

Supporting information

One-pot catalytic conversion of methanol to C6-C21 hydrocarbons over bi-functional MFe₂O₄ (M = Ni, Zn, Mn, Co) catalysts

Huilong Lai,^{a,b} Zailei Zhang,^b Fangna Gu,^{b,*} Zhengming Yi,^{a,*} Ziyi Zhong,^c and Fabing Su^{b,*}

^a *School of Chemical Engineering, Xiangtan University, Xiangtan 411105, Hunan, China*

^b *State Key Laboratory of Multiphase Complex Systems, Institute of Process Engineering, Chinese Academy of Sciences, Beijing 100190, China*

^c *Institute of Chemical Engineering and Sciences, A*star, 1 Pesek Road, Jurong Island, Singapore 627833, Singapore*

*Corresponding author: fngu@ipe.ac.cn (F. Gu); YIZM@xtu.edu.cn (Z. Yi); fbsu@ipe.ac.cn (F. Su),

Tel.: +86-10-82544850; Fax: +86-10-82544851

S-1: synthesis conditions of catalysts

Table S1 The synthesis conditions used for prepared catalysts.

Sample	Ni(CH ₃ COO) ₂ (mmol)	Zn(CH ₃ COO) ₂ (mmol)	Mn(CH ₃ COO) ₂ (mmol)	Co(CH ₃ COO) ₂ (mmol)	FeCl ₃ (mmol)	CH ₃ COONa (mmol)	HOCH ₂ CH ₂ OH(mL)	H ₂ O (mL)
NiO	2.0	–	–	–	–	18	40	40
ZnO	–	2.0	–	–	–	18	40	40
Mn ₃ O ₄	–	–	2.0	–	–	18	40	40
Co ₃ O ₄	–	–	–	2.0	–	18	40	40
Fe ₃ O ₄	–	–	–	–	2.0	18	40	40
NiFe ₂ O ₄	1.0	–	–	–	2.0	18	40	40
ZnFe ₂ O ₄	–	1.0	–	–	2.0	18	40	40
MnFe ₂ O ₄	–	–	1.0	–	2.0	18	40	40
CoFe ₂ O ₄	–	–	–	1.0	2.0	18	40	40
Ni _{0.5} Co _{0.5} Fe ₂ O ₄	0.5	–	–	0.5	2.0	18	40	40
Zn _{0.5} Co _{0.5} Fe ₂ O ₄	–	0.5	–	0.5	2.0	18	40	40
Mn _{0.5} Co _{0.5} Fe ₂ O ₄	–	–	0.5	0.5	2.0	18	40	40

S-2: The XPS spectra of ZnFe₂O₄ catalyst reduced at 340 °C with H₂

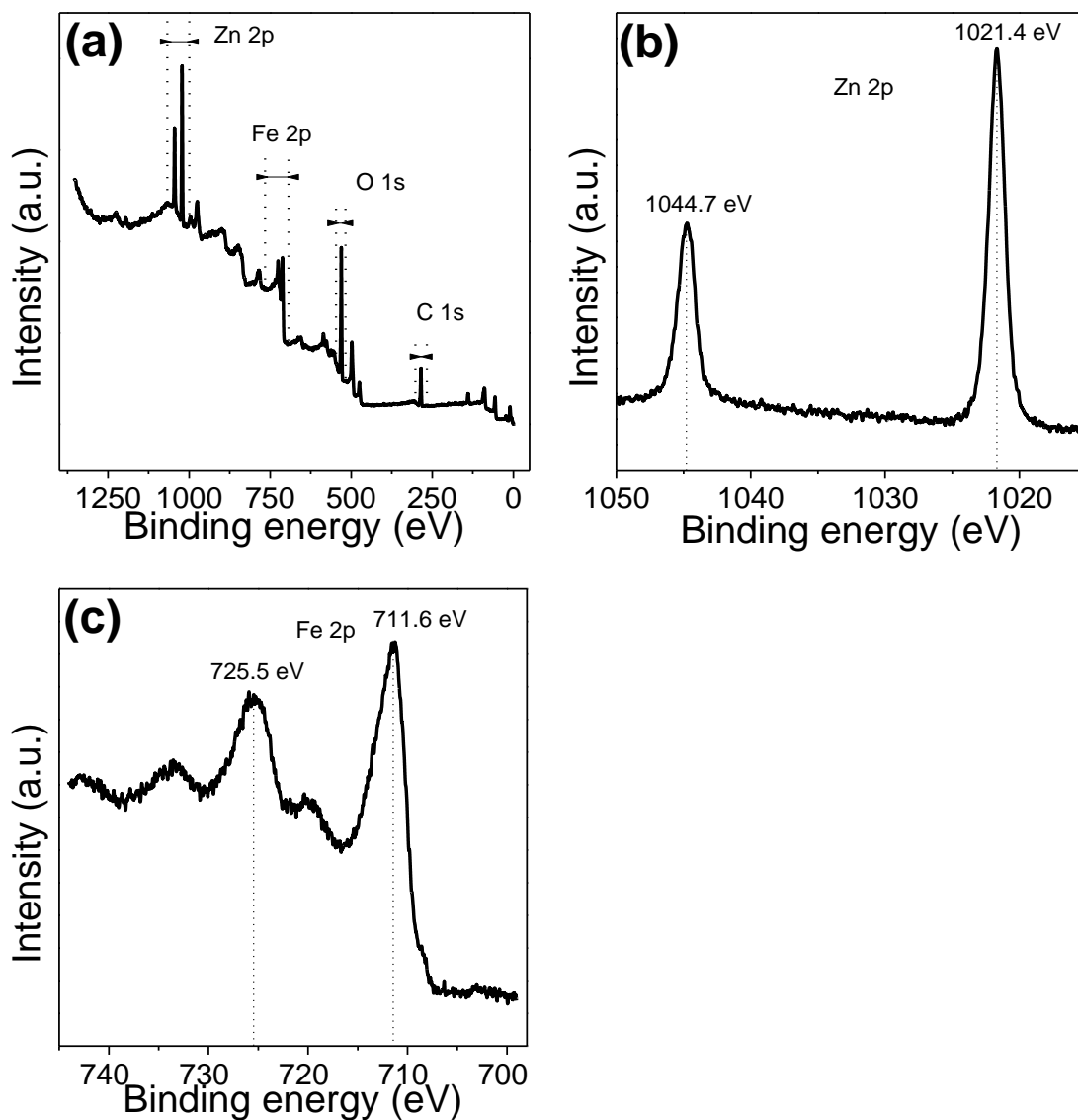


Fig. S1 XPS spectra of the ZnFe₂O₄ catalyst: (a) wide spectrum, (b) Zn2p and (c) Fe 2p spectrum.

