

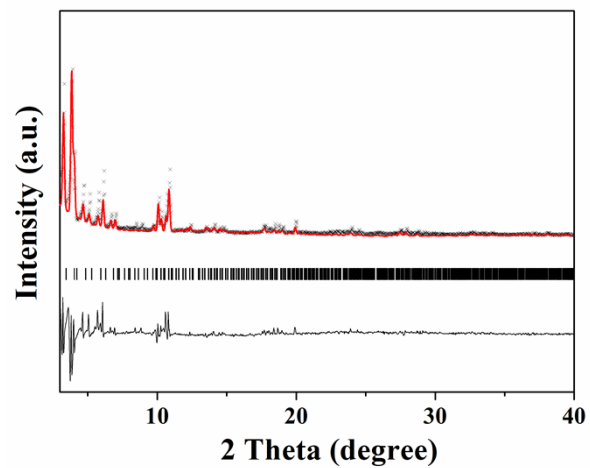
## Supporting Information (ESI†)

### **Porous metal–organic framework MIL-100(Fe) catalyst as an efficient catalyst for selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>**

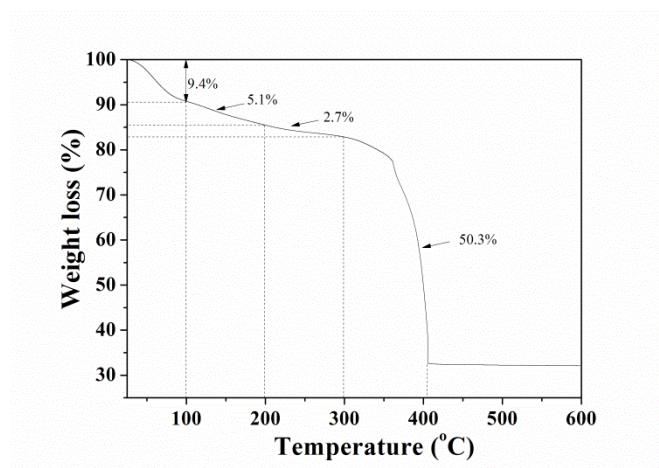
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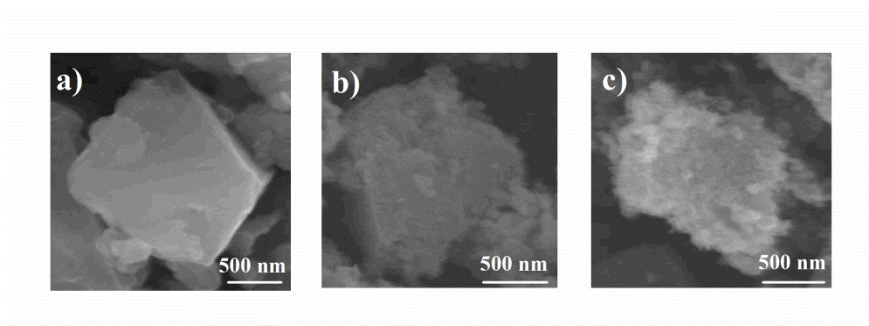
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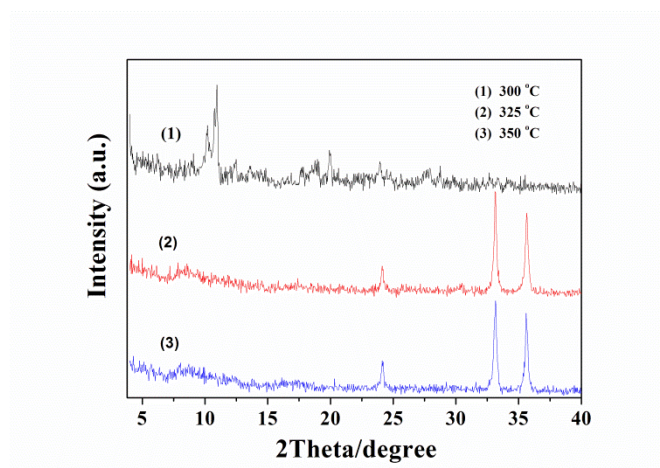
**Figure S1** Rietveld refinement plot for as-synthesized MIL-100(Fe) in the space group  $Fd-3m$  (NO. 227).



