Improving CO₂/N₂ separation performance by nonionic surfactant Tween containing polymeric gel membranes

Liang-liang Dong, Chun-fang Zhang, Yao-yao Zhang, Yun-xiang Bai*, Jin Gu, Yu-

ping Sun, Ming-qing Chen

1. Gas sorption method

(1) In order to eliminate gases present in the system and the sample, the system was evacuated by opening Valves 2 and 3 and closing Valve 1 for 3 h.

(2) Close Valves 2 and 3. Slowly open Valve 1 to make the gas progressively enter into the reference chamber until a required CO_2 pressure (P_1) was achieved in the reference chamber, and then Valve 1 was closed.

(3) Slowly opening Valve 2 to allow CO_2 in the reference chamber to enter into the sample chamber to contact the sample. After a constant pressure (P_2) was achieved, an equilibrium sorption was achieved. The quantity (mol) of CO_2 absorbed in the membrane can be calculated from

$$q_0 = \left[\left(p_1 - p_2 \right) V_R - p_2 \left(V_S - V_m \right) \right] / RT$$

where Vm is the volume of the membrane sample, and R and T are gas constant and temperature, respectively.

(4) The reference chamber pressure was increased to P by repeating Step (2). Then, another equilibrium sorption at pressure P_e was achieved by repeating step (3). The accessorial sorption uptake of CO₂ can be calculated from

$$\mathbf{V}_{q} = \left[\left(p - p_{e} \right) Y_{R} - \left(p - p_{e} \right) \left(V_{S} - V_{m} \right) \right] / RT$$

Therefore, the overall quantity of CO_2 absorbed in the membrane at the pressure of *Pe* can be calculated from

$$q = \left[\left(p - p_2 + p \right) Y_R - p_e \left(V_R + V_S - V_m \right) \right] \frac{T_0}{T P_0 V_m}$$

This step was repeated to obtain the sorption uptakes of CO₂ at different pressures.



Fig. S1 Schematic diagram of gas sorption setup: 1, 2, 3-needle valve; 4-reference volume; 5sample volume; 6-digital vacuum-pressure gauge

2. Photographs of PEBA2533/Tween-50 membranes



- Fig. S2 Photographs of PEBA2533/Tween-50 membranes (a) PEBA2533/Tween20-50 membrane; (b) PEBA2533/Tween21-50 membrane; (c) PEBA2533/Tween80-50 membrane
- 3. Thermal analysis of gel membranes



Fig. S3 DSC thermograms of the PEBA2533 and PEBA2533/Tween membranes (a): PEBA2533 and PEBA2533/Tween20 membranes (b): PEBA2533 and PEBA2533/Tween21 membranes (c): PEBA2533 and PEBA2533/Tween80 membranes

The neat PEBA2533 is a microphase-separated thermoplastic elastomer and has two dominant endothermic peaks as seen by DSC. The low temperature melting point, T_m (PTMO), is ascribed to melting of crystals of the polyether blocks and occurs about 0~20 °C. The high temperature melting point, T_m (PA), is attributed to melting of polyamide crystals and exists approximately 140~160 °C. During the first heating run for all PEBA2533/Tween gel membranes, there is a large peak appearing at about 80 °C and disappearing at the second heating run. This phenomenon is ascribed to the evaporation of humidity or residual solvent [1].

[1] R. A. Zoppi and C. G. A. Soares, *Adv. Polym. Tech.*, 2002, **21**, 2-16.