S-3: XRD of used catalyst

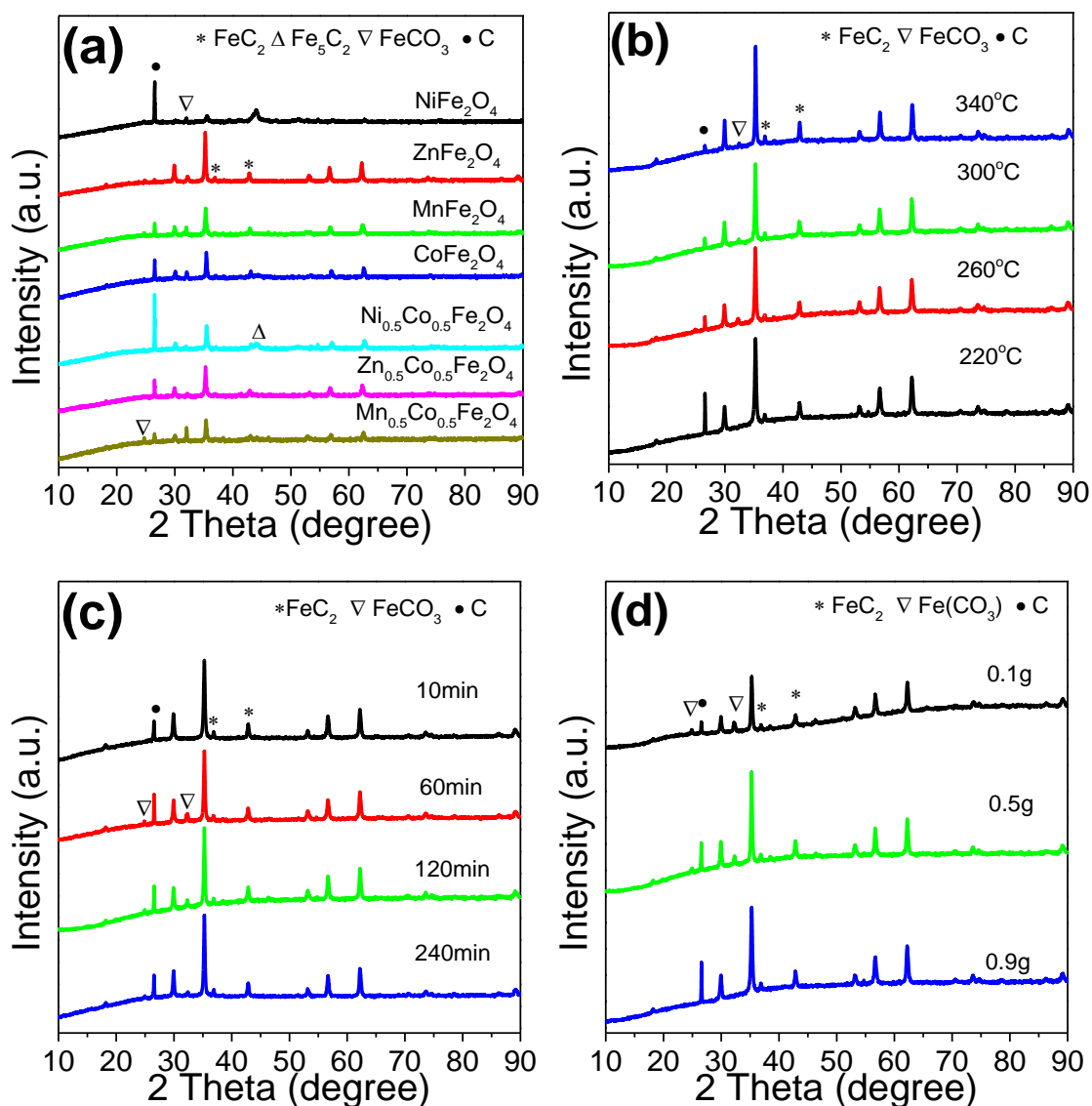


Fig. S2 XRD patterns of the used catalysts: (a) MFe₂O₄ and M_{0.5}Co_{0.5}Fe₂O₄ after reaction at 280 °C for 3 h, (b) ZnFe₂O₄ reacted at different temperature, (c) different reaction time, and (d) different catalyst amount.