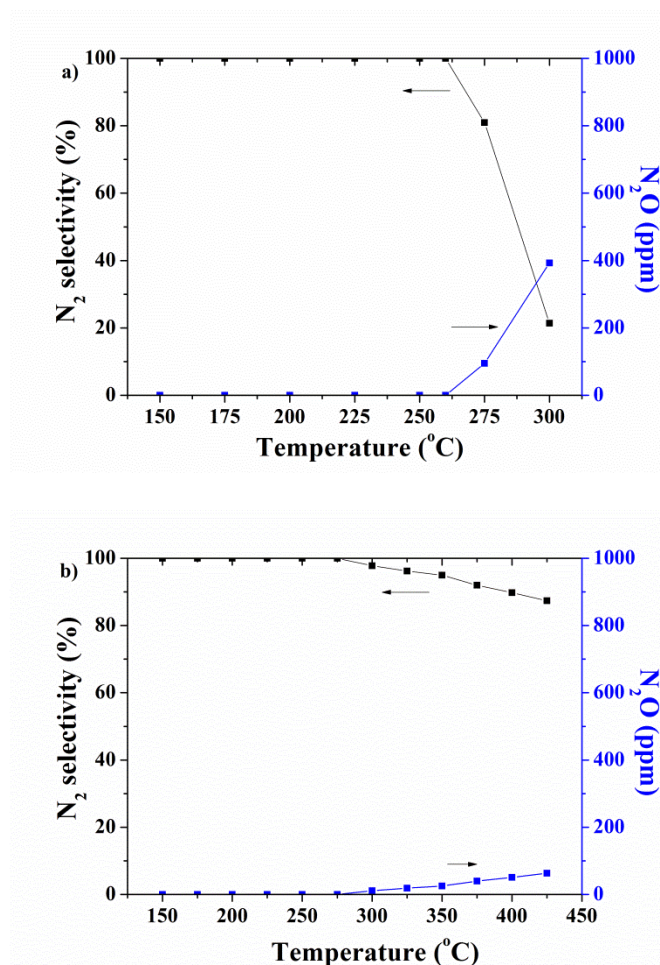
**Figure S2** TGA under air (5 °C /min heated rate) of MIL-100(Fe).



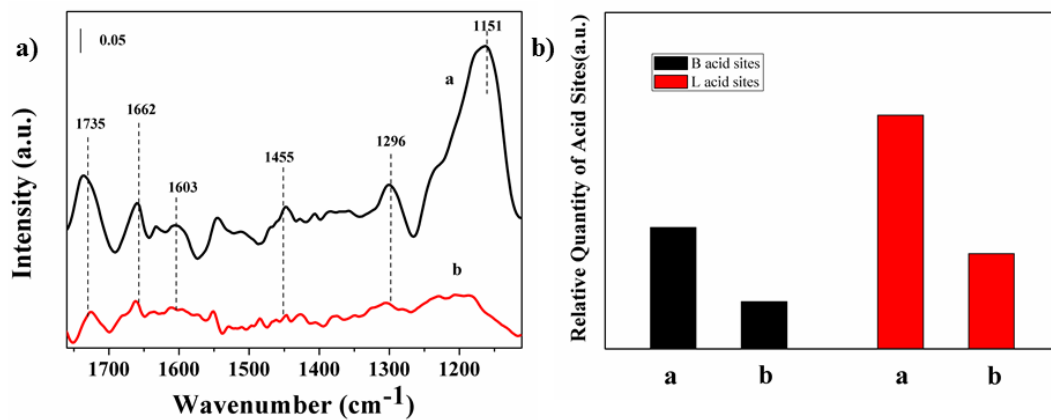
**Figure S3** SEM image of MIL-100(Fe) after catalytic activity test at a) 300 °C ; b) 325 °C; c) 350 °C.



**Figure S4** Powder X-ray diffraction pattern of MIL-100(Fe) after catalytic activity test at a) 300 °C; b) 325 °C; c) 350 °C.



**Figure S5** a) N<sub>2</sub> selectivity and N<sub>2</sub>O formation of MIL-100(Fe) catalyst; b) N<sub>2</sub> selectivity and N<sub>2</sub>O formation of V<sub>2</sub>O<sub>5</sub>-WO<sub>3</sub>/TiO<sub>2</sub> catalyst. Reaction condition: [NH<sub>3</sub>] = 500 ppm, [NO<sub>x</sub>] = 500 ppm, [O<sub>2</sub>] = 4%, N<sub>2</sub> balance and GHSV = 30,000 h<sup>-1</sup>.



**Figure S6** a) comparison of  $\text{NH}_3$  adsorption over MIL-100(Fe) catalysts before (a) and after durability test with  $\text{SO}_2$  and  $\text{H}_2\text{O}$  (b) at 250 °C; b) relative quantity of acid sites over these MIL-100(Fe) catalysts.