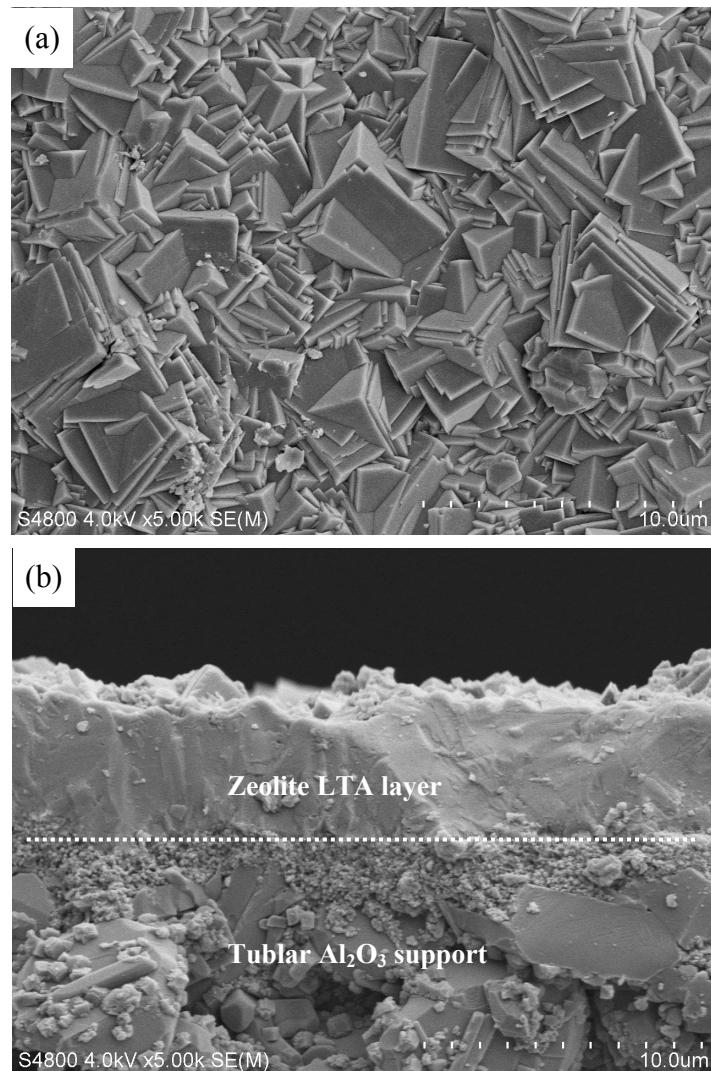
**Figure S2.** Top view FESEM image of the zeolite LTA membrane at low magnification prepared on polydopamine modified Al<sub>2</sub>O<sub>3</sub> disk.

**Figure S3**



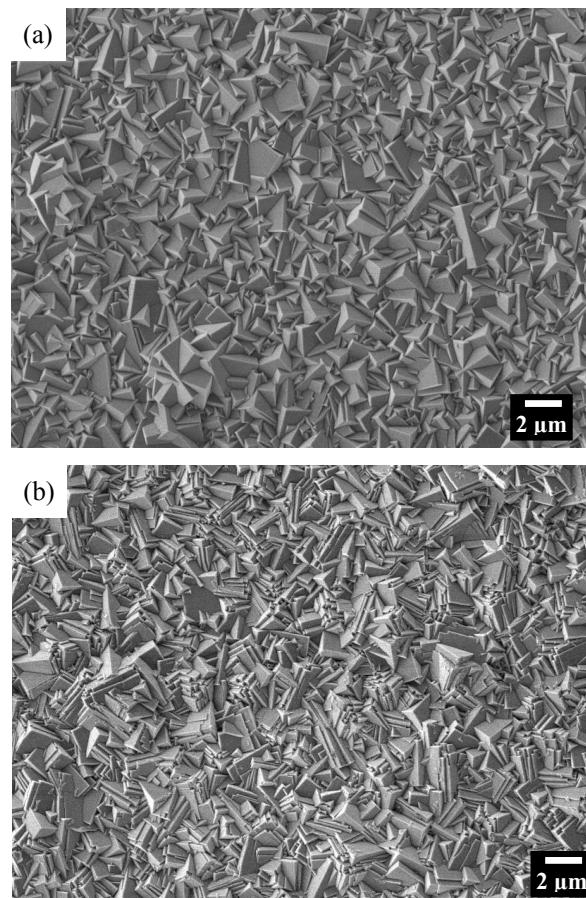
**Figure S3.** XRD patterns of the  $\text{Al}_2\text{O}_3$  support (a), zeolite LTA membrane prepared on polydopamine functionalized  $\text{Al}_2\text{O}_3$  support (b), and zeolite LTA powder (c). (●):  $\text{Al}_2\text{O}_3$  support, (not marked): zeolite LTA.