S-4: SEM and elemental mapping characterization

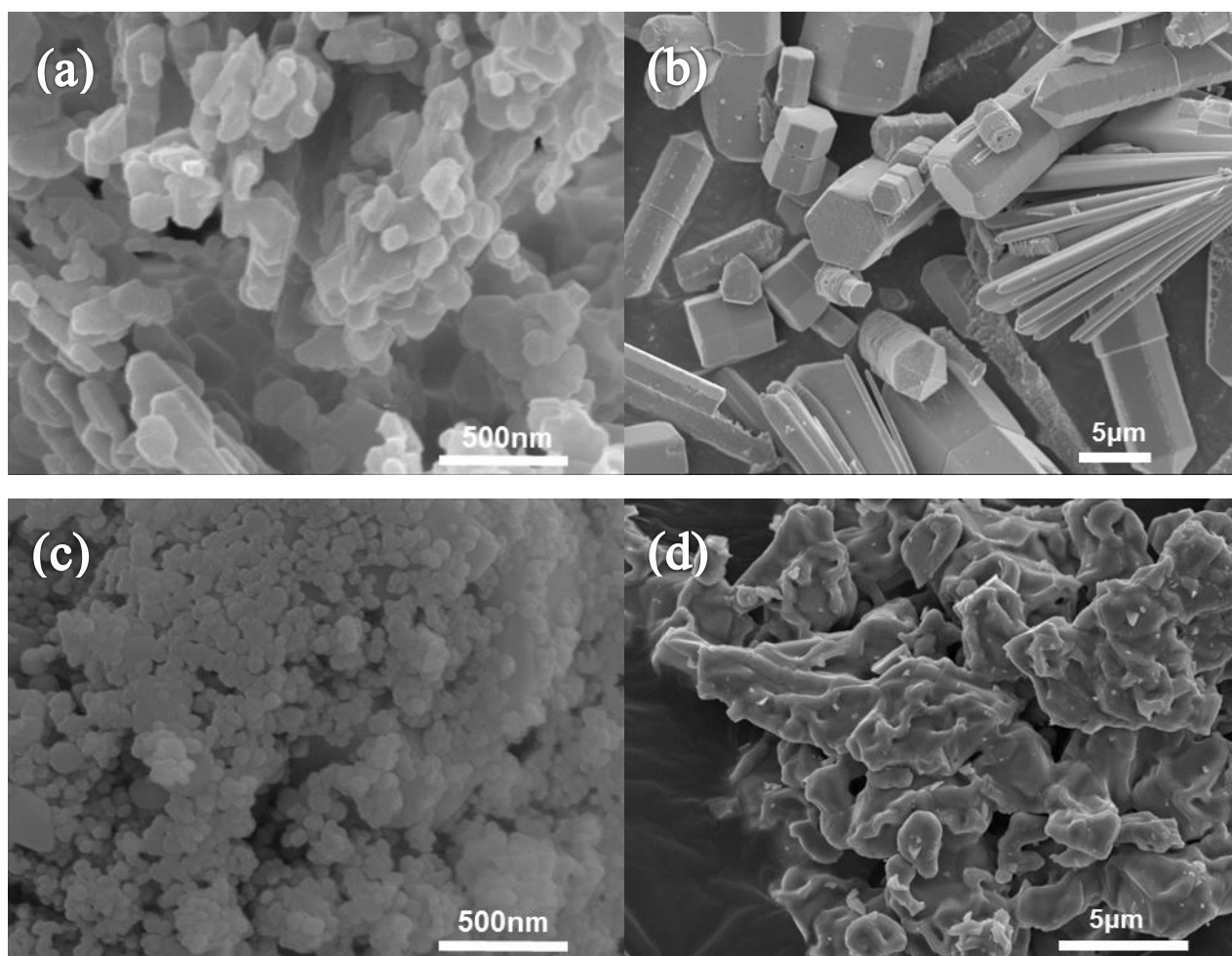


Fig. S3 SEM images of the catalysts: (a) NiO, (b) ZnO, (c) Mn₃O₄, and (d) Co₃O₄.

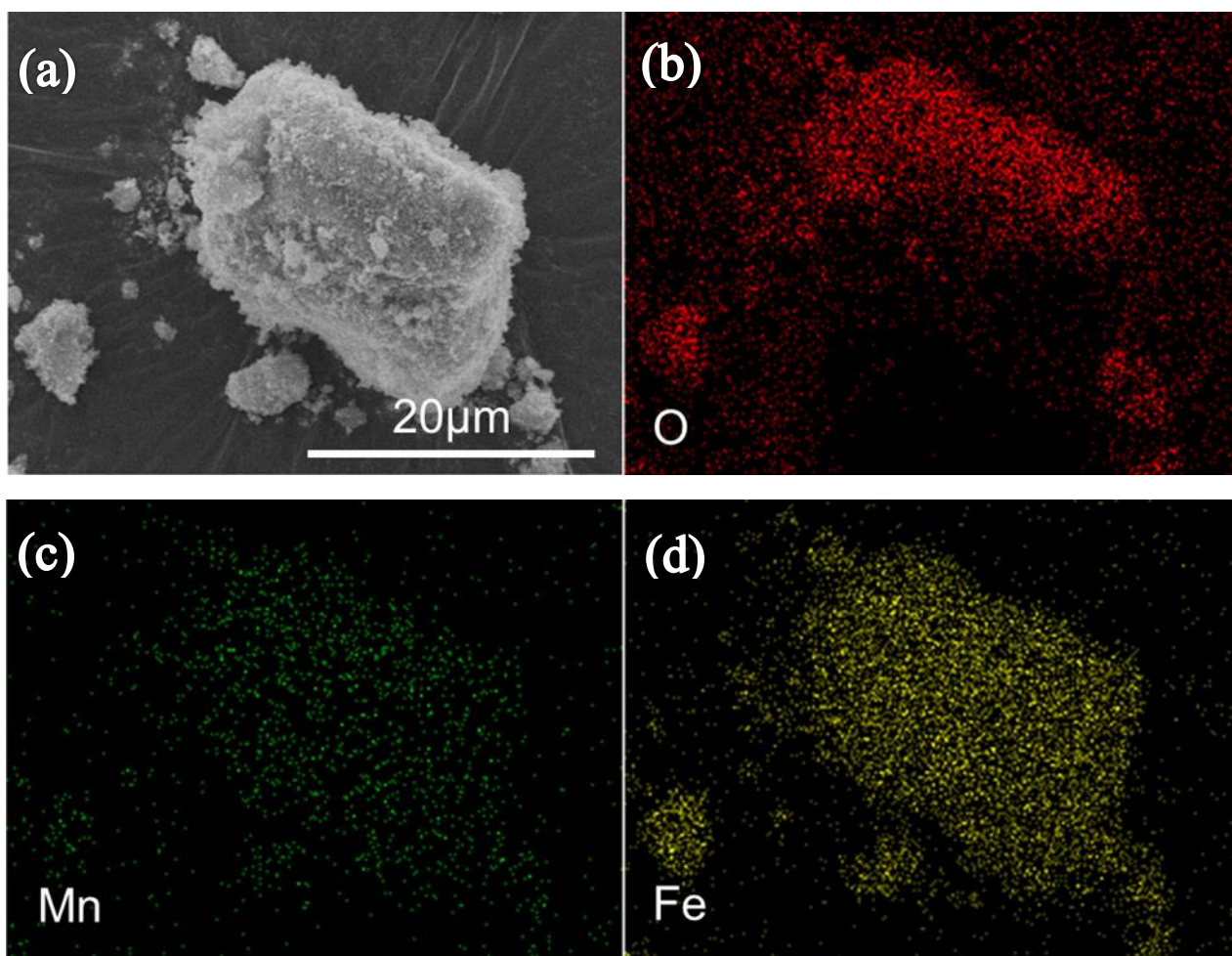


Fig. S4 SEM image of MnFe₂O₄ (a) and the corresponding elemental mapping images of O (b), Mn (c), and Fe (d).

