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- Supporting Information -

2 Enhanced Electrochemical Reduction of Carbon Dioxide to

3 Formic Acid Using a Two-layer Gas Diffusion Electrode in

4 Microbial Electrolysis Cell

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Electrode	E/V	$R_{\rm S}/\Omega$	Q_{1}	<i>n</i> ₁	R_1/Ω	$Q_2/Q_2/Q_2^{-1} s^n cm^{-2}$	<i>n</i> ₂	R_2/Ω
SE	-1.2	1.431	4.154×10 ⁻⁵	1	0.900	2.392×10 ⁻³	0.782	20.730
	-1.3	1.421	4.160×10 ⁻⁵	1	0.919	2.534×10 ⁻³	0.778	9.101
SGDE	-1.2	1.290	1.143×10 ⁻⁶	0.922	0.994	4.641×10 ⁻³	0.732	16.030
	-1.3	1.307	8.046×10 ⁻⁵	0.959	0.925	5.221×10 ⁻³	0.712	8.143

23 Table S1 Simulated data of equivalent circuits for the Nyquist plots of impedance.





1 Electrolyte, 2 Pump, 3 Flowmeter, 4 Cathode (a: SE, b: SGDE), 5 Titanium wire, 6 Ag/AgCl electrode, 7 PEM, 8 Electrochemical workstation, 9 Anode, 10 Gas chamber.

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Figure S1 Schematic overview of the MEC systems employed in this work. (a) MEC with the SE cathode: the catholyte was saturated with CO_2 before each electrolysis run, and CO_2 was continuously sparged into the catholyte during the electrolysis. (b) MEC with the SGDE cathode, CO_2 was continuously fed into the gas chamber during the electrolysis.



32 Figure S2 XRD pattern of the SGDE. $Cu_{0.64}Zn_{0.36}$ is the major composition of the 33 brass mesh.



Figure S3 EDX spectrum of the Sn-loaded brass mesh in the SGDE. Cu and Zn are
the baseline elements of the brass mesh. Ni, Tl and Al are the impurities of the brass
mesh.



39 Figure S4 XPS spectrum of Sn3d in the Sn-loaded brass mesh of the SGDE.



41 Figure S5 The degree of inhibition of HER and of enhancement of reduction42 reactions for the SGDE compared to the SE.



44 Figure S6 Equivalent circuit used for fitting of the impedance. R_s: solution resistance,
45 R₁: interfacial ohmic resistance, R₂: charge transfer resistance, CPE₁ and CPE₂:
46 constant phase element, Q₁: CPE₁ value, Q₂: CPE₂ value, n₁: coefficient of CPE₁, n₂:
47 coefficient of CPE₂.



50 **Figure S7** Voltage and power density (a) and cathode and anode potential (b) of MFC





53 Figure S8 Schematic of ERCF for the SGDE (upper) and the SE (lower).



S9

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Figure S9 ERCF experimental results obtained with the SE and the SGDE in CEC.
Current density is expressed as the current used for producing formic acid divided by
the geometric area of the SE and the SGDE.

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It can be seen that formic acid can be detected from both electrodes at a cathode 59 potential of -1.2 V. Current density and FE_{HCOOH} increased when the cathode potential 60 shifted in negative direction to -1.8 V, but they decreased when the cathode potential 61 shifted from -1.8 V to -2.0 V. The FE_{HCOOH} value of 79.27 ± 1.52 % (at -1.8 V) is the 62 highest one reported in literature when using Sn electrodes under similar conditions¹. 63 When the cathode potential was more positive than -1.8 V, ERCF became more slack 64 due to the low standard potential of CO_2/CO_2^- in aqueous media (-2.33 V vs SCE²). 65 Whereas when it was more negative than -1.8 V, side reactions (such as HER) 66 emerged. This is in accordance with the CV results which showed that HER occurred 67



68 at cathode potential more negative than ca. -1.7 V.





Figure S10 Dependence of the anode potential during ERCF run in MEC with the SE
cathode (a) and the SGDE cathode (b) on the applied cathode potential .

In a MEC system, with the assistance of the potential generated from microorganism 73 catalyzed anodic oxidation reaction, lesser power supply is needed to initiate ERCF 74 than that in a CEC. Meanwhile, the anode potential can influence the electron 75 liberating capacities of the microorganism³. Therefore, the anode potential hold the 76 key to achieve higher product yield and FE_{HCOOH} at the cathode in our MEC systems. 77 In preliminary MEC experiments under constant cathode potential mode, we found 78 that the anode potential shifted to more positive values during the electrolysis and that 79 the shifting rate of the anode potential increased when the applied cathode potential 80 shifted to a more negative value. This may be attributed to the fact that the protons 81 and electrons released by the biodegradation of organic compounds in the anodic 82 chamber were unable to meet the needs of the cathode reaction ⁴. A high anode 83 potential will throttle the microorganism catalytic activity. We found that anodic 84 microorganisms were inactivated at an excessive positive potential (e.g. > +1 V) after 85 an electrolysis of 2 h in most of the cases. Hence, an electrolytic period of 2 h and an 86 applied cathode potential from -0.9 V to -1.2 V were adopted in this work for 87 protecting the microorganisms at the anode. After each ECRF test in MEC, the anode 88 microorganisms recovered in a short time. ERCF in MEC mode with the SGDE 89 cathode could be further enhanced by using advanced anode materials with larger 90 specific surface area, such as graphite brush. 91

93 **References**

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