**Figure S4**



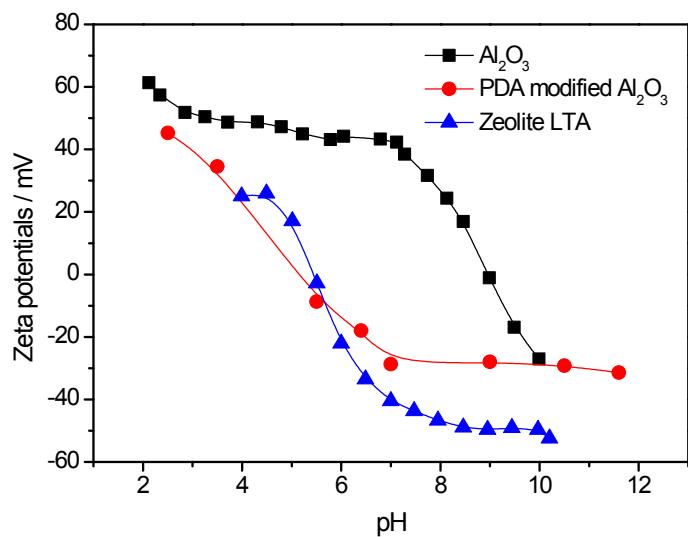
**Figure S4.** Top view (a) and cross-section FESEM images of the zeolite LTA membrane prepared on polydopamine functionalized  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> tubes.

**Figure S5**



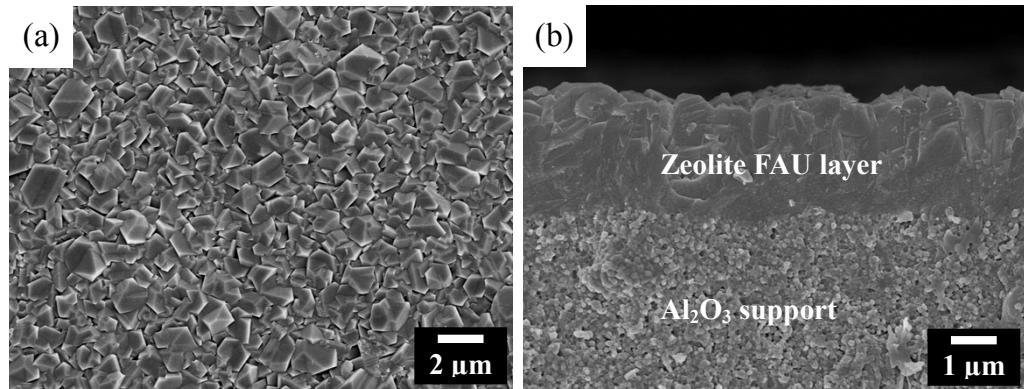
**Figure S5.** Top view FESEM images of the zeolite LTA membrane prepared on PDA-modified glass plate (a) and stainless steel disk (b).

**Figure S6**



**Figure S6.** Zeta potential of  $\text{Al}_2\text{O}_3$  (A. Huang, et al, *Chem. Mater.* **2010**, *22*, 4353), PDA modified  $\text{Al}_2\text{O}_3$  and zeolite LTA particles (A. Huang, et al, *Chem. Mater.* **2010**, *22*, 4353) suspended in water as function of pH.