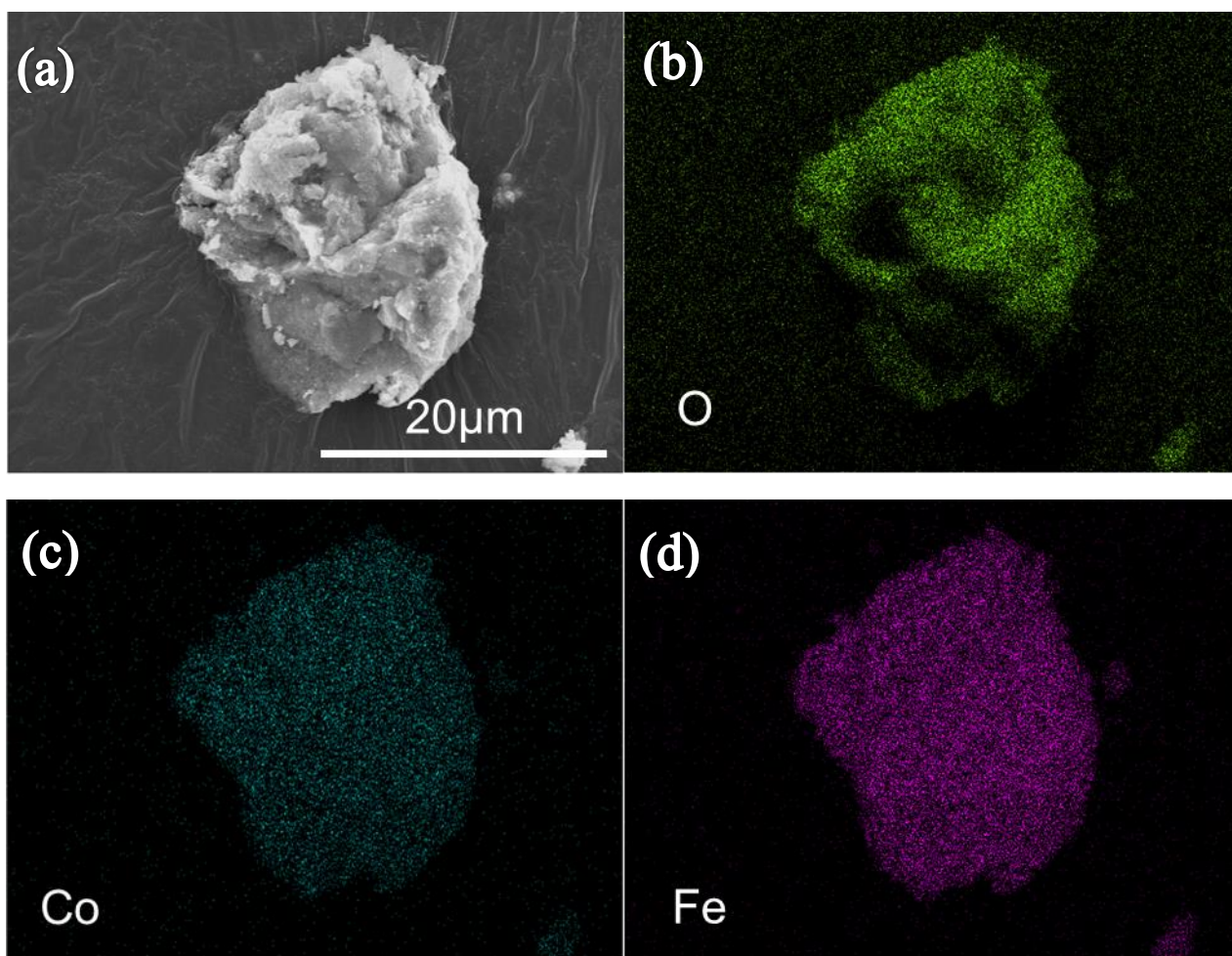


Fig. S5 SEM image of CoFe₂O₄ (a) and the corresponding elemental mapping images of O (b), Mn (c), and Fe (d).

S-5: The composition of C6-C21 hydrocarbon products under different conditions

Table S2 The composition of C6-C21 hydrocarbon in liquid products over MFe_2O_4 catalysts. (peak area %)

Entry	C6-C21 hydrocarbon	Catalyst			
		NiFe_2O_4	ZnFe_2O_4	MnFe_2O_4	CoFe_2O_4
1	2,4-dimethyl-Pentane	N/A	N/A	3.55	N/A
2	1,3-dimethyl-Cyclopentane	0.87	N/A	N/A	N/A
3	ethyl-Cyclopentane	N/A	N/A	N/A	0.95
4	2-methyl-Hexane	1.97	1.95	N/A	4.52
5	3-methyl-Hexane	1.81	2.30	N/A	4.95
6	3-Methyl-2-hexene	N/A	0.97	N/A	N/A
7	2,4-dimethyl-Hexane	2.11	3.14	N/A	N/A
8	1-Heptene	N/A	N/A	10.69	N/A
9	Heptane	5.65	14.76	7.88	21.21
10	2-methyl-Heptane	1.24	1.02	N/A	N/A
11	3-methyl-Heptane	N/A	N/A	N/A	3.92
12	4-methyl-Heptane	N/A	N/A	N/A	N/A
13	2-Heptene	N/A	1.20	3.73	N/A
14	3-Heptene	N/A	N/A	N/A	N/A
15	p-Xylene	N/A	N/A	N/A	1.01
16	Ethyl benzene	N/A	N/A	N/A	1.02
17	1-Octene	N/A	N/A	9.58	N/A
18	Octane	4.95	15.56	6.62	16.23
19	2-Octene	N/A	N/A	2.53	N/A
20	2-methyl-Octane	N/A	2.62	N/A	3.76
21	3-methyl-Octane	N/A	1.48	N/A	2.02
22	4-methyl-Octane	N/A	N/A	N/A	N/A
23	1-methyl-Indan	N/A	N/A	N/A	0.54
24	1-Nonene	N/A	N/A	6.96	N/A
25	Nonane	4.01	13.16	5.6	10.23
26	cis-2-Nonene	N/A	N/A	4.47	N/A
27	Decane	4.99	10.09	N/A	5.91
28	2-methyl-Decane	N/A	N/A	N/A	0.65
29	3-methyl-Decane	N/A	N/A	N/A	N/A
30	2-methyl-Nonane	N/A	0.95	N/A	1.15
31	3-methyl-Nonane	N/A	1.54	N/A	1.57
32	4-methyl-Nonane	N/A	1.04	N/A	2.26
33	5-(2-methylpropyl)-Nonane	N/A	0.93	N/A	0.87
34	1-Decene	N/A	N/A	3.96	N/A
35	Undecane	N/A	N/A	4.21	3.08

36	1-ethyl-2-heptyl-Cyclopropane	N/A	N/A	2.33	N/A
37	1-Decene	N/A	N/A	1.61	N/A
38	1-Undecene	N/A	N/A	2.28	N/A
39	Undecane	N/A	N/A	3.59	N/A
40	1-Undecene	N/A	N/A	1.74	N/A
41	1-Undecene	N/A	N/A	1.13	N/A
42	1-Dodecene	N/A	N/A	1.41	N/A
43	Dodecane	6.37	12.18	3.53	1.76
44	nonyl-Cyclopropane	N/A	N/A	1.46	N/A
45	3-Tetradecene	N/A	N/A	0.96	N/A
46	Tridecane	3.71	3.66	2.06	0.90
47	Tetradecane	2.15	2.57	1.22	N/A
48	Hexadecane	3.80	2.88	N/A	N/A
49	(2,3-dimethyldecyl)-Benzene	N/A	N/A	N/A	0.81
Total peak area %		43.63	94	93.1	89.32

Note: Data in this table represent the percentage of peak area detected by GC/MS. "Total peak area %" represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. "N/A" represents not available.

Table S3 The composition of C6-C21 hydrocarbon in liquid products over $M_{0.5}Co_{0.5}Fe_2O_4$ catalysts.

(peak area %)

Entry	C6-C21 hydrocarbon	Catalyst		
		$Ni_{0.5}Co_{0.5}Fe_2O_4$	$Zn_{0.5}Co_{0.5}Fe_2O_4$	$Mn_{0.5}Co_{0.5}Fe_2O_4$
1	2,4-dimethyl-Pentane	N/A	N/A	3.41
2	2-methyl-Hexane	2.43	N/A	N/A
3	3-methyl-Hexane	2.04	2.49	3.4
4	Heptane	10.1	14.61	17.29
5	2-Heptene	N/A	1.95	N/A
6	3-methyl-Heptane	2.06	4.19	3.17
7	Toluene	N/A	N/A	N/A
8	2,4-dimethyl-Hexane	N/A	15.62	14.42
9	Ethyl benzene	N/A	N/A	1.23
10	5-methyl-Undecane	N/A	N/A	3.16
11	Octane	12.64	N/A	N/A
12	2-Octene	N/A	0.97	N/A
13	2-methyl-Octane	2.71	N/A	N/A
14	3-methyl- Octane	1.79	2.36	2.15
15	4-methyl- Octane	N/A	2.38	N/A
16	2,4,6-trimethyl-Octane	N/A	N/A	5.95
17	o-Xylene	N/A	N/A	N/A
18	p-Xylene	0.88	N/A	N/A
19	Nonane	12.09	11.56	10.26
20	4-methyl-Nonane	1.55	N/A	1.99
21	2-methyl-Nonane	1.12	N/A	0.99
22	3-methyl-Nonane	1.42	0.98	1.28
23	2,5-dimethyl-Nonane	0.57	N/A	N/A
24	5-(2-methylpropyl)-Nonane	0.44	N/A	N/A
25	Decane	8.76	7.7	N/A
26	2-methyl-Decane	0.76	N/A	1.17
27	3-methyl-Decane	0.68	N/A	1.04
28	4-methyl-Decane	0.56	N/A	N/A
29	Indane	N/A	N/A	N/A
30	1,3-dimethyl-Benzene	0.68	N/A	0.96
31	(2,3-dimethyldecyl)- Benzene	N/A	N/A	N/A
32	2-methyl-Decane	N/A	N/A	N/A
33	(2-methyloctyl)-Benzene	3.63	N/A	N/A
34	3-methyl-Decane	N/A	N/A	N/A
35	1-methyl-2-(2-propenyl)-Benzene	N/A	N/A	N/A
36	1-methyl-Indan	N/A	N/A	N/A
37	Undecane	5.35	5.06	3.02
38	4-ethyl-Octane	N/A	N/A	N/A

39	Dodecane	2.35	5.28	N/A
40	Tridecane	1.67	1.95	N/A
41	Tetradecane	1.02	N/A	N/A
42	Hexadecane	N/A	1.20	N/A
Total peak area %		77.3	78.3	76.38

Note: Data in this table represent the percentage of peak area detected by GC/MS. “Total peak area %” represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. “N/A” represents not available.

Table S4 Effect of reaction temperature on the composition of C6-C21 hydrocarbon in liquid products over ZnFe₂O₄ catalyst. (peak area %)

Entry	C6-C21 hydrocarbon	Reaction temperature					
		240 °C	260 °C	280 °C	300 °C	320 °C	340 °C
1	2-methyl-Hexane	N/A	2.44	1.95	2.84	N/A	N/A
2	3-methyl-Hexane	N/A	2.21	2.30	3.22	3.181	2.98
3	3-Methyl-2-hexene	N/A	N/A	0.97	2.47	3.45	2.79
4	2,4,6-trimethyl-Heptane	N/A	N/A	N/A	N/A	N/A	3.61
5	Octane	2.20	N/A	N/A	N/A	N/A	N/A
6	1-Heptene	14.45	3.95	N/A	N/A	N/A	N/A
7	Heptane	3.03	13.79	14.76	18.16	17.25	14.85
8	2-Heptene	N/A	5.00	1.20	3.57	N/A	3.16
9	3-Heptene	N/A	2.76	N/A	1.71	6.43	1.50
10	2-methyl-Heptane	N/A	N/A	3.02	N/A	N/A	1.73
11	3-methyl- Heptane	N/A	N/A	N/A	N/A	N/A	3.06
12	2,4-dimethyl-Hexane	N/A	N/A	3.14	3.25	N/A	N/A
13	1-Octene	10.41	1.71	N/A	N/A	N/A	N/A
14	Octane	2.97	12.97	15.56	16.36	15.53	14.53
15	2-Octene	N/A	3.39	N/A	2.03	N/A	1.81
16	3-Octene	N/A	2.10	N/A	N/A	3.82	N/A
17	2-methyl-Octane	N/A	N/A	2.62	N/A	N/A	N/A
18	4-methyl-Octane	N/A	1.97	N/A	3.00	3.11	3.66
19	3-methyl-Octane	N/A	1.41	1.48	1.69	1.68	1.86
20	2,6,6-trimethyl-Octane	N/A	N/A	N/A	N/A	N/A	1.33
21	1-Nonene	9.13	1.39	N/A	N/A	0.83	N/A
22	2-Nonene	N/A	4.16	N/A	1.42	1.76	1.58
23	Nonane	2.91	10.61	13.16	12.04	11.41	11.84
24	2-methyl-Nonane	N/A	N/A	0.95	N/A	N/A	1.27
25	3-methyl- Nonane	N/A	N/A	1.54	1.22	1.19	1.47
26	4-methyl- Nonane	N/A	N/A	1.04	N/A	N/A	1.59
27	5-(2-methylpropyl)- Nonane	N/A	N/A	0.93	0.95	0.92	1.18
28	1-Decene	6.96	1.82	N/A	N/A	N/A	N/A
29	Decane	2.76	7.50	10.09	7.51	7.99	7.29
30	trans-3-Decene	N/A	N/A	N/A	0.79	1.01	N/A

31	5-methyl-Decane	N/A	N/A	N/A	N/A	3.79	N/A
32	1-Undecene	5.18	N/A	N/A	N/A	N/A	N/A
33	Undecane	2.55	5.67	N/A	5.14	4.41	3.73
34	Dodecane	2.27	4.34	12.14	3.30	2.78	2.90
35	Tridecane	3.5	3.33	3.66	N/A	1.68	0.66
36	1-Tridecene	6.54	N/A	N/A	N/A	N/A	N/A
37	4,6-dimethyl-Dodecane	N/A	N/A	N/A	2.07	N/A	N/A
38	Tetradecane	3.66	2.70	3.66	1.37	1.09	N/A
39	1-Pentadecene	1.68	N/A	N/A	N/A	N/A	N/A
40	Pentadecane	3.63	1.96	N/A	N/A	N/A	N/A
41	Hexadecane	2.96	1.30	2.88	0.82	N/A	N/A
42	Heptadecane	3.62	N/A	N/A	N/A	N/A	N/A
43	3-Octadecene	2.30	N/A	N/A	N/A	N/A	N/A
44	Eicosane	1.41	N/A	N/A	N/A	N/A	N/A
45	Heneicosane	4.90	N/A	N/A	N/A	N/A	N/A
Total peak area %		99.02	98.48	97.05	94.93	89.521	90.38

Note: Data in this table represent the percentage of peak area detected by GC/MS. "Total peak area %" represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. "N/A" represents not available.