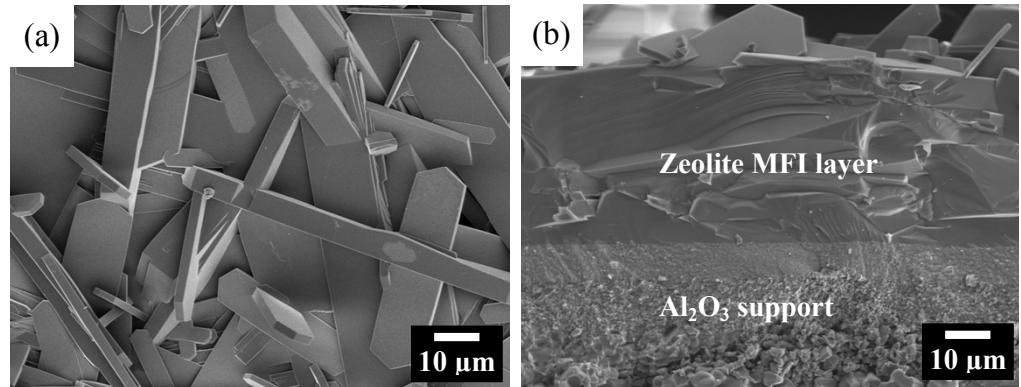
**Figure S7**



**Fig. S7.** Top view (a) and cross-section (b) FESEM images of the zeolite FAU membrane prepared on PDA-modified Al<sub>2</sub>O<sub>3</sub> disks.

For synthesis of the zeolite FAU membrane on the PDA-modified  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> disk, a clear synthesis solution with the molar ratio of 70Na<sub>2</sub>O : 1Al<sub>2</sub>O<sub>3</sub> : 20SiO<sub>2</sub> : 2000H<sub>2</sub>O, was prepared by mixing aluminate solution and silicate solution at room temperature according to the procedure reported elsewhere [A. Huang, N. Wang and J. Caro, *J. Membr. Sci.* 2012, **389**, 272]. The PDA-modified or non-modified  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> disks were horizontally placed face down in a Teflon-lined stainless steel autoclave, and then the synthesis solution was poured into. After in-situ growth for 24 h at 348 K, the solution was decanted off and the membrane was washed with deionized water several times, and then dried in air at 383 K over night for characterization or permeation measurement.

**Figure S8**



**Fig. S8.** Top view (a) and cross-section (b) FESEM images of the zeolite MFI membrane prepared on PDA-modified Al<sub>2</sub>O<sub>3</sub> disks.

For synthesis of the zeolite MFI membrane on the PDA-modified  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> disk, a clear synthesis solution with the molar ratio of 1TBABr : 2NaOH : 10SiO<sub>2</sub> : 600H<sub>2</sub>O, was prepared by mixing TBABr, NaOH and silicate solution in water at room temperature according to the procedure reported elsewhere with minor modification [H. Chen, C. Song and W. Yang, *Microporous Mesoporous Mater.* 2007, **102**, 249]. The PDA-treated or non-treated  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> disks were horizontally placed face down in a Teflon-lined stainless steel autoclave, and then the synthesis solution was poured into. After in-situ growth for 48 h at 453 K, the solution was decanted off and the membrane was washed with deionized water several times, and then dried in air at 383 K over night for characterization or permeation measurement.

**Table S1**

**Table S1.** Comparisons of the pervaporation properties of the as-synthesized zeolite LTA membrane prepared in this study with literature data.

Supports	Seeding	Mixtures (A / B)	Concentration (A wt%)	T (K)	Flux (kg/ m <sup>2</sup> h)	$\alpha_{A/B}$	References
Mullite tube	Yes	H <sub>2</sub> O/EtOH	10	348	2.08	42000	S1
ZnO <sub>2</sub> tube	No	H <sub>2</sub> O/i-PrOH	10	343	0.5	5000	S2
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	Yes	H <sub>2</sub> O/i-PrOH	5	343	1.67	10000	S3
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/EtOH	5	318	0.23	8300	S4
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/i-PrOH	5	343	1.02	9481	S5
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/i-PrOH	5	343	1.49	3781	S6
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	Yes	H <sub>2</sub> O/EtOH	5	393	4.3	5600	S7
		H <sub>2</sub> O/i-PrOH			5.6	6000	
TiO <sub>2</sub> coated stainless-steel	No	H <sub>2</sub> O/EtOH	5	318	0.86	54000	S8
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	Yes	H <sub>2</sub> O/EtOH	10	348	5.6	5000	S9
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	Yes	H <sub>2</sub> O/EtOH	2.65	333	2.1	2140	S10
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/i-PrOH	5	343	1.67	4700	S11
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/EtOH	10	338	0.51	10000	S12
Polymer-zeolite CHFs	No	H <sub>2</sub> O/EtOH	10	348	9.2	>10000	S13
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	Yes	H <sub>2</sub> O/EtOH	10		2.6	>10000	S14
				333	2.06	>10000	
$\alpha$ -Al <sub>2</sub> O <sub>3</sub> tube	No	H <sub>2</sub> O/EtOH	5	348	2.58	>10000	This study
				358	3.28	>10000	
				373	4.13	>10000	

### References

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