Table S5 Effect of reaction time on the composition of C6-C21 hydrocarbon in liquid products over ZnFe₂O₄ catalyst. (peak area %)

Entry	C6-C21 hydrocarbon	Reaction time					
		10 min	30 min	60 min	120 min	180 min	240 min
1	2,4-dimethyl-Pentane	N/A	N/A	1.88	N/A	N/A	N/A
2	1-Heptene	10.47	6.33	4.00	N/A	N/A	N/A
3	Heptane	4.91	11.34	13.66	13.39	18.16	16.60
4	2-Heptene	N/A	N/A	N/A	N/A	3.57	N/A
5	3-Heptene	N/A	5.58	7.05	6.75	1.71	5.62
6	2-methyl-Hexane	N/A	1.62	N/A	2.86	2.84	2.72
7	3-methyl-Hexane	N/A	1.74	2.22	2.41	3.22	2.98
8	2,4-dimethyl-Hexane	N/A	N/A	N/A	3.26	3.25	3.09
9	3-Methyl-2-hexene	N/A	N/A	N/A	N/A	2.47	2.65
10	1-Octene	8.87	4.30	2.22	N/A	N/A	N/A
11	2-Octene	N/A	N/A	N/A	N/A	2.03	N/A
12	Octane	5.14	11.18	13.32	13.25	16.36	15.48
13	3-methyl-Octane	N/A	N/A	1.42	1.43	1.69	1.60
14	4-methyl-Octane	N/A	N/A	N/A	2.44	3.00	2.91
15	5-ethyl-2-methyl-Octane	N/A	N/A	N/A	5.57	N/A	N/A
16	3-Octene	N/A	4.69	5.05	5.01	N/A	3.48
17	1-Nonene	7.27	4.72	3.02	7.87	N/A	N/A
18	Nonane	4.91	9.44	10.81	10.62	12.04	11.3
19	2-Nonene	N/A	2.55	2.59	2.45	1.42	1.57
20	3-methyl-Nonane	N/A	N/A	N/A	N/A	1.22	N/A
21	5-(2-methylpropyl)-Nonane	N/A	N/A	N/A	N/A	0.95	N/A
22	1-Decene	5.34	1.55	N/A	N/A	N/A	N/A
23	Decane	4.64	7.40	7.82	8.14	7.51	8.03
24	1-Decene	1.02	2.02	N/A	1.63	N/A	N/A
25	trans-3-Decene	N/A	N/A	N/A	N/A	0.79	0.96
26	1-Undecene	4.34	1.47	N/A	N/A	N/A	N/A
27	Undecane	4.78	6.47	6.10	N/A	5.14	4.76
28	3-Dodecene	N/A	N/A	1.86	N/A	N/A	N/A
29	1-Dodecene	3.27	N/A	N/A	N/A	N/A	N/A
30	Dodecane	4.59	5.10	4.53	4.97	3.30	3.12

31	Tridecane	4.09	3.77	3.30	2.21	N/A	1.97
32	1-Tridecene	2.34	N/A	N/A	N/A	N/A	N/A
33	4,6-dimethyl-Dodecane	N/A	N/A	N/A	N/A	2.07	N/A
34	3-Tetradecene	1.03	N/A	N/A	N/A	N/A	N/A
35	7-methyl-Tridecane	N/A	N/A	N/A	N/A	N/A	1.11
36	3-Octadecene	1.75	N/A	N/A	N/A	N/A	N/A
37	Tetradecane	3.91	3.33	2.62	1.82	1.37	1.31
38	1-Pentadecene	1.25	N/A	N/A	N/A	N/A	N/A
39	Hexadecane	7.46	4.16	3.77	N/A	0.82	N/A
40	Heptadecane	3.27	1.24	1.22	N/A	N/A	N/A
41	Octadecane	2.20	N/A	N/A	N/A	N/A	N/A
42	Nonadecane	1.81	N/A	N/A	N/A	N/A	N/A
43	Heneicosane	1.34	N/A	N/A	N/A	N/A	N/A
Total peak area %		100	100	98.46	96.08	94.93	91.26

Note: Data in this table represent the percentage of peak area detected by GC/MS. "Total peak area %" represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. "N/A" represents not available.

Table S6 Effect of catalyst amount on the composition of C6-C21 hydrocarbon in liquid products over ZnFe₂O₄ catalyst. (peak area %)

Entry	C6-C21 hydrocarbon	catalyst amount			
		0.1 g	0.3 g	0.5 g	0.9 g
1	3-ethyl-1-Pentene	N/A	1.38	N/A	N/A
2	2-methyl-Hexane	2.57	3.19	2.86	1.87
3	3-methyl-Hexane	3.36	3.44	2.41	2.46
4	2,4-dimethyl-Hexane	N/A	N/A	3.26	3.20
5	Heptane	17.32	19.13	13.39	14.48
6	2-Heptene	2.4	N/A	N/A	1.7
7	3-Heptene	N/A	1.94	6.75	N/A
8	2-methyl-Heptane	2.21	2.32	N/A	N/A
9	4-methyl-Heptane	1.13	1.12	N/A	N/A
10	3-methyl-Heptane	3.13	2.96	N/A	N/A
11	Octane	16.2	16.8	13.25	15.44
12	2-Octene	0.81	N/A	N/A	1.00
13	3-Octene	N/A	0.92	5.01	N/A
14	4-methyl-Octane	3.23	3.15	2.44	3.18
15	3-methyl-Octane	1.68	1.60	1.43	1.71
16	Nonane	12.44	12.12	10.62	12.89
17	5-ethyl-2-methyl-Octane	N/A	5.59	5.57	N/A
18	1-Nonene	N/A	1.19	7.87	N/A
19	cis-2-Nonene	N/A	N/A	2.45	N/A
20	4-methyl-Nonane	1.22	1.09	N/A	N/A
21	2-methyl- Nonane	1.06	1.02	N/A	1.02
22	3-methyl-Nonane	1.72	1.54	N/A	1.44
23	Decane	8.66	8.16	8.14	9.5
24	1-Decene	N/A	N/A	1.63	N/A
25	4-methyl- Decane	0.80	N/A	N/A	N/A
26	2-methyl-Decane	0.78	N/A	N/A	0.97
27	5-(2-methylpropyl)-Nonane	1.03	N/A	N/A	1.18
28	Undecane	6.15	N/A	N/A	7.16
29	Dodecane	4.03	3.64	4.97	4.93
30	4,6-dimethyl-Dodecane	N/A	N/A	N/A	3.47
31	Tridecane	2.89	N/A	2.21	N/A
32	Tetradecane	1.91	1.71	1.82	2.21
33	Hexadecane	1.20	3.57	N/A	1.33
Total peak area %		97.93	97.58	96.08	91.14

Note: Data in this table represent the percentage of peak area detected by GC/MS. “Total peak area %” represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. “N/A” represents not available

Table S7 The composition of C6-C21 hydrocarbon in liquid products over ZnFe₂O₄ catalyst for 4 runs reactions. (peak area %)

Entry	C6-C21 hydrocarbon	Four circles			
		Run1	Run2	Run3	Run4
1	2,3,4-trimethyl-Pentane	N/A	1.33	1.38	N/A
2	2-methyl-Hexane	2.86	3.14	4.12	4.28
3	3-methyl- Hexane	2.41	3.68	4.69	4.65
4	1-Nonene	5.11	N/A	N/A	N/A
5	Heptane	13.39	17.69	19.24	19.15
6	2-Heptene	N/A	1.84	1.21	1.30
7	3-Heptene	4.25	N/A	N/A	N/A
8	3-Heptene	2.50	N/A	N/A	N/A
9	2-methyl-Heptane	N/A	3.42	3.47	3.94
10	3-methyl-Heptane	N/A	4.15	4.08	4.28
11	4-methyl-Heptane	N/A	N/A	N/A	1.34
12	2,5,5-trimethyl-Heptane	N/A	0.81	0.80	0.78
13	3-Methyl-2-hexene	N/A	N/A	N/A	2.48
14	2,4-dimethyl-Hexane	3.26	N/A	N/A	N/A
15	p-Xylene	N/A	N/A	N/A	0.63
16	Octane	13.25	17.21	16.56	16.82
17	3-Octene	5.01	N/A	N/A	N/A
18	2-methyl-Octane	N/A	4.13	4.12	4.31
19	4-methyl-Octane	2.44	N/A	N/A	N/A
20	3-methyl- Octane	1.43	2.26	2.19	2.32
21	1-Nonene	1.44	N/A	N/A	N/A
22	Nonane	10.62	12.58	11.65	11.65
23	3-methyl-Nonane	N/A	2.00	1.93	2.01
24	4-methyl-Nonane	N/A	1.57	1.53	1.52
25	5-methyl-Nonane	N/A	0.74	0.71	0.78
26	cis-2-Nonene	2.45	N/A	N/A	N/A
27	1-Nonene	1.32	N/A	N/A	N/A
28	2,5-dimethyl-Nonane	N/A	0.80	0.83	0.82
29	5-(2-methylpropyl)-Nonane	N/A	1.09	1.09	1.09
30	Decane	8.14	7.74	7.24	6.88
31	1-Decene	1.63	N/A	N/A	N/A
32	2-methyl-Decane	N/A	0.84	0.87	0.84
33	3,6-dimethyl-Decane	N/A	N/A	0.64	N/A
34	5-ethyl-2-methyl-Octane	5.57	N/A	N/A	N/A
35	Undecane	N/A	4.47	4.36	3.84
36	Dodecane	4.97	2.36	2.4	3.36
37	Tridecane	2.21	2.54	2.61	0.93
38	Tetradecane	1.82	N/A	N/A	N/A
Total peak area %		96.08	96.39	97.72	100

Note: Data in this table represent the percentage of peak area detected by GC/MS. "Total peak area %" represents the total peak area percentage of C6-C21 hydrocarbons among the detected products. "N/A" represents not available.

S-6: The synthesis and characterization of supported ZnFe₂O₄

We also choose different supports to load the ZnFe₂O₄ to test catalytic activity of selective conversion of methanol to C6-C21 hydrocarbons. In this paper, α -Al₂O₃, γ -Al₂O₃, CB (carbon black), GCB (graphitized carbon black) and CNT (carbon nano tube) were used as supports.

Catalysts Synthesis

In a typical synthesis, Zn(CH₃COO)₂•4H₂O (3.0 mmol), FeCl₃•6H₂O (6.0 mmol), and CH₃COONa•3H₂O (54 mmol), and CB (0.4 g) were dissolved/dispersed in a mixture solution containing HOCH₂CH₂OH (120.0 mL) and deionized water (120.0 mL) to form a homogeneous slurry, which was subsequently sealed in a stainless steel autoclave and heated at 200 °C for 48 h to obtain the desired product. The resulting precipitate was collected by centrifugation; washed with distilled water and absolute ethanol; and finally, dried in vacuum at 80 °C for 24 h to obtain the ZnFe₂O₄/CB composite. Other catalysts were synthesized the same as the ZnFe₂O₄/CB, except use α -Al₂O₃, γ -Al₂O₃, GCB, CNT to replace CB.

Catalytic activity of supported catalyst

Fig. S6 show XRD patterns of supported ZnFe₂O₄ catalysts. the observed diffraction peaks from the XRD patterns at 2θ values of 30.1, 35.6, 43.4, 57.3, and 62.8° correspond to the lattice planes of (220), (311), (400), (511), and (440) respectively, indicating the formation of ZnFe₂O₄ (JCPDS 01-089-1012), While the others peaks correspond to lattice planes of supports, respectively. The crystal size of corresponding bare ZnFe₂O₄ and supported ZnFe₂O₄ catalysts was calculated by Scherrer equation and summarized in Table S8. When ZnFe₂O₄ supported on α -Al₂O₃, γ -Al₂O₃, CB, GCB and CNT, size of ZnFe₂O₄ nanoparticles become smaller. As we can see from Figure S7a, the component of gas product of supported catalysts was almost the same with bare ZnFe₂O₄ catalyst,

except that $\text{ZnFe}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3$ had more H_2 and less CH_4 . Fig. S7b presents the liquid products of methanol conversion over ZnFe_2O_4 supported catalysts. After ZnFe_2O_4 loaded on different supports, reaction activity of conversion methanol to hydrocarbons decreased. This may be that the addition of supports covers the active sites of ZnFe_2O_4 .

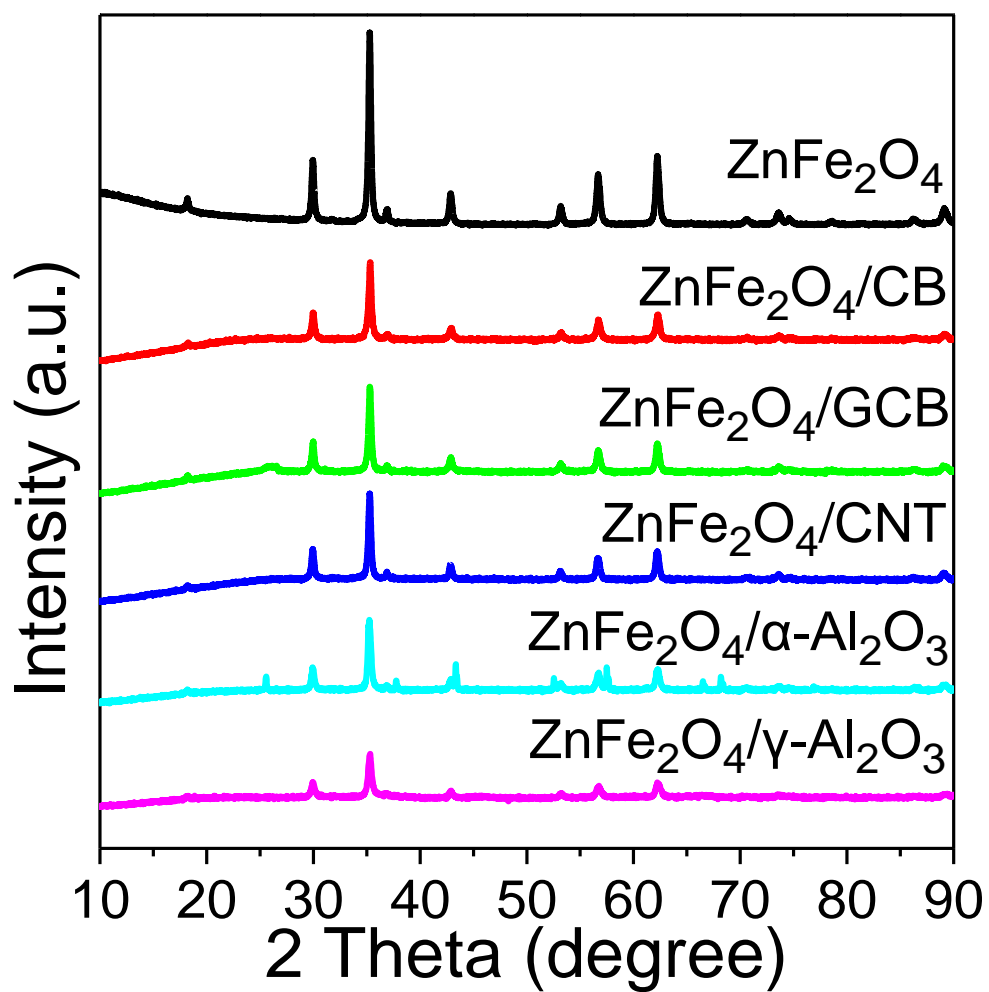


Fig. S6 XRD patterns of supported ZnFe₂O₄ catalysts.

Table S8 Crystal size of bare and supported ZnFe₂O₄ catalysts.

Sample	Crystal size ^a
ZnFe ₂ O ₄	29.4
ZnFe ₂ O ₄ /α-Al ₂ O ₃	22.8
ZnFe ₂ O ₄ /γ-Al ₂ O ₃	22.6
ZnFe ₂ O ₄ /CB	26.6
ZnFe ₂ O ₄ /GCB	27.0
ZnFe ₂ O ₄ /CNT	27.9

^a Crystal size, derived from XRD by Debye–Scherrer equation.

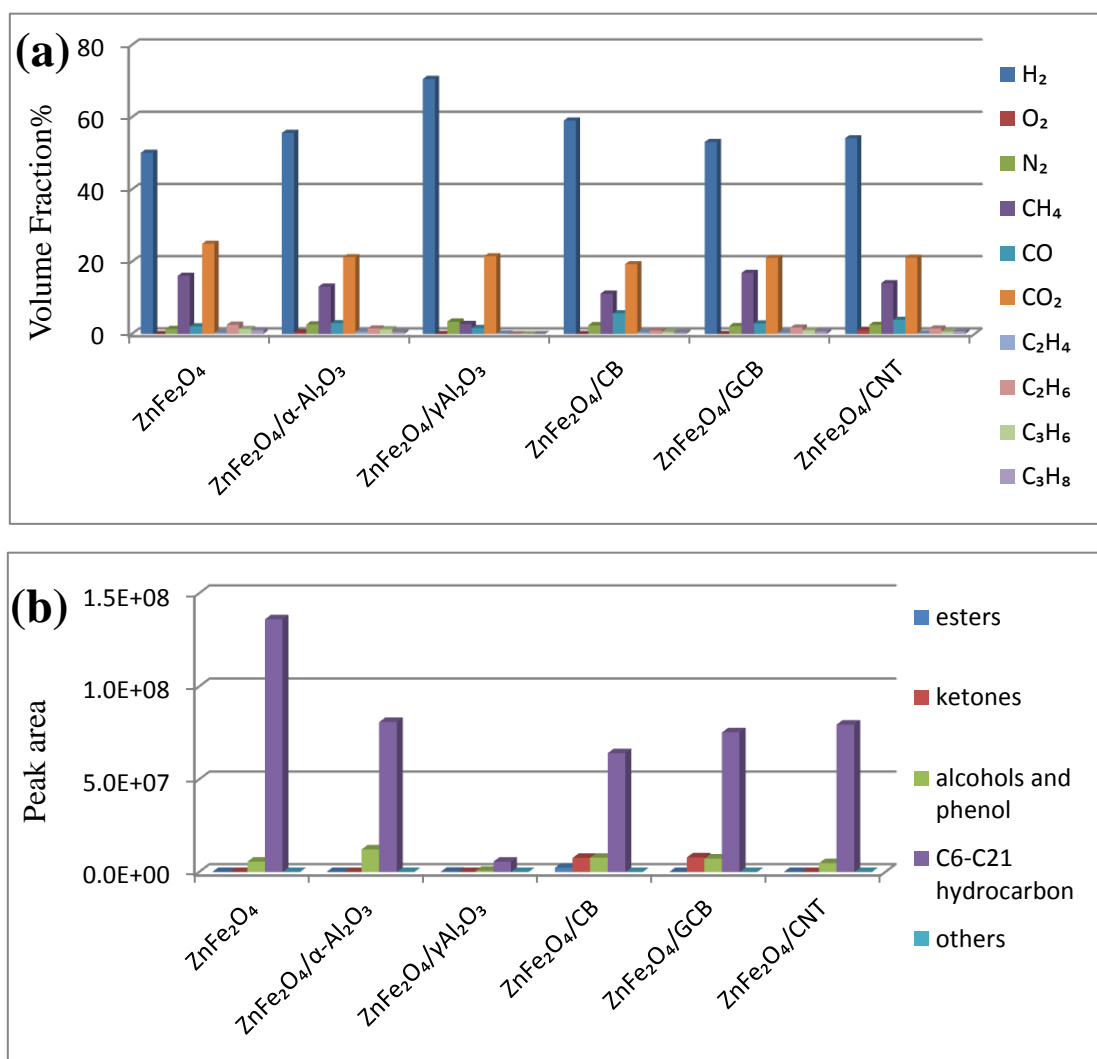


Fig. S7 Distributions of gas (a) and liquid (b) products over supported catalysts. (Reaction conditions: 0.5 g catalyst, 30 mL methanol, 120 min, 300 °C.)